Breaking the Upper Bound of Siloxane Uptake: Metal-Organic Frameworks as an Adsorbent Platform

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Biogas, regarded as a promising renewable energy source, still needs to be upgraded. This calls for the removal of the most prominent contaminants, among others the octamethylcyclotetrasiloxane (D4) molecule. Herein, high throughput computational screening in tandem with synthesis and adsorption testing revealed the hydrophobic Zr-MOF PCN-777 as an optimal D4 adsorbent with record gravimetric (1.8 g g^{-1}) and volumetric (0.49 g cm^{-3}) uptakes, alongside a reversible and fast adsorption/desorption process, good cyclability and easy regeneration. This MOF was demonstrated to encompass an ideal combination of mesoporous cages and chemical functionality to enable an optimal packing of the siloxane molecules and their efficient removal while maintaining the process highly reversible thanks to moderately high host/guest interactions. This work highlights the efficacy of an integrated workflow for accelerating adsorbent selection for a desired application, spanning the entire pipeline from method validation to computational screening, synthesis and adsorption testing towards the identification of the optimal adsorbents.

1. Introduction

Biogas capture from landfill sites or wastewater treatment 2 plants is identified as an appealing strategy to procure a re-3 newable energy fuel, simultaneously promoting a reduction in 4 greenhouse gas emissions and an increase in waste treatment 5 profitability¹. The use of biogas as an energy green resource 6 critically calls for a substantial increase of its CH₄ quality by re-7 moving gaseous and vapour impurities resulting from anaerobic 8 digestion processes¹. One prominent class of biogas impurities 9 are the linear (denoted "L") and cyclic (denoted "D") silox-10 anes, as degradation by-products of silicone polymers from 11 packaging, construction, cosmetics, and household items^{2,3}. 12 This family of molecules is also known to damage subsequent 13 energy recovery systems, e.g. combustion engines, fuel cells 14 and steam reformers, via their decomposition into amorphous 15 silica on heated surfaces that leads to abrasive solid deposits 16 on critical machinery, and to inactivation of gas reforming 17 catalysts⁴. Octamethylcyclotetrasiloxane commonly labelled 18 D4 is the most representative siloxane species present in biogas, 19 which spans from 50 to 70% of the total siloxane content due to 20 its relatively low water solubility (56 μ g l⁻¹) and its significant 21 vapour pressure $(196 Pa at 303 K)^{3-1}$ 22

Multiple technologies have been proposed to mitigate the 23 presence of siloxanes in biogas outlet streams, including min-24 eral acid/base scrubbing, deep chilling, or iron oxide beds, 25 often working in tandem to remove other impurities⁶. The 26 physisorption-based removal of D4 by porous filters is also a 27 promising alternative, due to its relatively low potential ener-28 getic cost, while avoiding the use of environmentally hazardous 29 chemicals^{7,8}. A variety of conventional adsorbents has been 30 envisaged for siloxane elimination, including activated carbons⁹, 31 zeolites¹⁰, and silicas¹¹. However, these materials suffer from 32 several drawbacks that limit their use, in particular insuffi-33

cient uptake and/or incomplete regeneration under standard conditions. Moreover, downstream biogas commonly contains a proportion of water, which can compete with D4 sorption when using hydrophilic adsorbents^{6,12}. Therefore, finding a high capacity adsorbent capable of removing siloxanes under moderate humidity conditions in a reversible manner remains a challenge.

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Metal-Organic Frameworks (MOFs) are one of the most re-41 cent classes of porous adsorbents. These coordination polymers 42 are built from the assembly of metal nodes and organic multi-43 dentate linkers to form architectures of different dimensionality 44 from 1D to $4D^{13-15}$. Their near-infinite diversity, thanks to 45 a wide set of building blocks, has made this class of porous 46 solids promising for applications in gas/vapour adsorption/sep-47 aration^{16,17}, catalysis¹⁸, and sensing^{19,20} among others. Their 48 high and uniform porosity combined with extensive chemical 49 tunability of their pore walls suggest that MOFs may hold 50 promise as candidates for siloxane adsorption. Insofar only two 51 studies have attempted to investigate the potential of MOFs for 52 D4 removal. Mito-Oka and co-workers²¹ proposed DUT-4(AI) 53 ([AI(OH)(2,6-ndc), DUT: Dresden University of Technology), 54 a wine rack-like MOF, as a first potential adsorbent. Although 55 its hydrophobicity makes this MOF attractive for D4 elimination 56 under humidity, its adsorption capacity of 0.15 g s^{-1} , estimated 57 through single component by TGA measurements, is rather 58 low and its regeneration can only be achieved at very high tem-59 perature, over 523 K, resulting from a high confinement of D4 60 (kinetic diameter of 8.6 Å) in its channels (9 Å \times 9 Å). More 61 recently, MIL-101(Cr) (Cr₃O(OH)(H₂O)₂(btc)₃, MIL: Material 62 of Institute Lavoisier), a well-known highly porous MOF incor-63 porating two types of mesoporous cages with diameters of 29 64 Å and 34 Å was demonstrated to exhibit a much higher D4 65 uptake of $0.95 \,\mathrm{g \, g^{-1}}$ at 298 K, however its regeneration was 66 only possible upon heating at 423 K under vacuum²². Further, 67 since MIL-101(Cr) is known to be highly hydrophilic²³ we can 68 expect a substantial drop of its D4 uptake performance even 69 under low-relative humidity. Indeed, neither of these MOFs 70 tested so far combines a large D4 uptake, low-energy regenera-71 tion and hydrophobicity to avoid a preferential adsorption of 72 H₂O over D4 under low to moderate relative humidity. 73

To date, only a very small number of MOFs has been sampled for this application, and therefore relied on researchers' 75 intuition to identify promising adsorbents. There are, however, 76

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Fig. 1: Workflow of the strategy applied to identify the best MOFs for D4 adsorption, narrowing down candidates from top to bottom through synergistic computational (left) and experimental (right) actions. The final MOF candidate, PCN-777, is highlighted.

a myriad of hydrophobic MOFs that might perform better for 77 D4 adsorption. Since it is unfeasible to individually test the 78 performances of all the existing MOFs, several high throughput 79 computational screening (HTCS) workflows have been devised 80 which identified promising MOFs for diverse adsorption-related 81 applications^{24–29}. However, such a computational strategy can 82 only be successful if conducted in strong interplay with a care-83 ful analysis of the best-predicted MOF performers in terms of 84 chemical/thermal stability under the target working conditions 85 as well as ease of synthesis/activation. This enables the selec-86 tion of the MOF candidate with the best overall compromise 87 for further adsorption testing to confirm the expectation. 88

With this in mind, we herein devise a hand-in-hand 89 90 computational-experimental strategy whose workflow is summarized in Fig. 1. As a first stage, the CoRE (Computation-Ready, 91 Experimental) MOF 2019 database³⁰ was computationally 92 screened with the objective to identify hydrophobic materials 93 showing a D4 uptake higher than the current MOF benchmark, 94 e.g. MIL-101(Cr). Notably, the microscopic models used to de-95 scribe both MOF and D4 were validated by a good agreement 96 between the simulated D4 uptake and our own experimental 97 data collected on the two MOFs mentioned above, i.e. MIL-98 101(Cr) and DUT-4 (AI). From the top 56 predicted MOF 99 performers, we selected the Zr carboxylate-based mesoporous 100 101 PCN-777 (PCN for Porous Coordination Network) for further 102 experimental testing. This MOF was demonstrated to exhibit not only a record D4 uptake (1.8 g s^{-1}) to date for a crystalline 103 porous material, but also exceptional cycling and low-energy 104 regeneration without the need for thermal treatment, while 105 its confirmed hydrophobicity strongly suggests a preservation 106 107 of its adsorption performance under low to moderate relative humidity conditions. An in-depth analysis of the adsorption 108 mechanism further revealed the dominant host-guest interac-109

tions that control the adsorption of the first D4 molecules and their effective packing in the whole porosity up to saturation.

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2. Methodology

2.1. Computational methods. We used the CoRE-MOF 2019 113 database³⁰ (over 14 000 MOFs), recently updated to remove 114 solvent molecules and disordered structures, to which we also 115 added further 29 well-known MOFs owing to their good chem-116 ical/thermal stability and permanent accessible porosity (listed 117 in Table S7 SI). The geometric characterization of MOFs, in-118 cluding pore limiting diameters (PLDs), densities, N₂-accessible 119 surface areas (SAs), pore volumes (PVs) and void fractions (ϕ), 120 were calculated by Zeo++ software³¹. All Monte Carlo simu-121 lations were performed with the RASPA simulation package³². 122 Henry coefficients of $H_2O(K_{H,H_2O})$ and isosteric enthalpy 123 of adsorption ($\Delta H^0_{st,H_2O}$) were initially computed at 298 K 124 for all MOFs using the Widom particle insertion method³³. 125 These simulations were carried out using $1\,\times\,10^5$ production 126 cycles and 5 \times 10⁴ cycles for equilibration. We applied the 127 same Widom insertion method to calculate isosteric enthalpy of 128 adsorption at low coverage for D4 in DUT-4(AI) and PCN-777 129 with the consideration of 1 imes 10⁶ production cycles and 5 imes130 10⁵ steps for equilibration. Continuous fractional component 131 Monte Carlo (CFCMC) simulations³⁴ were performed to evalu-132 ate the saturation D4 uptake of all the selected hydrophobic 133 MOFs at 298 K. All CFCMC simulations were carried out for a 134 total of $1\,\times\,10^4$ cycles with 5 $\times\,10^3$ cycles for equilibration. A 135 cycle consists of N Monte Carlo steps, where N is equal to the 136 number of molecules (which fluctuates during a CFCMC simu-137 lation). For each cycle, random insertion, rotation, translation 138 and continuous-fractional swap moves were attempted. The 139 D4/MOF and H_2O/MOF interactions were described by the 140 sum of van der Waals (Lennard-Jones) and Coulombic terms. 141

The electrostatic interactions were calculated by the Ewald 142 summation³⁵ while a cut-off radius of 12.8 Å was considered 143 for the van der Waals term. Indeed, unit cell dimensions were 144 increased to at least 25.6 Å in each three directions for all 145 MOFs and their frameworks were treated as rigid. Atomic 146 charges for all atoms in the MOFs were estimated using Ex-147 tended Charge Equilibration (Qeq) method as implemented 148 in RASPA³² and their LJ parameters were taken from the 149 UFF forcefield as currently employed ^{36,37}. H2O was modelled 150 using TIP4P/2005³⁸. D4 was described by a semi-flexible all 151 atom model with intramolecular parameters taken from the 152 consistent-valence force field (CVFF)³⁹ (Tables S1 to S5, SI) 153 while the LJ parameters for all atoms were taken from the 154 UFF forcefield as done in earlier work⁴⁰ and their charges were 155 calculated at the DFT level (Table S6, SI). 156

All the results of the HCTS are available as CSV files in the
 SI. A web-based explorer, which can be used to interactively
 display the dataset is available at https://pauliacomi.com/
 mof4d4.

2.2. MOF sorbents. The benchmark MIL-101(Cr) sample was 161 taken from a previous work⁴¹, with all textural characteris-162 tics as stated in reference. DUT-4(AI) was purchased from 163 Materials Center (TU Dresden, Germany). PXRD, TGA and 164 N₂ physisorption measurements for DUT-4(AI) are available 165 in the SI (Fig. S6). Brunauer-Emmet-Teller (BET) areas of 166 $3475\,m^2\,g^{-1}$ and $1610\,m^2\,g^{-1}$ were determined for MIL-101(Cr) and DUT-4(AI), respectively. PCN-777 was synthesised by op-167 168 timizing a previous published methodology⁴². Full synthesis 169 methodology, activation procedure and phase purity analysis 170 using TGA, PXRD and N_2 physisorption are given in the SI. 171 All samples were activated at 423 K under vacuum prior to 172 adsorption experiments. 173

2.3. Material characterization. PXRD patterns were recorded 174 on a Panalytical X'Pert PRO PXRD diffractometer with a Cu 175 K_{lpha} radiation source, in a Bragg-Brentano reflection geometry, 176 using a spinning sample holder with a low-background silicon 177 insert. N $_2$ isotherms at 77 K were recorded in a Micromeritics 178 Tristar manometric analyser (displayed in Fig. S8, SI). The 179 BET areas were calculated using the pyGAPS suite⁴³, with 180 the application of the Rouquerol rules for isotherm region 181 selection yielding a minimum Pearson correlation coefficient of 182 R = 0.997 (see Fig. S9 for resulting fitting). 183

2.4. D4 sorption experiments. Sorption measurements were 184 gravimetrically recorded using a dynamic method in a DVS Vac-185 uum instrument (Surface Measurement Systems, UK). In this 186 setup, a continuous adsorbate flow sourced from the headspace 187 of a reservoir enters the sample enclosure, passes the suspended 188 sample pan, and is entrained by a vacuum system. Pressure is 189 controlled by a butterfly valve located before the outlet. Uptake 190 is monitored by a magnetically suspended balance, capable of 191 measuring mass changes at a resolution of 0.1 µg. The entire 192 apparatus is kept in a temperature-controlled chamber to avoid 193 any condensation points. For each experiment, a stainless-steel 194 195 sample pan is first tared, then loaded with about 10 mg of 196 sample. The sample is activated in situ under dynamic vacuum $(1 \times 10^{-2} \text{ Pa})$ to 423 K. The adsorption-desorption isotherms 197 for D4 and H_2O and subsequent repeats were recorded at 198 303 K in the 0-10 Pa range of pressure. Adsorption cycling 199 was similarly recorded, switching between two setpoints of 200 low (0.5 Pa) and high pressure (10 Pa). The D4 used for the 201 sorption experiments was sourced from Sigma Aldrich, with 202 minimum 98% purity. 203

3.1. Pre-selection of hydrophobic MOFs. We first excluded 205 from our considered MOF database all structures with PLDs 206 lower than 6 Å, a threshold selected as the average between 207 the kinetic diameter of D4 (8.6 Å) and the effective diameter 208 of its constitutive inner Si-O ring (4.5 Å). A total of 1739 209 remaining non-disordered MOFs were further considered, their 210 geometric and textural properties, i.e. PV, SA, and ϕ , as well 211 as their density (ρ) being summarized in Fig. S1. As siloxane-212 rich biogas streams often contain water vapour, the optimal 213 D4 adsorbent should have a relatively low water affinity to 214 avoid competing adsorption. Moreover, hydrophobic MOFs 215 are known to possess increased resistance to the hydrolysis 216 of the metal-linker bond 44,45, alleviating long-term water sta-217 bility concerns. Therefore, we screened the water affinity of 218 the 1739 MOFs by computing their Henry coefficient of water 219 (K_{H,H_2O}) and the isosteric enthalpy of adsorption at infinite di-220 lution ($\Delta H_{st,H_2O}^0$) at 298 K using the Widom particle insertion 221 method ³³. This approach is generally applied in HTCS studies, 222 providing a quick way to gauge the hydrophobicity/hydrophilic-223 ity of MOFs^{36,46}. All the computational details including the 224 force fields used to describe both MOFs and water are provided 225 in the methodology section and SI. In the frame of biogas 226 upgrading, an extremely hydrophobic adsorbent is not required 227 since the water content usually ranges from 38% to 85% relative 228 humidity⁴, therefore the following thresholds were applied to 229 select MOFs with moderate to high hydrophobicity: $K_{H,H_2O} <$ 230 $1\times 10^{-5}\,{\rm mol\,kg^{-1}\,Pa^{-1}}$ and $\Delta H^0_{st,H_2O}<33\,{\rm kJ\,mol^{-1}}$ (below 231 the vaporization enthalpy of water $\sim 40 \text{ kJ mol}^{-1}$)⁴⁷. As a frame 232 of reference, the highly hydrophobic ZIF-8 is characterized 233 by $K_{H,H_{2O}} = 2.5 \times 10^{-6} \text{ mol kg}^{-1} \text{ Pa}^{-1}$ and $\Delta H^0_{st,H_{2O}} = 30 \text{ kJ mol}^{-1 48}$. Overall, among the 1739 MOFs, 811 structures 234 235 (47% of our material library) were predicted to fulfill these 236 two criteria. This hydrophobic MOF dataset encompasses 237 structures of density ranging from $0.24\,g\,cm^{-3}$ to $2.04\,g\,cm^{-3}$ 238 and with a wide range of geometric and textural features: 6 239 Å < PLD < 36 Å, 0.42 $<\phi<$ 0.90, 0.27 cm $^3\,{
m g}^{-1}<$ PV <240 $3.72\,\text{cm}^3\,\text{g}^{-1}$ and $320\,\text{m}^2\,\text{g}^{-1} < \text{SA} < 6700\,\text{m}^2\,\text{g}^{-1}$, as shown 241 in Fig. S1. 242

3.2. Prediction of the D4 uptake performance for the hy-243 drophobic MOFs. As a validation stage of the computational 244 method, the D4 uptakes for MIL-101(Cr) and DUT-4(AI) were 245 first predicted using the CFCMC approach described in the 246 methodology section and compared with the available exper-247 imental data. The simulated uptake for MIL-101(Cr), the 248 current best MOF performer, was found to be $1.03\,g\,g^{-1}$ vs. $0.95\,g\,g^{-1}$ as reported in the original experimental study $^{22}.$ We 249 250 equally confirmed the good agreement between the calculated 251 and the experimental D4 uptake by recording an additional 252 adsorption isotherm on a MIL-101(Cr) sample, finding a D4 253 capacity of 1.15 g s^{-1} at 298 K. The D4 uptake for DUT-4(Al) 254 was however predicted to be substantially higher $(0.42 \,\mathrm{g \, g^{-1}})$ 255 than the experimental value reported previously of $0.15 \text{ g} \text{ g}^{-121}$. 256 We therefore collected a D4 adsorption isotherm on a pristine 257 DUT-4(AI) sample, finding a D4 uptake of 0.5 g s^{-1} (Fig. S10), 258 more in line with our theoretical assessment. The lower D4 259 capacity reported in the original study is attributed to the 260 method used to quantify the adsorbed amount, based on mass 261 loss upon heating. It is likely that only a fraction of D4 was 262 released, since D4 was demonstrated to strongly interact with 263 DUT-4(AI) due to a high confinement in its pores²¹. 264

Overall, the good agreement between the simulated uptakes 265 and the corresponding experimental data for the previously 266 investigated MOFs served to validate both the applicability 267 of our computational method and the reliability of our experimental setup. This further highlights the importance of a dual 269

Table 1: Top 10 promising hydrophobic MOF materials identified for D4 uptake at 298 K.

MOF	PLD	SA	ρ	PV	ϕ	K_{H,H_2O}	$\Delta H^0_{st,H_2O}$	Gravimetric D4	Volumetric D4
	(Å)	$(m^2 g^{-1})$	$(g cm^{-3})$	$(cm^{3}g^{-1})$		$(molkg^{-1}Pa^{-1})$	$(kJ mol^{-1})$	uptake $(g g^{-1})$	uptake (g cm ⁻³)
FOTNIN (PCN-777)	28.36	2990	0.27	3.31	0.90	2.80×10^{-6}	7.82	2.68	0.72
RUTNOK	14.65	6200	0.24	3.72	0.90	6.70×10^{-6}	14.81	2.57	0.62
CUSYAR	12.18	5700	0.25	3.65	0.90	3.42×10^{-6}	8.15	2.35	0.59
WUHDAG	10.50	5500	0.29	2.99	0.87	4.69×10^{-6}	16.28	2.01	0.58
HOHMEX	14.89	5000	0.32	2.74	0.87	4.66×10^{-6}	13.24	1.97	0.63
ECOKAJ	17.58	3600	0.33	2.68	0.87	6.89×10^{-6}	17.20	1.97	0.65
DAJWET	26.59	5000	0.28	3.06	0.87	7.73×10^{-6}	17.92	1.93	0.54
RUBDUP	19.25	4200	0.30	2.90	0.87	3.79×10^{-6}	11.62	1.93	0.58
WUHCUZ	12.21	5500	0.30	2.91	0.87	3.75×10^{-6}	12.94	1.80	0.54
ADATAC	10.28	5130	0.34	2.57	0.87	4.16×10^{-6}	12.78	1.68	0.57

experimental-computational approach even prior to starting 270 the high-throughput screening. We then transitioned towards 271 the search for better performers amongst the 811 identified 272 273 hydrophobic MOFs. Fig. 2a reports their computed D4 uptakes vs. their $\Delta H^0_{st,H_2O}$ values at 298 K, with a similar correlation 274 depicted vs. K_{H,H_2O} in Fig. S4, SI. The dashed line represents 275 the current known upper bound for D4 uptake in MOFs, con-276 sidering MIL-101(Cr) as the benchmark sorbent $(0.95 \text{ g s}^{-1})^{22}$. 277 56 hydrophobic MOFs were predicted to be more attractive 278 candidates than MIL-101(Cr) on the basis of gravimetric D4 279 uptake. Common geometric and textural features of these 280 MOF candidates are void fractions ϕ larger than 0.81 and pore 281 volumes (PV) higher than $\sim 1.7 \, \text{cm}^3 \, \text{g}^{-1}$. Typically, the relation 282 between gravimetric D4 uptake and PV is shown in Fig. S3. 283

The 10 best MOFs showing the highest D4 uptakes ranging 284 from 1.68 to 2.68 g g^{-1} are highlighted in Fig. 2a by their 285 Cambridge Structural Database (CSD)⁴⁹ refcode and listed in 286 Table 1. Notably, all these identified candidates were found 287 to be highly hydrophobic with associated K_{H,H_2O} of about 288 $5 \times 10^{-6} \text{ mol kg}^{-1} \text{ Pa}^{-1}$ and their $\Delta H^0_{st,H_2O}$ ranging from 8 289 to 18 kJ mol⁻¹ which make these adsorbents also potentially 290 effective under moderate humidity conditions. Table 1 shows 291 that the highly hydrophobic FOTNIN is predicted to exhibit the 292 highest saturated D4 uptake (2.68 g g^{-1}) , in relation with its 293 high PV $(3.31 \text{ cm}^3 \text{ g}^{-1})$ and large mesoporous cages (33.7 Å)294 \times 28.4 Å). Remarkably, this gravimetric D4 loading translates 295 into a spectacular improvement as compared to MIL- $101(Cr)^{22}$. 296 RUTNOK (common name IRMOF- 76^{50}) gave almost a similar D4 uptake (2.57 g g⁻¹) as FOTNIN, in part due to similar 297 298 PV $(3.72 \text{ cm}^3 \text{ g}^{-1})$ and ϕ (0.9). Other candidates exhibit 299 high D4 uptakes, including CUSYAR (also known as MOF-300 210⁵¹), WUHDAG and WUHCUZ (NU-1104, and NU-1103⁵², 301

respectively). Full structural properties of these 10 MOFs ³⁰² including organic ligands and metal sites are given in Table S8. ³⁰³

In the scope of the practical application of a sorbent for a 304 filter bed or column, volumetric uptake is a reliable metric due 305 to its direct relation to equipment sizing. Trade-offs between 306 gravimetric and volumetric uptakes have been previously re-307 ported for the storage of various fluids using porous materials²⁶. 308 Fig. 2b shows the relation between the computed gravimetric 309 and volumetric D4 uptakes for the hydrophobic MOFs database. 310 Unlike gravimetric uptake which increases indefinitely, the vol-311 umetric uptake in porous materials is limited by the density 312 of the adsorbate fluid phase, to which it asymptotically ap-313 proaches as framework density decreases (and void fraction 314 increases)⁵³. Interestingly FOTNIN remains the top MOF 315 performer in terms of volumetric uptake as well $(0.72 \, \text{g cm}^{-3})$, 316 see Fig. 2b). This MOF (common name PCN-777⁴²) is built 317 from large planar tritopic linkers (4,4',4' '-s-triazine-2,4,6-triyl-318 tri-benzoate or TATB) coordinated to Zr_6 -oxoclusters in an 319 antiprismatic fashion, forming vertex-sharing supertetrahedra 320 surrounding a mesoporous cage of 33.7 Å as depicted in Fig. 2c. 321 These cages are interconnected by hexagonal windows (30 Å) 322 and are typically decorated by OH/H_2O moieties coordinated 323 to the remaining axial positions of the Zr_6 node. 324

3.3. Experimental assessment of the D4 sorption perfor-325 mance for the top MOF. While HTCS enabled a rapid and 326 effective screening on the performance indicator, additional 327 criteria, such as thermal/chemical stability, synthesis route, 328 activation conditions, precursor toxicity and linker availability 329 need to be considered to select the optimal adsorbents. We 330 therefore critically assessed PCN-777 prior to further experi-331 mental action. Our selection criteria for PCN-777 were (i) the 332



Fig. 2: (a) Predicted D4 uptake performance at 298 K for the hydrophobic MOF database plotted as a function of computed $\Delta H_{st,H_2O}^0$, and colour coded by void fraction, ϕ . Top performing 10 candidates are represented by different symbols in the legend. (b) Relation between gravimetric (g g⁻¹) and volumetric (g cm⁻³) D4 uptake for all MOFs at 298 K. Marker size represents PV while colour denotes ϕ . Dashed line represents the gravimetric and volumetric uptake of benchmark MIL-101(Cr)²². (c) Illustration of the structure of our promising material identified for D4 uptake, PCN-777. Zr, N, O, C, and H atoms are depicted in light blue, dark blue, red, dark grey, and light grey, respectively.



Fig. 3: (a) Single component adsorption/desorption isotherms for D4 (blue) and H_2O (red) collected at 303 K for PCN-777 in the pressure range of 0-10 Pa (corresponding to 0–0.05 p/p⁰ for D4). Solid and open symbols represent adsorption and desorption branches, respectively. (b) Comparison of the D4 capacity of MOFs investigated in the present study with other classes of porous materials (data from Wang *et al.*⁴), with error bars placed at one standard deviation of mean capacity. (c) 5 D4 sorption-desorption cycles recorded after the first two isotherms on PCN-777, in the same pressure range. (d) PXRD of pristine PCN-777 sample (black) and samples recovered after D4 cycling (blue) and water adsorption (red).

excellent known stability of the oxo-Zr-carboxylate metal node, at the origin of the high chemical and thermal resistance of the framework, alongside with (ii) the commercially available linker and well-controlled synthesis procedure documented elsewhere ^{42,54}. Indeed, this material was synthesised accordingly (details provided in the methodology section).

The D4 adsorption isotherm for PCN-777 was first recorded 339 up to 10 Pa at 303 K using a dynamic vapour sorption system 340 (experimental details in the methodology section). The re-341 sulting isotherm, depicted in Fig. 3a, exhibits a characteristic 342 type V shape⁵⁵ with a sharp D4 uptake increase above 7 Pa up to a maximum of $1.8 \, g \, g^{-1}$ that translates into $0.49 \, g \, cm^{-3}$. 343 344 This value is however lower than the predicted uptake due to 345 two combined reasons: (i) an incomplete evacuation of the 346 porosity (theoretical PV= $3.3 \text{ cm}^3 \text{ g}^{-1}$ vs the experimental one 347 of $2.2 \text{ cm}^3 \text{g}^{-1}$ determined through N₂ physisorption at 77 K, 348 in Fig. S8, SI) commonly observed for mesoporous MOFs^{56,57} 349 and (ii) only a partial accessibility of the super-tetrahedral 350 cages to D4 owing to their relatively small windows. Indeed, 351 while optimized activation procedures may recover more of 352 the expected porosity, the attained D4 uptake constitutes a 353 record among porous solids. This positions PCN-777 as the 354 crystalline porous material with the highest currently known D4 355 uptake, almost twice higher than the benchmark MIL-101(Cr), 356 357 5-10 times that of the most promising silicas and zeolites, and above the best performing activated carbons as illustrated in 358 Fig. 3b⁴. Notably, the step-like adsorption behaviour is ideal 359 from the application point of view of a breakthrough filter, 360 as it ensures a narrow mass transfer zone and minimises the 361 column dead zone at break point. Remarkably, the maximum 362 uptake for PCN-777 is attained at low pressure of 7 Pa that 363 makes this MOF highly promising for D4 removal in a gas 364 phase concentration below 75 ppm. 365

Throughout desorption (dotted line with open symbols in 366 Fig. 3a), a small hysteresis occurs with a width of about 367 1 Pa. Under complete vacuum, a minute amount of D4, about 368 0.1 g s^{-1} , i.e. 5% of total capacity, is retained in the struc-369 ture. We attribute this capacity loss to D4 molecules irre-370 versibly trapped in the super-tetrahedral cages or on a small 371 fraction of defect sites. Overall, PCN-777 acts as a highly 372 reversible D4-adsorbent. A second sorption cycle reveals the 373 excellent repeatability of D4 sorption by this MOF, with iden-374 tical condensation pressure and total uptake, the adsorption-375 desorption branches now overlapping in the very low-pressure 376 region (Fig. 3a). 377

To further investigate the D4 adsorption-desorption cyclabil-378 ity of PCN-777, a subsequent set of five cycles was recorded on 379 the same sample, covering the entire uptake range from fully 380 loaded to empty under a medium vacuum level of 0.5 Pa (see 381 Fig. 3c). No further capacity loss is observed after the initial 382 5 wt% from cycle 1 to cycle 2 with a pressure drop sufficient 383 to fully remove adsorbed D4 in every cycle without the need 384 of thermal treatment. This is a leap forward compared to the 385 previous MOF candidates, i.e. MIL-101(Cr) and DUT-4(AI). 386 The former was reported²² to be fully regenerable only at high 387 temperatures (outgassed under vacuum at 423 K), and we note 388 that vacuum alone was unable to fully desorb D4, with nearly 389 50% of siloxane remaining in the structure after desorption in 390 our experiments (Fig. S10, SI). D4 adsorption in DUT-4(AI) is 391 even more irreversible, owing to the strong confinement of the 392 siloxane molecules in its pores²¹, with essentially no desorption 393 observed under vacuum (Fig. S10, SI). The global sorption 394 kinetics was further qualitatively evaluated by observing the 395 equilibration time throughout cycling steps. Fig. 3c reveals 396 that an adsorption/desorption cycle can be achieved in less 397 than 30 minutes. Such a fast kinetics is a clear advantage 398



Fig. 4: Representative snapshots of the preferential sitting of D4 in the pores of PCN-777 at 298 K for increasing loading at (a) 10% with highlighted interactions distance between D4 and the MOF framework, and at (b) 40%, (c) 65%, and (d) 100% fractional loading (θ). Framework atoms (sticks) and D4 molecules (lines, and ball and sticks) are coded as Zr, N, O, Si, C, and H atoms in light blue, dark blue, red, yellow, dark grey, and light grey respectively. The separating distance is represented by dashed black lines and reported in Å.

for practical use. In addition, the water adsorption collected for PCN-777 further confirmed its predicted hydrophobicity and revealed that below P = 7 Pa, water loading is negligible, i.e. under 0.02 g g^{-1} (see Fig. 3a). This observation strongly suggests that PCN-777 is expected to maintain its high-level performance for D4 removal under low to moderate humidity working conditions.

Stability of PCN-777 after its use as a D4 adsorbent was 406 also evaluated by checking its crystallinity and porosity. PXRD 407 patterns recorded after the D4 cycling experiments show similar 408 Bragg peak positions and broadenings as the pristine material, 409 testifying that no amorphisation or decrease of crystallinity were 410 incurred (Fig. 3d). The same conclusion holds true for PCN-411 777 upon water adsorption. Further, N₂ adsorption isotherms 412 collected at 77 K for PCN-777 after H_2O and D4 adsorption 413 both present a similar shape than that of the pristine solid 414 (see Fig. S8). Slightly lower pore volume $(1.87 \text{ cm}^3 \text{ g}^{-1} \text{ vs} 2.20 \text{ cm}^3 \text{ g}^{-1})$ and BET area $(1544 \text{ m}^2 \text{ g}^{-1} \text{ vs} 1730 \text{ m}^2 \text{ g}^{-1})$ 415 416 were obtained for the material after D4 cycling compared to 417 the pristine solid, attributed to the small amount of D4 retained 418 in the porous framework during the first adsorption cycle. 419

3.4. Adsorption mechanism. A careful analysis of the adsorp-420 tion mechanism of D4 in PCN-777 was further explored by 421 considering MC simulations in the canonical ensemble with 422 423 increasing loading up to the saturation. At the initial stage of 424 adsorption, the coordinated OH/H_2O moieties of the MOF Zr_6 node pointing towards the pore were found to act as primary 425 adsorption sites (Fig. 4a). The D4 molecule interacts mostly via 426 its methyl group with an averaged separating $H(CH_3) - H(H_2O)$ 427 distance of 2.8 Å (see the radial distribution function plotted 428 for the corresponding pair in Fig. S5a) as illustrated in Fig. 4a. 429 This preferential sitting of D4 is associated with a moderately 430 high simulated adsorption enthalpy of 83.5 kJ mol^{-1} in line 431

with the isosteric heat of adsorption we assessed experimen-432 tally that ranges from 65 and 75 kJ mol⁻¹ (Fig. S11). Both 433 values are higher than the enthalpy of liquefaction of D4 at 434 303 K as $54.5 \text{ kJ} \text{ mol}^{-147}$. We further demonstrated that this 435 value remains substantially lower than the one simulated for 436 DUT-4(AI) (194.0 kJ mol⁻¹) for which the adsorption of D4 437 is governed by a high degree of confinement leading to an 438 irreversible process. This observation clearly states that the 439 adsorption energetics in PCN-777 offers a good compromise 440 to ensure an efficient adsorption of D4 as well as an almost 441 fully reversible and fast adsorption/desorption process. While 442 increasing the loading, D4 molecules tend to form a monolayer 443 near the wall of the cage owing to their interactions with both 444 the organic linkers and inorganic nodes of the MOF as shown 445 in Fig. 4b-c. Finally, at higher loading, the molecules form 446 multilayers and further occupy the whole cage corresponding 447 to the scenario of the capillary condensation (Fig. 4d). This 448 effective packing is governed by guest-guest interactions involv-449 ing averaged separating $H(CH_3)-H(CH_3)$ distance of 2.7 Å at 450 saturation (the radial distribution function plotted for this pair 451 is shown in Fig. S5b). Such pore filling mechanism has been 452 commonly observed in diverse mesoporous materials for a range 453 of molecules⁵⁸. Indeed, PCN-777 exhibits an ideal combination 454 of a large cage to enable an effective packing of the siloxane 455 molecules and the presence of moieties accessible to D4 to 456 favour moderately high host/guest interactions to ensure an 457 efficient trapping of the D4 molecules initially adsorbed. 458

4. Conclusions

In this work, a high throughput computational screening first identified a series of hydrophobic MOFs with octamethylcyclotetrasiloxane uptakes outperforming by far the performance of the conventional adsorbents. The best-predicted MOF performer, PCN-777, was synthesized and its predicted exceptional

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adsorption capacity for this typical contaminant present in bio-465 gas was further experimentally confirmed. This stable MOF 466 was demonstrated to exhibit record gravimetric (1.8 g g^{-1}) and 467 volumetric $(0.49 \,\mathrm{g}\,\mathrm{cm}^{-3})$ uptake alongside with a reversible and 468 fast adsorption/desorption process, very good cyclability and 469 easy regeneration under continuous pressure cycling owing to a 470 step-like sorption isotherm. The attractiveness of PCN-777 was 471 found to result from a synergistic combination of mesoporous 472 cages and chemical functionality pointing towards the center 473 of the cages to ensure moderately high host/guest interactions 474 and favour an efficient removal of D4 at low pressure and an 475 efficient packing of the siloxane molecules at higher pressure 476 while maintaining the process highly reversible. Moreover, its 477 hydrophobicity makes this MOF promising for the selective 478 removal of siloxanes in moderate humidity conditions. In a 479 broader sense, this study highlights the efficacy of an inte-480 grated workflow for accelerating the selection of adsorbents for 481 a target application, spanning the entire pipeline from method 482 validation to computational screening, synthesis, adsorption 483 testing and finally identification of the optimal candidates. 484

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490 Contributions

⁴⁹¹ Conceptualization: EG, PI, GR, SDV, GM. Computational in vestigation, methodology, data analysis: EG, and GM. Screen ⁴⁹³ ing data curation: EG. Visualization: PI. PCN-777 synthesis:
 ⁴⁹⁴ YK and JSK. Experimental investigation, methodology, data
 ⁴⁹⁵ analysis: PI and SDV. Writing – original draft: EG, PI, SDV,
 ⁴⁹⁶ GM. Writing – review and editing: all authors. Supervision:

497 JSK, SDV, GM.

498 Conflicts of interest

⁴⁹⁹ There are no conflicts of interest to declare.

500 References

- Themelis, N.J. and Ulloa, P.A. "Methane generation in landfills." *Renewable Energy*, 2007. 32(7):1243–1257. doi:10.1016/j.renene.2006.04.020
- Takuwa, Y.; Matsumoto, T.; Oshita, K.; Takaoka, M.; Morisawa, S.; and Takeda, N.
 "Characterization of trace constituents in landfill gas and a comparison of sites in Asia."
 J Mater Cycles Waste Manag, 2009. 11(4):305–311. doi:10.1007/s10163-009-0257-1
- Ohannessian, A.; Desjardin, V.; Chatain, V.; and Germain, P. "Volatile organic silicon compounds: The most undesirable contaminants in biogases." *Water Science and Technology*, 2008. 58(9):1775–1781. doi:10.2166/wst.2008.498
- Wang, G.; Zhang, Z.; and Hao, Z. "Recent advances in technologies for the removal of volatile methylsiloxanes: A case in biogas purification process." *Critical Reviews in Environmental Science and Technology*, 2019. **49**(24):2257–2313. doi:10.1080/10643389.2019.1607443
- Dewil, R.; Appels, L.; and Baeyens, J. "Energy use of biogas hampered by the presence of siloxanes." *Energy Conversion and Management*, 2006. 47(13-14):1711–1722. doi:10.1016/j.enconman.2005.10.016
- Kuhn, J.N.; Elwell, A.C.; Elsayed, N.H.; and Joseph, B. "Requirements, techniques, and costs for contaminant removal from landfill gas." *Waste Management*, 2017.
 63:246-256. doi:10.1016/j.wasman.2017.02.001
- Chin, K.F.; Wan, C.; Li, Y.; Alaimo, C.P.; Green, P.G.; Young, T.M.; and Kleeman,
 M.J. "Statistical analysis of trace contaminants measured in biogas." *Sci Total Environ*, 2020. **729**:138702
- Ajhar, M.; Travesset, M.; Yüce, S.; and Melin, T. "Siloxane removal from landfill and digester gas - a technology overview." *Bioresour Technol*, 2010. **101**(9):2913–2923
- Finocchio, E.; Garuti, G.; Baldi, M.; and Busca, G. "Decomposition of hexamethylcy clotrisiloxane over solid oxides". *Chemosphere*. 2008. 72(11):1659–1663
- Montanari, T.; Finocchio, E.; Bozzano, I.; Garuti, G.; Giordano, A.; Pistarino, C.; and Busca, G. "Purification of landfill biogases from siloxanes by adsorption: A study of silica and 13X zeolite adsorbents on hexamethylcyclotrisiloxane separation." *Chemical Engineering Journal*, 2010. 165(3):859–863. doi:10.1016/j.cej.2010.10.032
- Sigot, L.; Ducom, G.; and Germain, P. "Adsorption of octamethylcyclotetrasiloxane
 (D4) on silica gel (SG): Retention mechanism." *Microporous and Mesoporous Materials*, 2015. 213:118–124. doi:10.1016/j.micromeso.2015.04.016
- Schweigkofler, M. and Niessner, R. "Removal of siloxanes in biogases." *Journal of Hazardous Materials*, 2001. 83(3):183–196. doi:10.1016/S0304-3894(00)00318-6

 Férey, G. "Hybrid porous solids: Past, present, future." Chem Soc Rev, 2008. 37(1):191–214. doi:10.1039/B618320B

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- 14. Zhou, H.C.; Long, J.R.; and Yaghi, O.M. "Introduction to Metal–Organic Frameworks." Chemical Reviews, 2012. 112(2):673–674. doi:10.1021/cr300014x
- Evans, J.D.; Bon, V.; Senkovska, I.; Lee, H.C.; and Kaskel, S. "Four-dimensional metal-organic frameworks." Nat Commun, 2020. 11(1):2690. doi:10.1038/s41467-020-16527-8
- Siegelman, R.L.; Milner, P.J.; Kim, E.J.; Weston, S.C.; and Long, J.R. "Challenges and opportunities for adsorption-based CO ₂ capture from natural gas combined cycle emissions." *Energy Environ Sci*, 2019. **12**(7):2161–2173. doi:10.1039/C9EE00505F
- Lin, R.B.; Xiang, S.; Zhou, W.; and Chen, B. "Microporous Metal-Organic Framework Materials for Gas Separation." *Chem*, 2020. 6(2):337–363. doi:10.1016/j.chempr.2019.10.012
- Bavykina, A.; Kolobov, N.; Khan, I.S.; Bau, J.A.; Ramirez, A.; and Gascon, J. "Metal–Organic Frameworks in Heterogeneous Catalysis: Recent Progress, New Trends, and Future Perspectives." *Chem Rev*, 2020. **120**(16):8468–8535. doi:10.1021/acs.chemrev.9b00685
- Allendorf, M.D.; Dong, R.; Feng, X.; Kaskel, S.; Matoga, D.; and Stavila, V. "Electronic Devices Using Open Framework Materials." *Chem Rev*, 2020. **120**(16):8581–8640. doi:10.1021/acs.chemrev.0c00033
- Woellner, M.; Hausdorf, S.; Klein, N.; Mueller, P.; Smith, M.W.; and Kaskel, S. "Adsorption and Detection of Hazardous Trace Gases by Metal-Organic Frameworks." *Adv Mater*, 2018. **30**(37):1704679. doi:10.1002/adma.201704679
- Mito-oka, Y.; Horike, S.; Nishitani, Y.; Masumori, T.; Inukai, M.; Hijikata, Y.; and Kitagawa, S. "Siloxane D4 capture by hydrophobic microporous materials." *J Mater Chem A*, 2013. 1(27):7885. doi:10.1039/c3ta11217a
- Gargiulo, N.; Peluso, A.; Aprea, P.; Marino, O.; Cioffi, R.; Jannelli, E.; Cimino, S.; Lisi, L.; and Caputo, D. "Chromium-based MIL-101 metal organic framework as a fully regenerable D4 adsorbent for biogas purification." *Renewable Energy*, 2019. 138:230–235. doi:10.1016/j.renene.2019.01.096
- Zhao, H.; Li, Q.; Wang, Z.; Wu, T.; and Zhang, M. "Synthesis of MIL-101(Cr) and its water adsorption performance." *Microporous and Mesoporous Materials*, 2020. 297:110044. doi:10.1016/j.micromeso.2020.110044
- Simon, C.M.; Mercado, R.; Schnell, S.K.; Smit, B.; and Haranczyk, M. "What Are the Best Materials To Separate a Xenon/Krypton Mixture?" *Chem Mater*, 2015.
 27(12):4459–4475. doi:10.1021/acs.chemmater.5b01475
- Park, J.; Lively, R.P.; and Sholl, D.S. "Establishing upper bounds on CO₂ swing capacity in sub-ambient pressure swing adsorption via molecular simulation of metal-organic frameworks." J Mater Chem A, 2017. 5(24):12258–12265. doi:10.1039/C7TA02916K
- Moghadam, P.Z.; Islamoglu, T.; Goswami, S.; Exley, J.; Fantham, M.; Kaminski, C.F.; Snurr, R.Q.; Farha, O.K.; and Fairen-Jimenez, D. "Computer-aided discovery of a metal–organic framework with superior oxygen uptake." *Nat Commun*, 2018. 9(1):1378. doi:10.1038/s41467-018-03892-8
- Boyd, P.G.; Chidambaram, A.; García-Díez, E.; Ireland, C.P.; Daff, T.D.; Bounds, R.; Gładysiak, A.; Schouwink, P.; Moosavi, S.M.; Maroto-Valer, M.M.; Reimer, J.A.; Navarro, J.A.R.; Woo, T.K.; Garcia, S.; Stylianou, K.C.; and Smit, B. "Data-driven design of metal-organic frameworks for wet flue gas CO2 capture." *Nature*, 2019. 576(7786):253–256. doi:10.1038/s41586-019-1798-7
- Shi, Z.; Liang, H.; Yang, W.; Liu, J.; Liu, Z.; and Qiao, Z. "Machine learning and in silico discovery of metal-organic frameworks: Methanol as a working fluid in adsorption-driven heat pumps and chillers." *Chemical Engineering Science*, 2020. 214:115430. doi:10.1016/j.ces.2019.115430
- Yao, Z.; Sánchez-Lengeling, B.; Bobbitt, N.S.; Bucior, B.J.; Kumar, S.G.H.; Collins, S.P.; Burns, T.; Woo, T.K.; Farha, O.K.; Snurr, R.Q.; and Aspuru-Guzik, A. "Inverse design of nanoporous crystalline reticular materials with deep generative models." *Nat Mach Intell*, 2021. doi:10.1038/s42256-020-00271-1
- Chung, Y.G.; Haldoupis, E.; Bucior, B.J.; Haranczyk, M.; Lee, S.; Zhang, H.; Vogiatzis, K.D.; Milisavljevic, M.; Ling, S.; and Camp, J.S. "Advances, updates, and analytics for the computation-ready, experimental Metal–Organic framework database: CoRE MOF 2019." J Chem Eng Data, 2019. 64(12):5985–5998
- Willems, T.F.; Rycroft, C.H.; Kazi, M.; Meza, J.C.; and Haranczyk, M. "Algorithms and tools for high-throughput geometry-based analysis of crystalline porous materials." *Microporous and Mesoporous Materials*, 2012. 149(1):134–141. doi:10.1016/j.micromeso.2011.08.020
- Dubbeldam, D.; Calero, S.; Ellis, D.E.; and Snurr, R.Q. "RASPA: Molecular simulation software for adsorption and diffusion in flexible nanoporous materials." *Mol Simul*, 2016. 42(2):81–101
- Frenkel, D. and Smit, B. Understanding Molecular Simulation: From Algorithms to Applications, vol. 1. Academic press: London, 2002. ISBN 0-08-051998-9
- Rahbari, A.; Hens, R.; Ramdin, M.; Moultos, O.A.; Dubbeldam, D.; and Vlugt, T.J.H. "Recent advances in the continuous fractional component Monte Carlo methodology." *Molecular Simulation*, 2020. pp. 1–20. doi:10.1080/08927022.2020.1828585
- Ewald, P.P. "Die berechnung optischer und elektrostatischer gitterpotentiale." Ann Phys, 1921. 369(3):253–287
- Qiao, Z.; Xu, Q.; Cheetham, A.K.; and Jiang, J. "High-throughput computational screening of metal-organic frameworks for thiol capture." J Phys Chem C, 2017. 121(40):22208–22215
- Keskin, S.; Liu, J.; Rankin, R.B.; Johnson, J.K.; and Sholl, D.S. "Progress, Opportunities, and Challenges for Applying Atomically Detailed Modeling to Molecular Adsorption and Transport in Metal-Organic Framework Materials." *Ind Eng Chem Res*, 2009. 48(5):2355–2371. doi:10.1021/ie800666s
- Abascal, J.L. and Vega, C. "A general purpose model for the condensed phases of water: TIP4P/2005." J Chem Phys, 2005. 123(23):234505–234517
- Dauber-Osguthorpe, P.; Roberts, V.A.; Osguthorpe, D.J.; Wolff, J.; Genest, M.; and Hagler, A.T. "Structure and energetics of ligand binding to proteins: Escherichia coli dihydrofolate Reductase-Trimethoprim, a Drug-Receptor system." *Proteins: Struct, Funct, Bioinf*, 1988. 4(1):31–47
- Xu, R.G. and Leng, Y. "Solvation force simulations in atomic force microscopy." The 622 Journal of Chemical Physics, 2014. 140(21):214702. doi:10.1063/1.4879657
- Pillai, R.S.; Yoon, J.W.; Lee, S.J.; Hwang, Y.K.; Bae, Y.S.; Chang, J.S.; and Maurin, G. "N 2 Capture Performances of the Hybrid Porous MIL-101(Cr): From Prediction toward Experimental Testing." J Phys Chem C, 2017. 121(40):22130– 626

22138. doi:10.1021/acs.jpcc.7b07029

627

- Feng, D.; Wang, K.; Su, J.; Liu, T.F.; Park, J.; Wei, Z.; Bosch, M.; Yakovenko, A.;
 Zou, X.; and Zhou, H.C. "A Highly Stable Zeotype Mesoporous Zirconium Metal-Organic Framework with Ultralarge Pores." *Angew Chem Int Ed*, 2015. 54(1):149–154.
 doi:10.1002/anie.201409334
- 43. Iacomi, P. and Llewellyn, P.L. "pyGAPS: A Python-based framework for adsorption isotherm processing and material characterisation." *Adsorption*, 2019. 25(8):1533– 1542. doi:10.1007/s10450-019-00168-5
- 44. Burtch, N.C.; Jasuja, H.; and Walton, K.S. "Water Stability and Adsorption in Metal–Organic Frameworks." *Chemical Reviews*, 2014. 114(20):10575–10612. doi:10.1021/cr5002589
- 45. Wu, T.; Shen, L.; Luebbers, M.; Hu, C.; Chen, Q.; Ni, Z.; and Masel, R.I. "Enhancing
 the stability of metal-organic frameworks in humid air by incorporating water repellent
 functional groups." *Chem Commun*, 2010. 46(33):6120–6122
- Matito-Martos, I.; Moghadam, P.Z.; Li, A.; Colombo, V.; Navarro, J.A.R.; Calero,
 S.; and Fairen-Jimenez, D. "Discovery of an Optimal Porous Crystalline Material for
 the Capture of Chemical Warfare Agents." *Chem Mater*, 2018. **30**(14):4571–4579.
 doi:10.1021/acs.chemmater.8b00843
- Lemmon, E.W.; Bell, I.; Huber, M.L.; and McLinden, M.O. "NIST standard reference database 23: Reference fluid thermodynamic and transport properties-refprop, version 10.0, national institute of standards and technology." 2018
- Moghadam, P.Z.; Fairen-Jimenez, D.; and Snurr, R.Q. "Efficient identification of hydrophobic MOFs: Application in the capture of toxic industrial chemicals." *J Mater Chem A*, 2016. 4(2):529–536
- 49. Allen, F.H. "The cambridge structural database: A quarter of a million crystal structures and rising." Acta Crystallogr, Sect B: Struct Sci, 2002. 58(3):380–388
- 50. Oisaki, K.; Li, Q.; Furukawa, H.; Czaja, A.U.; and Yaghi, O.M. "A Metal-organic framework with covalently bound organometallic complexes." *J Am Chem Soc*, 2010.
 132(27):9262–9264
- 55. Furukawa, H.; Ko, N.; Go, Y.B.; Aratani, N.; Choi, S.B.; Choi, E.; Yazaydin, A.O.; Snurr, R.Q.; O'Keeffe, M.; Kim, J.; and Yaghi, O.M. "Ultrahigh
 Porosity in Metal-Organic Frameworks." *Science*, 2010. **329**(5990):424–428.
 doi:10.1126/science.1192160
- 52. Wang, T.C.; Bury, W.; Gómez-Gualdrón, D.A.; Vermeulen, N.A.; Mondloch, J.E.;
 Deria, P.; Zhang, K.; Moghadam, P.Z.; Sarjeant, A.A.; and Snurr, R.Q. "Ultrahigh
 surface area zirconium MOFs and insights into the applicability of the BET theory."
 J Am Chem Soc, 2015. 137(10):3585–3591
- 53. Bobbitt, N.S.; Chen, J.; and Snurr, R.Q. "High-throughput screening of
 Metal–Organic frameworks for hydrogen storage at cryogenic temperature." J Phys
 Chem C, 2016. 120(48):27328–27341
- Liu, H.; Xu, C.; Li, D.; and Jiang, H.L. "Photocatalytic hydrogen production coupled with selective benzylamine oxidation over MOF composites." *Angew Chem*, 2018.
 130(19):5477–5481
- 55. Thommes, M.; Kaneko, K.; Neimark, A.V.; Olivier, J.P.; Rodriguez-Reinoso, F.;
 Rouquerol, J.; and Sing, K.S.W. "Physisorption of gases, with special reference to
 the evaluation of surface area and pore size distribution (IUPAC Technical Report)."
 Pure and Applied Chemistry, 2015. 87(9-10):1051–1069. doi:10.1515/pac-2014-1117
- Nelson, A.P.; Farha, O.K.; Mulfort, K.L.; and Hupp, J.T. "Supercritical Processing as a Route to High Internal Surface Areas and Permanent Microporosity in Metal-Organic Framework Materials." *Journal of the American Chemical Society*, 2009.
 131(2):458–460. doi:10.1021/ja808853q
- 57. Park, Y.K.; Choi, S.B.; Kim, H.; Kim, K.; Won, B.H.; Choi, K.; Choi, J.S.; Ahn,
 W.S.; Won, N.; and Kim, S. "Crystal structure and guest uptake of a mesoporous
 metal-organic framework containing cages of 3.9 and 4.7 nm in diameter." Angew
 Chem, Int Ed, 2007. 46(43):8230–8233
- Rouquerol, J.; Rouquerol, F.; Llewellyn, P.L.; Maurin, G.; and Sing, K. Adsorption by Powders and Porous Solids : Principles, Methodology and Applications. 2013. ISBN 978-0-08-097035-6