Production of Methane by Catalytic Decarboxylation of Methyl Formate as a Liquid Surrogate

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Abstract

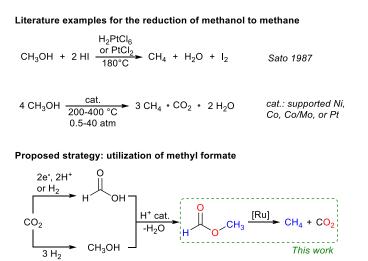
Methane is a widely utilized molecule, primarily sourced from fossil fuels and it finds numerous applications in the energy sector. More sustainable sources of methane include the conversion of organic wastes or gaseous CO_2 . An alternative would be to use a sustainable C_1 intermediate able to form methane. To this end, this work demonstrates the utilization of methyl formate as a liquid surrogate for methane, and its selective decomposition by catalytic decarboxylation. This reaction exhibited excellent yields, exceeding 90%, and the method can be expanded to produce several alkanes from alkyl formates.

Introduction

Natural gas is mostly composed of methane and accounts for 25 % of the primary energy consumed in the world, totaling 4,038 billion m³ in 2021.¹ The current extraction of natural gas is primarily sourced from fossil fuels. However, efforts to transition towards more sustainable productions have led to the development of alternative methods. Some companies aim to reduce their carbon footprint by producing and using local, low-carbon energy. Biogas facilities employ anaerobic digestion to produce methane,² and methane can also be produced by the chemical hydrogenation of CO₂ to methane (the Sabatier reaction).³ The former method relies on methanogens, capable of digesting organic wastes in anaerobic conditions.⁴ This process produces methane in a mixture with CO_2 , which requires further purification. Conversely, the direct CO_2 hydrogenation to methane, often demands harsh conditions (200-400°C, 5-15 bar).

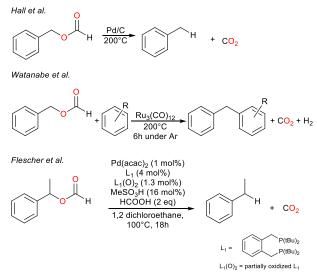
To achieve methane production from sustainable sources and milder conditions, one idea involves conducting the reaction in stages through an intermediary C₁ molecule capable of yielding methane. Methanol emerges as a viable candidate for this intermediary because it is the C₁ compound with the closest oxidation state to methane. It can be produced from CO₂ hydrogenation,⁵ a process implemented in Iceland with the "George Olah CO₂ to renewable methanol plant" demonstrates the maturity of the process.⁶ Nevertheless, the reduction of the C–O bond of methanol is challenging and requires most of the time heterogeneous metal catalysts working under harsh conditions (typical conditions use 300-400°C, under 0.5-40 bar of H₂).⁷ In the homogenous phase, Sato imagined in 1987 a reaction to form methane from methanol in the presence of two equivalents of a strong acid (HI) and a platinum catalyst (Scheme 1, top).⁸ Although the reaction conditions are harsh, this strategy remains, to our knowledge, one of the few homogeneous paths, together with hydrosilylation,⁹ to produce methane starting from methanol. In a broader context, many strategies are used for directly reducing alcohols to alkanes in organic synthesis, including the Barton-Mac Combie reaction, the use of hydrosilanes,¹⁰ the oxidation-Wolff Kischner sequence,¹¹ the dehydration-

hydrogenation sequence,¹² and others.¹³ However, these methods do not apply to methanol and require relatively toxic reagents and/or generate waste that adds to processing challenges. As an alternative to these shortcomings, we propose to reduce methanol with formic acid (FA) via the intermediate formation of methyl formate, FA being itself obtainable from CO₂ electroreduction¹⁴ or hydrogenation (Scheme 1, bottom).¹⁵



Scheme 1. top: Representative examples for the reduction of methanol to methane. Bottom: strategy for the use of methyl formate as a liquid surrogate for methane

Methyl formate is readily obtained by esterification of FA with methanol. When using it as a liquid surrogate for methane, the main challenge relies in designing an efficient decarboxylation of this alkyl formate. Only few examples have been reported in the literature for the decarboxylation of organic formates and they mostly concern activated benzyl formates (Scheme 2). In 1970, Hall used palladium on carbon at 200 °C to convert benzyl formate to toluene with a yield of 97%.¹⁶ Watanabe used benzyl formate as a benzylating reagent for arenes through decarboxylation using [Ru₃(CO)₁₂] at 200 °C.¹⁷ However, the reactive benzyl cation or radical formed under these conditions can activate the C-H bond in benzene, making recombination with the hydride to form toluene challenging with $[Ru_3(CO)_{12}]$ alone. In 2015, Fleischer demonstrated a single-step esterification and reductive decarboxylation from benzylic alcohols and formic acid using a palladium complex and an acid additive.¹⁸ To our knowledge, the only example of activation of the C-O bond of an alkyl formate other than benzyl formate has been reported by Jenner, who showed that under CO, [Ru₃(CO)₁₂], and methyl iodide as an additive, methyl formate isomerizes to acetic acid at 200 °C.¹⁹ Interestingly, minor quantities of methane were also formed as side-products. Herein, we report on the selective decarboxylation of methyl formate into methane, its scale up, and the extension of the catalytic methodology to other alkyl formates.



Scheme 2: State of the art in the decarboxylation of benzyl formates

Results and Discussion

Starting with the system proposed by Jenner, we wished to quantify the amount of methane produced in the absence of CO, upon decomposition of methyl formate with $[Ru_3(CO)_{12}]$: When methyl formate is heated at 160 °C in the presence of 3 mol% of $[Ru_3(CO)_{12}]$ and 20 mol% of Lil in THF, we observed after 24 h a conversion of 55 %, however forming 14 % of methanol and 13 % of methyl iodide, from the decarbonylation and nucleophilic substitution of methylformate respectively. No other product was observed in ¹H NMR, leading us to conclude that the remainder consisted of methane and CO₂, both identifiable in the NMR spectrum and GC chromatogram.

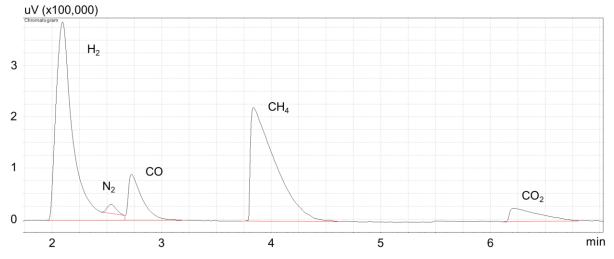
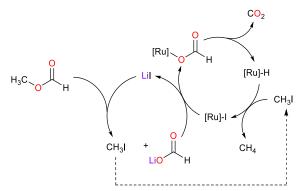


Figure 1: Analysis of the head fraction of the gaseous phase of the experiment with Ru₃(CO)₁₂ as a catalyst (3 mol%) and lithium iodide as an additive (20 mol%) after 3 days of reaction at 160 °C

The decarboxylation reaction thus led to the formation of methane in 28 % yield. In order to improve the efficiency and the selectivity, we considered a plausible mechanism with intertwined catalytic cycles that involve: (i) facilitating the cleavage of the C–O bond of methyl formate by nucleophilic substitution, using lithium iodide, to form methyl iodide and lithium formate, (ii) decarboxylating the formate on the catalyst to form a metal hydride intermediate and (iii), transferring this hydride equivalent to methyl iodide, yielding methane (Scheme).²⁰



Scheme 3: Proposed mechanism for the formation of methane from methyl formate

Table 1 Optimization of reaction conditions										
H_3C H_3C H_4 H_4C H_4 H_4C H_4 H_4 CO_2 H_4 H_4 CO_2 H_4										
	H H		Ru OAc	P Ph Ph Ph Ph Ph Ph Ph Ph Ph Ph Ph Ph Ph						
	1		2	3		4 <i>P</i> = PPh ₂				
Entry	Cat.	Addit.	Solvent	Conv (%) ^[a]	CH ₃ I (%) ^[a]	CH ₃ OH (%) ^[a]	CH ₄ (%) ^[b]			
1	1	Lil	THF-d ₈	23	15	8	-			
2	2	Lil	THF- <i>d</i> ₈	14	< 5	< 5	-			
3	3	Lil	THF- <i>d</i> ₈	95	< 5	7	86			
4 ^[c]	4	Lil	THF-d ₈	100	< 5	< 5	95			
5	4	-	THF- <i>d</i> ₈	-	-	-	-			
6	-	Lil	THF- <i>d</i> ଃ	14	11	< 5	-			
7 ^[c,d]	4	Lil	THF- <i>d</i> ₈	8	5	< 5	-			
8	4	Lil	C_6D_6	12	8	< 5	-			
9	4	Lil	CD₃CN	80	_[e]	9	_[e]			
10	4	Lil	DMF-d7	97	-	24	73			
11	4	Lil /LiBF4	THF- <i>d</i> ₈	19	19	-	-			
12	4	LiBr	THF- <i>d</i> ଃ	69	< 5 ^[f]	< 5	64			
13	4	Nal	THF- <i>d</i> ₈	< 5	-	-	-			
14	4	KI	THF- <i>d</i> ₈	< 5	-	-	-			
15	4	Ph ₄ Pl	THF- <i>d</i> ₈	< 5	-	-	-			

Reaction conditions : 0.14 mmol MeOCHO, 3 mol% catalyst, additive 20 mol%, 0.6 mL solvent, 3 days, 160 °C, [a] Determined by ¹H RMN of crude mixture, mesitylene was used as internal standard, [b] computed by difference between conversion and yield of liquid products (ESI for more details), [c] reaction time of 24 h, [d] 100°C, [e] degradation of acetonitrile, [f] CH₃Br

First, a screening of catalysts was performed, using four ruthenium complexes known for their ability to form hydride species and/or perform decarboxylation reactions.²¹ The decarboxylation of methyl formate was first tested with 3 mol% of [(MACHO)RuH(CO)Cl] 1, efficient in the transfer hydrogenation of esters.^{21a} After 3 days at 160 °C in the presence of 20 mol% of Lil, we observed 23 % conversion, but only methyl iodide and methanol were observed by ¹H NMR in 15 and 8 % yield respectively (Table 1, Entry 1). The acetate complex [(MACHO)Ru(OAc)₂] 2 led to lower conversion and only side-products were detected. (Table 1, Entry 2,). The combination of rac-P4 and [(p-cymene)Ru(OAc)₂] **3** was also tested, as it was described by Gonsalvi et al. to be efficient in the decarboxylation of formic acid to H₂ and CO₂.^{21b} The conversion is significant (95%) after 3 days, and only traces of methyl iodide and 7% methanol are observed (Table 1, Entry 3). Finally, [(triphos)Ru(OAc)₂] 4, also used in the disproportionation of formic acid,²² was found to be the most efficient catalyst and full conversion was observed after 24 h, resulting in the selective formation of methane in 95 % yield: only traces of methanol and methyl iodide were observed (Table 1, Entry 4). Lowering the temperature to 100°C was however detrimental to the catalytic activity, which drastically decreased, and only 8% of methyl formate was converted into methanol and methyl iodide: no methane was observed in ¹H NMR (Table 1, Entry 5). Blank experiments (Table 1, Entries 5 and 6) confirmed that both Lil and the ruthenium complex are required to obtain methane. Furthermore, Lil alone is able to form iodomethane, which supports our mechanistic hypothesis where iodomethane is a key intermediate of the reaction.

The influence of the solvent was then tested: replacing THF with an apolar solvent, benzene d_6 , led to a very low (12 %) conversion and mostly methyl iodide was observed (Table 1, Entry 8,). In acetonitrile, the reaction did not form methane or methyl iodide, and only methanol as well as unidentified peaks were detected (Table 1, Entry 9), which may arise from the decomposition of acetonitrile.²³ In DMF- d_7 , methane was formed in 73 %yield, albeit together with 24 % of methanol after three days of reaction (Table 1, Entry 10).

Other additives were also tested, starting with LiBF₄ which, according to Han,²⁴ facilitates the cleavage of the C–O bond in aryl methyl ethers. In that case however, the catalytic activity was totally lost even though methyl iodide was still formed (Table 1, Entry 11). Switching lithium iodide to use larger cations such as potassium, PPh₄⁺, or sodium was also deleterious to the catalytic activity, and no conversion was observed (Table 1, Entries 13, 14 and 15,). Replacing Lil with LiBr allowed the formation of methane in 64 % yield, with only traces of MeBr and MeOH (Table 1, Entry 12). Such modifications did not improve the catalytic activity further, and we continued to use 3 mol% of **4**, together with 20 mol% of Lil, in THF, at 160 °C, for the rest of the study. Incidentally, on this optimized system, when methyl formate and Lil are replaced by a 1:1 mixture of lithium formate and methyl iodide, we observed, after 24 h at 160 °C, a conversion of 78 % and an intense peak of methane in ¹H NMR, confirming our previous mechanistic hypotheses.

We then tested this system to other alkyl formates to assess its versatility. The reactions were performed under optimized conditions, monitoring the reaction by ¹H NMR until the maximum conversion was reached (Table 2). While full conversion for methyl formate was obtained in 24 hours (Table 2, Entry 1), ethyl formate was decomposed much more slowly (91 % conversion in 7 days), mainly producing ethane together with traces of the decarbonylation product (ethanol) and the elimination product, ethylene (Table 2, Entry 2). No reaction was observed with butyl formate. When benzyl formate was used, full conversion was observed in less than 48 hours, but the selectivity dropped, and only 48 % toluene was obtained (Table 2, Entry 3). Side-products include 32 % of benzyl alcohol and 8 % of benzaldehyde. These

compounds may have been formed through decarbonylation of the formate, leading to benzyl alcohol. The latter can be further dehydrogenated to benzaldehyde.²⁵ To enhance selectivity, we employed the more sterically hindered catalytic system **3** expected to exhibit reduced C–H bond insertion in benzyl formate, thus minimizing decarbonylation. As anticipated, this led to improved selectivity, with 84% toluene observed after 48 hours of heating (Table 2, Entry 4).

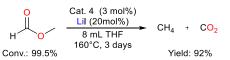
$R \xrightarrow[O]{} H \xrightarrow[]{} \frac{\text{Cat. (3 mol%)}}{\text{THF-d}_{8,} 160 \ ^{\circ}\text{C}} R - H + CO_{2}$								
Entry	, Substrate (R)	Cat.	Reaction time ^[b]	Conv. (%) ^[c]	Observed products			
1	CH ₃	4	24 h	100	CH₄ < 5 % CH₃OH < 5 % CH₃I			
2	CH_3CH_2	4	7 days	91	C_2H_6 major 7 % CH ₃ CH ₂ OH C ₂ H ₄ traces			
3	Ph-CH ₂	4	48 h	100	48 % PHCH₃ 32 % PhCH₂OH 8 % PhCHO 12 % PhCH₂I			
4	Ph-CH₂	3	48 h	98	84 % PHCH₃ < 5 % PhCH₂OH 8 % PhCHO			

[a] Reaction conditions: 0.14 mmol alkyl formate, 3 mol% catalyst, Lil 20 mol%, 0.6 mL THF-*d*₈, 160 °C.

[b] Reaction time until the maximum conversion was reached.

[c] Determined by $^1\mbox{H}$ RMN of the crude mixture, mesitylene was used as internal standard

Finally, to showcase the applicability of the reaction on a larger scale, the decarboxylation of methyl formate was carried out in a 50 mL Parr autoclave (Scheme). For this experiment, the concentration of methyl formate and the volume of the reaction were increased respectively from 0.24 M and 0.6 mL at NMR scale to 0.7 M and 8 mL. After 3 days of reaction, we were pleased to observe an increase in pressure from 1.0 to 5.9 bar, and GC analysis of the gas phase showed that it was composed of a 62/32/6 % mixture of methane, CO₂ and H₂ (the more soluble CO₂ was also detected by NMR, in the liquid mixture, accounting for the lower percentage than methane), corresponding to 91 % yield. In ¹H NMR, only traces of methyl formate remained, together with 7.5 % of methanol. The production of methane reached 132 mL (T = 285 K, $\Delta P = 4.9$ bar) for a 0.36 mL input of methyl formate. This validated that methyl formate could indeed serve as a liquid surrogate containing 27 wt% of methane. It could be used as a means to transport it in a safe manner, and generate methane at high pressure for further use.



Scheme 4 Scale up for the decarboxylation of methyl formate into methane

Conclusion

In this communication, the decarboxylation of methyl formate to methane was achieved using a ruthenium triphos bis acetate catalyst and lithium iodide as an additive in THF, with yields up to 95 %. The reaction involves methyl iodide and lithium formate as key intermediates. A small scope of alkyl formates was tested and the reaction proved applicable to ethyl formate and benzyl formate. A scale-up reaction showcased the production of 132 mL of methane from 0.36 mL of methyl formate, the latter serving as a liquid surrogate containing 27 wt% methane.

Acknowledgements

For financial support of this work, we acknowledge the CEA, CNRS, the European Research Council (ERC Consolidator Grant Agreement no. 818260), as well as VEOLIA and SIAAP. Vincent ROCHER and Sabrina GUERIN (SIAAP) and Guillaume BASLER and Arnaud SELAS (VEOLIA) are warmly thanked for fruitful discussions regarding the valorisation of organic waste and their digestion to methane.

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