

1 **Electrochemical wastewater refining: a vision for circular chemical manufacturing**

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3 Dean M. Miller¹, Kristen Abels¹, Jinyu Guo¹, Kindle S. Williams¹, Matthew J. Liu¹, William A. Tarpeh^{1,2*}

4 ¹Department of Chemical Engineering, Stanford University, Stanford, CA, 94305, United States

5 ²Department of Civil and Environmental Engineering, Stanford University, Stanford, CA, 94305, United
6 States

7
8 *Corresponding author, Email: wtarpeh@stanford.edu. Address: 443 Via Ortega, Room 387, Stanford CA,
9 94305, United States. Telephone: (650) 497-1324

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Abstract

Wastewater is an underleveraged resource; it contains pollutants that can be transformed into valuable high-purity products. Innovations in chemistry and chemical engineering will play critical roles in valorizing wastewater to remediate environmental pollution, provide equitable access to chemical resources and services, and secure critical materials from diminishing feedstock availability. This perspective envisions **electrochemical wastewater refining**—the use of electrochemical processes to tune and recover specific products from wastewaters—as the necessary framework to accelerate wastewater-based electrochemistry to widespread practice. We define and prescribe a use-informed approach that simultaneously serves specific wastewater-pollutant-product triads and uncover mechanistic understanding generalizable to broad use cases. We use this approach to evaluate research needs in specific case studies of electrocatalysis, stoichiometric electrochemical conversions, and electrochemical separations. Finally, we provide rationale and guidance for intentionally expanding the electrochemical wastewater refining product portfolio. Wastewater refining will require a coordinated effort from multiple expertise areas to meet the urgent need of extracting maximal value from complex, variable, diverse, and abundant wastewater resources.

Introduction: Wastewaters: the next frontier for chemical refining

Modern resource sustainability challenges present timely opportunities to circularize conventionally linear chemical processes.

The chemical sciences are responsible for providing commodities that support and advance societal needs at meaningful scale. From fermentation processes developed nearly ten thousand years ago to the discovery and production of medicines like penicillin in the 20th century, chemical processes have been iteratively developed to meet dynamic global demands. Modern chemical refining, which provides chemical commodities from readily available feedstocks, began in the 1850s when the first oil well was drilled in Pittsburgh, Pennsylvania.¹ The first century of refining focused primarily on crude oil distillation for lamp fuel and heat, until the burgeoning 1940s automobile industry increased demand for complex and pure petrochemical fuels. Hydrocarbon cracking, steam methane reforming, and catalytic reforming enabled an expanded petrochemical product portfolio including fuels, lubricants, monomers, and solvents. These advances enabled improvements in quality of life that in turn increased the volume and variety of manufacturing processes that produce commodity chemicals, including Haber-Bosch for ammonia, industrial fermentation for alcohols, and polymerization for synthetic rubbers and plastics. Now centralized refineries and manufacturing facilities convert a few raw material inputs (crude oil, air, natural gas, water, biomass) into the countless chemicals that sustain modern life. Over the course of the 20th century, refineries achieved state-of-the-art integration, flexibility towards variations in raw material, energy efficiency, and above all economies of scale. Generally, today's chemical manufacturing has prioritized high-volume production and distribution and ultimately established linear extract-react-emit economies. As these priorities expand today to include climate change and the environmental and health effects of solid, gaseous, and waterborne anthropogenic pollutants, there is a renewed critical need for chemical manufacturing to fulfill its mandate of meeting humanity's current and future needs at scale. Twenty-first century state-of-the-art chemical manufacturing must enable circular economies by maximizing resource efficiency, minimizing environmental impacts, sustaining quality of life amidst growing pollution, and diminishing feedstock availability.

Wastewater refining can address multifaceted modern challenges.

To meet global sustainability goals, circular chemical manufacturing mines and converts discharges to products and process inputs. Reaching net-zero manufacturing emissions by 2050² has primarily motivated the reuse of solid and gaseous emissions via carbon capture & utilization (CCU),³ plastic recycling,⁴ and refining biomass.⁵ In contrast, liquid emissions (i.e., wastewaters) have been understudied, although they can also help achieve circular manufacturing.^{6,7} Wastewaters carry dissolved contaminants that, left untreated, disrupt coastal and river ecosystem biodiversity, exacerbate food scarcity, threaten human water supplies, and contribute to

72 greenhouse gas emissions.⁸ Instead of emitting or removing contaminants, refining wastewater contaminants
73 into purified products could supply myriad chemical commodities (e.g., fertilizers, monomers, acids, bases,
74 biomass). Potable water is one resource that is already recovered from wastewater, and could address the 40%
75 of the global population that experiences freshwater scarcity.⁹ **Wastewater refining**—the use of chemical
76 transformations to convert wastewater pollutants into tunable manufactured chemical commodities—builds on
77 resource recovery to expand the portfolio of products beyond species already present in wastewaters. This
78 approach can address several sustainability goals, including the United Nations Sustainable Development Goals
79 (SDGs)⁹ designed “to end poverty, protect the planet, and ensure that by 2030 all people enjoy peace and
80 prosperity.” Refining all the resources present in diverse, abundant wastewaters could enhance access to
81 fertilizers (SDG 2), promote responsible resource consumption and production (SDG 12), reduce pollutant
82 emissions (SDGs 13, 14), transform industry and infrastructure (SDG 9), and reduce freshwater scarcity (SDG
83 6). We therefore aim to tackle these circular, sustainable, and climate-adaptive goals by producing chemical
84 products from complex, unrefined wastewater streams.
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87 **Table 1.** Definitions (alphabetical) of terms relevant to wastewater treatment, chemical manufacturing, and
 88 electrochemical wastewater refining.

Term	Definition	Reference
Circular manufacturing	Manufacturing that converts waste products, components, and materials into commodity products	10
Distributed manufacturing	Decentralized production of a commodity at a smaller scale relative to conventional, centralized production of the same commodity	11,12
Electrocatalysis	Electrochemical redox reactions mediated by the transfer of electrons through a catalyst active site	11
Electrochemical separations	Separations processes that involve the use of electrochemical driving forces	13
Potable reuse	The use of highly treated municipal wastewater to augment the raw water supply	14
Primary treatment	The first step of wastewater treatment when materials are removed by flotation or sedimentation	15
Reactive separations	An integration of reaction and separation imposed at the system, unit process, sub-unit process, or molecular scale	16
Resource recovery	Extraction/recovery of valuable entities from waste. In the case of wastewater, recoverable resources include energy, materials/chemicals, and water	6
Secondary treatment	The second step in most wastewater treatment systems when organic contaminants are removed by biological processes	15
Stoichiometric electrochemical conversions	Homogeneous phase reactions facilitated by electrogenerated reactants	17
Tertiary/advanced treatment	Further treatment of wastewater secondary treatment effluent to remove pollutants like nutrients, metals, or trace organics	15
Use-informed research	Scientific investigation driven by context-specific details of the applied problem area to (1) generate fundamental findings relevant to concrete global challenges and (2) generalize mechanistic understanding of applied technologies to diverse use cases	This work
Use-inspired research	Scientific investigation whose rationale, conceptualization, and research directions are motivated by potential use cases	18
Value proposition	A benefit of an approach to meet a stakeholder need	19
Wastewater(s)	Aqueous effluents from domestic, urban, industrial, or agricultural activities	20
Wastewater-based electrochemistry	The science and engineering of electrochemistry applied to wastewater treatment, resource recovery, or refining	This work
Wastewater refining	The use of chemical processes to tune and recover specific, desired products from wastewater resources	This work

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90 To draw an analogy to oil refining: “crude” wastewaters are promising manufacturing feedstocks because
91 they are abundant, resource-rich, and underutilized. Wastewaters are abundant globally— 2.2×10^{15} L of
92 wastewaters (54% of all freshwater withdrawals) are discharged annually from municipalities, agriculture, and
93 industry.²⁰ One hundred moles of wastewater are emitted from anthropogenic practices for every mole of CO₂
94 emitted.²¹ Like oil, wastewaters are rich in chemicals that sustain modern society: nutrients (N, P, K), minerals
95 (Ca, Mg, S), metals (Li, Co, Ni), and fine chemicals (pharmaceuticals) (Table 2). However, 80% of wastewaters
96 are not adequately treated before discharge.²⁰ Current wastewater management simultaneously induces
97 environmental damage and discharges resources worth over USD 100 billion annually (Figure 1). Wastewaters
98 are underutilized because we underestimate their role in chemical manufacturing and because we lack the
99 chemical processes to extract their value. The varied scales of wastewater (e.g., household, municipality,
100 manufacturing site) could facilitate distributed manufacturing, especially if refining processes are co-located
101 with processes that generate wastewater. In turn, distributed manufacturing (Table 1) can reduce transport-
102 related costs and energy consumption.^{22,23} Establishing frameworks for valorizing pollutants in various
103 scenarios, especially as wastewaters increase in volume with population and chemical manufacturing, can drive
104 innovation towards wastewater refining processes.

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106 Wastewater refining will require a library of chemical unit processes that target, convert, and separate
107 specific contaminants into purified products. We focus here on electrochemical wastewater refining processes
108 for three reasons: (1) they valorize pollutants to products, unlike conventional wastewater treatment; (2) they
109 can directly leverage renewable electricity as a driving force; and (3) they enable additional benefits, including
110 process control and modularity. Conventional wastewater treatment tends to focus on meeting discharge
111 regulations via pollutant removal. Recent efforts have aimed to recover existing compounds in wastewater, such
112 as ammonium and phosphate,²⁴ but have not achieved the potential of wastewater refining, which expands the
113 portfolio of possible products via chemical transformations. Thermochemical driving forces are insufficient for
114 refining wastewater resources because of prohibitive energy requirements for phase-change reactions and
115 separations associated with the high specific heat capacity of water. Because 80% of existing separations are
116 thermochemical (e.g., crude oil distillation), separations already account for 10-15% of the world’s energy
117 consumption and are high priorities for decarbonization.²⁵ Wastewater refining requires its own fit-for-purpose
118 driving force to achieve 21st century circular resource economies.²⁶ **Electrochemical driving forces, powered
119 by renewable electricity, are uniquely poised to valorize solutes through electrocatalysis,
120 stoichiometric electrochemical conversions, and electrochemical separations.** Electrochemistry also
121 boasts facile process control (electrode free energy via potential and reaction rate control via current),
122 replacement of chemical oxidants and reductants with electrons, and a high degree of modularity. This
123 modularity is needed to manage the varied composition of wastewaters, which requires tunable processes to
124 convert contaminants into products with varying uses (Table 2). Fortunately, driving selective reactions and
125 separations at solid-liquid interfaces (instead of the bulk solution) is precisely where electrochemistry thrives.
126 The vision of electrochemical wastewater refining is to leverage electrochemical driving forces to circularize
127 and decarbonize manufacturing of chemical products that are indistinguishable at point of consumption from
128 those produced in conventional linear processes.

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Table 2. Aqueous wastewater resources, their uses in as commodity chemicals, and the biogeochemically-relevant wastewaters that contain them.

Wastewater contaminant	Uses	Wastewaters
Ammonia/ammonium	Fertilizer, disinfectant, coolant, precursor to synthetic nitrogenous products	Municipal wastewater, hydrolyzed urine, agricultural/fertilizer runoff
Nitrate	Fertilizer, nitric acid counterion	Agricultural/fertilizer runoff, livestock industry wastewater, post-secondary treatment municipal wastewater, nuclear powerplant brine
Urea	Fertilizer, resin, personal care products	Fresh urine, agricultural/fertilizer runoff
Carbonate/bicarbonate	Buffer, cement	Agricultural/fertilizer runoff, industrial brines, municipal wastewater, urine, geothermal brine
Sulfate	Fertilizer, sulfuric acid counterion	Municipal wastewater, urine, industrial brine, seawater reverse osmosis concentrate, oil & gas produced brine, geothermal brine
Sulfide	Precursor to organosulfur compounds	Post-anaerobic treatment municipal wastewater
Potassium	Fertilizer, counterion to industrial salts/bases, medicine	Municipal wastewaters, urine, seawater reverse osmosis concentrate, geothermal brine, oil & gas produced brine
Magnesium	Fertilizer, structural metal, construction materials, medicine	Municipal wastewater, fresh urine, seawater reverse osmosis concentrate, geothermal brines, oil & gas produced brine
Calcium	Fertilizer, construction materials, personal care products, medicine	Municipal wastewater, fresh urine, seawater reverse osmosis concentrate, geothermal brine, oil & gas produced brine
Phosphate	Fertilizer, detergent, food additives	Municipal wastewater, urine, agricultural/fertilizer runoff, industrial brine
Lithium	Batteries, ceramics, lubricant, medicine	Geothermal brine, lithium-ion battery waste leachate, oil & gas produced brine, seawater reverse osmosis concentrate
Cobalt	Alloys, batteries, catalysts, pigments & dyes	Lithium-ion battery waste leachate
Nickel	Alloys, electroplating, batteries	Lithium-ion battery waste leachate
Copper	Wire & cable, electronics, architecture	Lithium-ion battery waste leachate
Organic matter	Fertilizer, biorefinery feedstocks	Municipal wastewater, urine, livestock industry wastewater, groundwater, landfill leachate

Dyes	Clothing & textiles, personal care products, food preparation, packaging	Industrial wastewater, municipal wastewater
Pharmaceuticals	Medicine	Municipal wastewater, urine, pharmaceutical industry wastewater, landfill leachate
Per- and polyfluoroalkyl substances (PFAS)	Cookware, clothing & textiles, foam, plastic, rubber, personal care products	Municipal wastewater
Arsenic	Lead alloys, car batteries, pesticide, animal feed additive, medicine	Municipal wastewaters groundwater, industrial wastewater
Gold	Coinage, jewelry, electronics	Municipal wastewaters
Silver	Coinage, jewelry, electronics	Municipal wastewaters

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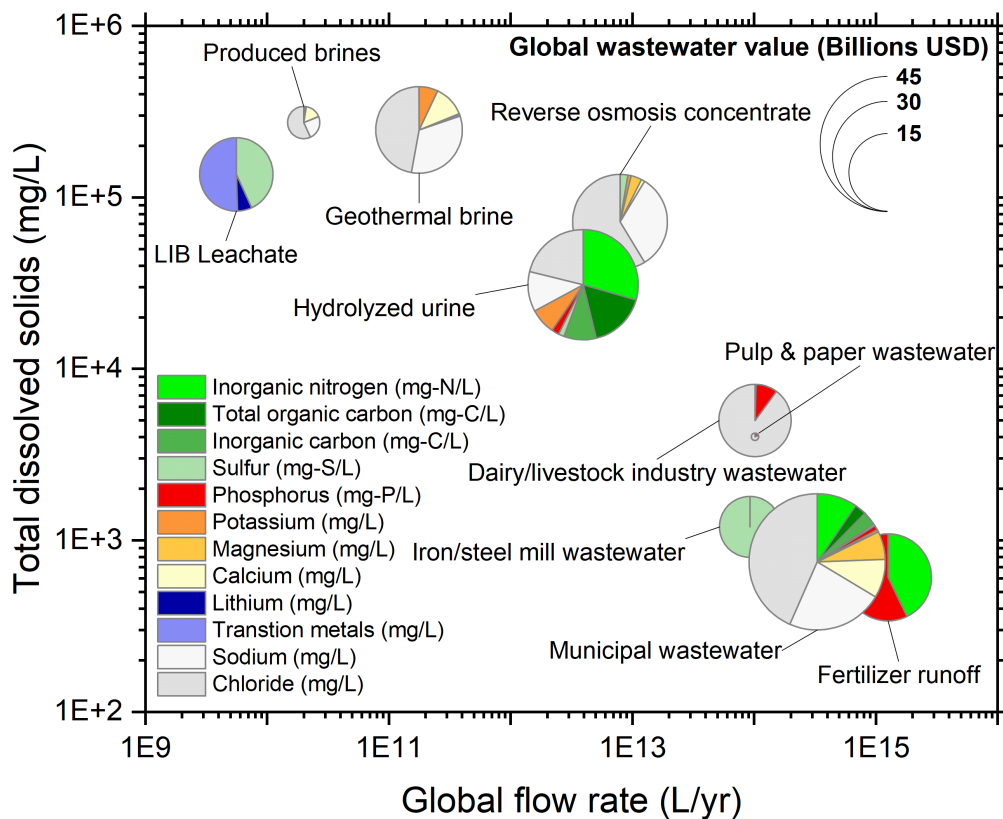
Closing the gap between opportunity and practice for wastewater refining

137 The central thesis of this article is that electrochemical wastewater refining presents tractable challenges
138 and impactful opportunities that require integrated fundamental and applied advances from chemical scientists.
139 Ultimately, wastewater-based electrochemistry must address pervasive sustainability challenges and reach
140 meaningful deployment in 27 years (by 2050), much less time than 20th century refining took to develop (60
141 years). Integrating one unit process into wastewater treatment using the traditional fundamental-to-applied
142 research framework normally take decades;²⁷ the urgent need for refining to achieve the benefits of
143 implementation necessitates coordination across fields and across unit processes as early as possible in
144 technology development.⁶ Use-inspired research that acknowledges these pressing realities is necessary but
145 insufficient to meet the challenge of revolutionizing chemical manufacturing. This perspective describes use-
146 informed research (Table 1) that addresses fundamental, applied, and even policy questions in parallel (rather
147 than in series) and ensures relevance to applications throughout process design while enabling tunability to
148 diverse scenarios. By analogy to wastewater refining, carbon capture & utilization (CCU) is a rapidly maturing
149 field that is investigated academically and pursued industrially; CCU feedstocks range from flue gas to direct air
150 capture, and products include fuels, syngas, and organic commodities.^{28,29} Similar open challenges exist in
151 electrochemical wastewater refining: selective reactions and separations must be improved at multiple scales
152 through sorption, catalysis, transport, separations, and reactor engineering. The breadth of wastewater
153 contaminants and products requires contributions from the fundamental chemical sciences to extract the full
154 potential from wastewater contaminants, especially with selective recovery from complex mixtures. Even for
155 existing water treatment processes, practitioners report one of their largest knowledge gaps as understanding
156 underlying treatment mechanisms.²⁴

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158 Thus, realizing electrochemical wastewater refining will require coordinated electrochemical research in
159 fundamental investigations and applied use cases, which have historically been viewed as disparate or sequential
160 thrusts. We will show that use-informed electrochemical wastewater refining is a prime example of the contrary:
161 that (1) fundamental research can directly serve applications and (2) applied research uncovers new fundamental
162 phenomena. Applying approaches like systems thinking, quantitative sustainable design, and integrated reactive
163 separations^{26,30} can facilitate answers to fundamental molecular scale questions at the same time as, or enabled
164 entirely by, engineering the process itself. Using this integrated approach instead of siloed investigations for
165 electrochemical wastewater refining will accelerate meaningful progress to match the scale and urgency required
166 to address global resource imbalances and environmental perturbations.

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168 We aim not only to encourage crosstalk among interdisciplinary chemical fields, but to scaffold new
169 discussions within the wastewater refining framework. This shift in focus underscores a need to standardize
170 challenges and metrics around a coherent electrochemical wastewater refining vision, which includes three
171 major thrusts: electrocatalysis, stoichiometric electrochemical conversion, and electrochemical separations. We

172 also aim to systematically introduce readers to the scenario-dependent applications, opportunities, and
173 objectives in wastewater using case studies of specific wastewater-pollutant-product combinations. In this
174 perspective, we define the opportunities and associated metrics for fundamental electrochemical refining
175 research (Section 1); highlight progress and challenges toward achieving the wastewater refining vision in
176 electrocatalysis, stoichiometric electrochemical conversions, and electrochemical separations (Section 2); and
177 enumerate specific resource needs and tools we can leverage to achieve the future wastewater refining product
178 portfolio (Section 3). These sections motivate a call to action for electrochemical researchers to elevate use-
179 inspired research to use-informed research in the dynamic and critically important field of wastewater refining.

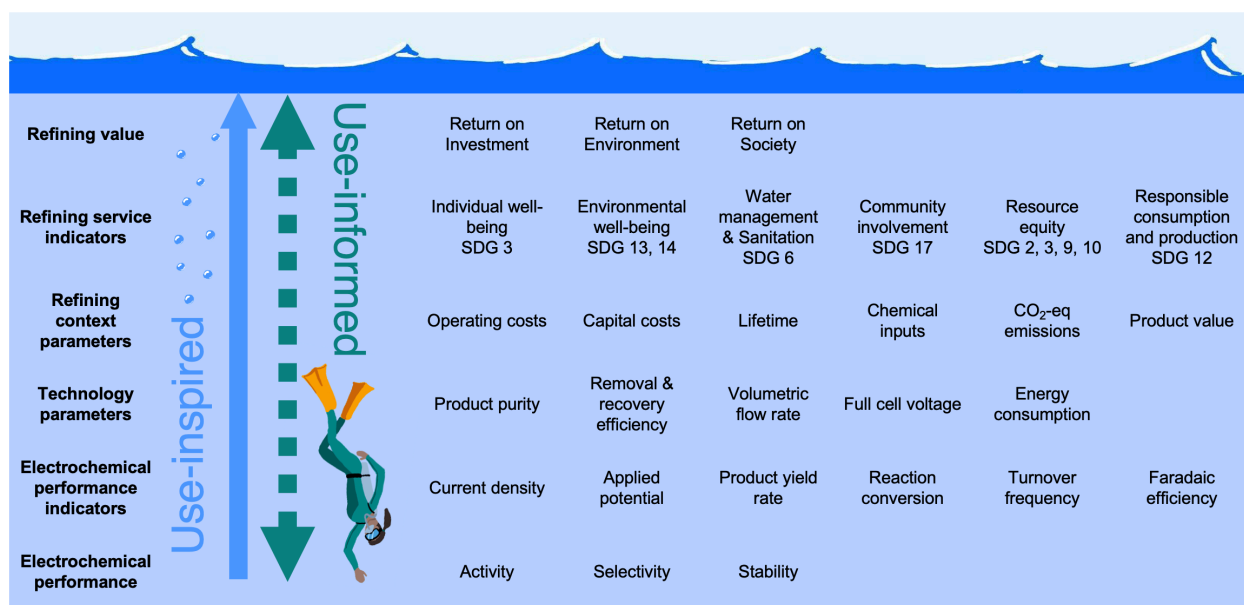


182 **Figure 1.** Pie charts of common wastewaters plotted as a function of global flow/generation rate (x-axis) and
 183 total dissolved solids concentration (y-axis). The size of each slice represents solute mass fraction and the size
 184 of each pie chart represents global annual value. Value was calculated by multiplying the concentration of an
 185 element in each wastewater by the corresponding global flow rate and the consumer price of the most common
 186 product in conventional manufacturing for that element (e.g., urea for inorganic nitrogen). Sodium and chloride
 187 were not included in the value calculations, but we show their mass fractions from available data. Wastewater
 188 composition, volumetric flow rate, and chemical value data was compiled from available data in literature
 189 (Supporting Information).
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 192 Because wastewaters vary widely across several categories, guiding frameworks are needed to prioritize
 193 underexplored opportunities for wastewater refining. Wastewaters are primarily characterized by the domestic,
 194 urban, industrial, and agricultural activities that generate them. They can be further classified as point or non-
 195 point source, where point sources are aggregated at a single location (e.g., sewer municipal wastewater
 196 treatment plants), and non-point sources are released over a large area (e.g., stormwater or fertilizer runoff
 197 initiated by heavy rainfall). Diverse effluent compositions result from several factors, including type of human
 198 activity (municipal, agricultural, or industrial discharges), biogeochemical location (source and destination of
 199 wastewater), and type of treatment (e.g., secondary effluent). Within any of these categories, wastewaters can
 200 vary spatiotemporally and will thus exhibit a range of concentrations of primary (N, P, K) and secondary (Mg,
 201 Ca, S) macronutrients, metals (Li, Mn, Co, Ni, Cu, Zn), and organic and inorganic C (Figure 1).²⁰ This variability
 202 underscores the need for an informed framework to categorize, prioritize, and diversify valorization efforts.
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204 In Figure 1, we propose four core wastewater properties to guide wastewater refining efforts: (1) total
 205 dissolved solids (y-axis, i.e., concentration of solutes), (2) global flow rate (x-axis), (3) theoretical monetary value
 206 of refinable resources (size of each circle), and (4) mass composition of refinable resources (subsections of each
 207 circle; calculation details in Supporting Information). Several observations can be gleaned from this wastewater
 208 refining framework. **First**, the concentration and total volume of target resources vary by several orders of
 209 magnitude. For example, ammonia-nitrogen in human urine is two to three orders of magnitude more
 210 concentrated than nitrate-nitrogen in fertilizer runoff; however, because the global flow rate of urine is nearly
 211 three orders of magnitude smaller than that of fertilizer runoff, the two wastewaters contain similar amounts
 212 of nitrogen (16-30 Tg-N in urine, 19-48 Tg-N in fertilizer runoff).^{20,31-36} **Second**, dissolved solids compositions
 213 vary drastically between wastewaters. **Third**, these variations present numerous value propositions for each
 214 feedstock, especially with fundamental breakthroughs in selective reactions and separations. For municipal
 215 wastewater, several resources are present in comparable concentrations and enable production of commodity
 216 chemicals (e.g., ammonia, nitric acid, sulfuric acid, sodium hydroxide), fertilizers (e.g., ammonium sulfate,
 217 ammonium phosphate, ammonium nitrate, potassium chloride, struvite), building materials (e.g., calcium
 218 hydroxide), and metal smelting precursors (e.g., magnesium chloride).^{34,37,38} In this perspective we focus on the
 219 fundamental refining challenges for commonly detected inorganic constituents, which will likely be integrated
 220 with other circular manufacturing efforts such as biomass refining or plastic recycling.³⁹⁻⁴⁴ Note that estimates
 221 of extractable value from any wastewater are limited by the state of aqueous characterization. Compared to
 222 municipal wastewater and urine, industrial and agricultural effluents are under-characterized in terms of both
 223 target compounds and non-target competitors that may influence refining. To extract maximum value from
 224 wastewater refining, accurate compositions that account for spatiotemporal variability are needed for all
 225 wastewater types.

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Figure 2. A ladder of refining-relevant descriptors (left) that span from fundamental electrochemical performance and performance indicators (bottom), to applied technologies and associated context parameters, to value and value indicators of deployed systems (top). Examples of the metrics for each characteristic level are provided to the right. Examples of refining value indicators are motivated by the Sustainable Development Goals (SDGs) listed. Use-inspired research primarily moves unidirectionally from fundamental to applied, much like bubbles rising in the ocean. Use-informed research moves bidirectionally between fundamental and applied considerations such that (1) fundamental findings remain relevant to concrete value propositions and (2) applied demonstrations are understood mechanistically so they can be generalized to diverse use cases.

237 Any value proposition for wastewater refining contains three parts: a wastewater, a pollutant, and a desired
238 product. Prioritizing which wastewater-pollutant-product combination to pursue requires advancing basic
239 research from use-inspired to use-informed (Figure 2). Use-inspired research, the predominant paradigm, aims
240 to address a relatively distant problem area by generating fundamental knowledge that may lead to practical
241 solutions (upward in Figure 2). In contrast, use-informed studies use context-specific details to prioritize and
242 motivate fundamental questions that more immediately address problems encountered in practice (bidirectional
243 in Figure 2). A use-informed refining study would begin with a top-down approach to discern the economic,
244 environmental, and societal **refining value** provided by scientific innovation. Economic services (ROI, return
245 on investment) generate monetary value from technological investments, environmental services (ROE, return
246 on environment) mitigate deleterious effects of pollutant emissions, and societal services (ROS, return on
247 society) bolster community-level infrastructural capabilities for equitable access to critical resources. These use-
248 informed services should be specific to each wastewater-pollutant-product combination; for example, refining
249 nutrients in municipal wastewater to fertilizers poses substantial ROI, ROE, and ROS. Economically, municipal
250 wastewaters are low-cost chemical feedstocks ($\text{NH}_3/\text{NH}_4^+$, $\text{H}_2\text{PO}_4^-/\text{HPO}_4^{2-}$) that could improve profit
251 margins and introduce new revenue streams for manufacturers. We estimate that recovering nitrogen as
252 ammonia from existing, seweraged municipal wastewaters could yield USD 6.3 billion per year.^{31,45} The
253 environmental benefits of circular fertilizer production are twofold; resituating discharged aqueous nutrients
254 (16.6 Tg-N, 3 Tg-P globally)³¹ mitigates surface water ecosystem disruptions like algal blooms that overconsume
255 oxygen,⁴⁶ and reduces reliance on conventional fossil-fuel powered industrial processes. Electrochemical
256 wastewater refining can achieve a return on society via modular electrified installations that proactively refine
257 wastewaters at their point of generation. Distributed wastewater collection and refining also enables
258 communities to produce their own resources (independent of existing supply chains), promote sanitation
259 access, and mitigate damage to their local ecosystems.^{20,47,48} While ROI is readily and quantitatively comparable
260 to conventional processes, quantitative ROE and ROS requires participation from local stakeholders invested
261 in context-specific environmental justice and community-based implementation. Tools like life-cycle
262 assessment (LCA) and quantitative sustainable design (QSD) can concretize ROE and ROS as **refining service**
263 **indicators**.^{49,50} This relatively mature example of nitrogen and phosphorus fertilizers from municipal
264 wastewater demonstrates the value of use-informed research. Adding the top-down approach beginning with
265 the refining values informs which research questions to pursue and how more fundamental findings are
266 translated to practice.

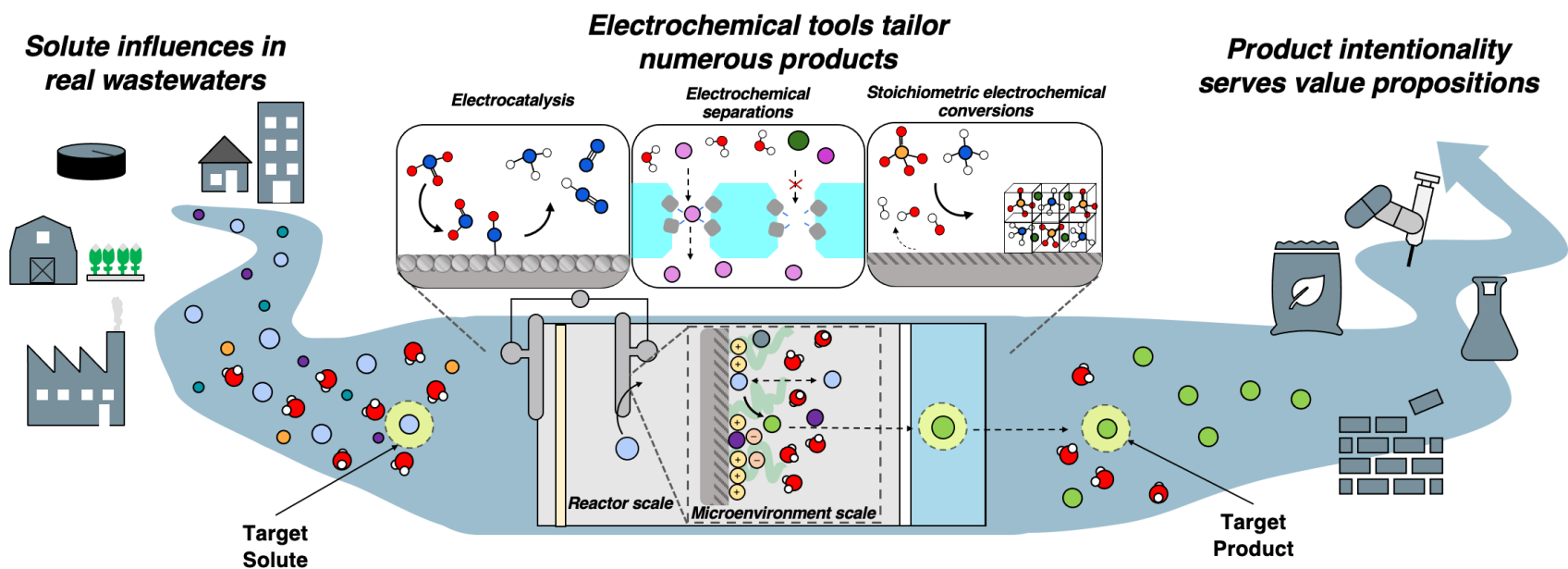
267
268 Continuing with the example of use-informed municipal wastewater refining of nutrients, refining values
269 are connected to research efforts by specific SDGs that serve as **refining service indicators**.⁵¹ The QSD
270 framework supports the informed deployment of sustainability research using a shared lexicon across
271 disciplines that delineates broad qualitative goals (e.g., SDG 6 Clean Water and Sanitation), quantitative
272 indicators that assess progress towards goals (e.g., percentage of population with regular access to improved
273 sanitation), and target values of indicators with endpoints and time tables (e.g., halve the number of people
274 without access to improved sanitation by 2030).⁴⁹ Refining services will be provided by specific technologies;
275 **refining context parameters** highlight the system performance metrics that govern deployment feasibility in
276 specific scenarios. Use-informed research must pursue practical knowledge gaps in these refining context
277 parameters for a specific wastewater-pollutant-product triad to cross the “valley of death” in both directions
278 between fundamental and applied electrochemistry research.⁵² For electrochemical wastewater refining, a survey
279 of wastewater treatment engineers and technicians highlighted the most critical **technology parameters** used
280 to assess process feasibility, including energy consumption (e.g., MJ/kg-N) and removal/recovery efficiency
281 (e.g., normalized to influent concentration as a percentage) in municipal wastewater systems.²⁴ As an example
282 of a study that reports such practical parameters, electrochemical stripping (ECS), an electro dialysis-based
283 ammonia recovery process, was recently evaluated in terms of energy consumption per mass ammonia
284 recovered (compared to a suite of conventional nitrogen removal processes) as a function of influent nitrogen
285 concentration and device operating conditions.⁵³ This study also reports **electrochemical indicators** in
286 experimental nitrogen refining research (e.g., cell potential, current density, product yield rate) and identifies
287 membrane transport as the limiting step for these parameters. In addition to quantifying electrochemical
288 performance and optimization opportunities with indicators relevant to the applied problem space,

289 investigation of ECS in real urine also uncovered unexpected aqueous phenomena: naturally-occurring organic
290 radical scavengers in urine *enhance* performance by impeding ammonia consumption by active chlorine radical
291 species formed at the anode interface.⁵⁴ Bridging fundamental and applied considerations in wastewater
292 nitrogen refining will be paramount as the fields of electrocatalysis (e.g., nitrate reduction), stoichiometric
293 electrochemical conversions (e.g., struvite precipitation), and electrochemical separations (e.g., ammonium-
294 selective electromigration) aim to refine more nitrogenous products from more wastewaters. These use-
295 informed efforts that broaden the scope of wastewater refining will require investigating fundamental
296 **electrochemical performance** (activity, selectivity, and stability) and phenomena in increasingly large-scale,
297 refining-relevant conditions to deconvolute the effects of numerous wastewater constituents and operating
298 conditions. While this discussion has focused on how applied use cases guide the relevance of fundamental
299 studies (i.e., top-down in Figure 2), use-informed research communication should be bidirectional. Achieving
300 feedback loops between applied performance and fundamental insights requires investigating processes with
301 clearly articulated wastewater, pollutant, and product combinations. In the remainder of this perspective, we
302 highlight key advances in specific refining thrusts and identify nascent opportunities that electrochemical
303 researchers can address.
304

Section 2: Advances made and advances needed in use-informed electrochemical wastewater refining

Existing centralized municipal wastewater treatment primarily employs processes that remove pollutants to minimize ecosystem damage. Removal is accomplished in stages, each with distinct target molecules (e.g., dissolved organic carbon) and objectives (e.g., effluent concentration below 10 mg C/L). Primary treatment that separates solids from wastewater was invented in the 1860s to avoid sewer clogging.⁵⁵ The Industrial Revolution accelerated increases in urban wastewater volume due to population growth, which discharged dissolved organic carbon that stimulated aerobic bacterial activity and depleted oxygen in aquatic ecosystems. Secondary treatment was invented in the 1910s to convert this dissolved organic carbon into carbon dioxide using aerobic bacteria in aeration tanks.⁵⁶ Throughout the 20th century, advanced (i.e., tertiary) treatment was developed to target other deleterious pollutants such as nitrogen (nitrification-denitrification), phosphorus (chemical precipitation), bacteria (chlorination/UV), dilute metals (coagulation), and trace organic contaminants (advanced oxidation processes).²⁴ Due to their high operational costs and chemical input needs, municipal wastewater treatment plants are still not universal.^{57–59} More recently, wastewater treatment plants have taken on new roles as water resource recovery facilities, targeting recovery of potable water and commodity chemicals.^{60,61} Whereas removal achieves pollutant mitigation, and recovery achieves circular manufacturing in a limited nature (i.e., separation without conversion), wastewater refining will enable tunable generation of a diverse portfolio of commodity chemicals from wastewaters. As several wastewater treatment plants in the U.S. face significant reinvestment requirements (\$271 billion nationwide) towards the end of their usable lifetime, there are timely opportunities to explore disruptive, integrated electrocatalytic technologies focused on upgrading wastewater pollutant removal to resource refining.⁵⁸

Two major technical advances are needed to realize use-informed electrochemical wastewater refining: (1) improved understanding and control of interfacial microenvironments, and (2) strategic co-investigation of fundamental material properties and relevant operating conditions. In this section, we detail each of these advances across case studies that represent categories of electrochemical wastewater refining techniques: electrocatalysis, stoichiometric electrochemical conversions, and electrochemical separations (Figure 3). Electrocatalysis converts reactive pollutants like nitrate into diverse products. Stoichiometric electrochemical conversions, in which electrogenerated species react with contaminants, captures and purifies elements like phosphorus. Finally, interfacing selective materials with electrochemistry, like selective membranes with electro dialysis, extracts critical materials like lithium from wastewaters. Iteratively engineering catalysts, electrodes, electrolytes, and reactive separations at multiple scales (from microenvironment to full reactor) will accelerate progress towards tunable wastewater valorization and enable informed decisions between available wastewater refining processes.



340
 341 **Figure 3.** Conceptual figure showing the connection between wastewaters, pollutants, and products through electrochemical reactions and separations.
 342 Real wastewaters influence target solute delivery to reactive sites that form diverse products that serve various value propositions. Electrochemical tools
 343 facilitate this diverse product portfolio, and include three major approaches: electrocatalysis, stoichiometric electrochemical conversions, and
 344 electrochemical separations. Molecular-scale phenomena can be controlled at the reactor scale and at the microenvironment scale, allowing for engineering
 345 of reactive separations toward products of interest.
 346

347 **Subsection 2A: Wastewater-based electrocatalysis: Nitrate reduction**

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349 Electrochemical processes can circularize global nitrogen flows, which have been skewed by reactive nitrogen
350 discharges in fertilizer runoff and municipal wastewater generated by Haber-Bosch ammonia manufacturing.
351 The global rate of reactive nitrogen (NH_3 , NO_3^-) generation by Haber-Bosch and N_2 -fixing plants and bacteria
352 is now double the rate of removal by wastewater treatment and biological systems; the nitrogen cycle has been
353 pushed so far past its planetary boundary that there are high risks of irreversible environmental changes.⁶² The
354 field of nitrogen electrocatalysis includes the dinitrogen reduction reaction (N_2RR) that produces ammonia
355 from air, and the ammonia oxidation reaction (AOR) that removes aqueous pollutants as inert dinitrogen; we
356 focus on the nitrate reduction reaction (NO_3RR) to ammonia because it uniquely exemplifies electrochemical
357 wastewater refining by converting an aqueous pollutant into a commodity chemical. In fact, nitrate is the most
358 commonly reported drinking water pollutant violation,^{63,64} and ammonia is the conventional precursor to all
359 synthetic nitrogenous products.^{45,65}

360
361 To date, heterogeneous NO_3RR electrocatalysis has focused primarily on designing catalysts, specifically
362 single metals (e.g., Pt, Cu, Co, Fe, Ti), alloys (e.g., CuNi, PtRu), and semiconductors (e.g., TiO_2 , MoS_2).⁶⁶⁻⁷⁰
363 Modified electrocatalyst composition and structure have been investigated to understand and enhance catalytic
364 performance (overpotential, activity, and selectivity). Nitrate adsorption and reduction to nitrite are typically
365 rate-determining for single metal surfaces.^{71,72} The overall eight-electron, ten-proton transfer reaction pathway
366 diverges from adsorbed NO^* , and catalyst identity influences NO_3RR selectivity toward N_2 , N_2O , and NH_3 as
367 products.⁷³ Catalysts that do not bind strongly to nitrate or nitrogenous intermediates (e.g., Ti) can form nitrite
368 in significant quantities that may be subject to cascading reduction reactions at the catalyst surface.⁶⁴
369 Comprehensive discussions of intrinsic catalyst reactivity are covered in other reviews,^{66,74-76} but the sensitivity
370 of NO_3RR product selectivity to catalyst identity is one avenue for tunable product distributions. Despite
371 abundant fundamental work, few demonstrations of NO_3RR to ammonia have employed real or use-informed
372 simulated wastewaters for comparative catalytic performance.^{77,78} These proof-of-concept developments in
373 wastewater environments enable comparison of novel electrochemical processes to existing wastewater
374 treatment and thermochemical manufacturing. The applied nature of performance in relevant conditions is
375 both informed by and informative for fundamental understanding of the electrolyte and electrocatalyst sides of
376 the catalytic microenvironment.⁷⁹⁻⁸²

377
378 Activity and selectivity of NO_3RR is as much a function of electrolyte composition as of electrocatalyst
379 identity. Inhibitory, promoting, or neutral effects of wastewater environments guide feasibility of direct
380 treatment for specific wastewaters and inform needs for electrolyte engineering. Systematically increasing
381 electrolyte complexity from ideal solution to real wastewater can prioritize the effects of electrolyte properties
382 on observed electrocatalytic mechanisms. A recent framework for aqueous solution complexity in separations
383 research⁸³ can apply to wastewater-based electrocatalysis. Although the first-order rate law of NO_3RR
384 incentivizes the use of highly concentrated wastewaters, the largest refining opportunities exist for dilute
385 agricultural waste streams that contribute the majority of nitrate emissions. Because nitrate and co-existing
386 contaminants vary across wastewaters, insights from studies that mimic highly concentrated wastewaters may
387 not apply to more relevant dilute streams. These differences in bulk electrolyte composition also influence
388 catalytic microenvironment properties (e.g., interfacial pH, ion concentrations), which in turn dictate product
389 selectivity via interactions between electrocatalysts and reactants (both near-surface and adsorbed).⁶³ Freely
390 diffusing NO_3RR intermediates (like HNO_2) can further react in the aqueous phase to produce NH_2OH , N_2O ,
391 or NH_3 . The strong influence of the electrolyte on NO_3RR motivates electrolyte engineering informed by
392 fundamental understanding of the microenvironment with the same level of rigor as in electrocatalyst
393 engineering. Prior NO_3RR work has highlighted strong dependencies of activity and selectivity as a function of
394 bulk nitrate concentration and pH at transition metal and alloy surfaces.^{76,84} Leveraging electroanalysis (e.g.,
395 rotating disk electrode voltammetry, scanning electrochemical microscopy), spectroscopic characterization
396 (e.g., ATR-SEIRAS, XRR), and computational simulation (e.g., continuum modeling, molecular dynamics) can
397 improve molecular scale understanding of the local electrolyte environment that advances experimental
398 observations to mechanistic insights.⁸⁵ Improved spatiotemporal resolution of the microenvironment will guide

399 electrolyte engineering strategies at the macro- (e.g., flow rate, pre-catalysis contaminant separation) and micro-
400 scales (e.g., ionomers to modulate interfacial pH, delivery of reactants, interfacial charge⁸²) to achieve desired
401 product distributions from specific electrolyte compositions. Thus, sole use of catalyst benchmarks such as
402 current density oversimplifies the NO₃RR problem space; supplemental use-informed metrics related to energy
403 consumption, volume-specific conversion, and longevity referenced to a specific wastewater composition are
404 more relevant.

405
406 Electrolyte and wastewater composition can be differentiated via integrated unit processes that combine
407 electrochemical reactions and separations (i.e., reactive separations). Separations and catalysis are normally
408 considered distinct areas of research, but can be integrated as reactive separations across multiple length scales
409 to achieve electrochemical wastewater refining. At the microscale, separations can mediate reactant and product
410 transport between bulk electrolytes and interfacial microenvironments.⁸⁶ In turn, changes in
411 microenvironments, such as basification observed during NO₃RR, can influence catalytic activity and selectivity.
412 At the macroscale, integrated reactive separation processes can leverage membrane-separated cell architectures
413 to control electrolyte composition amidst variable influent wastewater compositions. Furthermore, NO₃RR
414 must be designed for selective product formation and reactive separation of those products from wastewaters.
415 The paucity of separations work to capture dilute nitrate and recover ammonia^{77,87} represents a significant gap
416 in NO₃RR research despite an abundance of work in ammonia recovery from ammonium/ammonia-laden
417 wastewaters using reactive separations architectures.^{53,54} By analogy to highly integrated oil refining, in which
418 waste heat is often reused, electrochemical process intensification could involve integrating cathodic and anodic
419 reactions to maximize input energy efficiency, such as coupled carbon dioxide reduction (CO₂RR) and alcohol
420 oxidation.^{88,89} Multiple refining processes could be integrated, like NO₃RR and struvite precipitation for
421 simultaneous nitrogen and phosphorus recovery. Enhancing refining capabilities can incentivize collection of
422 decentralized wastewaters (e.g., fertilizer runoff) that are seldom collected. Reactive separations present
423 opportunities to broaden and deepen wastewater-based electrocatalysis research centered on circular
424 manufacturing.

425
426 Beyond nitrate reduction, the principles of wastewater-based electrocatalysis can apply to other elements
427 (including carbon and sulfur) and to bidirectional redox reactions, especially those that traverse the same
428 intermediates in forward and reverse reactions (e.g., AOR and NO₃RR). The CO₂RR field has recently
429 interrogated the effect of electrolyte composition, mass transport, electrocatalyst structure, and reactor design
430 on activity and selectivity.⁹⁰ A desire to diversify the CO₂RR product portfolio has motivated selective
431 manufacturing of complex multicarbon products (beyond CO or CH₄) that should be mirrored for wastewater
432 refining.^{91–94} Sulfide oxidation and sulfate reduction could be explored depending on the contaminant,
433 wastewater, and desired product. In both cases, integrated reactions for multiple elements could lead to organic
434 products that contain C-N or C-S bonds, such as amines, ureas, and thioureas.⁹⁵ Tailoring products with
435 oxidation reactions may be of equal importance in wastewater refining, underscored by the roughly equal mass
436 of nitrogen in nitrate- and ammonium-laden wastewaters (Section 1). Generally, understanding the effects of
437 coupled macro- and micro-scale operating conditions (electrolyte, catalyst, potential, pH, mass transport) on
438 intermediate and final product(s) formation remains a gap in refining research.

439
440
441

Subsection 2B: Stoichiometric electrochemical conversions: Struvite precipitation

Stoichiometric electrochemical conversion, or noncatalytic electrogeneration of reactants, can valorize phosphorus discharges that (like reactive nitrogen) exceed planetary boundaries and stimulate eutrophication.⁶² Phosphorus is distinct because it is mined from the earth's crust; its finite nature is predicted to strain the cost and availability of agriculture.⁹⁶ Conventional wastewater treatment employs chemical or biological treatment to remove phosphorus. Chemical addition of calcium carbonate causes precipitation of phosphate minerals; addition of iron (III) chloride or aluminum (III) sulfate cause coagulation and flocculation of insoluble metal hydroxyphosphates.⁹⁷ Enhanced biological phosphorus removal leverages heterotrophic bacteria to store phosphorus and release it after cells are separated from mainstream wastewater.⁹⁷ Upgrading removal processes toward recovery and reuse requires enhanced selectivity among possible products, including multicomponent fertilizers such as ammonium struvite ($\text{NH}_4\text{MgPO}_4 \cdot 6\text{H}_2\text{O}$) and potassium struvite ($\text{KMgPO}_4 \cdot 6\text{H}_2\text{O}$), or other products such as hydroxyapatite ($\text{Ca}_5(\text{PO}_4)_3\text{OH}$; ceramics) and iron phosphate (FePO_4 ; pesticide). All of these minerals require bulk basification and cation addition⁹⁸ that can preclude distributed installations due to prohibitive cost, supply chains, and downstream treatment to balance pH or remove surplus salts. Stoichiometric electrochemical precipitation (a subset of stoichiometric electrochemical conversions) can circumvent chemical additions to recover phosphorus minerals. Two major approaches can be leveraged: (1) electrochemical dosing of Mg using sacrificial anodes⁹⁹ or (2) near-electrode basification using chemically inert cathodes.¹⁰⁰ In contrast to wastewater-based electrocatalysis, stoichiometric electrochemical phosphate precipitation has achieved significant process-focused engineering¹⁰¹ and demonstration in real wastewater environments.¹⁰² These advances have facilitated comparisons of electrochemical struvite precipitation to conventional phosphorus removal and non-electrochemical phosphorus recovery.¹⁰³ However, critical knowledge gaps regarding the role of the electrochemical interface in determining product identity, purity, and uniformity present barriers to rationally engineering operating conditions and cell architectures for generalizable application to various wastewater compositions, use cases, and process needs.

Electrochemical struvite precipitation could benefit from improved fundamental understanding of the reaction microenvironment to inform rational improvements for devices in real wastewaters. To date, electrochemical struvite precipitation work has mapped the effects of macroscale parameters (current density, applied potential, bulk electrolyte composition) to macroscale performance (removal efficiency, product selectivity, energy consumption).¹⁰¹ But precipitation reactions are inherently interfacial, especially when reactants are generated electrochemically and their production rate influences the purity and throughput of recovered products.¹⁰⁴ Both interfacial pH basification¹⁰⁰ and magnesium dosing⁹⁹ are subject to microenvironment effects because the speciation of magnesium precipitates, passivating oxide layers, and dissolved magnesium in the wastewater depends on local electrolyte composition. The microenvironment composition during precipitation is inherently sensitive to local operating conditions like hydrodynamics, electrode material and geometry, and electric field. Microenvironment chemical activities, acid dissociation constants, and solubility products govern the relative rates of competitive precipitation reactions and therefore selectivity. The kinetics of nucleation and growth under supersaturated local conditions can be controlled by modulating reactant concentrations at well-defined electrode-electrolyte interfaces.¹⁰⁵ Improved characterization can provide critical information on interfacial pH and ion concentrations. Electroanalytical tools like rotating disk electrode (RDE), rotating ring-disk electrode, (RRDE) or scanning electrochemical microscopy (SECM) could be employed to directly measure interfacial pH during precipitation.¹⁰⁶ *Operando* infrared spectroscopy could identify transient precipitate speciation. Electrochemical quartz crystal microbalance (EQCM) could measure product formation rate. To translate these interfacial insights to rational choice of operating conditions and cell architectures, multiphysics models (microkinetic, solution phase chemical equilibria, precipitation kinetics) could be developed.¹⁰⁷ With experimentally validated models, fundamental microenvironment research can build on existing observations to make findings generalizable and actionable to different use cases.

Phosphorus must be both precipitated and purified for wastewater refining, which motivates reactive separation unit processes with rationally designed operating conditions and reactor architectures. In addition

494 to connecting interfacial phenomena to observed performance, reactive separations can improve process
495 metrics such as electrode lifetime, energy efficiency, and product selectivity and purity. Direct control over
496 reactant concentrations has been demonstrated with peptide coatings to locally modulate the concentration and
497 conformation of magnesium ions, lowering the overpotential of magnesium oxidation and significantly
498 increasing removal efficiency.¹⁰⁸ Similar methods could co-locate reactants to broaden product selectivity, such
499 as potassium struvite instead of ammonium struvite,¹⁰⁹ by overcoming local K_{sp} challenges. Potassium
500 precipitation presents unique challenges, such as the lower pK_{sp} of potassium struvite (11.7) compared to
501 ammonium struvite (13.26), making supersaturation less favorable.¹¹⁰ Engineering separations at the microscale
502 can overcome this barrier by controlling the reaction interface through hydrodynamics, stabilizing agents, or
503 electrode modifications; it could also control important product quality parameters like crystal size
504 uniformity.¹¹¹ For all products, passivation remains a challenge because it increases energy consumption and
505 lowers activity, even when the cell is operated galvanically (i.e., no electrochemical bias applied).¹⁰⁴ Enhancing
506 electrode lifetime will require strategies to either facilitate or avoid deposition of competing precipitates on the
507 electrode. Replacing or regenerating passivated electrodes in a batch or semi-batch process could be impractical
508 and costly at scale. Fluidized bed reactors with inert beads (e.g., glass) could agitate and remove precipitated
509 products from electrodes.¹¹² This design achieves localized separation of the product from the interface, which
510 will equilibrate by enhancing precipitation. Electrochemical precipitation research will need to focus on the
511 purity and uniformity of the product formed and how separations will be achieved in a scalable reactor system.
512

513 In summary, the effects of fundamental electrochemical reaction phenomena extend beyond catalysis to
514 stoichiometric electrochemical conversions like electrochemical precipitation. In the case of struvite, products
515 not swept away from the interface impart influence reaction kinetics and thermodynamic solid and aqueous
516 speciation. Product removal then readjusts the microenvironment, affecting product speciation and reaction
517 kinetics. Complex interfacial phenomena present a challenge to product selectivity and uniformity, but also an
518 opportunity for product tunability. Importantly, these considerations could build from advances in
519 electrocoagulation,¹⁰³ although purity requirements may be more stringent for precipitation. The fundamental
520 considerations in this section could also extend to stoichiometric reactions like reductive amination where
521 electrogenerated species (aldehydes or ketones generated by alcohol oxidation) react in solution phase (with
522 amines/ammonia and dissolved H_2) to produce higher molecular weight amines.
523

524 **Subsection 2C: Interfacing selective materials with electrochemistry: Lithium recovery**

525
526 Advances in selective separation materials are needed to meet chemical manufacturing product purity
527 standards from impure wastewater sources and complex solute mixtures. In many sectors, traditional
528 separations processes can be replaced with electrochemically-driven separations to reduce energy and chemical
529 inputs. For example, there is urgent demand for critical materials (e.g. lithium, cobalt, and rare earth elements)
530 to support the rapid growth of the energy storage sector.¹¹³ Lithium demand is rising rapidly with the growth
531 of the electric vehicle market; conventional supplies (ores and salar brines) are projected to fall short of demand
532 between 2023 and 2027.¹¹⁴ Lithium-containing oil and gas produced water and geothermal brines (teralibers
533 generated per day) could help close the projected lithium supply-demand gap and introduce an additional
534 wastewater-derived revenue source. Despite many brines containing 50-1000 ppm lithium,^{115,116} the co-
535 existence of other impurities (e.g., Na⁺, Ca²⁺, Fe³⁺, H₂S) at drastically higher concentrations (e.g., >60,000 ppm
536 Na⁺, >30,000 ppm Ca²⁺)¹¹⁷ presents a challenge for high-purity lithium extraction. Conventional separation
537 techniques such as evaporation, crystallization, ion exchange, and solvent extraction exhibit low productivity,
538 high chemical inputs, high water use, and waste generation. Electrochemical separations can overcome these
539 barriers and handle large salinity variations across various relevant wastewaters, including battery leachate,
540 geothermal brines, and oil and gas produced water brines.^{115,118} In fact, the National Alliance for Water
541 Innovation identifies electrified separation processes as one of six main research priorities in their 2021 resource
542 extraction sector technology roadmap.¹¹⁸ The continued development of selective materials, including
543 membranes for selective electrodialysis (S-ED) and electrodes for electrically switched ion-exchange (ESIX), is
544 a critical factor in the advancement and industrial-scale adoption of these processes. Electrified separation
545 processes such as ESIX and S-ED systems could render lithium recovery from wastewaters feasible.^{119,120} Just
546 as improvements in activity, product selectivity, and stability are pursued for electrocatalysis, so are
547 improvements in separation selectivity, ‘activity’ (e.g., flux or adsorption capacity), and stability (e.g., fouling
548 resistance, cyclic regenerability) of selective electrochemical separation materials. These improvements are
549 especially needed for ion-selective separations, a fundamental challenge and emerging research frontier that
550 requires molecular design and evaluation.^{121,122,123} Thus, this section highlights key research challenges and
551 opportunities remaining for interfacing selective materials with electrochemistry in the context of lithium
552 recovery from brines and battery leachate.

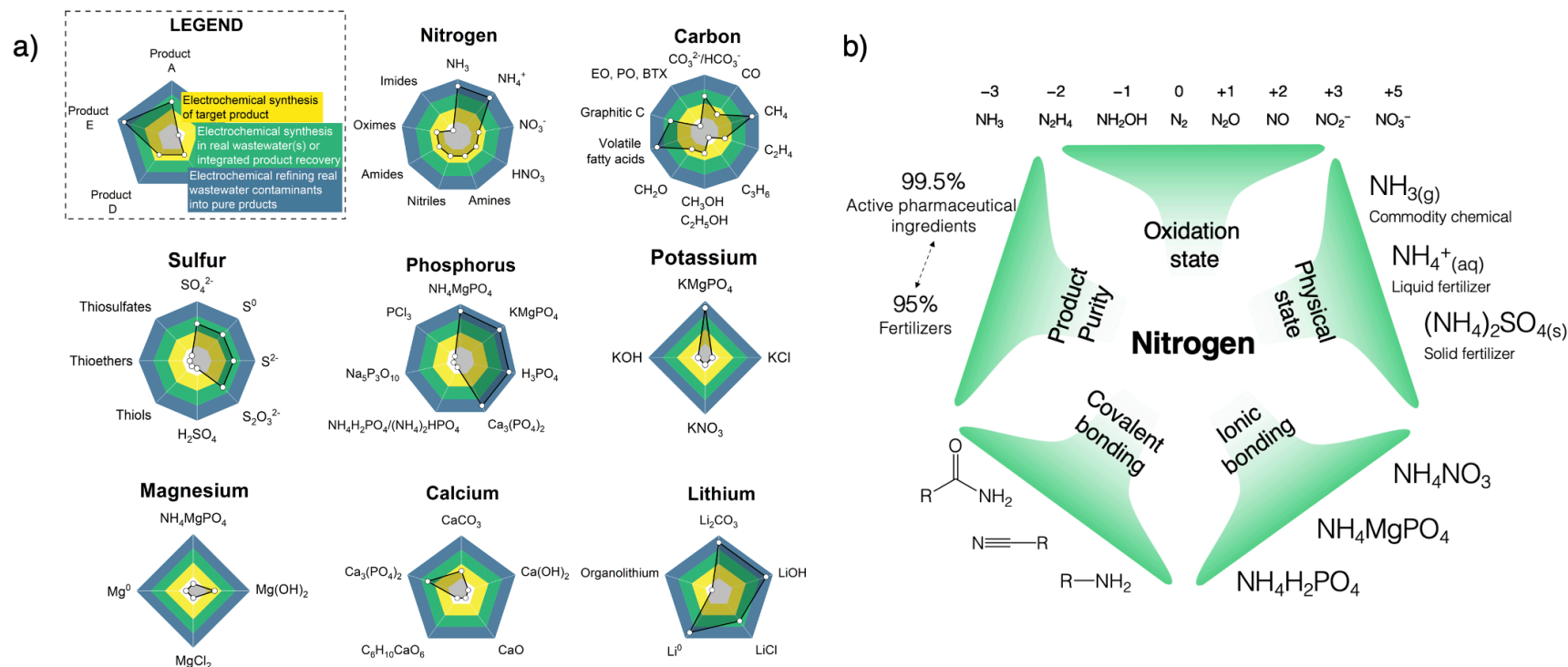
553
554 Industrial implementation of ion-selective separations requires the development of selective materials
555 (electrodes for ESIX, membranes for S-ED) informed by improved understanding of interfacial
556 microenvironments across various wastewaters. For ESIX (where electrochemical biases drive ion separations
557 at the electrode-electrolyte interface), lithium-selective ion insertion materials have been studied, including
558 lithium iron phosphate (LFP) and spinel lithium manganese oxide (LMO). While unamended LFP materials
559 offer promising Li/Mg insertion selectivities (e.g., reducing brine Mg/Li molar ratio from 38.4 to 0.34)¹²⁴,
560 improvements in the more challenging Li/Na monovalent separation are still needed. Electrode coatings have
561 been leveraged to improve intercalation selectivity, including TiO₂ and polydopamine as coatings on LFP
562 electrodes that enhance Li/Na selectivity by factors of 2.1 to 16.4.^{125,126} These hydrophilic coatings were
563 specifically designed to control the interfacial microenvironment by increasing electrode-electrolyte contact and
564 acting as an additional diffusive barrier to Na. This barrier lowers the Li insertion overpotential and enhances
565 Li insertion selectivity. Selective electrodialysis membranes under investigation include cation exchange
566 membranes, ion-imprinted membranes, and mixed matrix membranes containing metal-organic or covalent-
567 organic frameworks.¹²⁷ These membranes are generally less selective than ESIX electrodes, with Li/X
568 selectivities ranging from 6.4 to 65 (compared to 1.8×10^4 for ESIX electrodes).¹²⁸ In the most challenging
569 case of Li/Na separation, most commercial membranes exhibit Li/Na selectivity values near or below one due
570 to the similar characteristics (e.g., size, valence) of Li and Na.¹²⁷ As with ESIX electrodes, improved
571 understanding and control of the microenvironment (electrolyte-membrane interface) is required to enhance
572 membrane separation performance. Considerations of microenvironment thermodynamics and kinetics at the
573 bulk electrolyte-membrane interface are remarkably similar to electrocatalysis: competing cations at water-
574 material interfaces influence near-surface electrolyte transport, transport of species from the solution-
575 membrane interface to the membrane bulk influence near-surface electrolyte restructuring, and the potential

576 drop across a membrane is a function of electrochemical driving force and Donnan potentials (arising from
577 electrolyte and membrane composition). The impacts of these microenvironment features are non-trivial;
578 complex electrolyte compositions and varying driving forces are known to alter membrane separation
579 performance, making material comparison and evaluation challenging.¹²⁹ Selectivity metrics are often measured
580 under diffusive operation, where total ion flux is low and flux-coupling effects may impact selectivity.^{130,131} Use-
581 informed assessment under high flux S-ED conditions could help evaluate the permeability-selectivity trade-
582 off under regimes in which flux-coupling effects are avoided and the depleted diffusion layers at the membrane-
583 solution interface impact kinetic control of ion transport.^{132,133} Continued development of ion transport theory
584 and related transport models would greatly support membrane design efforts; for example, models accounting
585 for the complex architecture of functionalized membranes (e.g., fractional free volume, ion exchange capacity,
586 ion-membrane interactions), the added complexity of multi-component electrolytes, solution-phase hydrated
587 ion migration, and electro-driven permeation would help guide further enhancements in membrane design for
588 enhanced performance in various wastewater compositions and operating conditions.

590 As in electrocatalysis and stoichiometric electrochemical conversions, maximizing electrochemical
591 separation performance requires integrated design of both material properties and operating parameters.
592 Performance includes selectivity, ‘activity,’ and stability that influence metrics such as product purity,
593 component lifetime, and energy consumption. In membrane-based S-ED, an inherent trade-off exists between
594 selectivity and permeability; in ESIX, electrode stability is closely tied to selectivity and the degradation that
595 occurs due to competing ion intercalation. Thus, both materials design and electrochemical process
596 optimization (e.g., reactor design, current density profiles, fouling control) applied to complex, realistic
597 electrolyte compositions are required for a more complete understanding of a technology’s translational
598 potential. With ESIX, pulsed-rest and pulse-rest-reverse electrochemical intercalation methods have been used
599 to lower intercalation overpotentials and limit Na intercalation that could compromise structural stability by
600 expanding electrode lattices.¹²⁵ These advances demonstrate how the combined tuning of selective electrode
601 materials and electrochemical methods can improve selectivity and prolong electrode lifetime (over 10 cycles).¹²⁵
602 However, deployment requires validated stability lasting hundreds to thousands of electrochemical cycles.
603 Because S-ED membrane separation performance depends strongly on operating conditions (electrochemical
604 driving force, electrolyte composition), process-level studies of S-ED permeability and selectivity are also sorely
605 needed to unite fundamental selectivity studies with informed process engineering.¹¹⁹ In both S-ED and ESIX,
606 a shift beyond fundamental batch selectivity studies to flow-through investigations would accelerate translation,
607 enable tuning of operational parameters, and guide the design of next-generation separation materials and
608 processes.

610 Interfacing selective materials with electrochemistry shows great potential for reduced capital costs,¹³⁴
611 chemical inputs,¹³⁵ and emissions¹³⁶ compared to conventional separation techniques.¹³⁷ Recommendations of
612 future directions for electrified separations research are provided in the context of lithium recovery; however,
613 these recommendations apply broadly to ion-ion separations at large, such as metal recovery from acid mine
614 drainage.^{138,139} From a molecular perspective, use-informed design of selective materials can be facilitated by a
615 more well-developed understanding of ion transport mechanisms and the reporting of more standardized
616 selectivity metrics.¹¹⁹ Moving from the molecular scale to the process scale, the integration of selective materials
617 into electrochemical processes also necessitates future work in engineering reactor design, process optimization,
618 and fouling control to bring bench-scale studies to the pilot-scale and beyond.

619 Section 3: Expanding the wastewater refining portfolio
 620



621
 622 **Figure 4.** (a) A comparison of the “state-of-the-art” product portfolios for conventional manufacturing and electrochemical methods. The shape of each
 623 radar plot is set by the number of common conventional products containing each element. The colored levels of (a) indicate three levels of maturity in
 624 refining capabilities. The white innermost level indicates no electrochemical processes targeting the specified product. The yellow first level indicates an
 625 electrochemical process achieves the specified product from a common wastewater contaminant; the green second level indicates growing maturity, either
 626 by electrochemical synthesis using a real wastewater or by integrated product recovery; the blue third level of electrochemical refining is achieved when
 627 integrated recovery of a pure product is achieved in a real wastewater. The third level is not indicating that electrochemical processes are competitive with
 628 conventional manufacturing in terms of cost, rate, efficiency, etc., but that electrochemical research has demonstrated significantly mature refining
 629 technology of a real wastewater contaminant and may be prepared for pilot-scale and field testing. Qualitatively, the vision of electrochemical refining is
 630 to maximize the area of the shaded region for each element. For carbon, we include ethylene oxide (EO), propylene oxide (PO), and benzene, toluene,
 631 and xylene (BTX) as a single product category for brevity. References can be found in the Supporting Information. Panel (b) provides five axes that
 632 electrochemical processes can leverage to diversify products from a wastewater contaminant with nitrogen as an example. Note that not all five axes apply
 633 to every element.

634 One of the hallmark achievements of chemical sciences in the 20th century is the breadth and volume of
635 chemically manufactured products. The electrochemical wastewater refining product portfolio must expand to
636 meet existing and emerging resource needs that are conventionally supplied by centralized refining processes.
637 In Figure 4a, we show progress by element in academic electrochemical research for producing chemical
638 products from common wastewater contaminants represented qualitatively as the shaded area in each radar
639 plot. Compared to conventional manufacturing, the current electrochemical wastewater refining portfolio spans
640 fewer chemical products; target products are not chosen with sufficient rationale to maximize the shaded areas
641 and meet the full potential of circular manufacturing from aqueous waste. Figure 4a presents a framework to
642 analyze the state-of-the-art and future needs of selective target molecule formation from real wastewaters with
643 integrated product recovery. Other circular manufacturing fields have defined the same challenge of expanding
644 future product portfolios, including CCU,⁹² biorefineries,¹⁴⁰ plastic recycling,¹⁴¹ and oil refining beyond gasoline
645 production.¹⁴² Use-informed approaches are needed to define the potential of electrochemical wastewater
646 refining to decarbonize and circularize production of a wide array of compounds from aqueous contaminants
647 (e.g., P, Li, reactive N). In addition, the distributed nature of electrochemical processes can reduce transport
648 emissions, enhance equitable resource distribution, and minimize disposal costs. Broadening the wastewater
649 refining portfolio with use-informed approaches can expand the associated refining values (Section 1) and help
650 reach urgent aspirations including the SDGs, net-zero emissions targets, and increasingly stringent water quality
651 regulations. The rationale for choosing target products must be guided by these refining values, and product
652 requirements must be clearly and explicitly defined based on demands of the specific refining context. To
653 achieve these requirements, electrochemical processes can expand the product portfolio along five distinct axes
654 (Figure 4b): **oxidation state**, **physical state**, **purity**, **ionic bonding** and **covalent bonding**. Each axis for
655 each element should be use-informed by the broader challenges in wastewater treatment and circular resource
656 manufacturing. In the following paragraphs, we provide examples of how each axis influences product utility.
657

658 The **oxidation state** of elements like nitrogen determines the utility of refined products. Inorganic nitrogen
659 oxidation state determines product utility between fertilizers ($\text{NH}_3/\text{NH}_4^+$, NO_3^-), basic chemicals (NH_3 , N_2 ,
660 N_2O , NO , HNO_3), and specialty chemicals (N_2H_4 , NH_2OH). Although ammonia (fully reduced nitrogen) tends
661 to be the most common product targeted in literature, its primary role is as a basic chemical precursor for other
662 commercial nitrogenous products.⁶⁵ Although fertilizer uses 80-90% of produced nitrogen, it only represents
663 40% of the total market value of nitrogen.⁴⁵ Making the diverse products in the nitrogen portfolio requires basic
664 and specialty chemicals that serve as on-site process chemical inputs. For example, selective electrocatalysis
665 processes might reactively separate hydroxylamine or nitric acid as precursors to adiponitrile (nylon).⁶³
666 Additionally, process acids like nitric acid (70 million metric tons globally⁴⁵) and sulfuric acid (220 million metric
667 tons globally¹⁴³) are ubiquitously used to produce a wide portfolio of fertilizers (mono/diammonium phosphate,
668 ammonium sulfate, ammonium nitrate), petrochemicals, polymers, and batteries.¹⁴⁴ Beyond these conventional
669 needs, refining unit processes will also require acids and bases as absorbents (e.g., gas stripping processes),
670 regenerants (e.g., ion exchange), and electrolytes. Electrifying and localizing chemical production will reduce
671 refining technology reliance on existing supply chains and offset emissions from high temperature
672 thermochemical processes (e.g., wet contact process for sulfuric acid, Ostwald Process for nitric acid).¹⁴⁵
673

674 Most conventional “finished” nitrogenous products contain nitrogen in the -3 oxidation state but are
675 themselves not ammonia; they require **covalent bonding** with heteroatom C–N bond formation. Heteroatom
676 bonds like C–N and C–S are crucial functional groups in polymers, solvents, amino acids, and
677 pharmaceuticals.⁹⁵ Wastewater refining could produce the amine, amide, carbamate, thioester, and nitrile
678 precursors for these organic commodities. For example, acrylonitrile is used to make polyacrylonitrile (rubbers),
679 acrylonitrile-butadiene-styrene (plastics), and adiponitrile. Efforts to decarbonize organic production have
680 already incentivized aqueous electrochemical production of traditionally petrochemical products via CO_2RR
681 from waste carbon feedstocks.⁹² CO_2RR now targets complex C_{2+} products like ethylene by designing catalytic
682 interfaces and processes for C–C coupling. Truly negative emissions chemical manufacturing must use
683 emission-less nitrogen and sulfur feedstocks to make heteroatom bonds. Wastewaters are abundant sources of
684 aqueous carbon, nitrogen, and sulfur—a promising combined feedstock for circular organic synthesis instead
685 of conventional siloed reactant sources.

686
687 **Ionic bonding** describes inorganic fertilizers that provide nutrients to plants in various salt mixtures.
688 Large- and small-scale growers use a breadth of fertilizer blends to address variable (e.g., rainfall events), region-
689 specific (e.g., soil consistency/type, soil pH, water and nutrient retention, mineralized N), and crop-specific
690 (e.g., nutrient utilization rate) parameters.¹⁴⁶ Consequently, refining products will need to match flexible farming
691 demands. While electrochemical refining has primarily targeted nitrogen and phosphorus, potassium (the third
692 plant micronutrient) is under explored but strained in sub-Saharan Africa because mineable potash is scarce.^{32,147}
693 Selectively extracting ionic components like potassium could complement nitrogen and phosphorus recovery
694 for complete macronutrient refining of fertilizers and other commodity chemicals, like potassium hydroxide.
695

696 **Product purity** is inextricably linked to the utility of manufactured chemicals, including lithium. Basic
697 chemical grade lithium products used in the glass, ceramics, and grease manufacturing industries typically
698 require 95-99% purity, while specialty battery-grade lithium products (anticipated to account for over 90% of
699 2040 global lithium production end-use) require purities exceeding 99.5%.¹¹⁶ Lithium products are traditionally
700 high-purity crystalline Li_2CO_3 or $\text{LiOH}\cdot\text{H}_2\text{O}$, which may be derived from intermediate lithium products such
701 as concentrated LiCl or Li_2SO_4 solutions. Selective electrochemical separations must account for product value
702 based on purity when developing and assessing new materials, and establishing and reporting benchmarks for
703 selectivity and production rate.
704

705 **Physical state** influences how chemicals will be transported, stored, and used. Aqueous fertilizers are more
706 useful at the point of generation with on-site fertigation systems, while liquid ammonia, solid urea, or crystalline
707 salt products are more amenable to transport because they are more nutrient-dense. Liquid fertilizers provide
708 plants immediate access to nutrients while solid fertilizers like pelletized urea must first dissolve into the soil.
709 Reactive separations could be developed with more intention to match the product physical state to a specific
710 use case. New reactive separations introduce new interfacial phenomena to investigate, exemplifying a use-
711 informed approach that avoids optimizing systems that provide suboptimal solutions.¹⁴⁸
712

713 Target products in electrochemical wastewater refining must be sufficiently tunable and scalable to leverage
714 the distributed nature of wastewater generation. While global production volumes are useful, use-informed
715 local demands and values influence the potential of wastewater-pollutant-product combinations in practice.
716 With narrow product portfolios, refined products would need to be shipped back to centralized plants for
717 thermochemical conversion, which could impose transport costs, energy demand, and environmental impacts
718 that nullify the equity, economic, and environmental benefits of point-of-generation wastewater refining. In
719 short, the scale of refining values cannot be divorced from the scale of wastewater generation.¹⁴⁹
720 Electrochemical wastewater refining could also create entirely new process pathways that do not exist in
721 conventional manufacturing:
722

- 723 (1) In conventional lithium refining, sequential processes are used to transform solutions into Li_2CO_3 and
724 subsequently $\text{LiOH}\cdot\text{H}_2\text{O}$, requiring chemical additions and generating significant quantities of solid
725 waste.¹¹⁶ Integration of membrane electrolysis with electrochemical separation technologies could
726 produce $\text{LiOH}\cdot\text{H}_2\text{O}$ directly from Li-laden wastewaters, avoiding inefficiencies in conventional
727 processes.
- 728 (2) Stoichiometric electrochemical precipitations can be used to extract products beyond fertilizers, such
729 as calcium oxide or hydroxide—key components of concrete, mortar, and plaster—that are normally
730 produced by mining calcium carbonate from large quarries and calcining at 900°C .¹⁵⁰
731

732 Electrocatalysis, stoichiometric electrochemical conversions, and electrochemical separations could enable
733 integrated and distributed manufacturing for numerous products through controlled electron transfers that
734 mimic industrial or biological pathways to common commodities.¹⁵¹ Tunable electrocatalysis for refining may
735 require producing, stabilizing, and separating intermediates and controlling their delivery to distinct active
736 sites.^{152,153} For example, nitrite (formed by NO_3RR at Ti)⁶⁴ could be isolated and directed in cascading reduction
737 reactions toward inorganic products like ammonium, nitrous oxide, or nitric oxide at MoS_2 .^{154,155}

738 Electrocatalytic co-reduction of NO_3^- and CO_2 to form amines and amides is promising for heteroatom bond
739 formation, which could be achieved in complex wastewater electrolytes.^{154,156,157} Co-reduction makes use of
740 reaction intermediates, either surface bound or in the diffusion layer, to form heteroatom bonds.⁹⁴ Thus,
741 engineering electrocatalytic microenvironments (catalyst active sites, interfacial pH, aqueous species transport,
742 intermediate stabilization, pulsed electrolysis¹⁵⁸) could promote more tunable inorganic and organic product
743 formation. A complete electrocatalytic nitrogen refining system might employ multiple catalysts, electrolytes,
744 operating conditions, or reactors for cascading reduction reactions to make a range of nitrogenous products.
745

746 Designing active sites for catalytic reaction, intermediate stabilization, and product separation can expand
747 beyond heterogeneous interfaces, which are abundant but not universal in conventional chemical
748 manufacturing. Enzymes have transition metal centers that exchange electrons with electroactive mediators and
749 active sites with high reactant and product selectivity. Thus, enzymes can be leveraged to enable selective and
750 complex chemical synthesis or to serve as blueprints for the rational design of molecular catalysts.¹⁵⁹ However,
751 molecular catalysts are typically understudied for wastewater applications because they most readily operate in
752 the same phase as reactants and products, making catalyst recovery and reuse difficult. Membrane-separated
753 cells, insoluble catalyst supports, and catalyst immobilization (all of which could be co-developed with catalysts)
754 could serve as viable options for translating homogeneous catalysis into practice.^{160,161} Analogous approaches
755 for heteroatom bond formation in stoichiometric electrochemical conversions are also underexplored. For
756 example, reductive amination to produce amines from ammonia and alcohols or aldehydes is prominent in
757 biomass upgrading, but not for wastewater despite numerous ammonia-rich wastewater feedstocks.^{162,163}
758 Synthesizing higher molecular weight molecules in the wastewater environment can also minimize needs for
759 dedicated separation steps of reaction intermediates⁹⁴ and enable facile separation processes like size exclusion.
760 The concept of biomimicry also applies to selective electrochemical separations.¹⁶⁴ Nature's highly selective
761 separations are achieved by complexation of solutes with enzymes and membrane transporter proteins.^{165,166}
762 These proteins may be purified, extracted, and incorporated into membrane materials or redox-tunable
763 adsorption sites, or otherwise copied through synthetic chemistry.
764

765 The non-exhaustive examples provided are feasible tools that may expand the wastewater refining product
766 portfolio with systematic, use-informed rationale. The reactant and wastewaters from which these products are
767 derived will also need to expand. For instance, there is pressing need to develop oxidation processes to refine
768 prominent (yet under-researched) reduced contaminants like ammonia or sulfide. Additionally, interrogating
769 the full portfolio of feasible products in a process may be useful because even conventionally undervalued
770 products may be intermediates in electrochemical manufacturing. We propose there are countless reactions and
771 separations in chemical refining that electrochemistry may be poised to address, and that electrochemical
772 wastewater refining is a useful framework to pursue exploratory fundamental research toward critically needed
773 applied solutions.
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780 **Concluding Remarks**

781
782 The future of chemical refining needs to achieve multifaceted economic, environmental, and societal value
783 propositions at multiple scales to address the urgency of 21st century imperatives. Climate change, water scarcity,
784 ecosystem health, and equitable resource access are intimately connected to aqueous pollution, highlighting the
785 need and opportunity for circular, electrified chemical manufacturing from wastewaters. Wastewater refining
786 must do more than supplant 20th century linear, centralized chemical refining paradigms. It must adapt to
787 growing and changing communities with complex chemical resource needs and variable wastewater
788 compositions. The sheer number of pollutants, resources, and wastewaters requires systematic, coordinated
789 investigations to make measurable progress in the time scale needed. Solutions must be designed to target value
790 propositions for specific use cases. Studies should draw a clear connection to how they might fit into a process
791 flow diagram within the electrochemical wastewater refining framework. Use-informed studies that translate
792 value propositions to measures of technology performance will ensure relevance to applications throughout the
793 design process.

794
795 Electrochemistry is a powerful tool to refine the numerous pollutants in complex wastewater electrolytes
796 through electrocatalysis, stoichiometric electrochemical conversions, and electrochemical separations. We
797 assert that the research questions underlying burgeoning wastewater-based electrochemical processes are
798 simultaneously fundamental and applied. Electrochemical refining research therefore needs to be as circular as
799 the chemical manufacturing we aim to achieve. Fundamental research cannot be siloed as a linear predecessor
800 to applied research; the feedback between the two will facilitate richer scientific insights and more optimal
801 technologies. To this end, we provide use-informed recommendations for electrochemists and electrochemical
802 engineers:

- 803
804 • Maintain relevance: Electrochemical research motivated by global wastewater challenges should be
805 grounded in quantifiable wastewater-pollutant-product value propositions.
- 806 • Engineer reactive separations processes at multiple length scales: The influence of the
807 microenvironment should be correlated to the performance of the reactor, while controlled
808 perturbations at the reactor scale can be used to investigate the microenvironment.
- 809 • Diversify use cases: Electrochemical phenomena in complex electrolytes should be investigated and
810 explained with sufficient mechanistic insight to tune to multiple value propositions and to integrate
811 with multiple unit processes.
- 812 • Catalogue progress: Quantitative performance of reactor components, reactors, and systems should be
813 compared to conventional benchmarks in both water treatment and chemical manufacturing.

814
815 Electrochemical refining research will rely on broadening participation of traditionally non-wastewater-
816 focused fields to realize a diversified product portfolio. Wastewater refining also provides an opportunity for
817 multiple disciplines to leverage their approaches. Novel reactions and separations will require down-selecting
818 permutations of catalysts, materials, and reactors in use-informed operational frameworks. The recent push to
819 use biological systems like enzymes as blueprints for electrocatalysis is but one example of how seemingly
820 disparate research disciplines converge in the wastewater space.¹⁵⁹ We hope to galvanize cross-disciplinary
821 participation around an understanding of the opportunities and knowledge gaps in wastewater refining.
822 Ultimately, this coordination has the potential to reframe unwanted, underutilized, non-ideal, aqueous pollution
823 as chemical feedstocks to support a modern circular, sustainable, equitable human society.

825 **Supporting Information**

826

827 Supporting tables for wastewater compositions and flow rates, chemical product monetary values, and
828 representative instances of wastewater-relevant electrochemistry. This material is available free of charge via
829 the internet at <http://pubs.acs.org>.

830

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832

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