

## **Abstract**

 Low-field nuclear magnetic resonance (NMR) relaxation is a promising non-invasive technique for characterizing solid-liquid interactions within functional porous materials. However, the ability of the solid-liquid interface to enhance adsorbate relaxation rates, known as the surface relaxivity, in the case of different solvents and reagents involved in various chemical processes has yet to be evaluated in a quantitative manner. In this study, we systematically explore the surface relaxation characteristics of ten liquid adsorbates (cyclohexane, acetone, water, and seven alcohols, including ethylene glycol) confined within mesoporous silicas with pore sizes between 6 nm and 50 nm using low-field (12.7 9 MHz) two-dimensional <sup>1</sup>H  $T_1 - T_2$  relaxation measurements. Functional group specific relaxation phenomena associated with the alkyl and hydroxyl groups of the confined alcohols are clearly 11 distinguished; we report the dependence of both longitudinal  $(T_1)$  and transverse  $(T_2)$  relaxation rates 12 of these <sup>1</sup>H-bearing moieties on pore surface-to-volume ratio, facilitating the quantification and assignment of surface relaxivity values to specific functional groups within the same adsorbate molecule for the first time. We further demonstrate that alkyl group transverse surface relaxivities correlate strongly with the alkyl/hydroxyl ratio of the adsorbates assessed, providing evidence for a simple, quantitative relationship between surface relaxivity and interfacial chemistry. Overall, our observations highlight potential pitfalls in the application of NMR relaxation for the evaluation of pore size distributions using hydroxylated probe molecules, and provide motivation for the exploration of nuclear spin relaxation measurements as a route to adsorbate identity within functional porous materials.

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*Keywords:* Adsorption, porous materials, NMR relaxation, surface relaxivity, alcohols

#### **1. Introduction**

 Functional porous materials are widely applied in industrial fields such as catalysis [1, 2], gas 3 adsorption [3-5] and separations [6, 7]. Understanding and quantifying both the pore structure characteristics and solid-fluid interactions inherent to such materials is critical for the regulation and optimization of chemical processes, and the rational design of new systems. However, detailed characterisation efforts are often hampered by the optically opaque nature of such materials. Nuclear magnetic resonance (NMR) is a non-invasive and chemically selective technique for characterizing 8 porous materials [8-12]. Traditional NMR spectroscopy approaches provide structural information via chemical shift analysis, and are regularly applied to inform the solid state structures of porous materials, including oxides [13, 14], zeolites [15, 16], and porous coordination frameworks and polymers (such as metal-organic- and covalent-organic frameworks) [17-19]. However, for liquids confined within the pore structures of such materials, chemical shift resolution is usually significantly 13 limited by line-broadening effects (especially for standard <sup>1</sup>H NMR spectra, which typically exhibit narrow chemical shift ranges), which occur due to local magnetic field distortions caused by magnetic susceptibility differences at the solid-liquid interface [20, 21]. Dynamic NMR measurements are comparatively unaffected by this problem, and instead provide information on the molecular translational and rotational motion of confined species by assessing the decay rates of NMR signals over time [22], with typical means including pulsed field gradient (PFG) NMR diffusion [23] and NMR relaxation time measurements [24]. PFG NMR diffusion measurements are employed to investigate the mass transport of fluids in porous media [25-27], and to quantify the tortuosity of the attendant pore networks [28-32]. NMR relaxation measurements quantify the longitudinal (*T*1) and 22 transverse  $(T_2)$  relaxation time constants associated with confined fluids; these time constants are directly related to molecular dynamics and can provide valuable information on pore structure characteristics [33-36] and solid-liquid interactions [37-40], especially when screening adsorption processes in sorbents and in catalytically active systems [41-43].

26 Two-dimensional (2D)  $T_1 - T_2$  relaxation time correlation measurements are now employed widely to provide comprehensive information on nuclear spin relaxation processes in porous materials 28 [44-51]. Such measurements provide near-simultaneous information on the  $T_1$  and  $T_2$  relaxation characteristics of confined fluids [52], and further provide facile access to the dimensionless ratio of 30 relaxation time constants  $(T_1/T_2)$ , which has received particular attention as a non-invasive probe of the relative surface affinities of confined fluids [48-51]. Weber *et al*. [53] were the first to compare the surface interaction strengths of reagents and solvents within liquid phase catalytical systems based on 33 the acquisition of  $T_1/T_2$  values from 2D correlation measurement, and demonstrated the ability of such

 data to differentiate multiple proton relaxation environments associated with different adsorbates simultaneously. Robinson *et al*. [54] observed that polar-protic adsorbates (short chain alcohols and carboxylic acids) confined to mesoporous silica with a single pore size showed two distinct relaxation 4 populations within 2D  $T_1 - T_2$  correlations when using short echo times and low-magnetic-field 5 strengths, which were significantly different from a single correlation peak of confined water [48, 55]. These correlation peaks were assigned to different proton environments associated with adsorbate alkyl 7 ( $C_x$ <sup>1</sup>H<sub>y</sub>) and hydroxyl groups ( $-\text{O}^1$ H), with these assignments supported by the relative integrated 8 intensities of the observed peaks  $[54]$ ; such observations have since been extended to  $C_3$  hydrocarbons within mesoporous gamma alumina [56], and are consistent with the work of Ward-Williams *et al*. on the fast field cycling relaxation dynamics of confined methanol [57-59].

 Due to the decreased molecular mobility at the solid-liquid interface, together with dipolar coupling interactions between adsorbates and spins embedded within the pore surface, the relaxation 13 rates  $(T_i^{-1}, i \in \{1, 2\})$  of liquids confined within porous materials will be enhanced compared to the 14 associated unrestricted bulk liquid [60]. For typical systems exhibiting a low concentration of pore surface-bound paramagnetic species, the enhanced relaxation rates of confined liquids are linearly 16 related to the surface-to-volume ratio of the porous material [61]. The scaling factor that quantifies the 17 ability of the solid-liquid interface to enhance relaxation is termed the surface relaxivity [62], and is usually calibrated by independent measurements of pore characteristics and enhanced relaxation rates [63]. While surface relaxivity quantification provides a potential approach to assess the structural characteristics of liquid-saturated porous materials based on the measurement of relaxation responses alone [64-66], a problem of significant concern is that even in materials with a single, well-defined pore size, confined probe liquids with multiple proton environments may exhibit multiple significantly 23 different relaxation rates [54], corresponding to a variety of surface relaxivities. Molecules exhibiting multiple proton environments associated with different functional groups are common in organic and synthetic chemistry, and include solvents and reagents (e.g. methanol and 2-propanol) used for the 26 functionalization of porous materials [67], and in catalytic reactions [53, 68]. Notably, the relationship between the enhanced relaxation rates of these different functional groups and the surface-to-volume ratio of confining pore structures is still unclear, which hinders extensive exploration of the pore structure characteristics and interfacial phenomenon of fluid-saturated functional porous materials using NMR. As such, in this study we systematically evaluate the surface relaxation characteristics of a series of ten common solvents confined to four commercial mesoporous silicas with nominal (meso)pore diameters between 6 nm and 50 nm. We demonstrate the clear identification of functional group specific relaxation characteristics associated with the different proton-bearing chemical moieties

1 (alkyl and hydroxyl groups) of the polar protic adsorbates assessed, and for the first time quantify the 2 different surface relaxivities of these groups.

#### 3 **2. Surface Relaxation Theory**

4 For liquid-saturated porous media, the observed relaxation rates  $T_{i,obs}^{-1}$  (where  $i = 1$  for 5 longitudinal and  $i = 2$  for transverse relaxation) of confined spin-bearing fluids may be expressed as 6 a linear combination of bulk, surface and diffusion terms  $[64, 69]$ :

$$
\frac{1}{T_{1,\text{obs}}} \approx \frac{1}{T_{1,\text{bulk}}} + \rho_1 \frac{S}{V},
$$
\n(1)\n  
\nbulk surface\n  
\n
$$
\frac{1}{T_{2,\text{obs}}} \approx \frac{1}{T_{2,\text{bulk}}} + \rho_2 \frac{S}{V} + at_e^{(k-1)}.
$$
\n(2)\n  
\nbulk surface diffusion

7 Here,  $T_{i,obs}$  are the observed relaxation time constants of the confined liquid,  $T_{i,bulk}$  are the time 8 constants of the unrestricted bulk liquid, and  $S/V$  is the surface-to-volume ratio of the confining pore 9 structure. The terms  $\rho_i$  are the (spatially averaged) surface relaxivities of the solid-liquid interface; 10 formally, these terms quantify the enhanced rates of nuclear spin relaxation which occur within the 11 adsorbed surface layer of fluid-filled pore structures, and may be expanded as  $\rho_i = \lambda/T_{i, \text{surf}}$ , where  $\lambda$ 12 is the thickness of the adsorbed surface layer across which surface enhanced relaxation rates occur, 13 and  $T_{i, \text{surf}}$  are the relaxation time constants of adsorbates within that layer [56]. Collectively, this 14 surface term therefore provides sensitivity to both surface and interfacial chemistry (via  $\rho_i$ ) and 15 material pore structure (via  $S/V$ ). The diffusion term provides a perturbation to observed transverse 16 relaxation ( $T_{2,obs}$ ) as a result of spin diffusion through effective magnetic field gradients within the 17 confining pore structure, which originate from magnetic susceptibility contrast at the solid/liquid 18 interface  $[70]$  ( $T_1$  relaxation is unaffected by such susceptibility contract effects  $[71]$ ), while the term 19  $t_e$  is the experimental echo time within the NMR pulse sequence. For non-viscous liquids confined to 20 mesoporous media (with pore diameters between 2 and 50 nm), the parameters  $k$  and  $a$  are well-21 defined [69], with  $k = 1$  and  $a = \gamma^2 g^2 \ell_s^4/(120D)$ . Here  $\gamma$  is the gyromagnetic ratio of the <sup>1</sup>H nucleus, 22 g is the average magnetic field gradient across the pore structure of interest,  $\ell_s$  is the length scale of 23 the confining pore structure, and D is the self-diffusion coefficient of the confined liquid. As  $g \sim \Delta \chi B_0$ , 24 i.e. such gradients scale in magnitude with both susceptibility contrast  $\Delta \chi$  and applied magnetic field 25 strength  $B_0$ , the influence of this diffusion term on observed transverse relaxation rates may be 26 mitigated by the application of comparably low magnetic field strength NMR equipment, as was 27 performed in this study (see Section 3.2). As such, Equations (1) and (2) may be rewritten in terms of 1 – enhanced relaxation rates  $(T_{i,E}^{-1})$ , such that

$$
\frac{1}{T_{i,E}} = \frac{1}{T_{i,\text{obs}}} - \frac{1}{T_{i,\text{bulk}}} = \rho_i \frac{S}{V},\tag{3}
$$

2 where surface relaxivity values  $(\rho_i)$  can be evaluated using a linear fit between  $T_{i,E}^{-1}$  and measured pore 3 surface-to-volume ratio  $(S/V)$ . It should be noted that a precondition of Equation (3) is the fast 4 diffusion assumption of surface relaxation [61]. For the fast diffusion (also termed surface-limited 5 relaxation [72]), the diffusion rate through the pores is significantly more rapid than the rates of surface 6 relaxation. Conversely, slow diffusion (also termed diffusion-limited relaxation [72]) refers to 7 situations where surface relaxation rates are significantly more rapid than diffusion across the pore 8 [73]. The parameter  $\kappa_i$  separates fast diffusion ( $\kappa_i \ll 1$ ) and slow diffusion ( $\kappa_i \gg 1$ ) according to [61, 9 74]:

$$
\kappa_i = \frac{\rho_i}{2D} \cdot \frac{\alpha V}{S},\tag{4}
$$

10 where  $\alpha$  is geometric factor that takes values  $\alpha = 1, 2$  and 3 for slit, cylindrical and spherical pores, respectively. When the fast diffusion assumption is not satisfied, spatially averaged surface relaxivities can be calculated using a more general form that applies to the intermediate regime between fast and slow diffusion [74].

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### **3. Methods**

## **3.1. Materials and Sample Preparation**

 CARiACT Q-series mesoporous silica gel materials (Q6, Q15, Q30, and Q50) comprising spherical particles of nominal diameter 1.7−4.0 mm were supplied by Fuji Silysia Chemical Ltd. (Japan); the number in the Q-series silica label indicates the reported average pore diameter in units of nm. Cyclohexane (Ajax Finechem, >99.0%), acetone (EMSURE, >99.8%), methanol (ChemSupply Australia, >99.9%), ethanol (ChemSupply Australia, >99.5%), 1-propanol (ChemSupply Australia, >99.8%), 1-butanol (ChemSupply Australia, >99.0%), 2-propanol (ChemSupply Australia, >99.5%), 2-butanol (ChemSupply Australia, >99.0%), ethylene glycol (ChemSupply Australia, >99.9%) were used as received. Deionized water was provided on site.

 To homogenize the surface hydroxyl environments of the Q-series silicas, each material was first refluxed in deionized water for 12 h, then dried in air at 110 ℃ for 24 h. For dried silicas, nitrogen isotherm analysis was conducted at 77 K using a Micromeritics ASAP 2020 Adsorption Analyser. The resulting Barrett-Joyner-Halenda (BJH) desorption pore size distributions and pore volumes, together with Brunauer-Emmett-Teller (BET) adsorption specific surface areas, are provided in Supporting Information Note 1. Furthermore, the surface hydroxyl density of each silica material was measured using the liquid phase deuterium exchange technique proposed by Penrose *et al*. [75] (see Supporting Information Note 2).

 For NMR relaxation analysis, dried silicas were generally soaked in excess liquid for at least 48 20 h at room temperature (25 $\pm$ 1 °C). For the more viscous probe liquids explored (ethylene glycol, 1- butanol and 2-butanol) an additional heating process was applied (50 ℃ for 5 h) to ensure that the solvents could adequately penetrate the silica pore network. The silicas were then separated from the excess liquid and rolled on a pre-soaked filter paper to remove interparticle liquid. They were then 24 quickly transferred to sealed 7 ml glass vials to minimize liquid evaporation; filling factors [76] for 25 each saturated silica sample were found to be  $\geq$  0.94 and were assessed gravimetrically. Each sample 26 consisted of approximately 6.5 g of imbibed silica (corresponding to  $\sim$  240 particles), facilitating well- averaged measurements of the surface-adsorbate interactions present between each imbibed liquid and the pore surfaces present throughout the mesoporous silicas investigated. A total of 10 separate bulk 29 liquids ( $\sim$  5 ml) were also individually sealed in 7 ml glass vials.

# **3.2. NMR Hardware and Relaxation Measurements**

NMR relaxation measurements were performed using a benchtop Oxford Instruments GeoSpec

1 NMR spectrometer equipped with a 0.3 T parallel plate magnet array (providing a <sup>1</sup>H frequency of *v*<sub>0</sub>=12.7 MHz at the default magnet temperature of  $T_d = 30$  °C) and 53 mm Q-sense probe. All sample vials were placed in the centre of the magnet bore, as confirmed via the acquisition of a one-dimensional profile image before analysis.

 $5$   $T_1 - T_2$  relaxation correlation data were acquired using the 2D radio frequency (RF) pulse 6 sequence shown in Figure 1 [52]. Here, a 180° RF pulse first rotates the sample magnetization from 7 the z-axis (aligned parallel to the static magnetic field) to the −z-axis, initiating longitudinal relaxation 8 (along the +z direction) towards thermal equilibrium within the variable recovery time *τ*, which 9 encodes  $T_1$ . A 90° RF pulse then rotates the sample magnetization into the x-y plane, and is followed 10 by a train of *n* 180° RF refocusing pulses separated by an echo time *t*e, generating *n* spin echoes of 11 magnitude  $S(\tau, nt_c)$  (black data point in Figure 1), which decay in magnitude according to  $T_2$ . The pulse 12 sequence was cycled with *m* different *τ* recovery times, forming a (*m* × *n*) data surface which encodes 13 both  $T_1$  and  $T_2$  relaxation information. For imbibed silica samples,  $T_1$  was encoded using  $m = 64$ 14 logarithmically spaced  $\tau$  recovery times from 1 ms to 6 s. In general,  $T_2$  was encoded by recording 15 magnitude of  $n = 18000$  echoes separated by an echo time of  $t<sub>e</sub> = 100 \,\mu s$ , although for the cyclohexane-16 saturated silica samples  $n = 48000$  echoes was employed to capture the full  $T_2$  decay of the system. 17 For bulk liquid samples,  $T_1$  was encoded by using  $m = 32$  logarithmically spaced  $\tau$  recovery times from 18 1 ms to 25 s. In general,  $T_2$  was encoded by recording magnitude of  $n = 48000$  echoes with an echo 19 time  $t_e = 300 \,\mu s$ ; the bulk acetone sample used  $n = 62000$  echoes. All measurements employed 4 repeat 20 scans to provide signal averaging, and the recycle delay between each repeat scan was 15 s ( $\gg$ 5 × T<sub>1</sub>), 21 resulting in an acquisition time of approximately 80 minutes.





**Figure 1**. Schematic diagram of the  $T_1 - T_2$  <sup>1</sup>H radio frequency (RF) pulse sequence applied in this work. Thick and thin 25 bars represent 180 and 90° RF pulses, respectively, while the black data point represents the measured spin echo magnitudes 26 *S*( $τ$ ,  $nt$ ). The variables  $τ$ ,  $n$  and  $t$ <sub>c</sub> are defined in the main text.

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### 1 **3.3. Data Processing**

2 The acquired data surface resulting from  $T_1 - T_2$  relaxation correlation measurements is described 3 by a 2D Fredholm integral equation [77]:

$$
\frac{S(\tau, nt_c)}{S(\infty, 0)} = \iint K_{12}(\tau, T_1, nt_c, T_2) F(T_1, T_2) d\log_{10}(T_1) d\log_{10}(T_2) + \varepsilon(\tau, nt_c),
$$
 (5)

4 where  $S(\tau, nt_e)/S(\infty, 0)$  is the normalized spin echo magnitude, and  $\varepsilon(\tau, nt_e)$  is the experimental 5 noise;  $F(T_1, T_2)$  is the targeted distribution of  $T_1$  and  $T_2$  relaxation time constants, while the kernel 6 function  $K_{12}(\tau, T_1, nt_e, T_2)$  describes the expected form of  $T_1$  and  $T_2$  relaxation across the experimental 7 pulse sequence employed:

$$
K_{12}(\tau, T_1, nt_e, T_2) = \left\{1 - 2\exp\left(\frac{-\tau}{T_1}\right)\right\} \exp\left(\frac{-nt_e}{T_2}\right). \tag{6}
$$

According to Equations (5) and (6),  $F(T_1, T_2)$  can be acquired by a numerical inversion (often termed a Laplace inversion or inverse Laplace transform) based on the acquired 2D relaxation data. In the presence of experimental noise, a stable distribution of relaxation time constants was achieved by using 11 Tikhonov regularization [78], with the degree of smoothing determined by the Generalised Cross 12 Validation method [79]. The resulting  $T_1 - T_2$  relaxation correlation distributions were limited to (200  $\times$  200) values with output ranges (10<sup>-4</sup> to 10<sup>1</sup>) s in each dimension. The above numerical inversions were performed using a fast Laplace inversion algorithm written by Mitchell *et al*. [80] in MATLAB (MathWorks Inc.).

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#### 1 **4. Results and Discussion**

## 2 **4.1. Relaxation Correlation Measurements of Confined Adsorbates**

3 Figure 2 demonstrates  $T_1 - T_2$  correlation data from cyclohexane and acetone (considered here as 4 prototypical apolar aprotic and polar aprotic adsorbates, respectively) confined within the mesoporous 5 silicas Q6, Q15, Q30 and Q50. As all interparticle liquid was removed prior to NMR analysis (see 6 Section 3.1), the observed relaxation phenomena must characterise confined liquids within the silica 7 pore structures. A single, narrow relaxation time distribution is observed in each case, which following 8 the simple surface relaxation theory described in Section 2 indicates that the materials explored here 9 do not demonstrate a hierarchical pore structure; this observation is supported by pore size distributions 10 detailed in Supporting Information Note 1. Importantly, as relaxation correlation peak shapes are 11 highly sensitive to experimental noise [77], we focus here only on the modal relaxation times of such 12 peaks (termed  $\langle T_1 \rangle$  and  $\langle T_2 \rangle$ ), together with their modal ratio  $\langle T_1/T_2 \rangle$ , which is quantified at the naximum value of each correlation peak. As a useful example, the observed  $\langle T_1/T_2 \rangle$  ratios for Q15 14 are indicated by red dashed diagonal lines in Figure 2. D'Agostino *et al*. [48] and Robinson *et al*. [49] 15 found that the  $\langle T_1/T_2 \rangle$  ratio can be related directly to the adsorption energy of liquids within 16 heterogeneous catalyst supports, and this ratio is now generally considered a rapid and non-invasive 17 probe of the surface affinities of liquids absorbed in porous materials [42, 51]. As shown in Figure 2, 18 the  $\langle T_1/T_2 \rangle$  ratio of cyclohexane  $(\langle T_1/T_2 \rangle \approx 1.12)$  in Q15 is lower than that of acetone within the same neterial ( $\langle T_1/T_2 \rangle \approx 1.44$ ). This result indicates that the surface affinities of these adsorbates can be 20 ranked as cyclohexane < acetone, which is consistent with the order of the relative polarity values of 21 these molecules [81].

22 Figure 3(a-h) shows  $T_1 - T_2$  correlation data acquired from confined polar protic adsorbates in 23 Q6, Q15, Q30 and Q50, including deionized water, four primary alcohols (methanol, ethanol, 1- 24 propanol, and 1-butanol), two secondary alcohols (2-propanol and 2-butanol), and one polyol (ethylene 25 glycol). The  $\langle T_1/T_2 \rangle$  ratio of water  $(\langle T_1/T_2 \rangle \approx 7.15)$  in Q15 is larger than that of both acetone and 26 cyclohexane, likely reflecting the comparably stronger interaction between adsorbed water and the 27 polar surfaces of the silica pores. For confined alcohols, two distinct correlation peaks are clearly apparent in each data set, which are characterised by different  $\langle T_1 \rangle$  and  $\langle T_2 \rangle$  values (and in some cases  $\langle T_1/T_2 \rangle$  ratios; detailed relaxation time values are provided in Supporting Information Note 3). Given 30 that no hierarchical structure is present in these materials, this observation is attributed to the existence 31 of multiple different proton relaxation environments within each polar protic adsorbate, consistent with 32 our recent work using both Q15 silica [54] and mesoporous gamma alumina [56]. To further verify 33 these correlation peak assignments, Figure 3(i) details the observed alkyl/hydroxyl ratio of each

 adsorbate calculated from the integrals of the two correlation peaks in our Q15 data; a strong correlation between observed and expected alkyl/hydroxyl ratios is evident. The clear observation of hydroxyl group relaxation across the entire series of alcohols assessed is attributed to the low magnetic 4 field strength and short echo time employed here [56, 58, 82]. Furthermore, in extension to our 5 previous research  $[54]$ , these data demonstrate – to the best of our knowledge – the first reported observation of functional group resolved nuclear spin relaxation within polyol (ethylene glycol) saturated mesoporous silicas, demonstrating and extending the unique ability of low-field NMR relaxation to non-invasively observe and identify functional group specific relaxation phenomena associated with a wide range of organic solvents and reagents confined to porous materials.

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 $\begin{array}{c} 12 \\ 13 \end{array}$ **Figure 2.** <sup>1</sup>H  $T_1-T_2$  correlation plots of confined (a) cyclohexane and (b) acetone in Q6, Q15, Q30 and Q50 mesoporous 14 silicas. Solid diagonal lines indicate the relaxation time ratio  $T_1/T_2 = 1$ , while red dashed diagonal lines indicate the observed modal relaxation time ratio  $(T_1/T_2)$  of each correlation peak in O15 as example; repo 15 observed modal relaxation time ratio  $(T_1/T_2)$  of each correlation peak in Q15 as example; reported uncertainties in  $(T_1/T_2)$ 16 correspond with the observed standard deviation in peak maximum across three repeat measurements on the same sample.<br>17 The molecular structure of each adsorbate is indicated in each case, where C, O, and aprotic H atom The molecular structure of each adsorbate is indicated in each case, where C, O, and aprotic H atoms are colored gray, red, and blue, respectively.

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**Figure 3**. 2 <sup>1</sup>H *T*1−*T*<sup>2</sup> correlation plots of confined (a) deionized water, (b-e) primary alcohols [(b) methanol, (c) ethanol, (d) 3 1-propanol, and (e) 1-butanol], (f-g) secondary alcohols [(f) 2-propanol and (g) 2-butanol], and (h) ethylene glycol in Q6,<br>3 015, 030 and 050 mesoporous silicas. Solid diagonal lines indicate the relaxation time ratio 4 Q15, Q30 and Q50 mesoporous silicas. Solid diagonal lines indicate the relaxation time ratio  $T_1/T_2 = 1$ , while the red<br>5 dashed diagonal lines indicate the observed modal relaxation time ratio  $\langle T_1/T_2 \rangle$  of each corr dashed diagonal lines indicate the observed modal relaxation time ratio  $\langle T_1/T_2 \rangle$  of each correlation peak in Q15 as an example; reported uncertainties in  $\langle T_1/T_2 \rangle$  correspond with the observed standard deviation in 6 example; reported uncertainties in  $\langle T_1/T_2 \rangle$  correspond with the observed standard deviation in peak maximum across three<br>7 repeat measurements on the same sample. The molecular structure of each adsorbate is indicat 7 repeat measurements on the same sample. The molecular structure of each adsorbate is indicated in each case, where C, O, aprotic H and protic H are colored gray, red, blue and yellow, respectively. Correlation peaks at 8 aprotic H and protic H are colored gray, red, blue and yellow, respectively. Correlation peaks at long and short  $T_2$  are assigned to aprotic alkyl groups  $(C_x^1H_y)$  and protic hydroxyl groups  $(-O^1H)$ , respectively. (i 9 assigned to aprotic alkyl groups (C<sub>x</sub><sup>1</sup>H<sub>y</sub>) and protic hydroxyl groups (−O<sup>1</sup>H), respectively. (i) Observed alkyl/hydroxyl ratio 10 of each adsorbate (acquired from the integrated ratio of the two observed correlation peaks) in Q15 only as a function of 11 expected alkyl/hydroxyl ratio (acquired from the number ratio of aprotic and protic H atoms). The dashed line in (i) denotes 12 parity between the two axes; error bars are generally smaller than the depicted data points and indicate the observed 13 standard deviation from three repeat measurements on the same sample.

1 Figure 4(a) provides a summary of the modal relaxation time ratios  $\langle T_1/T_2 \rangle$  of both hydroxyl and alkyl <sup>1</sup>H groups of alcohols imbibed within Q15. For both primary and secondary alcohols, the  $\langle T_1/T_2 \rangle$ 3 ratio of the hydroxyl group decreases as a function of increasing carbon chain length, while the alkyl 4 group increases, demonstrating the opposite trend. The metric  $\Delta \langle T_1/T_2 \rangle = \langle T_1/T_2 \rangle_{\text{hydroxyl}}$  $\langle T_1/T_2 \rangle$ <sub>alkyl</sub> (where subscripts define either the hydroxyl or alkyl ratio) provides a simple approach to 6 quantify the difference in  $\langle T_1/T_2 \rangle$  ratio between functional groups, and in previous work has been 7 observed to correlate strongly with adsorbate acidity [54]. Specifically, a higher degree of adsorbate 8 acidity (indicated by low *pK*<sup>a</sup> values) leads to facile surface-adsorbate proton exchange between 9 surface and adsorbate hydroxyl groups; such dynamics lead to the observed hydroxyl relaxation 10 characterisatics of our adsorbates exhibiting solid-like properties with simultaneously longer  $T_1$  times and shorter  $T_2$  times (corresponding to large  $\Delta \langle T_1/T_2 \rangle$ ), while adsorbate alkyl groups do not undergo 12 such proton exchange. As shown in Figure 4(b), ethylene glycol also conforms to the above trend, 13 which is demonstrated to hold across the range of mesopore sizes examined here. The effect of adsorbate acidity on  $\Delta \langle T_1/T_2 \rangle$  is more obvious for alcohols confined in small pore-size silicas; this 15 observation is attributed to the very short hydroxyl  $T_2$  times observed for these materials, which result 16 in correspondingly large  $\langle T_1/T_2 \rangle$ <sub>hydroxyl</sub> values.





**18** Figure 4. (a) Summary of the modal relaxation time ratios  $\langle T_1/T_2 \rangle$  of both hydroxyl and alkyl <sup>1</sup>H groups of imbibed 19 alcohols in Q15. (b) Correlation between the difference in modal relaxation time ratios of hydroxyl and alkyl groups 20  $\Delta \langle T_1/T_2 \rangle$  and adsorbate  $pK_a$ . 21

#### **4.2. Dependence of Enhanced Relaxation on Pore Surface-to-Volume Ratio**

 In this section, we further explore the dependence of the enhanced relaxation rates of the above series of confined adsorbates on silica pore surface-to-volume ratio (*S*/*V*, as measured by gas sorption; 4 see Section 3.1). We again use the modal relaxation time constants of the confined liquids, as well as 5 values from equivalent measurements of unrestricted bulk liquids (see Supporting Information Note 6 3), to calculate enhanced relaxation rates  $((T_{i,E})^{-1})$ .

 Figure 5 shows the dependence of longitudinal and transverse enhanced relaxation rates of confined cyclohexane and acetone on *S*/*V*. For cyclohexane, both the longitudinal and transverse relaxation data of all materials scale linearly with *S*/*V*. For acetone, data acquired from Q15, Q30 and Q30 again scales linearly within *S/V*, while the calculated enhanced relaxation rates of Q6 appear anomalous. In each case, the resulting linear fits show unexpectedly large (non-zero) y-intercepts, which are inconsistent with Equation (3). We rationalize this observation by considering the simple relaxation rate contribution theory proposed by Faux *et al*. [83]. Considering the typical biphasic fast exchange model for a liquid-saturated pore, adsorbates may be found either within the adsorbed surface layer near the pore walls, or within a bulk-like region (the "pore bulk") towards the centre of the pore. While the overall observed relaxation rates are a weighted average of the rates within these two regions, a complete description must also recognise that the inherent relaxation rates of each region are influenced by the existence of the other (specifically, via intermolecular dipolar coupling interactions, which facilitate the microscopic magnetic fluctuations responsible for nuclear spin 20 relaxation [82]). The relaxation rates of the pore bulk (now termed  $T_{i,pb}^{-1}$ ) therefore comprise a linear 21 combination of contributions from both bulk-bulk interactions  $(T_{i,bb}^{-1})$  and interactions between the pore 22 bulk and the adsorbed surface layer  $(T_{i,bl}^{-1})$ , such that  $T_{i,pb}^{-1} = T_{i,bb}^{-1} + T_{i,bl}^{-1}$ . This expression is different to that governing relaxation within entirely unrestricted bulk liquid, which will contain no contribution 24 from  $T_{i,bl}^{-1}$ , such that  $T_{i,bulk}^{-1} \equiv T_{i,bb}^{-1} < T_{i,pb}^{-1}$ , resulting in an underestimation of pore bulk relaxation rates in our measurements and hence non-zero y-intercepts when fitting our data using Equation (3). 26 Calculated  $T_{i, pb}$  values are provided in Supporting Information Note 4; however, given the above observation does not significantly influence the linear correlations observed in our results, in the remainder of this work we focus exclusively on the gradient of our linear fits, rather than further discussion of the resulting intercepts.

 Figure 6(a-b) shows the dependence of longitudinal enhanced relaxation rates for both the alkyl and hydroxyl groups of confined polar protic adsorbates on *S*/*V*. These data demonstrate a clear linear relationship for all adsorbates up to  $S/V \sim 200 \mu m^{-1}$ , as predicted by Equation (3), while high  $S/V$  data acquired from Q6 again lies outside of the predicted trend. Conversely, Figure 6(c-d) shows an

 excellent linear relationship between the transverse enhanced relaxation rates and *S*/*V* for both the alkyl 2 hydroxyl groups of confined species across all four mesoporous silicas investigated (up to  $S/V \sim 600$ )  $\mu$ m<sup>-1</sup>). While fully elucidating upon the origin of the (partially) anomalous relaxation behavior shown by Q6 is the subject of ongoing investigations, we suggest the non-conformity of these data may arise from subtle differences in pore surface chemistry between different silica materials, which will be accentuated by the very large *S/V* values inherent to Q6. We note that overall measured Q6 surface 7 hydroxyl density values are equivalent to that of Q15 ( $a_{OH} \sim 3.7$  nm<sup>-2</sup>; see tabulated data in Supporting Information Note 2); however, such data does not take into account the potential for different types of surface hydroxyl groups (isolated [Si-O-H], hydrogen bonded [Si-O-H···O(H)-Si] or geminal [Si- (OH)2]) or their microscopic distribution across the pore surface, nor do these data inform on the surface accessibility of very low levels of any paramagnetic contaminants present.

 Importantly, under the fast diffusion assumption of surface relaxation, the gradient of our linear 13 fits in Figures 5 and 6 may be directly interpreted as the surface relaxivities  $(\rho_i)$  of each spin-bearing group at the attendant solid/fluid interface. The validity of applying this assumption was evaluated using Equations (4) (verification details are provided in Supporting Information Note 5); our 16 calculations resulted in a maximum value of  $\kappa_i = 0.026 \ll 1$ , confirming that all the experimental systems assessed here satisfy the requirement for fast diffusion. The resulting surface relaxivity values 18 are detailed in Table 1 (further data is provided in Supporting Information Note 4). We note from these 19 data that for both the alkyl and hydroxyl groups of our adsorbate series, fitted  $\rho_2$  values are found to 20 be universally larger than the resulting  $\rho_1$  values; such results are consistent with previous investigations on the surface relaxivities of confined water in porous silica [51, 84], and demonstrate quantitively that solid-liquid interactions within our saturated mesoporous silicas enhance transverse 23 nuclear spin relaxation rates to a greater degree than longitudinal relaxation rates. However, Supporting Information Note 4 further details the uncertainties obtained from our linear fitting process; for 25 multiple adsorbates, uncertainties in values of the longitudinal surface relaxaivity  $\rho_1$  are unacceptably large (>100 % in some cases), precluding any detailed evaluation of these data. As such, in the remainder of this work we focus on interpretation of the transverse surface relaxaivity values alone.



**Figure 5**. Dependence of the (a) longitudinal enhanced relaxation rates  $((T_{1,E})^{-1})$ , and (b) transverse enhanced relaxation 3 rates  $((T_{2,E})^{-1})$  of confined cyclohexane and acetone on the pore surface-to-volume ratio  $(S/V)$  of mesoporous silicas. Lines 4 indicate a linear fit to the data (detailed fitting results are provided in Supporting Information Note 4). For cyclohexane, this fitting is based on the complete Q6, Q15, Q30, and Q50 data set. For acetone, fitting is b this fitting is based on the complete Q6, Q15, Q30, and Q50 data set. For acetone, fitting is based on only Q15, Q30, and Q50 data.





**Figure 6**. Dependence of the longitudinal enhanced relaxation rates  $((T_{1,E})^{-1})$  for (a) alkyl groups, and (b) hydroxyl groups 3 in confined polar protic adsorbates, together with transverse enhanced relaxation rates  $((T_{2,E})^{-1})$  for (c) alkyl groups, and 4 (d) hydroxyl groups of confined polar protic adsorbates on the pore surface-to-volume ratio (*S/V*) of mesoporous silicas.<br>5 Lines indicate a linear fit to the data (detailed fitting results are provided in Supporting In 5 Lines indicate a linear fit to the data (detailed fitting results are provided in Supporting Information Note 4). For longitudinal relaxation each fit is based on the data (detailed noting Q15, Q30, and Q50 data. For tra 6 longitudinal relaxation each fit is based on only Q15, Q30, and Q50 data. For transverse relaxation each fit is based on the complete Q6, Q15, Q30, and Q50 data set.



# 2 **Table 1**. Longitudinal and transverse surface relaxivities from the linear fits detailed in Figures 5 and 6.

3 \* Fitting based on Q15, Q30, and Q50 data only

#### 1 **4.3. Transverse Surface Relaxivity and Molecular Structure**

 Given the strong dependence of functional group resolved transverse enhanced relaxation rates on silica pore *S/V*, it is of interest to explore how adsorbate structure correlates with transverse surface 4 relaxivity more closely. Fitted  $\rho_2$  values are summarised in Figure 7(a); the  $\rho_2$  of water is 0.0818  $\pm$  0.0122 μm/s, which is close to the ranges reported previously by D'Orazio *et al*. (0.109-0.214 μm/s for porous silica glass [84]) and Krzyżak *et al*. (0.12-0.17 μm/s and 0.18-0.20 μm/s for mesoporous 7 silica materials MCM-41 and SBA-15, respectively [51]). Notably, for confined alcohols, the  $\rho_2$  value of each hydroxyl group is consistently 5-20 times that of the corresponding alkyl group. We rationalize this difference by recalling that hydrogen bond mediated adsorption interactions will dominate the 10 alcohol/silica interface  $[54]$ . Such interactions lead to short dipolar coupling distances r between surface and adsorbate hydroxyl groups. As surface relaxation rates generally scale with such distances 12 as  $T_{2,\text{surf}}^{-1} \propto r^{-3}$  [85], this adsorption mode will increase hydroxyl surface relaxation rates (leading to 13 large associated surface relaxivity values  $\rho_2 = \lambda/T_{2\,{\rm surf}}$  relative to those of the corresponding alkyl 14 group; the resulting hydroxyl  $\rho_2$  values will also be further enhanced by the surface-adsorbate proton exchange interactions discussed in Section 4.1. It is of further interest to consider that values of the 16 length scale  $\lambda$  (which defines the thickness of the adsorbed surface layer across which surface enhanced relaxation dominates) are therefore expected to be different when considering alkyl or hydroxyl group relaxivity. For hydroxyl groups, we propose that this length scale will be on the order of surface-19 adsorbate hydrogen bonding distances  $(\lambda \sim 3 \text{ Å})$ , while for alkyl groups this may extend one or more molecular layers from the pore surface. We note that these suggestions are in keeping with concept of the distance of closest approach between interacting dipoles within the formal theory of surface relaxation [72].

23 As illustrated in Figure 7(a), alkyl group  $\rho_2$  values for the four primary alcohols investigated are 24 ranked: methanol  $(0.0093 \pm 0.0016 \text{ \mu m/s})$  < ethanol  $(0.0170 \pm 0.0046 \text{ \mu m/s})$  < 1-propanol  $(0.0277 \pm 0.0046 \text{ \mu m/s})$ 25 0.0022  $\mu$ m/s) < 1-butanol (0.0285 ± 0.0036  $\mu$ m/s), while alkyl group  $\rho$ <sub>2</sub> values for secondary alcohols 26 are ranked: 2-propanol  $(0.0280 \pm 0.0055 \,\mu\text{m/s})$  < 2-butanol  $(0.0430 \pm 0.008 \,\mu\text{m/s})$ . These trends track 27 well with the known order of surface affinity within these adsorbates, which increase both with 28 increasing carbon chain length and upon moving from primary to secondary alcohols [49, 54]. In 29 Figure 7(b) we provide a clear illustration of this apparent dependence on molecular structure by 30 evaluating the alky/hydroxyl ratio of each adsorbate. Importantly, this plot demonstrates a strong, 31 linear relationship between transverse surface relaxivity and alcohol structure, providing – to our 32 knowledge – the first evidence of simple, quantitative relationships between surface relaxivity and 33 adsorbate chemistry. Large relative uncertainties in hydroxyl group  $\rho_2$  values unfortunately preclude

the assignment of any significant trends in these data as a function of varying molecular structure.

 Finally, due to the obvious distinction between alkyl and hydroxyl groups along the *T*<sup>2</sup> dimension of the relaxation correlation plots in Figure 3, we further extracted one-dimensional (1D) *T*<sup>2</sup> decays 4 from our 2D correlation data. Calculations of the corresponding  $\rho_2$  values from these 1D data reveal 5 an almost identical correlation with alkyl/hydroxyl ratio as demonstrated in Figure 7(b) (see Supporting Information Note 6), demonstrating that the acquisition of simple 1D *T*<sup>2</sup> data may be applied as a rapid means of assessing functional group resolved transverse surface relaxivities.





**Figure 7**. (a) Transverse surface relaxivities  $(\rho_2)$  of the alkyl group and hydroxyl group of confined polar protic adsorbates in mesoporous silica. (b) Transverse surface relaxivities of the alkyl group as a function in mesoporous silica. (b) Transverse surface relaxivities of the alkyl group as a function of adsorbate alkyl/hydroxyl ratio (acquired from the number ratio of aprotic and protic H atoms). The molecular structure of each adsorbate is indicated in each case, where C, O, aprotic H, and protic H atoms are colored gray, red, blue, and yellow, respectively. Dashed lines in (b) show a linear fit to each data set.



### **5. Conclusion**

2 To summarize, in this study we have investigated the <sup>1</sup>H nuclear spin relaxation characteristics of ten different liquid adsorbates confined within mesoporous silicas with pore sizes between 6 nm and 50 nm. A single relaxation environment was observed for apolar aprotic (cyclohexane), polar aprotic 5 (acetone), and polar protic (water) adsorbates, with their modal  $T_1/T_2$  ratios reflecting increased surface affinity in turn. The different relaxation characteristics associated with the alkyl and hydroxyl groups of seven alcohols (methanol, ethanol, 1-propanol, 1-butanol, 2-propanol, 2-butanol, and ethylene glycol) were clearly distinguished across the full range of material pore sizes examine here, and differences in the modal *T*1/*T*<sup>2</sup> ratios between these moieties related to adsorbate acidity. Both the longitudinal and transverse surface relaxivities of the above adsorbates were evaluated quantitatively via a linear relationship between enhanced relaxation rates and pore structure surface-to-volume ratio, and for the first time, our results demonstrate clear differences in the surface relaxivity values of alkyl 13 and hydroxyl <sup>1</sup>H-bearing moieties on the same molecule; longitudinal relaxivity values were found to be universally lower than transverse relaxivity values, while a direct comparison between alkyl and 15 hydroxyl data reveals that the transverse surface relaxivities of adsorbate hydroxyl groups are  $\geq 5$  times greater than that of the associated alkyl group. Additional trends in transverse surface relaxivity data have also been identified, with alkyl group relaxivities clearly scaling with adsorbate alkyl/hydroxyl ratio.

 Overall, our results display a previously unrealized degree of complexity regarding the nuclear spin relaxation characteristics of confined adsorbate liquids. The clear persistence of functional group resolved relaxation phenomena, demonstrated here across a broad range of short chain polar protic hydrocarbon adsorbates (including the first observation of such phenomenon in polyol saturated media), and across the entire range of material pore sizes assessed, is also expected to facilitate new avenues for the characterization of interfacial processes within optically opaque hydroxylated porous materials, and is of direct relevance to the rational design of heterogeneous catalysts systems, where such interfaces are common. Our data, however, further highlight the significant degree of care required in accurately evaluating adsorption phenomena or material structural properties through NMR relaxation analysis. In particular, the realization of significantly different NMR surface relaxivities 29 associated with different <sup>1</sup>H-bearing groups on the same adsorbate molecule will be critical in avoiding the erroneous interpretation of relaxation data acquired from porous systems imbibed with complex probe fluids, for example in the evaluation of pore size distributions. In future work we will target an extension of these observations to covalently modified pore surfaces, and to an increased range of functional probe liquids.

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# **Author Contributions**

N.R. designed the research study. S.D. performed the NMR experiments with the aid of N.N.A.L. and

analysed the data. L.L. performed the gas sorption experiments. N.R, M.L.J, and E.F.M supervised the

research. S.D. and N.R. wrote the manuscript.

## **Notes**

The authors declare no competing financial interests.

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