Enhancement of CO₂ adsorption on activated carbons produced from avocado seeds by combined solvothermal carbonization and thermal KOH activation

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Abstract

A new strategy for ultramicroporous activated carbons production from avocado seeds was developed. Combined solvothermal carbonization and thermal KOH activation was conducted. Solvothermal carbonizations were performed in a stainless-steel autoclave lined with Teflon at the temperature of 180°C for 12 hours in three different liquids (water, methanol, isopropyl alcohol). Chars were activated by KOH. The carbonization combined with activation took place in the oven at 850 °C for one hour. All the samples were very good CO₂ sorbents. The highest CO₂ adsorption at a pressure of 1 bar was achieved for activated carbon produced using isopropanol. The best carbon dioxide adsorption was equal to 6.47 mmol/g at 0°C and 4.35 mmol/g at 20 °C.

Keywords CO₂ adsorption; Carbon capture; Avocado seeds; Ultramicroporous activated carbons; Selectivity; Solvothermal carbonization

Introduction

The emissions of anthropogenic CO_2 have caused a big impact on the global climate (Zhang et al. 2019). The CO_2 is mainly produced by fossil fuels combustion but also accompanies cement production, petrochemical, and other chemical processes (Huang et al. 2022). Activated carbons produced from waste biomass are very promising and low-cost materials for CO_2 adsorption (Creamer et al. 2014).

Some methods of activated carbons production from avocado seeds have been described in the literature. Avocado seeds were applied for activated carbon production for phenol removal from water (Rodrigues et al. 2011). The carbonization was performed in an oven at 800°C and then activated with CO₂ at 900°C. Carbon material with a low specific

surface area (206 m²/g) and a negligible volume of mesopores (0.048 cm³/g) and micropores (0.052 cm³/g) was obtained.

The procedure of activated carbon synthesis in a microwave oven using $ZnCl_2$ as an activator was described (Leite et al. 2017). A material with a relatively high specific surface area (1432 m²/g) and a low volume of mesopores (0.325 cm³/g) and micropores (0.119 cm³/g) was obtained. Such properties allowed this material to be used as sorbent of resorcinol and 3-aminophenol from aqueous solutions.

The procedure of activated carbons production from avocado seeds by pyrolysis at the temperature range 500 - 700°C and activation by $ZnCl_2$ was presented (Leite et al. 2018). Materials with a relatively high specific surface area (1122 - 1584 m²/g), medium mesopore volume (0.475 - 0.691 cm³/g) and low micropore volume (0.084 - 0.156 cm³/g) were obtained. Such properties allowed the use of these activated carbons as sorbents for amoxicillin, caffeine, captopril, enalapril, and meloxicam.

As an activating agent in the synthesis of activated carbons from avocado seeds, sulfuric acid was used at a temperature of 100°C (Bhaumik et al. 2014). A material with a very low specific surface area (14 m^2/g) and a very low pore volume 0.0323 cm³/g was received. This material was used for the adsorption of Cr(VI) ions from aqueous solutions.

The method of activated carbons production based on activation with H_3PO_4 at the temperature range 800 - 1000°C was described (Elizalde-González et al. 2007). The material with the highest blue 41 dye adsorption had a very low surface area (143 m²/g) and a very low pore volume 0.073 cm³/g.

The production of activated carbons from avocado seeds by carbonization in nitrogen or carbon dioxide at 600 - 1000°C was presented (Salomón-Negrete et al. 2018). The obtained materials exhibited very low specific surface area (52 - 300 m²/g), very low pore volume (0.051 - 0.172 cm³/g), and especially micropores (0.019 - 0.122 cm³/g). Such properties allowed using these activated carbons as sorbents of fluorine ions from aqueous solutions.

To the best of our knowledge, avocado seed as a source of activated carbon has been described, as of today, only in six publications listed above. The above review of the literature clearly showed that so far it has not been possible to develop a method of activated carbons production from avocado seeds with high microporosity, which is important for sorbents with high CO₂ adsorption.

In this work, we reported for the first time avocado seeds as carbon precursor for CO₂ sorbents. A new strategy for ultramicroporous activated carbons production from avocado seeds was developed. We demonstrate that by combination of solvothermal carbonization and

thermal KOH activation allowed to produce activated carbons with uniform ultramicropores (\sim 0.50 nm) and with the enhancement of CO₂ adsorption. Under 1 bar, the CO₂ adsorption at a temperature of 0°C ranged from 6.47 to 6.31 mmol/g and at 20°C from 4.13 to 4.13 mmol/g. According to our knowledge, these values are very high.

Materials and methods

Materials

The carbon precursor - avocado seeds were bought from supermarkets in Poland. The following reagents were purchased from Chempur (Piekary Śląskie, Poland): methanol, KOH, HCl 35-38%. Isopropyl alcohol was provided by P.P.H. Stanlab Sp. Z o. o. (Lublin, Poland). All chemicals mentioned above were of analytical grade.

Nitrogen (99.999% purity) and carbon dioxide (99.999% purity), obtained from Messer Polska Sp. z o. o. were used for adsorption and samples characterization.

Activated carbon synthesis

The dried avocado seeds were fine powdered. Solvothermal carbonizations of avocado seed in three different liquids (water, methanol, isopropyl alcohol) were performed in a stainless-steel autoclave lined with Teflon at the temperature of 180°C for 12 hours. The resulting chars were washed with deionized water and dried at 190°C.

The char was mixed with saturated KOH solution. The mass ratio of char : pure KOH was 1:1. The mixture was left for 3 hours and then dried at 190°C.

The dried mixtures were placed in a tubular furnace and heated to 850 °C under nitrogen flow. The carbonization combined with activation took place in the oven for one hour. Then samples were washed with deionized water until neutral pH was achieved. In the end, samples were dried at 190°C.

Characterization of the material

To obtain textural properties, nitrogen sorption isotherms at 77 K were investigated. The relative pressure from $9 \cdot 10^{-8}$ 8 to 0.99 were acquired using a sorption analyzer ASAP 2020 (Micromeritics). Brunauer–Emmett–Teller equation was used to determine the specific surface area (S_{BET}). From 5 to 10 adsorption points from 0.001 to 0.01 p/p₀ were utilized to calculate S_{BET}. Total pore volume was calculated on the basis of the nitrogen volume adsorbed at the relative pressure of 0.99. Micropore volume and pore size distribution were analyzed by DFT method.

The X-ray diffraction (XRD) patterns were collected on a X'Pert–PRO, Panalytical, Almelo X-ray diffractometer with 2 θ from 10 to 100°.

The field emission scanning electron microscopy (FE-SEM) images were taken by a SU8020 Ultra-High Resolution Field Emission Scanning Electron Microscope; Hitachi Ltd, under 5 kV voltage.

A sorption analyzer ASAP 2020 (Micromeritics) was applied to measure volumetric nitrogen and carbon dioxide uptake in a pressure range 0.02 - 1 bar, at a temperature of 0 and 20°C.

Results and discussion

The nitrogen sorption isotherms investigated at temperature of 77 K of activated carbons produced from avocado seeds using various liquids were presented in Fig. 1.



Fig. 1. Nitrogen sorption isotherms for activated carbons produced from avocado seeds using various liquids

On the basis of the isotherm shape illustrating the amount of adsorbed gas at a particular specified pressure, it is possible to define the porosity characteristics of the adsorbent surface (Rashidi et al. 2016). Isotherm can be classified as type I (Sing 1985). As enhanced adsorption at relatively low pressure (less than 0.1 bar) is evident, suggesting that the resulting carbons have a well-developed microporous structure. Moreover, it is visible that a further part of the isotherm reached a plateau that is horizontally aligned with the axis of relative pressure, which suggests that in the structure prevails microporosity (Thommes et al.

2015). The isotherm of C_MeOH was the highest and started from about 400 cm³/g. That means that this activated carbon was the most microporous.

AC	Sbet	Vtot	Vmicro	Vtot/Vmicro
	(m ² /g)	(cm ³ /g)	(cm ³ /g)	(%)
C_H20	1590	0.709	0.549	77.41
C_MeOH	2024	0.926	0.681	73.5
C_IzoOH	1464	0.631	0.506	80.2

Tab. 1. The textural properties of activated carbons produced from avocado seeds using various liquids

Tab. 1 compiled textural properties of activated carbons from avocado seeds. It was stated that all the materials were high porous. The specific surface area ranged from 1464 to 2024 m²/g, depending on the used liquid. The highest value was observed for methanol. The highest pore volume: $0.9262 \text{ cm}^3/\text{g}$ and micropore volume: $0.6813 \text{ cm}^3/\text{g}$ were achieved for methanol, and the lowest data occurred for isopropanol (V_{tot}=0.631, V_{micro}=0.506). The micropore content is very high for all the activated carbons. The highest micropore percentages were achieved for C_IzoOH. The values in Tab. 1 were in good agreement with Fig. 1.



Fig. 2. Pore size distribution for activated carbons produced from avocado seeds using various liquids

Fig. 2. presents the distribution of pore size calculated by the DFT method based on N_2 adsorption measured at 77 K. All the activated carbon exhibited four sharp peaks at 0.50, 0.86, 1.19, and 1.60 nm. The first one is the sharpest and the highest, indicating high content of ultamicropores that play an important role for CO_2 adsorption (Deng et al. 2015; Serafin et

al. 2017). C_H2O and C_IzoOH contained mostly micropores. For C_MeOH, mesopores in the 2-3 nm range were observed. Tab. 1 also showed that the C_MeOH contained more mesopores than the others activated carbons.



Fig. 3. XRD pattern for activated carbons produced from avocado seeds using various liquids

The carbon state of activated carbons was investigated by XRD method. A very broad, deformed peak between $18 - 21^{\circ}$ was observed. This signal can be attributed to the (002) surface of the turbostratic carbon (Wang et al. 2016). The peak of about 44° (100/101) was not visible, confirming the longitudinal dimension, the so-called aromatic sheets, of all the activated carbons were very small, and the materials were primarily amorphous (Wu et al. 2018; Zhang et al. 2022a).



Fig. 4. SEM images of activated carbons produced from avocado seeds using various liquids

Fig. 4 showed SEM images of activated carbons produced from avocado seeds using various liquids. All the materials were similar, with many cavities on the surface of the grains as a result of potassium hydroxide etching at the temperature of 850°C. The system of well-organized macropores was observed.

Potassium hydroxide reacted with carbon and the gases such as CO₂, H₂, H₂O were released making pores in carbonaceous structures (Lillo-Ródenas et al. 2003):

$$4 \text{ KOH} + \text{C} \rightarrow 4 \text{ K} + \text{CO}_2 + \text{H}_2\text{O}$$

 $6 \; KOH + C \; \rightarrow \; 2 \; K + 3 \; H_2 + 2 \; K_2 CO_3$

 $4 \text{ KOH} + \text{C} \rightarrow \text{K}_2\text{CO}_3 + \text{K}_2\text{O} + 2 \text{ H}_2$ $6 \text{ KOH} + 2 \text{ C} \rightarrow 2 \text{ K}_2\text{CO}_3 + 2 \text{ K} + 3 \text{ H}_2$ $4 \text{ KOH} + \text{C} \rightarrow \text{K}_2\text{CO}_3 + \text{H}_2\text{O} + 2\text{H}_2$ $2 \text{ KOH} + 2\text{C} \rightarrow 2\text{CO} + 2 \text{ K} + \text{H}_2$

KOH can also decompose according to:

 $2 \; \mathrm{KOH} \rightarrow \mathrm{K_2O} + \mathrm{H_2O}$

The produced gases can also be involved in various reaction. For example (Yang et al. 2017a):

 $C+ H_2O \rightarrow H_2 + CO$ $CO+ H_2O \rightarrow H_2 + CO_2$ $K_2O+ CO_2 \rightarrow K_2CO_3$ $4KOH + 2CO \rightarrow 2K_2CO + 2H_2O$ $C + CO_2 \rightarrow 2CO$ $2 KOH + CO_2 \rightarrow K_2CO_3 + H_2O$ $2 KOH + C + H_2O \rightarrow K_2CO_3 + 2H_2$

The produced potassium compounds: K₂CO₃, K₂O also could react with the char and influenced on the activated carbon properties.

The textural properties allowed us to assume that activated carbons produced from avocado seed by this new method can be suitable CO₂ sorbents. Tab. 2 showed the adsorption capacity of CO₂ at temperature of 0°C (q_{CO2_0C}) and 20°C (q_{CO2_20C}) and the adsorption capacity of N₂ at temperature of 20°C (q_{N2_20C}) at the pressure of 1 bar. Nitrogen adsorption was investigated in order to calculate the selectivity of CO₂ adsorption over N₂ in binary mixtures.

AC	q co2_0c	q co2_20c	Q N2_20C
	(mmol/g)	(mmol/g)	(mmol/g)
C_H20	6.31	4.30	0.64
C_MeOH	6.47	4.13	0.59
C_IzoOH	6.47	4.35	0.55

Tab. 2. The adsorption capacity of CO_2 and N_2 at 1 bar of activated carbons produced from avocado seeds using various liquids



Fig. 5. CO_2 adsorption isotherms at temperature of 0 °C measured for activated carbons produced from avocado seeds using various liquids

Fig. 5 showed CO₂ adsorption isotherms at the temperature of 0°C. All the isotherms were similar. The highest CO₂ adsorption at 1 bar and 0°C (6.47 mmol/g) was achieved for activated carbons produced using methanol and isopropanol. When water was applied, adsorption was slightly lower, namely 6.31 mmol/g. The adsorption values were very height compared to those presented by other researchers (Tab. 3).

The kinetic diameter of CO_2 molecules is 0.33 nm (D'Alessandro et al. 2010). The pores about two times larger than 33 nm are most favorable for CO_2 adsorption. The adsorption potential affected by CO_2 molecules from opposite walls in such micropores is the highest (Ghimire et al. 2019). All the samples were ultramicroporous, so the CO_2 adsorption was so high.

Biomass	qco2_0c	References
	(mmol/g)	
birch	4.50	(Kishibayev et al. 2021)
amazonian nutshells	5.13	(Serafin et al. 2021)
lignocellulose	5.20	(Parshetti et al. 2015)
walnut shell	5.22	(Yang et al. 2019)
palm sheath	5.28	(Zhang et al. 2022b)
rice husk	5.83	(He et al. 2021)
coconut shell	6.04	(Yang et al. 2017b)
andiroba shells	6.10	(Serafin et al. 2022)
hazelnut shell	6.44	(Ma et al. 2022)
avocado seeds	6.47	This work

Tab. 3. CO2 adsorption at 1 bar, 0 $^{\rm o}C$, and 25 $^{\rm o}C~$ on activated carbons produced from various sources



Fig. 6. CO_2 and N_2 adsorption isotherms at a temperature of 20 °C measured for activated carbons produced from avocado seeds using various liquids

Fig. 6 presented CO₂ and N₂ adsorption isotherms at a temperature of 20 °C. The values of the CO₂ adsorption at higher temperature were lower but still high. The highest CO₂ adsorption at 1 bar exhibited C_IzoOH (4.35 mmol/g), and the lowest adsorption (4.13 mmol/g) was observed over C_MeOH. The values of CO₂ adsorption at 20°C and 1 bar were strongly connected with microporosity, namely $V_{tot/}V_{micro}$ values. As was proved by the others (Wickramaratne and Jaroniec 2013), CO₂ adsorption on activated carbons at ambient conditions is strongly dependent on microporosity (Tab. 1). The decrease of the CO₂ adsorption took place.

Two two-parameter models (Freundlich and Langmuir,) and two three-parameter models (Toth and Sips) were applied to analyse the experimental adsorption isotherms. The Freundlich , Langmuir, Toth, and Sips equations were described in (Ayawei et al. 2017; Serafin et al. 2023).

The applicability of the equations to fit the experimental data was established using the least-squares method. The lowest values of the errors was obtained using Sips model for CO_2 and N_2 adsorption. The Sips model is given by the equation:

$$q = \frac{q_m \cdot b \cdot p^n}{1 + b \cdot p^n}$$

where:

q – the gas equilibrium adsorption at pressure p

p – equilibrium pressure

qm - the saturation capacity

b – equilibrium constant

n - exponential parameter representing the heterogeneity of the material

The obtained parameters were presented in Tab. 4.

Tab. 4. The Sips model	parameters and	l standard	l error ca	alculated	based or	n experimental	data
of CO2 and N2 adsorption	on						

AC	Temp.	$q_{\rm m}$	b	n	Error
	[oC}	[mmol/g]	[bar ⁻¹]		
Carbon dioxide					
C_H2O	0	14.86	0.74	0.76	$3.16 \cdot 10^{-03}$
	20	14.05	0.44	0.82	$1.66 \cdot 10^{-03}$
C_MeOH	0	26.35	0.33	0.77	$2.40 \cdot 10^{-03}$
	20	17.61	0.31	0.83	$6.78 \cdot 10^{-04}$
C_IzoOH	0	18.89	0.52	0.75	$3.44 \cdot 10^{-03}$
	20	12.28	0.55	0.81	$6.27 \cdot 10^{-04}$
Nitrogen					
C_H2O	20	3.53	0.19	0.98	$1.13 \cdot 10^{-05}$
C_MeOH	20	4.12	0.17	0.95	$1.80 \cdot 10^{-05}$
C_IzoOH	20	3.11	0.26	1.00	$1.21 \cdot 10^{-04}$

The saturation capacity decreased with the temperature increase, which confirmed the physical adsorption. The exponential parameters were close to one, proving the surface's homogeneity.

The N_2 adsorption measurements were performed to calculate the CO₂ adsorption selectivity over N_2 . The ideal adsorbed solution theory (IAST) (Myers and Prausnitz 1965) was applied to calculate the selectivity of carbon dioxide over nitrogen at 20°C. The selectivity of g1 over g2 is possible to calculate based on single adsorption isotherms of g1 and g1:

$$S_{(g1)} = \frac{\frac{x_{g1}}{y_{g1}}}{\frac{x_{g2}}{y_{g2}}}$$

where:

 $x_{g1}(x_{g2})$ – the molar fractions of g1 (g2) gas in the adsorbed phase $y_{g1}, (y_{g2})$ – the molar fractions of g1 (g2) gas in the bulk phase.

The accuracy of the IAST calculation was established for many gas mixtures on various sorbents (Herm et al. 2011; Lu et al. 2011).

Based on the IAST theory the selectivity of CO₂ adsorption for the equimolar mixture was calculated according to the equation:

$$S_{CO_2} = \frac{q_{CO_2(p)}}{q_{N_2(p)}}$$

The sorbents may be applied for CO_2 removal from flue gas. The content of CO_2 in off-gas depends on the kind of fossil fuels. If fuel gas is the energy source, the CO_2 concentration is about 10%. For coal burning, CO_2 concentration is equal to 15%. Taking into account, the CO_2 content in flue – gas, the selectivity of CO_2 over N_2 for 10% and 15 % CO_2 content was also calculated.

$$S_{(CO_{2}-10 \text{ or } 15)} = \frac{q_{CO_{2}}(p_{CO_{2}})}{p_{CO_{2}}} : \frac{q_{N_{2}}(p_{N_{2}})}{p_{N_{2}}}$$

 $q_i(p)$ - adsorption value of i at pressure pi

For carbon dioxide, p_{CO2} were equal 0.1 and 0.15. For nitrogen, p_{N2} were equal to 0.9 and 0.85. In order to establish CO₂ and N₂ adsorption at a given pressure, the Sips model was applied.



Fig. 7. The selectivity of CO_2 adsorption for the equimolar mixture of carbon dioxide and nitrogen at a temperature of $20^{\circ}C$

The selectivity of CO₂ adsorption for the equimolar mixture were presented in Fig. 7. The highest CO₂ adsorption was achieved over C_IzoOH activated carbon. Selectivity decreased with increasing pressure. The course of the curves was typical (Kiełbasa et al. 2022).

The selectivities of CO₂ adsorption over N_2 for typical flue gas concentrations 10 and 15% (S_{CO2_10}, S_{CO2_15}) were presented in Tab. 5. The highest selectivity was observed for C_IzoOH.

Tab. 5. The selectivity of CO_2 adsorption over N_2 for typical flue gas concentration 10 and 15% (SCO2_10, SCO2_15) were presented in

AC	Sc02_10	Sc02_15
C_H20	13	12
C_MeOH	12	11
C_IzoOH	17	15

Conclusions

In summary, we synthesized ultramicropore activated carbons from avocado seeds using combined solvothermal carbonization and thermal KOH activation method. The activated carbons with excellent textural properties (pore volume, micropore volume, and specific surface area) were successfully synthesized. All the samples were very good CO₂ sorbents. The micropores were very important for CO₂ adsorption. The highest CO₂ adsorption and CO₂ selectivity over N₂ were achieved for activated carbon obtained using isopropanol that exhibited the highest micropore percentage making this material a promising candidate for carbon dioxide removal from mixtures of gasses. The highest CO_2 adsorption at a pressure of 1 bar was achieved for C_Izo was equal to 6.47 mmol/g at 0°C and 4.35 mmol/g at 20 °C.

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