Enhanced photocatalytic degradation of organic contaminants in water by highly tunable surface microlenses

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² Abstract

Photocatalysis¹ is one of the dominant technologies used to enhance the efficiency of water 3 decontamination with light-based treatments. However, the effectiveness of photocatalysts is 4 usually limited by the irradiation conditions and the properties of the water matrix. In this 5 work, we have demonstrated the capability of surface microlenses (MLs) as a clean technology 6 for more efficient photocatalytic water decontamination. Random or ordered surface MLs 7 were fabricated from simple polymerization of nanodroplets produced in a solvent exchange 8 process. Both random microlenses (MLR) and microlenses array (MLA) could enhance the 9 photocatalytic degradation efficiency (η) of four representative pollutants, including methyl 10 orange (MO), norfloxacin (NFX), sulfadiazine (SFD), sulfamethoxazole (SMX), spiked in 11 ultra-pure water, synthetic natural water, or real river water. By controlling the conditions 12 of light treatment, η could be enhanced by up to 402 %. The effectiveness of surface MLs was 13 validated under both visible LED light and simulated solar light and for two photocatalysts 14 zinc oxide (ZnO) and titanium dioxide (TiO_2) . By reducing the concentration of the pho-15 tocatalysts from 100 to 5 mg/L and the intensity of irradiation intensity from 1 Sun to 0.316 Sun, our findings suggest that the enhancement factor by MLs was higher at lower catalyst 17 concentration, or at lower light intensity. Based on optical simulations and experimental 18 results, we demonstrated that surface MLs optimize the light distribution and promote the 19 formation of active species, which results in the enhancement of η . The use of MLs may serve 20 as a novel strategy to improve the photocatalytic degradation of micropollutants, especially 21 in places where the available light source is weak, such as indoors or in cloudy regions. 22

Keywords: surface microlenses, microlens array, focus effect, photocatalysis, water de contamination

Synopsis: MLs-enhanced photocatalysis degradation of organic contaminants in differ ent water matrices

27 Introduction

Photoreactions are widely applied in different fields,² such as data storage,^{3,4} display,⁵ light 28 generation,^{6,7} polymerization,^{8,9} and light-driven degradation.^{10,11} Many clean-energy tech-29 nologies for water treatment benefits from photoreactions.¹² For instance, solar-based water 30 disinfection utilizes solar energy to inactivate or eliminate pathogenic contaminants in wa-31 ter with portable containers, which is a low-cost and convenient method to provide safe 32 household water.^{13,14} In many types of photoreactions,¹⁵ photocatalysis, which is the pho-33 toreactions accelerated by photocatalysts, is one of the dominant technologies to remove 34 the organic micropollutants in natural water.^{16,17} The most common type of photocatalysis 35 in water treatment is heterogeneous photocatalysis with semiconductor materials, such as 36 titanium dioxide $(TiO_2)^{18}$ and zinc oxide (ZnO).¹⁹ The band gap of ZnO and TiO_2 can be 37 narrowed and be responsive to visible light.^{20,21} For example, the energy gap of ZnO reached 38 2.85 eV,²² while a TiO_2 -based catalyst had a band gap around 2.00 eV.²³ The action spec-39 tra of ZnO and TiO_2 also confirmed their response under visible light and solar light.^{24–26} 40 However, the application of photoreactions is often limited due to the inefficient utilization 41 of light.²⁷ 42

One of the main reasons that restrict the development of solar-driven photocatalytic 43 degradation of organic pollutants in the aqueous environment is the instability of solar light 44 under different scenarios.^{28,29} For example, sunlight is attenuated when the wastewater has 45 high turbidity³⁰ or the rainy and cloudy weather appears.³¹ As a result, the number of 46 photons that can be absorbed into the system decrease, so the activity of photocatalysts is 47 considerably inhibited. In order to maximize the potential of photocatalysts under insuffi-48 cient light, strategies to increase the number of species undergoing a photo process with a 49 given amount of photons are needed. Several strategies have been widely investigated for 50 this purpose, including incorporating light engineering design in photoreactors to improve 51 their performance,^{32,33} establishing a flow reactor to enhance the mass transfer or to shorten 52 the light path,³⁴ and preparing engineering photocatalytic materials for more efficient photo-53

catalysis.³⁵ Introducing lenses into photoreaction systems is a potential alternative because
of the ability of lenses to redistribute light.³⁶ The focusing effect of a lens creates high local
light intensity at the focal point, accelerating the local photoreaction rates.

Surface microlenses (MLs) are novel lenses with small dimensions and a large number 57 fabricated on a solid surface.^{37,38} There are several advantages from surface MLs in a photore-58 action process. First of all, surface MLs can be integrated into various reactors due to their 59 small dimensions.^{39,40} Besides, such lenses have short focal distances with strong near-field 60 focusing effect.^{41,42} Last but not the least, the MLs with well-controlled optical properties and 61 good durability can be prepared and flexibly modified by various methods.^{43,44} Commonly 62 used fabrication methods include laser writing, ^{45,46} hot embossing, ^{47,48} soft lithography, ^{49,50} 63 and drop-templating.^{51,52} The fabrication of surface MLs based on nanodroplet polymeriza-64 tion is one of the promising technologies that are highly tunable and affordable.⁵³ Through 65 this method, surface nano-/microlenses are obtained after the polymerization of surface 66 droplets formed in a solvent exchange.⁵⁴ Notably, the morphology and spatial arrangement 67 of surface nano-/microlenses are tunable⁵⁵ with the method, and the functional components, 68 such as plasmonic nanoparticles,⁴² can be introduced into the system conveniently. 69

In the work conducted by Dongare et al,⁵⁶ the feasibility of integrating lenses with light-70 driven membrane devices for water purification was demonstrated, where a higher energy 71 conversion rate of the device was achieved because of the focus effect of lenses. On a smaller 72 scale, the acceleration of the photoreactions by surface MLs was validated through the in-situ 73 photoreduction of silver nitrate⁴² and the direct photolysis of micropollutants.⁵⁷ Therefore, 74 such surface MLs are also expected to be effective in enhancing the solar-driven photocat-75 alytic degradation of contaminants in water. Implementing surface MLs based on the solvent 76 exchange process as a candidate strategy for enhancing photodegradation efficiency under 77 insufficient irradiation is worthy of investigation. However, the mechanisms of photocat-78 alytic degradation combined with surface MLs have not been explored, so as the influence 79 of the properties of MLs, photocatalysts, light sources, and water matrix on the degradation 80

⁸¹ process.

In this work, we evaluated the performance of surface MLs in enhancing the photocat-82 alytic degradation of four typical organic pollutants in river water, including methyl orange 83 (MO), norfloxacin (NFX), sulfadiazine (SFD), and sulfamethoxazole (SMX).^{58–60} Surface 84 MLs were photopolymerized from the nanodroplets obtained in a solvent exchange process⁶¹ 85 and could be flexibly tailored for better performance. The optimized spatial arrangement 86 of surface MLs was selected based on the light treatment results. The mechanisms of sur-87 face MLs-assisted photocatalytic degradation were investigated with experiments and optical 88 simulation. By tuning the light sources, irradiation intensity, water matrices, and the ge-89 ometry of reactors, the practical conditions with limited irradiation were simulated where 90 the influence of surface MLs on photocatalytic degradation efficiency is studied. Last but 91 not the least, we used two commercial photocatalysts with good stability and durability, ^{62,63} 92 ZnO and TiO_2 , to assess the applicability of surface MLs in varied catalytic processes. The 93 capability of surface MLs in promoting the photocatalytic degradation of organic pollutants 94 in water was validated. 95

³⁶ Experimental section

Fabrication and characterization of random surface microlenses and high-curvature microlens array on planar glass substrate

⁹⁹ Surface microlenses (MLs) were fabricated by photopolymerization of surface droplets under ¹⁰⁰ UV light, as shown in Figure 1 (a). The size and spatial distribution of surface MLs were ¹⁰¹ determined by the diameters and positions of surface droplets. The solvent exchange process ¹⁰² enabled us to flexibly control the formation of surface droplets and further adjust the proper-¹⁰³ ties of surface MLs.^{53,64} In the solvent exchange process, a self-assembled chamber was filled ¹⁰⁴ with a solution (solution A) which was a mixture of monomer, photoinitiator, ethanol, and ¹⁰⁵ Milli Q water. Then, Milli Q water saturated with monomer and initiator (solution B) was inserted into the chamber at a fixed flow rate. Consequently, surface droplets composed of
monomers and the photoinitiator formed on the substrates due to the oversaturation during
the solvent exchange process. When the substrate was homogeneously hydrophobic, surface
droplets grew and coalesced on the substrate, leading to the formation of surface MLs with
non-uniform size and spatial distribution (random MLs, MLR) after UV curing. On the
other hand, surface droplet arrays (MLAs) could be prepared on a pre-patterned substrate
with ordered hydrophobic microdomains.⁵⁵

Random surface MLs (MLR) for photocatalytic degradation system were prepared us-113 ing methyl methacrylate (MMA) ($\geq 98.5\%$, Alfa Aesar) as the monomer and 2-hydroxy-114 2-methylpropiophenone (96%, Fisher) as the photoinitiator. Solution A was prepared by 115 adding 8.0 vol% MMA and 0.8 vol% photoinitiator in 40 vol% ethanol aqueous solution. 116 Then, Milli Q water saturated with MMA and photoinitiator, namely solution B, was in-117 jected into the chamber at a flow rate of 50 mL/h. A glass slide homogeneously hydropho-118 bized with octadecyltrichlorosilane (OTS) (98.9%, Acros Organics, Fisher Scientific) was 119 placed on top of the chamber as the substrate for surface droplets and MLs. The OTS 120 coating of the substrate was prepared according to the procedure described by Zhang and 121 Ducker.⁶¹ The condition used to fabricate the random surface MLs was the optimized one in 122 our previous work.⁵⁷ After the standard solvent exchange process, the chamber filled with 123 liquid was sealed and horizontally set under UV light (365 nm, Analytik Jena UV lamp) for 124 15 min. 125

¹²⁶ Surface ML arrays (MLAs) in the photodegradation processes were fabricated with lauryl ¹²⁷ methacrylate (LMA, Acros Organics) as the monomer in solution A. The solubility of LMA ¹²⁸ in water was lower than MMA, leading to more stable surface droplets during the solvent ¹²⁹ exchange and uniformity of surface MLAs. The pre-patterned substrate used for droplet ¹³⁰ formation was decorated with circular hydrophobic microdomains arranged in an array, fab-¹³¹ ricated by a photolithography process on an OTS-coated glass slide. ⁵⁵ The diameter of each ¹³² circular domain was 5.0 μ m, and the spacing between two adjacent domains was 2.5 μ m.

By repeating the process of solvent exchange and UV curing, MLAs with higher curvature 133 could be achieved.⁶⁵ In this work, three rounds of solvent exchange-UV curing process were 134 performed. Solution A for the solvent exchange process was prepared by adding LMA and 135 the photoinitiator (1/10 volume of LMA) into ethanol, while solution B was the LMA and 136 photoinitiator saturated water. The LMA concentration in solution A in the three rounds of 137 solvent exchange was 2 vol%, 4 vol%, and 2 vol%, respectively, while the flow rate of adding 138 solution B into solution A was 8 mL/h, 4 mL/h, and 4 mL/h, correspondingly. The UV cur-139 ing step lasted for 15 min after each round of the solvent exchange process, after which the 140 high-curvature poly(lauryl methacrylate) (PLMA) MLs were obtained. The curvature of the 141 PLMA ML array could not further increase because the adjacent MLs would be connected 142 if more LMA were added on top of the MLs base. 143

Surface random MLs and ML arrays were observed under an optical microscope equipped 144 with a camera (Nikon H600l and Nikon DSFi3). The lateral size and surface coverage rate of 145 MLs were calculated by analyzing optical photos with Image J. The height of random MLs 146 and high-curvature MLs array was separately characterized with atomic force microscope 147 (AFM, Bruker, tap mode) and confocal microscope (Zeiss Axio CSM 700). A transmission 148 mode confocal microscopy (Leica SP8) was applied to measure the focal distance of MLs 149 in the array. An intensity profile was obtained after a vertical scanning of the ML array-150 decorated substrate. The focal distance was defined as the distance between the brightest 151 point in the intensity profile and the substrate surface. 152

¹⁵³ Fabrication and characterization of MLs-decorated glass vials

The surface MLs can also be immobilized on a curved surface. The inner surface of a glass vial (Fisherbrand Class A clear glass vial) with a volume of 30 mL was hydrophobized by coating OTS onto the surface. The vial with a hydrophobic inner surface was firstly filled with 12 mL of a solution (solution A) composed of 7.6 vol% MMA, 0.8 vol % photoinitiator, 45.8 vol% water, and 45.8 vol% ethanol. Then, Milli Q water saturated with MMA and



Figure 1: (a) Sketch of the fabrication process of surface MLs. The chamber height is 0.57 mm, the width is 12.2 mm, and the length is 56.0 mm (b) The experimental setup of light treatment with surface MLs and distributed catalysts particles. (c) Chemical structures of photodegraded pollutants, including methyl orange (MO), norfloxacin (NFX), sulfadiazine (SFD), and sulfamethoxazole (SMX)

photoinitiator (solution B) was dripped into the standing vial through two tubes and two 159 syringe pumps. The ends of the tubes were set at the opening of the vial, on the left side 160 and right side of the vial, respectively. The flow rate in each tube was fixed at 3 mL/min. 161 To fully replace solution A, 80 mL of solution B was added to the vial. During the solvent 162 exchange process, the excess liquid was discharged from the vial from the opening. After 163 the solvent exchange process, the vial was sealed and set under the UV lamp for 20 min. 164 After removing all remaining mixtures and the washing step, the PMMA MLs-decorated vial 165 was prepared. The morphology of the MLs-decorated vial can be observed with an optical 166 microscope. All the parameters mentioned above were optimized in our previous work.⁵⁷ 167

¹⁶⁸ Optical simulations of surface MLs on planar substrates

The optical simulations of surface MLs on planar substrates were conducted with Zemax 169 OpticStudio. The glass substrate decorated with MLs was set in a horizontal plane (X-Y 170 plane). A plane wave light source was set perpendicular to the horizontal plane (along the 171 Z axis) with an intensity of 21.64 W/cm^2 . Five horizontal light-flux detectors were set at 172 different depths in the solution below the MLs-decorated substrate to demonstrate the top-173 view light irradiation profiles of both MLR and MLA. A rectangular X-Z plane monitor 174 which crossed through the center of a single ML in the array was also designed to describe 175 the cross-sectional irradiation profile of the ML. 176

¹⁷⁷ Photocatalytic degradation of pollutants with surface MLs

The surface MLs were utilized in the photocatalytic degradation of common pollutants in natural water and wastewater to enhance the photodegradation efficiency (η). To evaluate the performance of random MLs and high-curvature ML array, the planar substrate with immobilized surface MLs was assembled in a homemade chamber for the light treatment of water that contained pollutants.(Figure 1 (b)) The light treatment was also conducted in the PMMA MLs-decorated glass vials to evaluate the efficiency of MLs on a curved surface on a larger scale. The pollutants involved in the degradation experiments include methyl
orange (MO, 85%, Sigma-Aldrich), norfloxacin (NFX, Alta aesar), sulfadiazine (SFD, 99.0101.0%, Sigma Aldrich), and sulfamethoxazole (SMX, analytical standard, Sigma Aldrich).
The aqueous solutions of these pollutants with the analyte concentration of 5 mg/L were
prepared with ultra-pure water (produced by Milli-Q Direct 16), synthetic river water, or
real river water as the solvent. For the solution with ultra-pure water as the solvent, the pH
value was measured at around 7 with a pH meter (Accumet AE150, Fisher Scientific).

To prepare the synthetic river water, 52.19 mg $Na_2SO_4 \cdot 10H_2O$ (Sigma Aldrich), 4.08 mg 191 $NaNO_3$ (\geq 99.0%, Sigma Aldrich), 106.96 mg $CaCl_2 \cdot 10H_2O$ (Sigma Aldrich), 100.81 mg 192 $NaHCO_3$ (certified ACS, Fisher Chemical), 101.30 mg $MgSO_4 \cdot 7H_2O$ (Fisher BioReagents), 193 2.56 mg humic acid (technical grade, Aldrich), and 5.32 mg alginic acid (Acros organics) were 194 dissolved in 1 L ultra-pure water. The real river water was collected from Whitemud Creek 195 to the North Saskatchewan River in Edmonton, Alberta, Canada at 9:30 am on April 26, 196 2022. Both the synthetic water and real river water were characterized by a total organic 197 carbon (TOC) analyzer (TOC-L Series, SHIMADZU), a pH meter (Accumet AE150, Fisher 198 Scientific), and ion chromatography (Dionex ICS-5000, Thermo Scientific). The synthetic 199 river water was at a pH value of 7.3, with a TOC value of 3.8 mg/L, and a COD value of 200 9.2 mg/L, while the river water was at a pH of 7.5, a TOC value of 25.6 mg/L, and a COD 201 value of 163.3 mg/L. The concentrations of ions in the synthetic are displayed in Table 1. 202 SMX and MO were spiked in the synthetic river water and the real river water for the light 203 treatment with the same concentration of 5 mg/L. 204

Table 1: Concentration of ions in the synthetic water (Unit: mM)

Ion type	$SO_4{}^{2-}$	Cl^{-}	NO_3^-	Na^+	Ca^{2+}	Mg^{2+}
Conc./mM	8.3	5.3	0.046	2.1	0.85	0.47

One of the commercialized photocatalysts, zinc oxide (ZnO, certified ACS powder, Fisher Chemical), was dispersed in the aqueous solutions containing different types of pollutants

by a sonication step for 20 min. All the solutions were stored in a dark environment at a 207 temperature of 4 °C except the light treatment process. The catalyst was dispersed in the 208 aqueous solutions with sonication in the dark environment for 30 min to ensure sufficient 209 adsorption of the pollutant on the surface of the catalysts. To assess the performance of 210 surface MLs with varied amounts of ZnO, multiple concentrations of ZnO dispersed in the 211 pollutant solutions (ultra-pure water as the solvent) were used, including 5 mg/L, 10 mg/L, 212 50 mg/L, and 100 mg/L. In addition to ZnO, titanium dioxide (TiO_2 , 21 nm primary particle 213 size, \geq 99.5%, Aldrich chemistry) was used to verify the efficiency of surface MLs under 214 different types of catalysts. To compare the performance of MLs when using two types 215 of catalysts, the initial concentrations of TiO_2 and ZnO were set at 5 mg/L. The band 216 gap of ZnO and TiO_2 was 3.26 eV and 3.25 eV, respectively, which were measured with 217 diffusion reflectance spectrum (Hitachi U-3900H) and Tauc plot (shown in Supplementary 218 information, Figure S1 (c-d)).⁶⁶ 219

Both the visible LED lamp (SOLIS-3C, Thorlabs) and the simulated solar light (SS200AAA 220 Solar Simulation Systems, Photo Emission Tech) were used as light sources for the photo-221 catalytic degradation of pollutants in water. The distance between the upper surface of the 222 reactor and the light source was fixed at 23.5 cm for the visible light LED and 35.7 cm for 223 the simulated solar light. A series of irradiation conditions (shown in Table 2) were tested 224 in this work by changing the light sources, the glass substrate, and the type of surface MLs. 225 The spectra of the irradiation above the reactors were collected with a portable spectrometer 226 (StellarNet Inc) at the top position of reactors, as shown in Figure 2 (a). In order to assess 227 the influence of the irradiation conditions listed in Table 2 on the irradiation exposed to the 228 treated solution, the spectra of light that transmitted through the top surface of the reactor 229 (Figure 2 (b-g)) were obtained by setting the detection sensor of a spectrometer under the 230 top surface of different reactors. The light intensities of the light sources were adjusted to in-231 vestigate the influence of the light intensity on the MLs-enhanced photocatalytic degradation 232 process. 233



Figure 2: Spectra of light from visible LED lamp (intensity: $21.64 W/m^2$) and from simulated solar light (intensity: 1 Sun) at the position of light treatment reactor. (a) Spectra of light from the visible LED lamp after transmitting through the air or top surface of the reactor. The zoomed-in spectra are shown in (b) (from 415 to 515 nm) and (c) (from 585 to 775 nm). (d) Spectra of the light from simulated solar light after transmitting through the air or the top surface of the reactor. The zoomed-in spectra are shown in (e) (from 285 to 435 nm) and (f) (from 820 to 775 nm).

Name C_0	Light source	Substrate type	MLs type
L-air		/	/
L-no MLs	Visible LED	Planar glass substrate	/
L-MLR		Planar glass substrate	MLR
L-MLA		Planar glass substrate	MLA
L-vial		Glass vial	/
L-MLs vial		Glass vial	MLR
S-air		/	/
S-no MLs		Planar glass substrate	/
S-MLR	Simulated solar	Planar glass substrate	MLR
S-MLA		Planar glass substrate	MLA
S-vial		Glass vial	/
S-MLs vial		Glass vial	MLR

 Table 2: Irradiation conditions

All the light treatments involved in this study are summarized in Table 3, and each con-234 dition is represented with its irradiation condition (listed in Table 2), the type of catalysts. 235 and the concentration of catalyst (unit: mg/L). The MLs-involved photocatalytic degrada-236 tion process was studied by various analytical instruments. The degradation efficiency (η) 237 is calculated based on the equation (1), where C_i is the initial concentration of a pollutant 238 after the adsorption of pollutants reached equilibrium and C_f is the final concentration of 239 the pollutant after the light treatment. For the solution containing pollutants prepared 240 with ultra-pure water, the concentration change of a pollutant could be identified with UV-241 visible spectroscopy (UV-vis, Thermo fisher, Genesys 150) based on the Beer-Lambert Law. 242 According to the Beer-Lambert Law, the absorbance (A) of an analyte in the solution is pro-243 portional to its concentration (C) if the analyte concentration is within a linear range. The 244 relationship between absorbance and concentration is shown in (2) (ε : molar attenuation 245 coefficient, L: light path). The concentrations of organic analytes involved in this work are 246 within the linear range, and the evidence was included in the supporting information (Figure 247 S1). Therefore, the η of a pollutant can be calculated by equation (3) by combining equation 248 (1) and (2). A_i and A_f are the absorbance at the representative peak⁶⁷ of a pollutant before 249

Light source	MLs type	Catalyst	Catalyst Conc. (mg/L)
	MLR	/	/
	MLA	/	/
	/	ZnO	100/50/10/5
Visible LED	MLR	ZnO	100/50/10/5
VISIBLE LLD	MLA	ZnO	100/50/10/5
	/	TiO_2	5
	MLR	TiO_2	5
	MLA	TiO_2	5
	/	ZnO	100/10
Simulated solar	MLR	ZnO	100/10
Simulated Solar	MLA	ZnO	100/10
	vial	ZnO	10
	MLs vial	ZnO	10

Table 3: Conditions of light treatment

²⁵⁰ and after the treatment, respectively.

$$\eta = \frac{C_i - C_f}{C_i} \times 100\% \tag{1}$$

$$A = \varepsilon C L \tag{2}$$

$$\eta = \frac{C_i - C_f}{C_i} \times 100\% = \frac{A_i - A_f}{A_i} \times 100\%$$
(3)

For the solution containing pollutants prepared with the synthetic water, the concentration changes of analytes were characterized by an ultra-performance liquid chromatographymass spectrum (UPLC-MS, ACQUITY UPLC H-Class, Waters). The method to detect SMX with UPLC-MS was included in supporting information. All solutions containing photocatalyst suspends were centrifuged for 10 min at 14,000 rpm, and then only the supernatant was used for analysis.

²⁵⁷ The performance of the photocatalysts is influenced by many factors associated with the

²⁵⁸ irradiation conditions (such as intensity, photon absorption, light scattering, etc.), catalyst ²⁵⁹ properties, adsorption of pollutants, properties of water matrices, and chemical properties ²⁶⁰ of organic contaminants. In order to show the enhancement of photocatalytic degradation ²⁶¹ efficiency obtained by implementing surface MLs, all the parameters except the usage of MLs ²⁶² were kept constant. The ability of surface MLs to enhance η of pollutants was quantified ²⁶³ with an enhancement factor (f) which was defined by the equation (4)

$$f = \frac{\eta_{(MLs+catalyst)}}{\eta_{catalyst}} \tag{4}$$

The reaction mechanisms may be further understood from the balance between the mass 264 of CO_2 generated from the complete degradation of organic contaminants and the mass 265 decrease in solutions containing contaminants.^{68,69} However, as shown in Figure 1 (b), our 266 reaction systems were fully sealed with negligible mass transfer from the system during the 267 irradiation. In addition, it was almost impossible to quantify the CO_2 production from our 268 systems due to the small volume of our samples and the dissolution of CO_2 in water. The total 269 amount of the model contaminant in the treated solution was 10 μg . Even from complete 270 degradation, only 17 to 22 μ g CO₂ would be produced at maximum. CO₂ production from 271 the photodegradation of organic contaminants in MLs-enhanced photocatalytic systems may 272 be conducted in the future after modification of the experimental set-up. Instead of mass 273 balance to monitor the reaction mechanism, the characterization of free radicals generated in 274 the photocatalytic system was feasible to reveal the degradation mechanism in the presence 275 of surface MLs.^{70,71} 276

The presence of free radicals in the photocatalytic degradation process was verified with an electron spin resonance (ESR) spectrum (Elexsys E-500, Bruker). The ultra-pure water dispersed with ZnO (10 mg/L) was irradiated by the visible LED lamp or the simulated solar light for 30 min before the ESR detection. 5,5-Dimethyl-1-pyrroline N-oxide (DMPO, Sigma Aldrich), as a spin-trapping agent, was used to capture the hydroxyl free radicals in the treated solution. DMPO was added to the treated solution with a concentration of ²⁸³ 5.7 g/L just before the light treatment started. The solution was added into quartz (CFQ) ²⁸⁴ EPR tubes (outside diameter: 5mm) to detect free radical signals immediately after the ²⁸⁵ irradiation. The ESR spectrum of methanol dispersed with ZnO (10 mg/L) under MLA was ²⁸⁶ also obtained after the irradiation by simulated solar light for 30 min (shown in supporting ²⁸⁷ information, Figure S2).

²⁸⁸ Results and discussion

²⁸⁹ Morphology and optical properties of MLs

The redistribution of light irradiation is determined by the morphology and spatial arrange-290 ment of surface MLs. The MLs on the pre-patterned substrate (MLA) are arranged in a 291 highly-ordered array with a uniform radius of 6.5 μ m due to the confinement of hydrophobic 292 domains, as shown in Figure 3 (b). The surface coverage rate and the contact angle of MLA 293 are 49 $^{\circ}$ and 63.7%, respectively. The light intensity profiles of MLA obtained from the 294 confocal microscope and optical simulation results of a single ML from the ML array are 295 displayed in Figure 3 (c) and (d), respectively. Due to the uniform size, the focal distances 296 of MLs in the array have the same value. From the light intensity profiles, it is found that 297 the focal points of MLA are located in a horizontal plane which is around 16 μm away from 298 the substrate. As a comparison, the focal distance of a single ML in the array is 16.5 μ m 290 according to the optical simulations. Therefore, the simulated focal distance is consistent 300 with that obtained from the confocal microscope. 301

Another type of surface MLs, represented with MLR, is fabricated on homogeneous substrates. MLR are randomly distributed on the planar substrate, and their diameters vary from 2 μ m to 200 μ m with a fixed contact angle of 7.5 °. The surface coverage rate of MLR is 47.2%. The focal distances of MLR differ due to the existence of the size distribution among them. Therefore, it is difficult to measure the focal distances of MLR with a confocal microscope.



Figure 3: Images of (a) random MLs (scale bar: 200 μ m) and (b) ML array (MLA) (scale bar: 10 μ m) obtained with optical microscope (c) The light intensity profile of MLA with confocal microscope (scale bar: 100 μ m) (d) The cross-sectional light intensity of a single ML in the array. The point with the highest irradiance value is the focal point. The position with z=0 is the substrate surface. The focal distance is the distance between the focal point and the substrate surface.



Figure 4: Top view intensity profile under (a) MLR and (b) MLA at the horizontal plane with the distance of 16.5 μ m, 115.5 μ m, 225.5 μ m, 665.5 μ m, and 797.5 μ m away from the substrate surface.

The top view intensity profiles of surface MLs in Figure 4 (a-b) exhibit the distribution 308 of irradiance at the horizontal plane with certain depths. At the depth of 16.5 μ m which 309 is close to the focal distances of MLA, the maximum incident flux value under MLA is the 310 highest, reaching 2.95×10^{-8} W. The number of the spots with the highest value is 400 on 311 the horizontal plane with an area of $2.25 \times 10^{-2} mm^2$. In comparison, the highest maximum 312 incident flux value under MLR is 2.26×10^{-7} W located at the depth of 225.5 μ m. However, 313 only two spots reach 2.26×10^{-7} on the horizontal plane under random MLs within the 314 same area. Therefore, the maximum total incident flux over the horizontal plane of MLA is 315 around 26 times larger than that of MLR. 316

When the depth increases, the maximum incident flux value under MLA significantly 317 drops, while the value under MLR first increases and then gradually diminishes. As the 318 depth changes from 16.5 μ m to 797.5 μ m, the maximum flux value under MLA decreases by 319 56%, while the value under MLR increases by 3.6 times. The variation of focal distances of 320 MLR avoids the sharp decay of irradiation intensity along the Z direction but also causes a 321 lower maximum total incident flux. In summary, the uniformity of focal distances of MLA 322 can reach a maximum flux, higher than MLR, but the decay irradiation intensity along the 323 Z axis is much more rapid. 324

³²⁵ Free radicals from MLs

Based on the spectra obtained by ESR (Figure 5), no obvious signals can be observed when 326 neither ZnO nor surface MLs is used in the light treatment. Under both visible LED light 327 and simulated solar light, a similar curve shape is observed if ZnO is added to the system. 328 As described in the literature,⁷⁰ the spectrum indicates that ·OH free radicals form with 329 the presence of ZnO. The formation of \cdot OH accelerates the degradation of pollutants. When 330 MLA is applied together with ZnO, the signals of free radicals become stronger under both 331 visible LED light and simulated solar light. Therefore, it is possible that more free radicals are 332 generated by utilizing MLA. Consequently, more free radicals could cause higher degradation 333

³³⁴ efficiency (η) .⁷²



Figure 5: Electron spinning resonance (EPR) spectra under different conditions after light treatment of 30 min. (The black curve is for the condition without ZnO particles and surface MLs. The light blue curve represents the treatment with only ZnO particles, while the dark blue curve is for both ZnO and MLA under a visible LED lamp. The light orange curve is for the conditions with only ZnO particles, while the dark orange curve is for both ZnO and MLA under a wisible the dark orange curve is for both ZnO and MLA under a visible the dark orange curve is for both ZnO and MLA under simulated solar light.)

Stronger signals of free radicals observed in the system with MLA could be attributed to 335 the higher light intensity at the focal points of MLs. Based on the second law of photochem-336 istry,^{73,74} higher light intensity leads to a higher concentration of reactive species, such as 337 hydroxyl free radicals in the MLs-enhanced photocatalytic system.^{75,76} The light intensity 338 at focal points of surface MLs increases by several times as shown by the optical simulation 339 results (Figure 4). A higher concentration of active species in the MLs-induced system is 340 confirmed by ESR characterization in our previous work.⁵⁷ Similar to the photolysis system 341 without catalysis, the ESR spectra in Figure 5 suggested that the photodegradation with 342 ZnO as the catalyst could also be accelerated, due to the larger amount of free radicals from 343 the focusing effect of surface MLs. 344

The increase in the concentration of free radicals is the consequence of the stronger local irradiance intensity in the presence of surface MLs. But the types of free radicals are not expected different from the situation without MLs, as the types are only determined by the light source and the type of photocatalyst. TiO_2 used in our experiments is a commercialized photocatalyst that has been widely studied.^{77,78} According to ESR results reported in the literature, we could conclude that hydroxyl free radicals form when TiO_2 acts as the photocatalyst, which promotes the degradation of organic pollutants.

³⁵² Influence of catalyst concentration on the efficiency of photocat-³⁵³ alytic degradation under visible light

The absorbance curves of the solutions containing different pollutants before and after light treatment are plotted in Figure 6. For the four pollutants treated under a visible LED lamp, slight enhancement can be observed by only applying surface MLs. By comparing the two types of surface MLs, MLA performs better than MLR since the decrease of absorbance peak is more obvious.

As shown in the second column of the plots in Figure 6, the reduction in absorbance values of all pollutants in the presence of ZnO particles improved. Such improvement becomes larger when we increase the initial concentration of ZnO. By combining surface MLs with ZnO particles, the absorbance peaks of pollutants further decrease. In the presence of ZnO, more reduction of absorbance is also observed with MLA compared with MLR, indicating the higher removal rates of pollutants with MLA.

The photodegradation efficiency of all pollutants under the visible LED light is plot-365 ted over the concentration of ZnO in Figure 7 (a). As the concentration of ZnO particles 366 increases, η of all four pollutants is enhanced. However, the enhancement of η by adding 367 dispersed ZnO particles into the solutions differs with the type of pollutants. For the pho-368 to degradation of MO with ZnO, η after the irradiation of 1 h is improved by 59.2% when the 369 ZnO concentration increases from 5 mg/L to 100 mg/L. For the other three pollutants, the 370 change of η after enhancing ZnO concentration from 5 mg/L to 100 mg/L is much smaller 371 than that of MO, which is 5.7% for NFX, 2.9% for SFD, and 2.3% for SMX. The pollutant 372 that is more difficult to degrade, which is SMX, has the least improvement when increasing 373 the concentration of ZnO. The different degradation mechanisms among the pollutants may 374 lead to the varied effectiveness of ZnO. Much higher η efficiency of MO degradation is pos-375



Figure 6: Representative absorbance spectra of pollutants (MO in (a-1) to (a-4), NFX in (b-1) to (b-4), SFD in (c-1) to (c-4), and SMX in (d-1) to (d-4)) with surface MLs and ZnO (under visible LED) after light treatment with 1 h.

sibly related to the sensitization mechanism for azo dyes. Charges are produced as the MO molecules are excited under irradiance and then injected in photocatalysts and oxidized dye for subsequent degradation.^{79,80} In contrast, the sensitization mechanism does not apply to other tree organic compounds, including NFX, SFD, and SMX, since they are transparent to the irradiation wavelengths. Regardless of the details in photodegradation mechanisms for those organic contaminants, the enhancement in η is achieved for all of them by adding ZnO.

Comparing with the situation only implementing ZnO or only surface MLs, the condition 383 with both MLs and ZnO shows higher η , indicating the synergistic effect in the surface MLs-384 enhanced photocatalytic system. By applying surface MLs in the photocatalytic degradation 385 process with ZnO as the catalyst, the distinguished enhancement of η can be confirmed in all 386 four pollutants. The variance in the enhancement of η resulted not only from using surface 387 MLs but also from the increase in ZnO concentration, which is similar to the situation only 388 with adding ZnO in the reaction systems. The photocatalytic degradation exhibited higher 389 η with MLA compared with that using MLR. The possible reason for the more outstanding 390 effect of MLA is the more efficient irradiation redistribution based on the highly-ordered 391 structure in MLA, which is also demonstrated in the optical simulations.⁸¹ 392

The enhancement factor for the MLs-enhanced photodegradation using ZnO as the cat-393 alyst is calculated with equation (4). As shown in Figure 7 (e-h), the enhancement factor 394 becomes lower at higher ZnO concentrations. The amount of active species is the key factor 395 determining the rate of photodegradation. In the photodegradation enhanced by ZnO and 396 surface MLs, the number of active species is up to the dosage of ZnO and the number of hot 397 spots created by MLs.^{42,82} The total number of active species (N_{total}) can be estimated using 398 Equation (5). In the equation, $N_{catalyst}$ is the number of active species generated due to the 399 excitation of ZnO, and N_{MLs} is the number of active species attributed to the focus effect 400 of MLs. The photocatalytic degradation efficiency is dependent on the number of active 401 species in the system. Therefore, the enhancement factor with MLs is positively related to 402



Figure 7: Photodegradation efficiency of (a) MO, (b) NFX, (c) SFD, (d) SMX using surface MLs and ZnO with different concentration (under visible LED). Enhancement of photodegradation efficiency of (e) MO, (f) NFX, (g) SFD, (h) SMX by using surface MLs

the ratio of N_{MLs} and $N_{catalyst}$ in Equation (6). With an increase in the concentration of 404 ZnO, $N_{catalyst}$ also increases while N_{MLs} is fixed, therefore, the enhancement factor drops 405 down.

$$N_{total} = N_{catalyst} + N_{MLs} \tag{5}$$

$$f \sim \frac{N_{total}}{N_{catalyst}} = 1 + \frac{N_{MLs}}{N_{catalyst}} \tag{6}$$

The enhancement factor in η of ZnO-photocatalyzed degradation by surface MLs is also 406 monitored with the elongated irradiation time of light treatment. The enhancement factor 407 for the four organic pollutants is plotted with the irradiation time in Figure 8. For MO 408 and SMX, the factor becomes smaller when the irradiation time increases from 1 h to 2 h. 409 Reversely, the factor grows in the photocatalytic degradation of NFX and SFD during a 410 longer treatment time. The difference in the enhancement factor not only is due to the type 411 of pollutants but is also related to the properties of MLs. The enhancement factor obtained 412 by MLR shows less change than that by MLA after the longer irradiation time. 413

⁴¹⁴ General enhancement of photocatalytic degradation with surface ⁴¹⁵ MLs under visible light

The effectiveness of surface MLs is verified by using a different catalyst in the photocatalytic degradation process. As shown in Figure 9 (a-d), more decrease in absorbance peaks is presented when TiO_2 is used as the catalyst compared to that without a catalyst. When combining TiO_2 with surface MLs, more organic pollutants are degraded than those in the treatment with only TiO_2 . After the same light treatment process, the MLA-enhanced photocatalytic degradation with TiO_2 has the most decrease in absorbance peak values.

The η values of all pollutants after the irradiation of 1 h with only TiO_2 or with both TiO_2 and MLs are displayed in Figure 9 (e). The η values of all four pollutants have been further



Figure 8: Enhancement factor of ZnO-photocatalyzed degradation efficiency of (a) MO, (b) NFX, (c) SFD, (d) SMX with surface MLs after irradiation time of 1 h and 2 h.



Figure 9: Representative absorbance curves of (a) MO, (b) NFX, (c) SFD, (d) SMX after the light treatment under the visible LED lamp for 1 h. (e) Photodegradation efficiency and (f) enhancement factor of TiO_2 -photocatalytic degradation efficiency of pollutants with surface MLs after irradiation time of 1 h.

⁴²⁴ improved after applying MLs in the photocatalytic degradation with TiO_2 . Moreover, MLA ⁴²⁵ shows more enhancement compared to MLR. The enhancement factor by using MLR and ⁴²⁶ MLA are shown in Figure 9 (f). The effect of surface MLs on the degradation catalyzed by ⁴²⁷ TiO_2 is similar to that catalyzed by ZnO. Therefore, surface MLs accelerate photocatalytic ⁴²⁸ degradation, regardless of the types of catalysts.

⁴²⁹ MLs-enhanced photocatalytic degradation under simulated solar ⁴³⁰ light

The representative absorbance spectra of SMX solution after the irradiation under different conditions are shown in Figure 10 (a-d). By comparing Figure 10 (a) and (c), it is found that the absorbance peak drops faster when the concentration of ZnO increases. As shown in Figure 10 (a) and (b), the decrease of absorbance peak value is higher when MLA is used in the light treatment. Such difference is also displayed in Figure 10 (c) and (d), where the concentration of ZnO changes to 10 mg/L.

The η values of all conditions presented in Figure 10 (a-d) are plotted in Figure 10 (e). For the concentration of ZnO equal to 100 mg/L, η reaches 72.4% within 3 h when both MLA and ZnO were used. To achieve a similar η with the ZnO concentration of 10 mg/L, around 5 h is required in the presence of MLA. The η under the simulated solar light is higher than that under the visible LED light due to the difference in light intensities and wavelength range.

The degradation efficiency of SMX with MLA is higher than that without MLA under the simulated light, which is the same phenomenon under visible light. The enhancement factors by MLA with two concentrations of ZnO under the simulated solar light are plotted with the irradiation time in Figure 10 (f). When the concentration of ZnO is 100 mg/L, the enhancement factor fluctuates around 1.2 as the irradiation time changes from 1 h to 3 h. For the photocatalytic degradation with a ZnO concentration of 10 mg/L, the enhancement factor by MLA is higher than that with 100 mg/L of ZnO. However, the factor drops from



Figure 10: Representative absorbance curve of SMX solution after the light treatment with (a) only ZnO particles with a concentration of 100 mg/L (b) both ZnO with a concentration of 100 mg/L and MLA (c) only ZnO particles with a concentration of 10 mg/L (d) both ZnO with a concentration of 10 mg/L and MLA under the simulated solar light. (e) Photodegradation efficiency and (f) enhancement factor of SMX under different conditions.

⁴⁵⁰ 1.6 to 1.4 as the irradiation time increases from 1 h to 8 h. The results under the simulated ⁴⁵¹ solar light reveal that the ordered spatial arrangement of MLs is optimal for photocatalytic ⁴⁵² degradation when the light source is closer to real solar light. The higher enhancement factor ⁴⁵³ under the lower concentration of ZnO further validates our assumption shown in Equation ⁴⁵⁴ (6) under simulated solar light.

The η of MLs-enhanced photocatalytic degradation of SMX is positively correlated with the intensity of simulated solar light in the range from 0.3 Sun to 1 Sun (Figure 11 (a-





Figure 11: Photodegradation efficiency of SMX after the irradiation for (a) 1 h and (b) 2 h under the irradiation of the simulated solar light with different intensities (c) The enhancement factor of η by using MLA during the irradiation for 1 h and 2 h

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the intensity of light is different. As the light intensity increases from 0.3 Sun to 1 Sun, the η increases from 2.1% to 5.6% with only ZnO after the irradiation of 1 h, while the η is enhanced from 4.3% to 9.0% by using ZnO combined with MLA. (Figure 11 (a)) The enhancement in η becomes larger when the irradiation time increases to 2 h based on Figure 11 (b).

In addition, the η of SMX with both of MLA and ZnO is always higher than that with only ZnO under varying light intensities. The enhancement factor obtained by using MLA is shown in Figure 11 (c). Under irradiation with the same light intensity, the change of the enhancement factor after adding the irradiation time from 1 h to 2 h is less than 0.6. The influence of irradiation on the performance of MLA is negligible in the first two hours of ⁴⁶⁸ photodegradation of SMX. The enhancement factor drops down when the intensity becomes
⁴⁶⁹ higher, showing that surface MLs perform better under irradiation with low light intensity.

470 MLs-enhanced photocatalytic degradation in a glass container

The MLs-enhanced photocatalytic degradation can be conducted in the MLs-decorated glass vials. As demonstrated in Figure 12 (a), the glass vial keeps transparent with surface MLs immobilized on the inner wall. In the microscopic image (Figure 12 (b)), surface MLs on the vial gave various sizes and random spatial distributions because of the homogeneous hydrophobic coating on the inner surface of the vial. The diameter of MLs displayed in the picture is from 1.40 μ m to 310 μ m. The surface coverage rate of the MLs is around 50%.



Figure 12: (a) Experimental set-up of ZnO-photocatalyzed degradation of SMX solution with the MLs-decorated vial (C(ZnO)=10 mg/L, C(SMX)=5 mg/L, pH=7.0) (b) The optical image of the MLs on the inner wall of a glass vial (c) Photodegradation efficiency of SMX with ZnO in a bare glass vial and an MLs-decorated vial (d) Enhancement factor of ZnO-photocatalyzed degradation with the MLs-decorated vial

The application of MLs-decorated vials can also enhance the η of degradation. As shown 477 in Figure 12 (c), the η of degradation with MLA obtained from UV Vis spectra (supporting 478 information, Figure S3) is always higher than that using only ZnO. Under the irradiation 479 of simulated solar light (1 Sun), the η of SMX with ZnO (10 mg/L) reaches 50.2% after 480 five hours of light treatment, while the value is further improved to 56.0% after using the 481 MLs-decorated vial. As demonstrated in Figure 12 (d), the enhancement factor by using 482 MLs-decorated vials is 1.60 after the irradiation for 1 h and then continuously decreases 483 with the irradiation time. 484

The degradation of SMX is significantly influenced by the concentration of SMX. When the concentration of SMX is less than 5 mg/L, a lower concentration of SMX results in a lower degradation rate.⁸³ The higher degradation rate with the existence of surface MLs directly leads to a lower concentration of SMX after irradiation. Therefore, the degradation rate of SMX with surface MLs drops faster than the process happening in the bare vial. As a consequence, the enhancement factor with MLs-decorated vials will decrease with time.

⁴⁹¹ Effect of water matrix on MLs-enhanced photodegradation

The photocatalytic degradation of SMX with ZnO can be enhanced with surface MLs not only in ultra-pure water but also in synthetic river water and real river water. The photo in Figure 13 (a) displays the collection point of the river water. By comparing the transmittance curves of different water matrices (Figure 13 (b)), we find that the transparency of synthetic water and river water is less than that of river water, especially in the wavelength ranging from 200 nm to 500 nm.

As displayed in Figure 13 (c), the η of SMX with both MLR and MLA is improved compared with that with only ZnO. Similar to the results observed in pure water, MLA has better performance than MLR in accelerating the photodegradation of SMX. The η with the same type of MLs and irradiation time in the synthetic water is lower than that achieved in the ultra-pure water (Figure 10 (e)). Compared with the enhancement factor



Figure 13: (a) A photo of the real river water collection site (b) Transmittance curves of three types of water matrices (c) Photodegradation efficiency of SMX in simulated water under simulated solar light (d) Enhancement factor of photocatalytic photodegradation efficiency of SMX achieved by MLR and MLA during 2 h and 5 h of irradiation. (e) Photodegradation efficiency of MO in the real river water under simulated solar light (f) Enhancement factor of photocatalytic photodegradation efficiency of MO obtained by MLA during 1 h, 2 h, and 5 h of irradiation.

with surface MLs in ultra-pure water during the same irradiation time, the enhancement factor in synthetic river water is higher. For example, the enhancement factor of MLR is 1.61 and 1.43 after 2 h and 5 h of irradiation, respectively. When using MLA, the factor is 3.0 for 2 h and 2.5 for 5 h (Figure 13 (d)).

The enhancement of photocatalytic degradation is also observed when using real river 507 water as the matrix. The photodegradation efficiency of MO in river water and the enhance-508 ment factor of η over the irradiation time are plotted in Figure 13 (e) and (f), respectively. 509 Without utilizing ZnO, around 14% enhancement is achieved by MLA after 5 h of irradia-510 tion. Compared with the condition without the catalyst and surface MLs, the degradation 511 efficiency of MO is enhanced by a maximum of 163% with only ZnO after 5 h of irradiation. 512 By setting MLA on the top of the light treatment chamber, the photocatalytic η of MO 513 is further improved under the same irradiation condition, which is 235% higher than the 514 control group and 27% higher than the group only with catalyst. 515

The difference in η and the enhancement factor after changing the water matrix into syn-516 thetic river water or real river water can be attributed to the variation in the transmittance 517 of water. The transmittance of the synthetic water in the range between 200 nm and 500 518 nm drops as displayed in Figure 13 (b), while the decrease in transmittance of river water is 519 even sharper. The decrease in the transmittance is possibly caused by more light absorption 520 of the synthetic river water and real river water. As a consequence, the irradiation intensity 521 in synthetic river water and river water should be lower than that in ultra-pure water, thus 522 the enhancement of η by surface MLs is higher (as displayed in Figure 11 (c)). 523

524 Conclusions

In summary, our work demonstrates the microlenses(MLs)-enhanced photocatalytic degradation efficiency of micropollutants in water. More free radicals generated in the presence of surface MLs contribute to higher degradation efficiency. The enhancement is generally

observed for all four targeted organic contaminants by using two kinds of photocatalysts. 528 The microlens array is more effective than random microlenses in the photodegradation of 529 all involved pollutants, which is attributed to the more effective redistribution of the irra-530 diation energy. The performance of surface MLs, represented by an enhancement factor, 531 varies with pollutants because of the difference in degradation mechanisms. Additionally, 532 the enhancement in the η of photocatalytic degradation is higher at a lower concentration 533 of the photocatalyst or under irradiation with lower intensity. Therefore, the results suggest 534 that surface MLs have the potential for applications where the excitation of photocatalysts 535 is suppressed. The feasibility of surface MLs in improving decontamination is also verified 536 in synthetic river water and a real river water matrix. In the next stage, surface MLs may 537 be tested in the light treatment of water samples containing multiple contaminants. 538

⁵³⁹ Supporting Information Available

Supplementary data to this article can be found in the document attached. Additional data
 include.

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