# **Computational Insights into Electrolyte-Dependent Li-ion Charge-Transfer Kinetics at the Li***x***CoO<sup>2</sup> Interface**

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**ABSTRACT:** Interface engineering remains a largely underexplored area and yet it holds the keys to high performance Li-ion batteries. It is the charge transfer across electrode-electrolyte interfaces, its inefficient energetics and sluggish kinetics that are oftentimes significant obstacles for achieving fast charging and high power regimes without compromising battery lifespan. This work propose a Boltzmann-averaged first principles workflow based on constant potential and constrained density functional theory for estimation of atomic scale factors influencing coupled ion-electron charge transfer kinetics across battery electrode-electrolyte interfaces. The approach estimates diabatic Li<sup>+</sup> interface energy landscapes as function of the interface character and operational conditions, needed to simulate charging/discharging currents. Experimental trends for the Li<sub>x</sub>CoO<sub>2</sub> (0.5≤*x*≤1.0) electrode in varied organic electrolytes with LiPF<sub>6</sub> and LiClO<sub>4</sub> salts are reproduced, identifying Li<sup>+</sup> transfer energy and Li<sup>+</sup> adsorption energy as decisive factors influencing the enhanced kinetics in LiClO<sub>4</sub>-based electrolytes over LiPF<sub>6</sub>, rationalized by a stronger surface interaction of  $ClO<sub>4</sub>$ .

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High power density and fast charging batteries are instrumental in the transition to electrified aerial, maritime, and terrestrial transportation.<sup>1–4</sup> Charge-transfer across interfaces of battery components plays a critical role in dictating charging/discharging kinetics where suboptimal Li-ion (Li<sup>+</sup>) transfer is a significant bottleneck impeding the performance of the battery. 5,6 This *interface challenge* pertains to both traditional and emerging Li-ion battery chemistries, including liquid<sup>6</sup>- as well as solid<sup>5</sup>-state electrolytes. Although interfacial engineering–via, e.g., advanced electrolyte formulations,<sup>7-10</sup> surface modifications,<sup>7,8,11</sup> and surface coatings<sup>7,8</sup>–has attracted substantial interest in the battery community in recent years,<sup> $7-11$ </sup> it remains a relatively underexplored area in the pursuit of rational battery design. Thus, enhancing the atomic- to macrolevel understanding of the interplay between electrode materials and electrolytes can provide guidance towards improved performance and lifespan of batteries.

Theoretical modeling offers a gauge to identify the role of atomic-scale factors in controlling observable charging/discharging rates and, thus, enables formulation of fundamental engineering principles.<sup>12-14</sup> Butler-Volmer (BV)<sup>15–17</sup> theory has traditionally been used to model interface charge transfer kinetics, where the classical physics-based BV is considered to reflect cases where ion transfer (IT) steps are rate limiting. In contrast, the influence of electron transfer (ET) on charge transfer kinetics, as described by Marcus-Hush-Chidsey (MHC)<sup>18-23</sup> theory, has lately been highlighted for both  $Li^+$  intercalation<sup>24–27</sup> as well as conversion<sup>28</sup> electrodes. In the more general case, mixed IT and ET rate control can be expected, motivating the recently introduced theory of coupled ion-electron transfer (CIET).<sup>14,29</sup> In CIET, IT and ET are assumed to occur simultaneously along a shared reaction coordinate,<sup>14,29</sup> where the description of IT in the classical rather than quantum regime distinguishing CIET from the related theory of coupled proton-electron transfer (CPET).<sup>30–33</sup> Similar to BV- and MHC-based approaches, the parameters needed for CIET can be directly evaluated from atomistic and first principles modeling, including solvent reorganization energy ( $\lambda$ ), electronic coupling ( $H_{DA}$ ) between donor and acceptor states, as well as ion adsorption ( $\omega_{Li}$ +) and ion transfer ( $\beta$ ) energies. While the dynamic nature of the interfaces can be captured using enhanced sampling molecular dynamics (MD) techniques,<sup>34,35</sup> the CIET parameters are derived from first principles calculations conducted at constant charge states in order to probe the free energy landscape before and after charge transfer–accessible via, e.g., constrained density functional theory (cDFT).<sup>36</sup> In addition, to reflect experimental conditions and to minimize the influence of finite cell-size effects, the calculations should be carried out at constant electrode potential (i.e., constant electron chemical potential or Fermi level), which can be achieved via electrochemistry-adapted DFT using, e.g., grand canonical potential approaches.<sup>37</sup> The CIET theory, hence, outlines a generally applicable framework that links atomic scale properties to battery performance, allowing for independent first principles evaluation of experimentally derived data as well as for in silico-guided materials design.

In this work, we develop a computational workflow based on CIET theory combined with constrained and constant potential DFT (**Scheme 1**) for analysis of the electronic and molecular properties that influence the IT and ET contributions to interface charge transfer resistance. The modeling approach complements previous efforts that sample the free energy landscape of battery interfaces using classical MD simulations, which focused on IT but neglects ET.<sup>35,38</sup> The approach also extends on earlier first-principles work on battery interface kinetics by accounting for electrode bias as well as the coupled transfer of ions and electrons.<sup>28,39</sup> By employing constant potential DFT, the approach ensures that the reaction landscape is explored under equal conditions as the addition/removal of ions from a finite model surface otherwise gives rise to spurious fluctuations of the electron chemical potential, associated with noisy or biased results.<sup>40</sup> Recent work on the LiFePO<sub>4</sub> and LiCoO<sub>2</sub> cathodes has, in addition, found that CIET models represents experimental data better than models that only reflect ET or IT.<sup>14,24,25,27,29</sup> From constrained DFT, it is possible to sample the reaction landscape for the reduced and oxidized charge states separately allowing for the evaluation of the diabatic energy profiles needed to obtain the chargetransfer parameters used in CIET. Using our framework, we can thus move closer to simulating realistic battery conditions, including accounting for simultaneous ET and IT, but also by emulating electrode potential, temperature, and ion concentration. The computational approach is benchmarked by reproducing measured current densities<sup>27</sup> at the state-of-the-art<sup>41</sup> Li<sub>x</sub>CoO<sub>2</sub> (LCO) electrode at varied states of charge (SOC;  $0.5 \le x \le 1.0$ ) and as a function of the composition of a liquid organic electrolytes based on ethylene carbonate (EC) and ethyl methyl carbonate (EMC) containing  $LiPF_6$  and  $LiClO_4$  salts. Our work provides insights into critical aspects towards improved interface kinetics, it explains the faster charge transfer kinetics observed in LiClO<sup>4</sup> electrolytes in terms of atomic scale properties, and sets the stage for future searches for battery materials with tailored interface properties.

Our computation framework to evaluate exchange current density within CIET framework is outlined in **Scheme 1** and summarized below, with more details available in **Note S1-S2**:

First, to simulate the cathode half-cell, models of the  $Li<sub>x</sub>Co<sub>2</sub>$ -electrolyte interface with  $x = \{0.50,$ 0.75, 1.00} are created from the rhombohedral  $(R\overline{3}m)$  LiCoO<sub>2</sub> scaffold structure, i.e., assuming topotactical (de)lithiation. The LCO surface is represented by a periodic  $(1, 2/3; 0, 4)$  supercell model of the  $(10\overline{1}4)$ facet, which is a commonly observed<sup>42</sup> and low energy<sup>43</sup> surface. (10<sup>1</sup>4) exposes Li-ion transport channels<sup>43</sup>–<sup>45</sup> that can exchange Li<sup>+</sup> with the electrolyte (illustrated in **Scheme 1**). Consistent with early battery cycles,<sup>46</sup>–<sup>48</sup> a pristine interface without a cathode-electrolyte interphase layer is considered. Electrolyte microenvironments are sampled as different adsorption structures. Leveraging our recent free energy molecular dynamics simulations on  $LCO(10\bar{1}4)$  interfaced with EC/EMC (3:7) electrolytes,<sup>38</sup> we extract local interface adsorption complexes of Li<sup>+</sup> coordinated to different numbers of electrolyte molecules and counterions ( $PF_6^-$  and  $ClO_4^-$ ) spanning a total coordination number (CN) of 3-6 and an anion CN (CNanion) of 0-2. Approximately 40 adsorption structure are sampled for every combination of SOC and

Li-salt. Input parameters to the CIET model are thereafter computed for each adsorption state as described below.

Second, charge transfer properties (*vide infra*) associated with the interface models are computed using constrained DFT (cDFT)<sup>49–51</sup> to ensure that the charge state is fixed at the LCO interface. cDFT is combined with constant potential DFT, $37$  where the electrode potential corresponds to the reversible potential (i.e., the open circuit voltage, OCV, when referenced to  $Li/Li^{+}$ <sup>52</sup> of the LCO half-cell at the given SOC. A graphene layer beneath the surface slab model acts as electron reservoir<sup>36</sup> (i.e., a computational charge collector), ensuring a continuous variation of the Fermi level (and thereby the potential) of the cell as electrons are added or subtracted. Using the constant potential scheme, the free energy landscape can be sampled at the same conditions facilitating fair comparison between states. Unless otherwise specified, these calculations are carried out in VASP<sup>53,54</sup> (version 6.3.2) using the PBE-D3(BJ) level of theory<sup>55–57</sup> and standard PAW<sup>58,59</sup> core potentials. To account for both directional and long-range solvation effects, hybrid explicit-implicit solvation models<sup>60,61</sup> are employed with the implicit part represented by VASPsol $^{60,61}$  using a dielectric constant of 20 corresponding to a 3:7 EC/EMC mixture.<sup>62</sup>

Third, to evaluate the electrode current density  $(i^{CIET})$  at varied interface properties and overpotential,  $\eta_f$  ( $\tilde{\eta}_f = \frac{e\eta_f}{k_B T}$  $\frac{e\eta_f}{k_B T}$ ), the computed charge transfer properties are inputted into the CIET<sup>14</sup> model (details in **Note S2**). The electron-coupled ion transfer version of CIET,<sup>14</sup> described by eq. 1-2, is found to best fit experimental data<sup>27</sup> and therefore used herein.

$$
i^{CIFT} = i^* \left( \frac{\tilde{c}_0(\omega_{Li^+})}{1 + e^{\tilde{\eta}_f}} - \frac{\tilde{c}_R}{1 + e^{-\tilde{\eta}_f}} \right) \operatorname{erfc} \left( \frac{\tilde{\lambda} - \sqrt{1 + \sqrt{\tilde{\lambda}} + \tilde{\eta}_f^2}}{2\sqrt{\tilde{\lambda}}} \right)
$$
(eq. 1)

$$
i^* = \frac{e\Delta_e(H_{\text{DA}}^2)}{h} \frac{1}{A_s} \frac{e^{-\Delta \tilde{G}_+^{\{T}}(\Delta E^{\{T\}})}}{\gamma_{\pm}^{\{T\}}}
$$
(eq. 2)

Above, *h* is the Planck constant and overline "~" indicating dimensionless variables normalized by the thermal energy  $(k_B T)$  or bulk concentrations. Some parameters are given by the ambient conditions, the material of choice, as well as the electrolyte composition. These include: the temperature (*T*); Li-ion concentration in LCO  $(c_R)$  and the electrolyte  $(c_0)$ ; as well as the area of a reaction site  $(A<sub>S</sub>)$ . Other properties are difficult or impossible to directly obtain from experiments, although they can be estimated by fitting procedures to, e.g., Tafel plots. Alternatively, the properties can be predicted through, e.g., the proposed computational workflow. These computed properties are: the adsorption energy of  $Li^+(\omega_{Li^+})$ ; the ion transfer energy ( $\beta$ ) over the reaction coordinate at a constant charge state ( $q$ ), which also determines the IT reaction barrier  $\Delta G_{\ddagger}^{IT}$ ; the solvent reorganization energy ( $\lambda$ ); as well as the electronic coupling matrix element  $(H_{\text{DA}}^2)$ . The latter is proportional to the electron chemisorption energy,  $\Delta_e$ . **Note S1-S2** provides a comprehensive overview of the computation of these charge transfer properties.

The above modeling framework provides the connection needed between atomic scale properties of electrodeelectrolyte interfaces and current densities, relating directly to battery power and charging performance. In the following, the computational workflow is used to gain insights into the charge transfer kinetics of the LCO cathode in varied electrolytes, identifying the key atomic factors controlling fast interface kinetics.

By simulating Li<sup>-/0/+</sup> vacancies at the LCO interface (Scheme 1A), we find that, under OCV, neutral Li vacancies are preferentially formed (i.e., Li<sup>+</sup>+e<sup>-</sup> leaves simultaneously) for all considered SOC (Figure S8). In addition, the relative chemical potential of Li  $(Li^+ + e^-)$ ,  $\mu_{Li^+ + e^-} = \mu_{Li}$ , at the interface compared to bulk LCO is 0.10, 0.11 and 0.22 eV for  $x = 0.50$ , 0.75, and 1.00, respectively, meaning that surface vacancies are preferred over bulk (**Figure 1.A**). In contrast, the first subsurface layer Li has approximately the same  $\mu_{1,i}$  as the bulk. By analyzing the site-projected DOS (Figure S4-S6) of the Li 2s band for Li<sup>+</sup> at the interface versus bulk LCO, it is found that the band center ( $\varepsilon_{Li2s}$ ) for surface Li<sup>+</sup> is higher compared to bulk, indicating a lower filing of bonding electronic states and, thus, weaker surface O-Li bonds (**Figure 1.B**). On the other hand, the subsurface Li<sup>+</sup> shows almost no difference in the Li 2s band center compared to bulk  $Li^+$ , explaining their stability. The  $\varepsilon_{Li2s}$  results correlate with shifts in the O 2p states ( $\varepsilon_{O2p}$ ) towards the Fermi level for surface O compared to bulk (**Figure 1.C**). Such shifts in  $\varepsilon_{02p}$  have been used to explain ion intercalation in terms of a reduced penalty for charge transfer associated with the upshift in  $\varepsilon_{02p}$  at the surface versus bulk due to a smaller O 2*s*-Co 3*d* band gap (**Figure S7**).<sup>63</sup> In brief, the Li vacancy results showcase that a lower concentration of  $Li<sup>+</sup>$  is expected at the interface compared to the bulk at OCV, but also that desorption/adsorption of Li<sup>+</sup> from/to the LCO surface is accompanied by oxidation/reduction of interface  $\text{Co}^{3+/4+}$ , corroborating the hypothesis of a coupled electron-ion mechanism of Li<sup>+</sup> transfer.

CIET barriers are computed for the cathode-electrolyte interface during charging/discharging following the steps outlined in **Figure 2.A**, where barriers are associated with both IT and ET steps (**Scheme 1.B)**. At the reversible potential of LCO (OCVs of 4.20, 3.95, 3.05 V versus Li/Li<sup>+</sup> for LCO at SOC  $x=0.50$ , 0.75, 1.00)<sup>52</sup>, the intercalation/de-intercalation equilibrium reads:

$$
Li^{+}(solv) + e^{-} + Co^{4+}(\textcircled{a}LCO) \rightleftharpoons Li^{+} \textcircCo}^{3+}(\textcircled{a}LCO) \qquad (eq. 3)
$$

The free energy profile of the Li<sup>+</sup> deintercalation reaction in Figure 2.B shows detailed steps where Li<sup>+</sup> is first in a LCO bulk intercalation state  $(1)$  in **Figure 2.A**). Li<sup>+</sup> then transitions via a surface state  $(2)$  in **Figure 2.A**), before reaching a Li<sup>+</sup> solvation complex at the outer Helmholtz plane (OHP,  $\widehat{3}$  in **Figure 2.A**) of the electric double layer. Ultimately Li<sup>+</sup> ends in the bulk electrolyte ( $\overline{4}$ ) in **Figure 2.A**). ET (coupled to IT) occurs in the step  $\overline{2}$   $\rightleftharpoons$   $\overline{3}$ ). This step is assumed to be the rate-limiting step based on previous experimental and MD studies.<sup>27,38</sup> Within the hypothesis of electron-coupled Li<sup>+</sup> transfer, we evaluate the barrier by computing two separate IT energy desorption profiles for the step  $(2) \rightleftharpoons (3)$  at constant charge states, *q*, corresponding to a reduced  $(q=q_R, i.e., Co^{3+})$  versus

oxidized ( $q=q_0$ , i.e., Co<sup>4+</sup>) surface, respectively. Estimating the coupling ( $\propto H_{DA}$ ) and reorganization energy ( $\lambda$ ) for ET between the  $q_0$  and  $q_R$  states along the IT desorption profiles provides the reaction barrier for each IT coordinate (*ξ*), with the minimal energy path corresponding to the most likely reaction pathway (red path in **Scheme 1.C**). Herein, the IT desorption profiles are computed using cDFT. An example is shown in **Figure 2.C** demonstrating that Li<sup>+</sup> desorption is endothermic at  $q_R$  and exothermic at  $q_0$ . These diabatic desorption profiles from  $(2) \rightleftharpoons (3)$  are found to be weakly sigmoidal but can, in order to simplify the implementation of a CIET model,<sup>14,29</sup> be approximated as linear with resulting  $R^2$  values of 0.90-0.95. Comparing the estimated free energy rection profiles and barriers along the joint ET-IT reaction coordinate holds the key to evaluating the variation in charge-transfer reaction kinetics from one interface to another.

To reflect the dynamic nature of the interface, different interfacial Li<sup>+</sup>-solvation configurations are sampled from recent MD simulations<sup>38</sup> to assess the average influence of the local coordination environments to the overall current density, revealing that the lowest energy adsorption complexes correspond to a total CN of 4-5 with CN<sub>anion</sub> of 0-1 and coordination to EC being slightly preferred over EMC, in agreement with the results of Aggarwal et al.<sup>38</sup> For each adsorption state,  $\omega_{Li}$ + is computed from a thermochemical cycle referenced to the average  $\mu_{Li}$ + of the bulk electrolyte (**Note S1.3** and **Scheme S1**). As seen in **Figure 3.A**, these low-energy complexes yield weakly endergonic Li<sup>+</sup> free energies of adsorption ( $\omega_{Li}$ +) in a narrow spread around 11 and 20 meV for ClO<sub>4</sub> and PF<sub>6</sub>. One key difference between ClO<sub>4</sub> and PF<sub>6</sub> relates to the bulk electrolyte reference state, with ClO<sub>4</sub> corresponding to a less favorable bulk solvation. Another important distinction between  $ClO_4^-$  and  $PF_6^-$  is the interplay between the anions and LCO (*vide infra*). For  $3 > CN > 5$  and  $CN_{\text{anion}} > 1$ ,  $\omega_{\text{Li}}$  is generally  $> 100$  meV, hence these structures are less probable and are found to have a small influence on the interface kinetics at typical operational temperatures (~300 K). Using the relative  $\omega_{Li+}$  values coming from different Li<sup>+</sup>-coordination complexes we can model the thermally-weighted CIET current density contribution from each adsorption state*,* and compute a total representative interface current via Boltzmann-averaging (with  $\mathbf{p}_j = \mathbf{p}_j[\omega_{i,j}, \beta, \lambda, H_{DA}]$  below, and Z representing the partition function estimated from the sampled states):

$$
i_{tot} = \langle i \rangle = \frac{1}{Z} \sum_j i_j^{CIFT}(\mathbf{p}_j) \exp\left(\frac{-\Delta \omega_{Li} + j}{k_B T}\right) \tag{eq. 3}
$$

The IT between the LCO surface and the OHP of the electrolyte encompasses the desolvation/solvation process of Li<sup>+</sup> and the ion transfer energy,  $\beta$ , is sensitive to the character and charge state of the electrode as well the electrolyte microenvironment at the interface (**Figure 3B**). Three results related to  $\beta$  will be highlighted. First, it is found that the reaction is approximately symmetric (i.e.,  $\beta \approx \beta_0 (q = q_0) \approx \beta_R (q = q_R)$ , and  $\alpha \approx 0.5$ ) for the low-energy adsorption states. This is reasonable at OCV conditions given the small deviation from equilibrium  $\mu$  (**Figure 2.B**), and the revealed reaction symmetry in agreement with the experimentally determined value of  $\alpha$ =0.48 for Li<sub>0.5</sub>CoO<sub>2</sub>

in LiPF<sub>6</sub> and carbonate electrolyte.<sup>64</sup> Second, one can estimate the IT-related reaction activation barrier,  $\Delta G_+^{IT}$ , from the  $\beta$  using eq. S12 resulting in  $\Delta G_4^{IT}$  values of 0.45 to 0.52 eV. These are close to the ~0.5 eV estimated by Yamada et al.<sup>65</sup> using electrochemical impedance spectroscopy for 0.5 M LiClO<sub>4</sub> salts in propylene carbonate. Last, **Figure 3.B** presents a clear trend when comparing LiClO<sub>4</sub> and LiPF<sub>6</sub> salts, revealing a slightly decreased  $\beta$  and associated lowered barrier in LiClO<sub>4</sub> electrolytes, which is in agreement with MD-simulated Li<sup>+</sup> IT energies using classical forcefields at constant charge state.<sup>38</sup>

To estimate the influence of ET on the charge transfer kinetics, average reorganization energies,  $\lambda$ , of ~109 and  $\sim$ 102 meV are computed for the PF<sub>6</sub> and ClO<sub>4</sub> electrolytes, respectively–a small but not insignificant difference (*vide infra*).  $\lambda$  together with the electronic coupling ( $H_{DA}$ ) are the important interface properties for the ET part of CIET.  $\lambda$  can be estimated for each IT coordinate ( $\xi$  in **Scheme 1**) by exploring pairs of Marcus parabolas (one each for the  $q_0$  and  $q_R$  states) that describe the change in chemical potential along the ET coordinate ( $\chi$  in **Scheme 1**), with details in **Note S1.2**. The  $\lambda$  values are estimated from the vertical energy difference when changing the charge state at the local energy minimum for the opposite charge state and obtained from the average value for the  $q_0$  and  $q_R$  states. Values reported in **Figure 3.C** correspond to the  $\lambda$  of the transition state IT coordinate.  $\lambda$  encompasses contributions from both the LCO and electrolyte parts of the interface. Regardless, the average  $\lambda$  values are close to the 90 meV estimated for bulk LCO (**Note S9**) as well as the 115 meV extracted from current-voltage response experiments for LCO.<sup>27</sup> Hence, one can conclude that the solvent effect on  $\lambda$  is small, both absolute and relative numbers. However, in contrast to the SOC–for which  $\lambda$  is almost insensitive–the minor variation in  $\lambda$  with the electrolyte composition has some influences on the relative current densities as discussed towards the end of this letter.

The other critical parameter determining the rate of ET, i.e. the electronic coupling  $(H<sub>DA</sub>)$  between the electron donor and acceptor states at the interface, shows no significance sensitive to the electrolyte but some dependence on the SOC of LCO.  $H_{DA}$  is herein computed using the approach of Van Voorhis and coworkers,<sup>49–51</sup> as implemented<sup>36</sup> in the GPAW modeling package.<sup>66,67</sup> Upon Li<sup>+</sup> interface adsorption (i.e., surface intercalation), Co<sup>4+</sup> at the LCO  $(x=0.5)$  surface is nominally reduced to  $Co<sup>3+</sup>$  as indicated by a small polaron localizing at around the CoO<sup>6</sup> octahedra (see insert of **Figure 2.C**). For SOC 0.5≤*x*≤0.75, bulk LCO is metallic (computationally and experimentally<sup>68,69</sup>) and electron transfer occurs from a delocalized subsurface to the bound surface state. Interestingly, the electrolyte has no significant influence on the electronic coupling and the computed  $H_{DA}$  for  $PF_6^$ and ClO<sub>4</sub> is close to 35 meV regardless of adsorption state for 0.5≤x≤0.75. A clear down shift to an average  $H_{DA}$ of ~22 meV is, however, seen as SOC changes to *x*=1.00. This change originates in the metal to semi-conductor phase transition of bulk LCO, which is experimentally known to occur over a biphase region at  $0.77 \le x \le 0.94$ ,<sup>68,69</sup> that leads to a change in the bulk donor state at  $x \approx 1.00$ . Hence,  $H_{DA}$  plays an important role in modulating the charge transfer kinetics as the SOC of LCO changes from  $x=0.50-0.75$  to  $x=1.00$ , whereas the relative influence of  $H_{DA}$  is insignificant when comparing the electrolyte compositions evaluated in this work.

Using the computed interface charge transfer parameters in **Figure 3** combined with the Boltzmann-weighted CIET formula in eq. 3, the computed current density, *i*, of the LCO electrodes is estimated as a function of the electrolyte character and the SOC of LCO (**Figure 4**). Remarkable agreements are found compared to experimentally reported polarization curves from Zhang *et al*. <sup>27</sup> The correspondence is good to excellent (within an order of magnitude). Experimentally, an increased state of charge of LCO generally yields higher *i* while ClO<sub>4</sub>based electrolytes outperforms  $PF_6^-$ , which are correctly reproduced by our simulated trends using the DFTcomputed parameters. These results corroborates that the computational framework outlined in this work is able to make predictions about the macroscopic effects on electrode kinetics from variations in molecular level details of a battery electrolyte and electrode, which is further discussed in the following.

The simulated trends shown in **Figure 4** can be rationalized by the favorable characteristics (large  $H_{DA}$  and/or small  $\beta$ ,  $\lambda$ , or  $\omega_{Li}$ +) of those individual interface adsorption states that give the largest overall contribution to the current density. The sensitivity analysis in **Figure S2** of all parameters entering in the CIET model indicate that the current density from a given adsorption state has a particular dependency on changes in  $H_{DA} > \beta \approx \lambda > \omega_{Li}$ , when varied within moderate bounds around the values corresponding to the most favorable state of the  $Li_{0.5}CoO_2$ interfaces with the ClO<sub>4</sub> electrolyte. In addition to this *intrinsic rate* of a given surface adsorption state, the influence of each state to the total reaction rate is weighted by its probability as evaluated by the relative value of  $\omega_{Li}$ +, hence giving the  $\omega_{Li}$ + property an added importance. Recall that, whereas  $H_{DA}$  is mainly affected by the SOC and insensitive to the electrolyte,  $\beta$ ,  $\lambda$ , and  $\omega_{Li}$  show electrolyte-dependency to some degree, hence all adsorbate states that give large contributions to the current density are associated with low values of  $\omega_{Li}$ ,  $\beta$  and  $\lambda$ . Of these structures, complexes containing anions ( $ClO_4^-$  or  $PF_6^-$ ) with  $CN_{\text{anion}}=1$  dominate. The results, moreover, suggest that a key underlying origin to the difference between  $ClO_4^-$  or  $PF_6^-$  is the more pronounced interaction of  $ClO_4^$ with the LCO surface; this yields a more beneficial adsorption of Li<sup>+</sup> at the OHP associated with a closer adsorption distance (~0.1 Å). The surface interactions of  $ClO_4^-$  is also associated with an additional stabilization of the surface and electrolyte during Li<sup>+</sup> solvation and desolvation that primarily affects the  $\beta$ , which is significantly more beneficial (i.e., smaller) for ClO<sub>4</sub>. In addition, the less favorable bulk  $\mu_{Li}$ + in the ClO<sub>4</sub> electrolyte compared to PF<sub>6</sub> yields a more favorable  $\omega_{Li}$ + at the interface for the case of ClO<sub>4</sub>, which has been previously explained by Aggarwal et al.<sup>38</sup> Although the bulk electrolyte effect, as well as influence of the LCO interaction difference of ClO<sub>4</sub> compared to  $PF_6^-$ , are weak to moderate, they are significant enough to alter the current density by an order of magnitude when adding up the contributions of  $\beta$ ,  $\lambda$ , and  $\omega_{Li}$ , with  $\beta$  defining the major part of the difference between the electrolytes.

Regarding the variation in the current density with the SOC of LCO, the simulated current densities follow experimental variations closely. The CIET model includes a dependency on the Li<sup>+</sup> concentration in LCO, which is the main factor contributing to the current density shift with SOC of  $0.5 < x < 0.8$  for  $Li<sub>x</sub>CoO<sub>2</sub>$ . However, as the SOC approaches full discharge, i.e.,  $x \approx 1.00$ , the current density of LCO is known to drop considerably.<sup>41</sup> This is reflected by our simulations showing a 3-4 order of magnitude current density decrease for  $x=1.00$  compared to  $x=0.50$  (**Figure S11**), which is primarily a consequence of the change in the  $H_{DA}$  with SOC (**Figure 3.D**).

Our work, focused on the  $LiCoO<sub>2</sub>$  intercalation-type cathode, suggests that the most influential atomic level features for enhanced interface kinetics pertains to ET properties of the electrode material surface and IT properties of the electrolyte. Surface engineering yielding stronger coupling,  $H<sub>DA</sub>$ , between electronic donor and acceptor states through, e.g., promotion of certain surface facets, doping, or coating outlines promising avenues for improvement. Of promise is, similarly, electrolyte design that tune the balance in the interaction of Li<sup>+</sup> with the electrolyte as well as the electrode surface providing a flat free energy landscape for Li<sup>+</sup> transfer with small  $\beta$ , and  $\omega_{Li}$ +. This work corroborate contemporary strategies in fast charging and high power battery design, but dresses the materials guidelines in an atomistic outfit aiming to benefit the nanoscale tailoring of battery material interfaces with improved charge transfer kinetics.

The modeling framework employed in this work offer a direct tool to assess charge transfer kinetics at electrode interfaces. This approach lends itself well to rationalization, finetuning, or testing of a limited selection of battery systems where refined understanding is required. However, the large computational overhead of the DFT methods prohibits high-throughput studies, why future work will target development of faster approximative methods to enable screening for improved battery components. In this direction, a few promising descriptors correlating with the  $\lambda$ ,  $\omega_{Li}$ ,  $\beta$ , and  $H_{DA}$  charge transfer properties are highlighted below: first,  $\lambda$  is known to correlate with the static and optical dielectric constants of the medium;<sup>70,71</sup> second, the electrostatic potential (ESP),<sup>72–74</sup> oxygen/lithium pDOS centers,<sup>63,75</sup> charge population analysis,<sup>76</sup> and the Crystal Orbital Hamilton Population (COHP)<sup>76,77</sup> are promising for estimations of  $\beta$ ; and, third,  $\omega_{Li}$  could be evaluated from solvation or ion-pairing energies.<sup>78,79</sup> Last, estimating  $H_{DA}$  is challenging, but positive results based on neural network models have been shown for molecular systems based on atomic orbital overlap and geometric descriptors.<sup>80</sup> In brief, future studies are encouraged to evaluate the herein employed charge-transfer property descriptors  $\lambda$ ,  $\omega_{Li}$ +,  $\beta$ , and  $H_{DA}$  through computationally efficient physics-derived or machine-learning/data-driven surrogate models.<sup>81-83</sup>

In summary, this study introduces and employs a computational workflow based on coupled ion-electron theory (CIET) of interface charge transfer. It is used to simulate the charging and discharging processes at  $Li<sub>x</sub>Co<sub>2</sub>$ -liquid EC/EMC electrolyte interfaces using charge transfer kinetic parameters derived from constrained and constant potential density functional theory (DFT) calculations. The simulations closely replicate experimental rate trends, indicating a notable preference for electrolytes containing the  $LiClO<sub>4</sub>$  salt over  $LiPF<sub>6</sub>$ , commonly used in commercial batteries. This preference is rationalized through the interplay of two factors closely linked to the solvent environment at the interface. First, LiClO<sub>4</sub> yields a more favorable adsorption energy ( $\omega_{Li}$ +) for Li<sup>+</sup> at the electric double layer of the interface through the more pronounced interaction of  $ClO<sub>4</sub>$  with the Li<sub>x</sub>CoO<sub>2</sub> surface compared to PF<sub>6</sub>. Second, the energetics of Li<sup>+</sup> transfer ( $\beta$ ) across the interface is more favorable for LiClO<sub>4</sub> compared to LiPF<sub>6</sub>, also a consequence of the slightly stronger interaction of  $ClO<sub>4</sub>$  with the Li<sub>x</sub>CoO<sub>2</sub> surface and the shorter  $ClO_4^-$ -binding distance. Based on our findings, our proposed workflow outlines a computational strategy to independently estimate charge transfer kinetics to gain atomic scale insight about the factors governing fast charge transfer and for the development of design guidelines for materials interfaces with enhanced power and charging performance in battery applications.

## **ASSOCIATED CONTENT**

#### **Supporting Information**

The Supporting Information is available free of charge.

Computational and modeling details; parameter sensitivity analysis CIET simulations; density of states plots; Li vacancy formation energies; polarization curve at *x*=1.00; reorganization energy analysis. (PDF)

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### **Author Contributions**

The manuscript was written through contributions of all authors. All authors have given approval to the final version of the manuscript. JHS conceived the research, performed the calculations, analyzed the data, and wrote the manuscript; PZ, AA, KG, DV, YZ, SP, MZB, YS-H, JWL, and AB analyzed the data and gave feedback on the manuscript; JWL supervised the research and obtained financial support.

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**Scheme 1. Interface charge transfer modeling.** In (**A**), sketch of a battery cell and (**B**) atomistic image of Li-ion transfer at the  $Li<sub>x</sub>CoO<sub>2</sub>(LCO)$ -electrolyte interface. In this work, 3:7 ethylene carbonate (EC):ethyl methyl carbonate (EMC) electrolytes containing  $0.5$  M LiPF<sub>6</sub> or LiClO<sub>4</sub> salts are considered. In  $(C)$ , overview of modeling framework containing four steps: in 1., showing a snapshot of a molecular dynamics simulation of the  $Li_{0.5}CO_2$  interface reproduced with permission from Aggarwal et al.<sup>38</sup>; in 2., example of distribution of charge transfer properties for two electrode-electrolyte interface systems computed with constant potential and constraint DFT; in 3. illustration of theory of coupled ion-electron transfer (CIET) kinetics that evaluates the excess chemical potential of the charge transfer reaction along the electronic (*χ*) and ionic (*ξ*) degrees of freedom, readapted from ref.<sup>29</sup> with permission; in 4., example of simulated polarization curve from estimated CIET parameters using the constant potential and constrained DFT (cDFT) modeling framework, as proposed in the current work. Color code in (**B**): Co (grey  $\bullet$ ); Li (green  $\bullet$ ); O (red  $\bullet$ ); C (brown  $\bullet$ ); H (white  $\circ$ ); F (dark green  $\bullet$ ); F (purple  $\bullet$ ).



**Figure 1. Li defect formation energies.** In (A), difference in Li (=Li<sup>+</sup>+e<sup>-</sup>) chemical potential relative to bulk for Li<sup>+</sup> in the surface and subsurface layer of  $LCO(10\bar{1}4)$ , respectively. In  $(B)$ , the difference shift in chemical potential with position is associated with a relative upwards shift in the 2s-band center  $(\varepsilon_{\text{Li2s}})$  of Li in the surface layer, leading to a reduced filling of bonding electronic states. In **(C)**, similar to **(B)** but with the O 2p-band center ( $\varepsilon_{02p}$ ) as descriptor.



**Figure 2. Li-ion transfer mechanism.** Schematic of the reversible Li-ion transfer mechanism at the LCO interface in **(A)**.  $(1) \rightarrow (4)$  corresponding to deintercalation, where intercalated Li<sup>+</sup> (1)) journeys via the LCO surface layer (2)) to a solvated adsorbed state in the outer Helmholtz plane ( $\circled{3}$ ), which is accompanied by oxidation of Co<sup>3+</sup> to Co<sup>4+</sup>, before reaching the bulk electrolyte (4). Li<sup>+</sup> prefers protruding ~1 Å from its original lattice position in the surface state (2)) under OCV so that Li<sup>+</sup> resides in the inner Helmholtz plane (IHP). In (B), excess chemical potential  $(\tilde{\mu}^{ex})$  diagram along reaction coordinate (i.e., joint IT-ET coordinate) for Li<sup>+</sup> transfer with the dotted box indicating the states explicitly treated by the CIET-DFT charge transfer model. In (C), desorption profiles for the lowest energy adsorption state in LiPF<sub>6</sub> electrolyte for the reduced (orange) and oxidized (blue) charge states. See **Figure S9** for a corresponding example for LiClO4. The inserts in **(C)** show examples inner (IHP) and outer (OHP) Helmholtz plane solvation structures for  $Li^+$  in the reduced charge state and in LiPF<sub>6</sub>-electrolyte, as well as an example of the localized polaron state. Color code: Co (grey ●); Li (green ●); O (red ●); C (brown ●); H (white  $\bigcirc$ ; F (dark green  $\bullet$ ); F (purple  $\bullet$ ).



**Figure 3. Computed charge transfer parameters.** DFT-estimated values for the  $\omega_{\text{Li+}}$ ,  $\beta$ ,  $\lambda$ , and  $H_{\text{DA}}$  of different Li<sup>+</sup> coordination complexes adsorbed onto the surface of  $Li_xCoO_2$ ,  $x = \{0.50, 0.75, 1.00\}$ . Distribution in  $\omega_{Li^+}$  is shown in (A) as a violin plot with (from the bottom) the 1<sup>st</sup> quartile, median, and 3<sup>rd</sup> quartile marked by horizontal lines. In (B), the average  $\beta$  = 1  $\frac{1}{2} [\beta_0 + \beta_{\rm R}]$  is plotted.



**Figure 4. Interface charge-transfer polarization curves.** Simulated (sim.) data obtained using the CIET theory in 0.5 M EC/EMC 3:7 electrolytes at 298 K based on the DFT-computed interface properties in **Figure 3**.  $|\tilde{\eta}_f|=6$  corresponds to a formal overpotential,  $\eta_f$ , of 0.155 V. Experimental (exp.) data from Zhang *et al.*<sup>27</sup> **Figure S10** includes the same data plotted on a linear scale indicating a relative error of the simulated data within 15% of experimental. On an absolute scale, the simulated data is within one order of magnitude compared to experimental data. Note that the current densities, *i*, are normalized by the reference current density,  $i_{\text{ref}}$ , corresponding to *i* at  $\tilde{\eta}_f$ =-6 of Li<sub>0.5</sub>CoO<sub>2</sub> in LiClO<sub>4</sub> for the simulated and experimental series, respectively.