Characterization of the permeation properties of membrane filters and sorption properties of
 sorbents used for polar organic chemical integrative samplers

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6 ABSTRACT. Polar organic chemical integrative samplers (POCIS) are promising devices for 7 measuring time-weighted average concentrations of hydrophilic compounds in aquatic 8 environments. However, the mechanism of POCIS uptake remains unclear. This study 9 characterizes the permeation properties of polyethersulfone and polytetrafluoroethylene and the 10 sorption properties of Oasis HLB (Waters), Envi-Carb (Supelco), and Oasis WAX (Waters) under 11 identical conditions via calibration experiments of the POCIS. Plant protection products, 12 neonicotinoid herbicides, and linear alkyl benzene sulfonates (LAS) were tested. The permeation 13 experimental results suggested that the penetration rate constants (k_m) with high K_{ow} values (K_{ow}) : 14 octanol-water partition coefficient) were low, which indicated that the sorption of chemicals on 15 the membrane may constitute a limiting factor for the permeation. The sorption experiments indicated that the sorption rate constants (k_s) depended on the type of sorbent instead of the K_{ow} 16 17 values. Low k_s/k_m ratios were obtained for chemicals with low K_{ow} values, which implied that the 18 POCIS uptake for highly hydrophilic compounds was controlled by both membrane and sorbent 19 kinetics. The $k_{\rm m}$ and $k_{\rm s}$ values corresponded to the model and predicted the values of the sampling 20 rates (R_s) for the LAS. These findings revealed the possibility of using k_s and k_m values to predict 21 $R_{\rm s}$ values.

- 22 KEYWORDS. plant protection products, pesticides, surfactant, passive sampling, sampling rate,
- 23 POCIS
- 24

25 GRAPHIC FOR TABLE OF CONTENTS (TOC)/ABSTRACT ART.



INTRODUCTION. Polar organic chemical integrative samplers (POCIS) have been used as a passive sampling device for hydrophilic contaminants ($0 < \log K_{ow} < 4$; K_{ow} : octanol–water partition coefficient) in aquatic environments (1). Sampling using these devices can obtain timeweighted average (TWA) concentrations of contaminants such as pesticides, pharmaceuticals, drugs, and munitions (1–12). TWA concentrations obtained from POCIS sampling were reported as being consistent with the mean concentrations estimated from grab sampling (1).

34 Sampling rate (R_s) values are required to quantify the concentrations of the contaminants for 35 POCIS sampling and must be obtained via time-consuming calibration experiments. Three types 36 of calibration experiments have been conducted in previous laboratory-based studies: static 37 renewal, tank, and static experiments. In previous static renewal experiments, a single POCIS 38 device was deployed for certain periods (typically 1–28 d) in a 1 L glass beaker with solutions 39 containing contaminants, and was refreshed every 1-2 days to avoid changes in contaminant 40 concentrations (1,5,6,8,9,13,14). In tank experiments, POCIS devices were deployed in a tank 41 filled with solution (typically 50–100 L) for certain periods (15–18). R_s values were also 42 estimated from the collected amount of contaminants on the sorbent in the POCIS devices used 43 in static renewal experiments and tank experiments. Static experiments were conducted in a 44 manner similar to static renewal experiments; however, the solution was not refreshed during the 45 course of the experiment (11,19–24). In these studies, the contaminant concentration decrement 46 in the solution was subsequently monitored to estimate the R_s values (11,19–24). All calibration 47 experiments for evaluating the R_s values are time-consuming tasks. For example, at least 28 d is 48 required to estimate the $R_{\rm s}$ value for the POCIS devices, which applied to field observations for a 49 28 d duration. Moreover, POCIS sampling targets several contaminants in aquatic environments. 50 Therefore, prediction methods for R_s values have been required in previous experiments (25).

51 The effects of environmental factors on $R_{\rm s}$ values have been investigated, such as temperature, 52 flow velocity, exposure scenario, and suspended sediment (9,26–28). However, the kinetics of 53 the POCIS uptake, which should control R_s values, are not fully understood. Previous studies 54 have reported that POCIS uptakes were controlled by membrane kinetics, thereby implying that 55 the R_s values may depend on the type of membrane instead of the sorbent type (29). However, 56 recent investigations have reported conflicting data regarding the POCIS uptake model 57 controlled by membrane kinetics. For example, Noro et al. (5) indicated that R_s changed when 58 different sorbents were used. In addition, Jeong et al. (30) revealed that the R_s values of POCIS 59 devices containing polyethersulfone (PES) membranes and polytetrafluoroethylene (PTFE) were 60 similar (30). Both investigations implied that sorbent kinetics may affect POCIS uptake. A recent 61 investigation demonstrated that R_s values may be predicted by a first-order chemical reaction 62 kinetic model with octanol-water dissociation constants and membrane-water distribution 63 coefficients (31). However, these experiments required 28 days to obtain the membrane–water 64 distribution coefficients (31). Thus, this model may not be suitable for predicting R_s values at 65 low costs.

This study characterizes the permeation properties of membranes and the sorption properties of 66 67 sorbents. First, a permeation experiment was conducted to estimate the penetration rate constants 68 of contaminants diffusing from the aqueous phase to the inside of a POCIS device through the 69 membrane. POCIS devices with polyethersulfone (PES) and polytetrafluoroethylene (PTFE) 70 membranes were used in this work. Second, the sorption rate constants of the contaminants on 71 the sorbent were estimated for the three studied sorbents; Oasis HLB (Waters), Envi-Carb 72 (Supelco), and Oasis WAX (Waters). Plant protection products (PPPs), neonicotinoid herbicides, 73 and surfactants were used. Then, the penetration rate and adsorption rate were compared to

estimate the rate-limiting step of POCIS uptake. Finally, the applicability of the R_s prediction

model, reported by Morin et al. (31), was evaluated using the penetration rate constants, sorption

76 rate constants, and R_s values.

77 MATERIALS AND METHODS.

78 Materials and chemicals

79 Oasis HLB, Oasis WAX (Waters, Milford, MA, USA), and ENVI-Carb (Supelco, Bellefonte,

80 PA, USA) were used as sorbents. Polyethersulfone (PES) microporous (0.1 µm pore size and

81 102–158 μm thickness) and hydrophilic polytetrafluoroethylene (PTFE) (0.1 μm pore size and 35

82 µm thickness) membranes were purchased from Nihon Pall Ltd. (Tokyo, Japan) and Advantec

83 Toyo Kaisha, Ltd (Tokyo, Japan), respectively, for the POCIS devices.

84 A neonicotinoid mixture solution (20 mg L^{-1} each) from FUJIFILM Wako Chemicals, Inc.

(Osaka, Japan) was used for the experiments. An acetonitrile solution containing 10 mg L⁻¹ of

86 acetamiprid- d_3 , clothianidin- d_3 , dinotefuran- d_3 , imidacloprid- d_4 , nitenpyram- d_3 , thiamethoxam-

 d_3 , and thiacloprid- d_3 was purchased from Hayashi Pure Chemical, Inc. (Osaka, Japan) and was

88 used as the internal standard for neonicotinoid pesticide analysis. An anionic surfactant mixture

89 (LAS) methanolic standard solution containing sodium decylbenzenesulfonate (C₁₀-LAS),

90 sodium undecylbenzenesulfonate (C_{11} -LAS), sodium dodecylbenzenesulfonate (C_{12} -LAS),

91 sodium tridecylbenzenesulfonate (C₁₃-LAS), and sodium tetradecylbenzenesulfonate (C₁₄-LAS)

92 at 1 g/L concentration was purchased from FUJIFILM Wako Chemicals Ind. (Osaka, Japan). A

93 sodium 4-dodecylbenzenesulfonate (RING-¹³C₆) 10 mg L⁻¹ methanolic solution was purchased

94 from Cambridge Isotope Laboratories, Inc. (Tewksbury, MA, USA) and used as an internal

95 standard for the LAS analysis. The PPPs standard reagents isoprocarb, fenobucarb, pyroquilon,

96 bromobutide, cyanazine, S-metolachlor, paclobutrazol, and furametpyr were obtained from

97 Wako Pure Chemical Ind. Methanol, acetone, and dichloromethane of pesticide-analysis grade

98 (FUJIFILM Wako Chemicals Ind.) were used for the experiments and clean-up processes during99 the analysis.

100 POCIS devices

101 Metal rings (inner diameter: 54 mm, outer diameter: 102 mm) were used in the POCIS devices

102 for this study. Three types of POCIS devices with 220 mg sorbent have been used in previous

103 reports. PES-Oasis HLB (PES-HLB) POCIS (6,9,32,33) as well as a combination of PES-ENVI

104 Carb (PES-EC) POCIS and PTFE-ENVI Carb (PTFE-EC) POCIS (5) have been used for PPPs

105 and neonicotinoid herbicides; whereas, PTFE-Oasis WAX (PTFE-WAX) POCIS has been used

106 for LAS (34). In this study, the same devices have been used.

107 *Permeation experiment*

108 A permeation experiment was conducted to estimate the penetration rate of contaminants 109 diffusing from the aqueous phase to the inside of the POCIS device. A glass bar (diameter, 5 110 mm; length, 10 mm) was installed in the POCIS devices instead of the sorbents. POCIS devices 111 with PES and PTFE membranes were tested. Before the permeation experiment, the POCIS 112 devices were deployed in ultrapure water for 1 h placed in glass beakers and agitated at 1500 113 rpm. Then, the POCIS devices containing the pure water were installed in 1 L glass beakers 114 (HARIO SCIENCE CO., LTD., Tokyo, Japan) containing a solution with 20 µg L⁻¹ contaminant 115 concentration for certain periods. The solution was agitated at 18 cm s⁻¹ under darkness at 20 °C 116 (6). This condition was the same as previously reported calibration conditions for POCIS devices (5,6,34). Following deployment, the membranes of the POCIS devices were cut to transfer the 117

118 solution from the POCIS device to glass tubes using glass Pasteur pipettes. Additionally, 3 mL of 119 the solution in the beaker was transferred into glass tubes using glass Pasteur pipettes. The 120 obtained samples were then pretreated prior to gas chromatography-triple quadrupole mass 121 spectrometry analysis (GC-MS/MS analysis) and liquid chromatography-triple quadrupole mass 122 spectrometry analysis (LC-MS/MS analysis). POCIS devices with PES membranes have 123 previously been used to detect PPPs and neonicotinoid herbicides (6.9, 10); whereas, POCIS 124 devices with PTFE membranes have previously been used to detect neonicotinoid herbicides and 125 LAS (5,34). Thus, PES membranes were tested for and neonicotinoid herbicides. The PTFE 126 membranes were tested for neonicotinoid herbicides and LAS.

127 Flow velocity measurements in POCIS devices

128 The flow velocity in the calibrated POCIS devices was measured using an Alabaster mass 129 transfer sensor (35). Alabaster cubes $(1 \times 1 \times 1 \text{ cm})$ were prepared from Alabaster plates 130 obtained from PaSOC (Kimswerd, Netherlands). The alabaster cubes were measured using 131 Vernier calipers to calculate their surface areas. They were then dried at 40 °C for 10 min and 132 weighed. An Alabaster cube was then installed in each POCIS device instead of the sorbent. The 133 POCIS devices were deployed for 1 h in a 1 L glass beaker filled with water. The water in the beakers was agitated at 18 cm s⁻¹ under darkness at 20 °C. This condition was the same as the 134 135 calibration used in previous studies (5,6,34). Following deployment, the alabaster cubes were 136 collected from the POCIS device. The deployed alabaster cubes were weighed after drying for 15 137 min at 40 °C. The flow velocities were estimated based on the dissolution rates of the alabaster 138 cubes, as described in a previous study (35).

139 Sorption experiment

Sorption experiments were conducted to estimate the adsorption rate of the contaminant onto the sorbent in the POCIS device. First, the agitation rate was determined to replicate the flow conditions in the POCIS devices. The adsorption rates were then estimated using the determined flow conditions.

144 The agitation rate, which had a flow velocity similar to that inside of the POCIS device in the 145 calibration experiment, was determined via the Alabaster mass transfer sensor (i.e., Alabaster 146 cubes). Briefly, the alabaster cubes were dried at 40 °C for 10 min and then weighed. Alabaster 147 cubes were installed in the center of a glass beaker (diameter: 53 mm; height: 70 mm) with 100 148 mL of water. The water in the beakers was agitated at several rates of rotation using glass magnetic stir pieces (diameter, 7 mm; length, 20 mm) under darkness at 20 °C. The flow 149 150 velocities were estimated based on the dissolution rate of the alabaster cubes as detailed in the 151 previous subsection.

152 The adsorption rate was estimated using the determined agitation rate. Sorbents (50 mg) were 153 weighed into glass beakers (diameter: 53 mm; height: 70 mm) containing 100 mL of contaminant solution (50 μ g L⁻¹ each). The solution was agitated at the determined rate for certain periods 154 155 using glass magnetic stir bars (diameter, 7 mm; length, 20 mm). The supernatant (1 mL) was 156 next transferred into glass tubes using glass syringes with syringe filters. The obtained samples 157 were pretreated before GC-MS/MS analysis and LCMS/MS analysis as previously noted. POCIS 158 devices with Oasis HLB sorbent have previously been used to detect both PPPs and 159 neonicotinoid herbicides (6,9,10). Devices with ENVI-Carb and Oasis WAX have also been 160 previously used to detect neonicotinoid herbicides and LAS, respectively. Thus, Oasis HLB was 161 evaluated for PPPs and neonicotinoid herbicides. ENVI-Carb and Oasis WAX were evaluated 162 for neonicotinoid herbicides and LAS, respectively.

The samples obtained in the glass tubes were pretreated prior to the GC-MS/MS and LC-MS/MS
analyses. Three types of pretreatments were used for PPPs, neonicotinoid herbicides, and LAS
analysis.

167 Ultrapure water was added to the glass tubes containing the PPPs samples to maintain a sample

168 volume of 3 mL. Dichloromethane (2 mL) was added to the glass tubes. The glass tubes were

169 shaken 50 times. The dichloromethane phases were collected into glass tubes using glass Pasteur

170 pipettes with 1 g of sodium sulfate in fritted solid phase extraction (SPE) tubes. Then,

171 dichloromethane (5 mL) was passed through sodium sulfate in the fritted SPE tubes and added to

the dichloromethane phase. The dichloromethane solution was evaporated to dryness using a

173 gentle nitrogen stream. Acetone (1 mL) containing 0.3% polyethylene glycol was added to the

174 glass tubes. The acetone solution was then collected in glass vials. The samples were then

analyzed via GC-MS/MS. An Agilent Technologies (Santa Clara, USA) 7890 GC linked to a

176 7000 mass selective detector was used in the selected ion monitoring mode. The detection limits

177 of the GC-MS/MS analysis were previously reported (9).

178 The samples (1 mL) of neonicotinoid herbicides and LAS were transferred into glass vials with

179 internal standards (400 μ g L⁻¹, 25 μ L). Samples were analyzed using LC-MS/MS. The LC-

- 180 MS/MS analytical conditions and detection limits have been reported in previous studies (34,36).
- 181 RESULTS AND DISCUSSION.

182 *Penetration rate constants*

The penetration rate constants (*k*_m) of PPPs, neonicotinoid herbicides, and LAS were estimated via the permeation experiments. PES membranes were tested for PPPs and neonicotinoid herbicides. The PTFE membrane was tested for neonicotinoid herbicides and LAS. The concentrations of the contaminants gradually increased with time in the POCIS device (Fig. S1). The permeation rate of this study should reflect the actual membrane kinetics for the POCIS uptake because the permeation experiment was conducted in the same manner as the calibration experiments of the POCIS devices (5,6,34).

190 $k_{\rm m}$ values were obtained by fitting the first-order reaction equation as follows:

191
$$C_p = C_e (1 - e^{-k_m t})$$
 (1)

where C_p (µg L⁻¹) is the concentration of the contaminants in the POCIS devices, C_e (µg L⁻¹) is 192 $C_{\rm p}$ at 120 min, $k_{\rm m}$ (min⁻¹) is the penetration rate constant, and t (min) is the time. The $k_{\rm m}$ values 193 194 are presented in Table 1. The $k_{\rm m}$ values of the PES membranes ($k_{\rm m, PES}$) ranged from 8.4 × 10⁻⁶ 195 (s-metolachlor) to 0.073 (dinotefuran) (min⁻¹) (Table 1). The $k_{\rm m}$ values of the PTFE membranes 196 $(k_{\rm m, PTFE})$ ranged from 1.1×10^{-3} (C₁₄-LAS) to 0.13 (dinote furan) (min⁻¹) (Table 1). The $k_{\rm m, PTFE}$ 197 values were higher than the $k_{m, PES}$ values because of the difference in the thickness of the 198 membranes (PTFE, 35 µm; PES, 100–150 µm). This result supports the findings of previous 199 investigations (5,37).

Table 1 Log K_{ow} , k_{m} , k_{s} , and R_{s} of plants protection products, neonicotinoid herbicides, and the linear alkylbenzene sulfonates.

LogKov	v k _m		ks			$R_{\rm s}$				Referen ce for $R_{\rm s}$
	min ⁻¹		\min^{-1}			$L d^{-1}$				
	PES	PTFE	HLB	EC	WAX	PES- HLB	PES- EC	PTFE- EC	PTFE- WAX	

plants protection products (PPPs)

Isoprocarb	2.27	4.6×10 ⁻³	_	0.27	_	_	0.294	_	_	-	Yabuki et al. 2016
Fenobucarb	2.79	1.6×10 ⁻⁵	_	0.37	_	_	-	_	_	_	
Pyroquilon	1.57	1.2×10 ⁻²	_	0.31	_	_	0.185	_	_	_	Yabuki et al. 2016
Bromobutide	3.47	3.7×10 ⁻³	_	0.30	_	_	0.191	_	_	_	Yabuki et al. 2016
Cyanazine	2.22	1.4×10 ⁻⁵	_	0.37	_	_	0.280	_	_	_	Ahrens et al. 2018
s-Metolachlor	3.13	8.4×10 ⁻⁶	_	0.37	_	_	0.338	_	_	_	Poulier et al. 2014
Paclobutrazol	3.2	1.5×10 ⁻⁴	_	0.36	_	-	-	_	_	_	
Furametpyr	2.36	1.2×10 ⁻⁵	_	0.40	_	-	-	_	_	-	
Neonicotinoid herbicides											
Dinotefuran	-0.55	7.3×10 ⁻²	0.13	0.037	0.039	_	0.106	0.106	0.308	_	Noro et al. 2019, 2020
Clothianidin	-0.13	6.9×10 ⁻³	0.11	0.22	0.056	_	0.242	0.113	0.27	_	Noro et al. 2019, 2020
Thiamethoxam	0.57	2.7×10 ⁻²	0.12	0.21	0.042	_	0.202	0.100	0.366	_	Noro et al. 2019, 2020
Imidacloprid	0.70	9.3×10 ⁻³	0.12	0.37	0.045	_	0.257	0.122	0.686	_	Noro et al. 2019, 2020
Acetamiprid	0.80	3.1×10 ⁻³	0.12	0.31	0.052	_	0.239	0.104	0.445	_	Noro et al. 2019, 2020
Thiacloprid	1.26	6.3×10 ⁻³	0.12	0.38	0.057	_	0.214	0.123	0.548	_	Noro et al. 2019, 2020

Linear alkylbenzene sulfonates (LAS)

C ₁₀ -LAS*	1.94	_	$1.7 \times 10_{-2}$	-	_	0.22	_	_	_	0.101	Noro et al. 2021
C ₁₁ -LAS*	2.43	_	8.1×10 _3	_	_	0.21	_	_	_	0.139	Noro et al. 2021
C ₁₂ -LAS*	2.92	_	4.3×10 _3	_	_	0.21	_	_	_	0.110	Noro et al. 2021
C ₁₃ -LAS*	3.42	-	2.7×10 _3	_	_	0.22	_	_	_	0.071	Noro et al. 2021
C ₁₄ -LAS*	_	_	1.1×10 _3	_	_	0.40	_	_	_	0.035	Noro et al. 2021

200

201 A correlation between the log k_m values and the log K_{ow} values (K_{ow} ; octanol–water partition 202 coefficient) is shown in Fig. 1. The $k_{\rm m PES}$ values and $k_{\rm m PTFE}$ values for the LAS were negatively 203 correlated with the K_{ow} values, thereby implying that sorption of the contaminants on the 204 membrane interfered with the permeation of the contaminants (37). The neonicotinoid herbicides 205 did not adsorb on the PTFE membrane, which resulted in constant $k_{m PTFE}$ values for the 206 neonicotinoid herbicides (Fig. 1 (5)). The mean $k_{\rm m PES}$ values of neonicotinoid herbicides in this 207 study (0.021 min⁻¹) were higher than those in a previous study conducted in cells (0.0053 min⁻¹) 208 (5). Note that the data were taken from Noro et al. (5) (Supplemental Table 4) and calculated 209 using Eq. (1). Water boundary layers (WBL) on both sides of the membrane in the cells may 210 have induced low $k_{\rm m}$ values in a previous study (28).





Figure 1. Log k_m vs. log K_{ow} . k_m : penetration rate constant (min⁻¹), K_{ow} : octanol–water partition coefficient. The solid lines indicate linear regressions.

215 No correlation between the $k_{\rm m}$ values and $R_{\rm s}$ values was observed (Fig. S2). However, diffusion

through the membrane may dominate mass transfers and POCIS uptake rates (29). This implies

that there may have been a degree of sorbent kinetics in the POCIS uptake.

218 Flow velocity determination

The flow velocity data in the POCIS device were required to conduct the sorption experiment because flow velocity can potentially affect the sorption rate. The Alabaster sensor along with the required agitation condition was used to determine the flow velocity in the POCIS device (35). It was calculated to be 0.06 cm s⁻¹.

A previous study indicated that WBL exists on the membrane when the flow velocity is above 6 $cm s^{-1}$ (28). Thus, WBL was expected to exist and affect the mass transfer in the POCIS devices in this study. The flow velocity outside the POCIS devices in the calibration experiments (18 cm s^{-1}) was above 6 cm s^{-1} , thereby implying that there was no WBL outside the POCIS device (6).

The flow velocity in the glass beakers was 0.06 cm s^{-1} in the condition described in "*Sorption experiment*". Thus, we concluded that this agitation condition replicated the flow velocity in the POCIS device.

230 Adsorption rate constants

231 The adsorption rate constants (k_s) of the PPPs, neonicotinoid herbicides, and LAS were estimated

via the adsorption experiments. Oasis HLB was used for PPPs and neonicotinoid herbicides.

233 ENVI-Carb was used for neonicotinoid herbicides, and Oasis WAX was used for LAS. The

234 concentrations of the contaminants gradually decreased with time in the beaker (Fig. S3). The k_s

values of this study should reflect the actual sorption kinetics for the POCIS uptake because the

adsorption experiments were conducted under a similar flow velocity condition as the

calibrations of the POCIS devices (5,6,34).

The adsorption rate constants were calculated by fitting the first-order reaction equation asfollows:

240
$$C_b = C_o e^{-\kappa_s t}$$
(2).

where C_b (µg L⁻¹) is the concentration of the contaminants in the beaker, C_0 (µg L⁻¹) is the initial value of C_b , k_s' (min⁻¹) is the apparent adsorption rate constant, and *t* (min) is the time.

Then, the k_s (min⁻¹) values were calculated from the k_s' values to correct for the influence of the sorbent mass as follows:

245
$$k_s = \frac{m_p}{m} \times k_s' \qquad (3)$$

where m_p (mg) is the mass of the sorbent in the POCIS devices (220 mg) and m (mg) is the mass of the sorbent weighed in the glass beakers (50 mg).

248 The results of the adsorption experiments and k_s values are shown in Fig. 2 and Table 1,

249 respectively. The $k_{\rm s \, HLB}$, $k_{\rm s \, EC}$, and $k_{\rm s \, WAX}$ values indicate the $k_{\rm s}$ values for the Oasis HLB, Envi-

250 Carb, and Oasis WAX, respectively.



Figure 2. Log k_s values for each sorbent. k_s : sorption rate constant (min⁻¹). Oasis HLB (HLB) was evaluated for PPPs and neonicotinoid herbicides. Envi-Carb (EC) was evaluated for neonicotinoid herbicides. Oasis WAX (WAX) was evaluated for the linear alkylbenzene sulfonates. Error bars show 1 σ .

255 The $k_{\text{s HLB}}$, $k_{\text{s EC}}$, and $k_{\text{s WAX}}$ values ranged from 0.037 (dinotefuran) to 0.40 (furametpyr), from

256 0.039 (dinotefuran) to 0.57 (thiacloprid), and from 0.21 (C₁₁-LAS, C₁₂-LAS) to 0.40 (C₁₄-LAS)

- 257 (min⁻¹), respectively (Table 1). The $k_{\rm s\,HLB}$ values of the neonicotinoid herbicides (0.039
- 258 (dinotefuran) 0.38 (thiacloprid)) were higher than those of the $k_{s, EC}$ values (0.037 (dinotefuran))
- 259 0.057 (thiacloprid)), whereas the sorption coefficients (K_d; L/kg) of the neonicotinoid

herbicides with Oasis HLB were lower than those with ENVI-Carb (5). This implies that the adsorption rate may depend on other characteristics (i.e., particle size) of the sorbent besides the capacity. The elevated k_s values of Oasis HLB may have resulted in the high R_s values for neonicotinoid herbicides compared to ENVI-Carb (Table 1) (5,6). Therefore, the sorption rate can be a parameter to predict the R_s values of highly hydrophilic compounds (log K_{ow} <2) such as neonicotinoid herbicides.

266 Relationship of K_{ow} and k_m/k_s ratio

The correlation between the K_{ow} values and k_s/k_m ratios was obtained to investigate the kinetics of the POCIS uptake (Fig. 3). The $k_{s HLB}/k_m PES$, $k_{s EC}/k_m PES$, and $k_{s WAX}/k_m PTFE$ ratios were positively correlated with the K_{ow} values, whereas $k_{s, EC}/k_m$, and PTFE ratios were constant. The high k_s/k_m ratios indicated that the adsorption rate was higher than the penetration rate. In short, permeation is the rate-limiting step for the POCIS uptake of contaminants with a high k_s/k_m ratio. Thus, the POCIS uptake kinetics of contaminants with high log K_{ow} values should be controlled by the membrane.



275 **Figure 3.** Log (k_s/k_m) vs. log K_{ow} . k_m : penetration rate constant (min⁻¹), k_s : sorption rate constant 276 $(\min^{-1}), K_{ow}$: octanol-water partition coefficient. Solid lines indicate linear regressions. The k_s 277 HLB values are the sorption coefficients of Oasis HLB for PPPs and neonicotinoid herbicides. The 278 $k_{\rm s EC}$ values are the sorption coefficients of Envi-Carb for neonicotinoid herbicides. The $k_{\rm s WAX}$ 279 values are the sorption coefficients of Oasis WAX for linear alkylbenzene sulfonates. The $k_{\rm m PES}$ 280 values are the permeation coefficients of polyethersulfonate (PES) membranes for PPPs and 281 neonicotinoid herbicides. The $k_{\rm m\,PTFE}$ values are the permeation coefficients of 282 polytetrafluoroethylene (PTFE) membranes for the neonicotinoid herbicides and the linear 283 alkylbenzene sulfonates.

The log $k_{\rm s \ EC}/k_{\rm m \ PES}$ ratios and the log $k_{\rm s \ WAX}/k_{\rm m \ PTFE}$ ratios were relatively low and ranged from – 0.27 to 1.9, resulting from the low $k_{\rm s \ EC}$ values and the high $k_{\rm m \ PTFE}$ values. Therefore, the uptakes of PES-EC POCIS and PTFE-WAX POCIS may be controlled by both the membranes and sorbents. The log $k_{\rm s \ HLB}/k_{\rm m \ PTFE}$ ratios were the lowest group in study, ranging from –0.53 to – 0.30, thereby implying that the sorbent kinetics may have dominated the uptake of the POCIS device with the PTFE membrane and the Oasis HLB for the neonicotinoid herbicides.

290 Implications for R_s predictions

The aforementioned experimental results have important implications for R_s predictions. Low k_m values were obtained for chemicals with low K_{ow} values, thereby indicating that the sorption of chemicals on the membrane may constitute a limiting factor for permeation (37). The k_s values depended on the types of sorbents instead of the K_{ow} values. Low k_s/k_m ratios were obtained for chemicals with low K_{ow} values, which implied that the POCIS uptake for the hydrophilic compounds was controlled by both membrane and sorbent kinetics. 297 k_s and k_m values may be helpful in selecting combination of membranes and sorbents for the 298 POCIS device. High k_s and k_m values may result in high R_s values. Accordingly, the R_s values of 299 the POCIS device with the PTFE membrane and Envi-Carb were higher than those of the device 300 containing the PES membrane and Envi-Carb (5). Therefore, a suitable combination of the 301 membrane and sorbent can be selected based on the k_m values, k_s values, and the adsorption 302 capacity for the duration and concentration of the contaminants in the sampling campaigns.

303 Additionally, R_s values may be predicted based on the modified first-order chemical reaction 304 model reported by Morin et al. (31) as follows:

$$\frac{1}{R_s} = A \times \left(\frac{1}{k_m} + \frac{1}{k_s}\right) (4)$$

306 where A (L⁻¹) is the proportionality coefficient. The $1/R_s$ values and $(1/k_m + 1/k_s)$ were compared 307 to validate the model (Fig. 4). The A value and the coefficient of determination (R^2) for the 308 regression line were 0.036 L and 0.94, respectively, for the PTFE-WAX POCIS measuring LAS 309 (Fig. 4). This implies that the model can be used as a potential R_s prediction tool. However, the 310 model did not fit the PPPs and neonicotinoid herbicides (Fig. 4). The difference in the molecular 311 structures among LAS is the length of the alkyl chain. The simple difference in the molecular 312 structure may induce a correspondence to the model with the experimental values obtained in 313 this study. This implies that the R_s prediction model can be applied to other families of molecules 314 with simple differences in their molecular structures, such as perfluoroocotanates and 315 perfluorooctane sulfonates. We are currently working on comprehensively predicting the R_s 316 values of a wide variety of contaminants, which will be detailed in a future study



Figure 4. $1/k_s + 1/k_m$ vs. $1/R_s$. k_m : penetration rate constant (min⁻¹), k_s : sorption rate constant (min⁻¹), R_s : sampling rate (L d⁻¹). The solid line indicates a linear regression.

CONCLUSIONS. km values of PPPs, neonicotinoid herbicides, and LAS were estimated via 320 321 permeation experiments. The $k_{\rm m}$ values were negatively correlated with $K_{\rm ow}$ values, which 322 implied that the sorption of the contaminants on the membrane interfered with the permeation of 323 the contaminants (37). The k_s values of the PPPs neonicotinoid herbicides, and LAS were 324 estimated via the adsorption experiments. The adsorption rate may depend on other 325 characteristics (i.e., particle size) of the sorbent besides the capacity. A correlation between the 326 K_{ow} values and the k_s/k_m ratios implied that the POCIS uptake kinetics of the contaminants with 327 high log K_{ow} values should be controlled by the membrane. Finally, the R_s prediction model was 328 successfully applied to the PTFE-WAX POCIS device developed for evaluating LAS. Future 329 work should ensure that the R_s prediction model can account for a wide variety of contaminants, 330 thereby avoiding time-consuming calibration experiments.

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334 Author Contributions

- 335 K. Noro, Y. Yabuki, and S. Nakamura conceived and designed the experiments. K. Noro, A.
- 336 Banno, J. Ono, and Y. Yabuki performed the experiments and chemical analysis. K. Noro wrote
- 337 the manuscript. Y. Yabuki, A. Banno, J. Ono, and S. Nakamura provided editorial assistance.

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341 Notes

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