

# Ruthenium complex hydride catalysts as a platform for ammonia synthesis

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## Abstract

Mild-condition ammonia synthesis from  $N_2$  and  $H_2$  is a long-sought-after scientific goal and a practical need, especially for the intensively pursued “Green Ammonia” production using renewable  $H_2$ . Under this context, there have been growing interests in the development of new catalysts for effectively catalyzing  $N_2+H_2$  to  $NH_3$ . Particular attention has been given to Ru-based catalysts because they are well known to be more active at lower temperatures and pressures than non-noble-metal based catalysts. Here, we demonstrate that a series of Ru complex hydrides  $A_n[RuH_m]$ , where A is alkali or alkaline earth metal,  $n=2, 3$  or  $4$  and  $m=6$  or  $7$ , exhibit universal and high catalytic activities that far exceed the benchmark Ru metal catalysts under mild conditions. Detailed investigations on the ternary Ru complex hydride catalytic system disclose that the kinetic behaviors depend strongly on the identity of alkali or alkaline earth metal cations. In clear contrast to the closed packed Ru metal catalyst, the unique configuration and synergized scenario of the Ru complex hydride center prefer a non-dissociative mechanism for  $N_2$  activation and hydrogenation, which provides a new platform for the design and development of efficient  $NH_3$  synthesis catalysts.

## Introduction

Ammonia, as one of the most important chemicals and carbon-free energy carriers, has a worldwide production of ~180 million tons per year, and is mainly produced by the industrial Haber-Bosch (HB) process with Fe-based catalyst<sup>1</sup>.

Currently, the large-scale and centralized HB process accounts for nearly 2% of the world's consumption of fossil fuels and consequently over 1% of the global anthropogenic CO<sub>2</sub> emissions, mainly due to the fact it employs fossil-fuel sourced H<sub>2</sub> and requires harsh operating conditions (400-500 °C, 100-300 bar)<sup>2</sup>. Therefore, there is an imperative to decarbonize ammonia industry and reduce the energy cost, which spurs recent interest in finding sustainable alternatives. Establishing a CO<sub>2</sub>-free, flexible-scale, distributed process capable of coping with the intermittent and variable renewable energy supplies may open a range of opportunities for the second ammonia revolution<sup>3</sup>.

As the electric power generated from renewable energy sources becomes more technically and economically viable, nowadays much efforts have been placed on the electrolysis Haber-Bosch process (*e*HB), where renewable electricity is used to electrolyze H<sub>2</sub>O to produce H<sub>2</sub>, separate N<sub>2</sub> from air and power the N<sub>2</sub>+H<sub>2</sub> to NH<sub>3</sub>, etc<sup>4-5</sup>. To improve its compatibility with the renewable electricity as well as to reduce the energy cost, the *e*HB process generally requires an active catalyst that can operate at lower pressures (< 50 bar) and lower temperatures (< 673 K)<sup>6</sup>. It is well known that Ru is more active than Fe under milder reaction conditions. However, the high kinetic barrier for N<sub>2</sub> direct dissociation and the severe poisoning effect of hydrogen on Ru metal surface render efficient NH<sub>3</sub> synthesis under lower temperatures (< 623 K) unattainable<sup>7</sup>. Under this scenario, new Ru based catalytic systems have been intensively explored in recent years, aiming at facilitating ammonia synthesis under mild conditions. For example, advanced materials such as electrides<sup>8</sup>, hydrides<sup>9-11</sup>, amides<sup>12-13</sup>, reducible metal oxides<sup>14-15</sup> have been developed as functional supports of Ru metal catalysts, which can strongly enrich the electron density of Ru and thus promote the cleavage of N<sub>2</sub> to form NH<sub>3</sub> on Ru metal surface under pressures below 5 MPa and temperatures below 673 K.

We recently reported that ruthenium complex hydrides Li<sub>4</sub>RuH<sub>6</sub> and Ba<sub>2</sub>RuH<sub>6</sub>, as an entirely new class of ammonia synthesis catalysts, performs extraordinarily well under more benign conditions (< 573 K, 1 MPa). The key to achieve efficient

ammonia synthesis under mild conditions lies in the unique configuration and function mechanism of the complex hydride center, which is clearly different from the Ru metal based catalysts. For ternary complex hydride catalyst  $\text{Li}_4\text{RuH}_6$  or  $\text{Ba}_2\text{RuH}_6$ , Ru is in an ionic state coordinated with Li(Ba) and H, and  $\text{N}_2$  undergoes non-dissociative hydrogenolysis over electron-rich  $[\text{RuH}_6]^{4-}$  complex center with the aid of surrounding Li/Ba cations and hydridic hydrogens ( $\text{H}^-$ ). Besides  $\text{Li}_4\text{RuH}_6$  and  $\text{Ba}_2\text{RuH}_6$ , there are abundant solid-state complex hydrides composed of various transition metal (TM) elements and alkali or alkali-earth (A) elements<sup>16</sup>. In the simplest compositions of these systems, all hydrogen atoms are bonded to the TM center giving the general chemical formula  $\text{A}_n^{\delta+}[\text{TMH}_m]^{\delta-}$  ( $m, n, \delta = 1, 2, 3 \dots$ ), where the homoleptic, anionic TM-hydrido complexes  $[\text{TMH}_m]^{\delta-}$  are stabilized by charge transfer from the surrounding alkali or alkali earth cations  $\text{A}^{\delta+}$ . In homogeneous  $\text{N}_2$  fixation, it is well known that molecular TM hydride complexes, with the hydride ligands being the source of both electron and proton, serves as a common platform for  $\text{N}_2$  activation<sup>17-18</sup>. In analogy to the configuration of molecular TM hydride complexes, the solid-state TM complex hydrides also show a lack of TM-TM bond and a plenty of electron-rich hydrido hydrogens, which might create a suitable structure and reacting environment for non-dissociative  $\text{N}_2$  activation and hydrogenation. In this work, ternary Ru complex hydride series, as one of the most well-characterized complex hydrides, was chosen as the typical representative to demonstrate the potency of complex hydrides in  $\text{N}_2$  fixation.

The open question here is whether other alkali or alkaline earth metal based ruthenium hydrides, such as  $\text{Ca}_2\text{RuH}_6$ ,  $\text{Na}_4\text{RuH}_6$  and  $\text{K}_3\text{RuH}_7$ , would resemble  $\text{Li}_4\text{RuH}_6$  or  $\text{Ba}_2\text{RuH}_6$  to achieve high catalytic performance for mild-condition ammonia synthesis, and whether a general approach for effective catalysis can be derived from the understanding of the cooperation and synergy of the Ru complex hydride center. This report starts with a systematical analysis on the structural and electronic configurations as well as the thermodynamic properties of the ternary Ru complex hydride series. Then, we demonstrate that these ternary complex hydrides

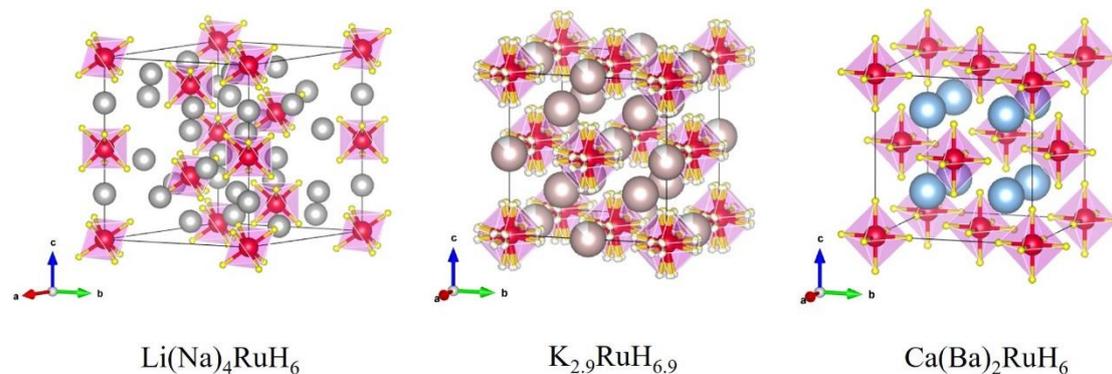
are chemically stable under ammonia synthesis conditions, and all studied complex hydrides can show superior performances under mild conditions when the ternary hydride sites are effectively exposed. Furthermore, the kinetic behaviors of these ternary complex hydride catalysts vary depending on the identity of the alkali or alkaline earth cations, but all of them show a balanced affinity towards H<sub>2</sub> and NH<sub>3</sub>, which provides a favorable scenario for effective ammonia synthesis. The catalytic reaction mechanism derived from the ternary ruthenium complex hydride catalysts are clearly different from that of the Ru metal based catalysts, and therefore provides a new strategy for the design and development of efficient NH<sub>3</sub> synthesis catalysts.

## Results and discussion

Ternary ruthenium complex hydrides have the general composition of A<sub>n</sub><sup>δ+</sup>[RuH<sub>m</sub>]<sup>δ-</sup> (A=Li, Na, K, Ca or Ba etc.; m=6 or 7; n=2, 3 or 4; δ=1, 2 or 3), where the [RuH<sub>m</sub>]<sup>δ-</sup> complex anions sit inside the framework of alkali or alkaline earth metal cations<sup>16, 19-20</sup>. These ternary complex hydrides are generally synthesized via reacting Ru metal and AH under pressurized hydrogen and elevated temperatures. As shown in Table 1, the crystal structure of Li<sub>4</sub>RuH<sub>6</sub> or Na<sub>4</sub>RuH<sub>6</sub> was determined to crystallize in the rhombohedral space group *R-3c*, while the K<sub>2.9</sub>RuH<sub>6.9</sub> (~K<sub>3</sub>RuH<sub>7</sub>), Ca<sub>2</sub>RuH<sub>6</sub> or Ba<sub>2</sub>RuH<sub>6</sub> was found to crystallize in the cubic space group *Fm-3m*. These Ru complex hydrides, with isolated [RuH<sub>m</sub>]<sup>δ-</sup> anions linked by alkali or alkaline earth metal cations, generally have a Ru-Ru distance higher than 4.99 Å, which is distinctly different from the closely packed Ru metal surface that has Ru-Ru distance of 2.71 Å. The Bader charge analyses of these ternary Ru complex hydrides reveal that alkali or alkaline earth atoms donate their electrons to [RuH<sub>m</sub>] becoming cations, where Ru atoms exhibit a partial defective charge state and H atoms are present in a partial hydrido form<sup>21</sup>. Given that the bonding in the A<sub>n</sub>RuH<sub>m</sub> series contains a strong ionic component, these Ru complex hydrides can be classified as mixed ionic-covalent bonding compounds.

**Table 1.** Properties of Ru complex hydrides including the space group, the lattice parameter of deuterides, the equatorial Ru-D bond distance, the Ru-Ru distance, the IR vibrational Ru-H stretching mode, the Bader's charges of Ru atom determined by AIM method,  $\Delta H$  of

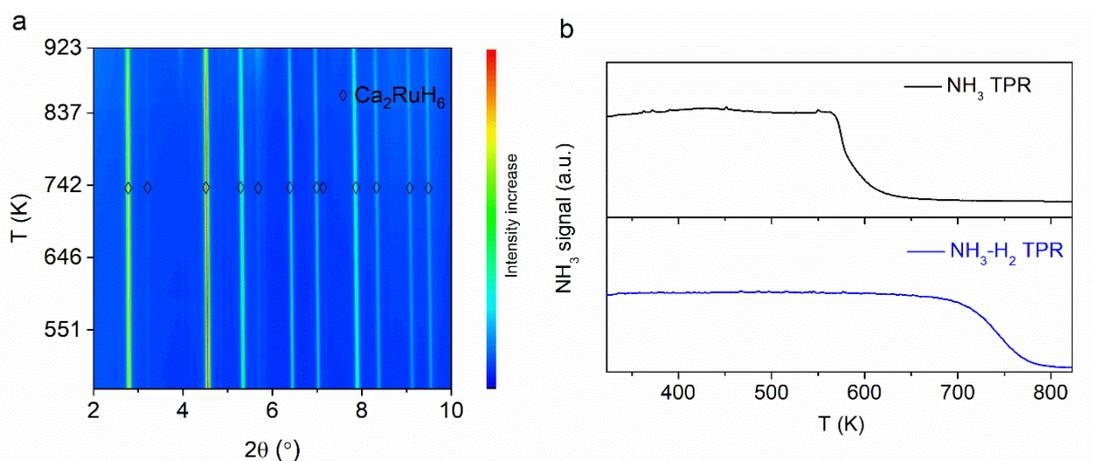
decomposition of the complex hydride ( $\Delta H_d$ ) via the reaction  $A_nRuH_m$  (solid)  $\rightarrow$  A or AH (solid) + Ru (solid) +  $H_2$  (gas) (see Table S1), and the corresponding decomposition temperatures ( $T_d$ ). The schematic crystal structures of  $Li(Na)_4RuH_6$ ,  $Ca(Ba)_2RuH_6$  and  $K_{2.9}RuH_{6.9}$  are shown above the table. The Ru, H, Li(Na), K and Ca(Ba) atoms are presented by red, yellow, light grey, light pink and light blue balls.



	Space group	Lattice parameter of deuteride (a, Å)	Ru-D bond distance (Å)	Ru-Ru distance (Å)	$\nu(Ru-H)$ ( $cm^{-1}$ )	Bader charge of Ru ( $\Delta q_{AIM}$ )	$\Delta H_d$ (kJ/mol $H_2$ )	$T_d$ (K)
$Li_4RuH_6$	$R-3c$	8.1663	1.7144	4.9994	1527	+0.45	93.1	840
$Na_4RuH_6$	$R-3c$	9.1449	1.7912	5.6780	---	+0.26	101.9	945
$K_{2.9}RuH_{6.9}$ ( $\sim K_3RuH_7$ )	$Fm-3m$	8.4539	1.6806	5.9778	---	---	85.8	855
$Ca_2RuH_6$	$Fm-3m$	7.2214	1.7001	5.1063	1559	-0.08	175.0	1425
$Ba_2RuH_6$	$Fm-3m$	8.0166	1.7236	5.6886	1438	0.08	154.7	1305

Thermodynamic analyses show that, analogous to the previously reported  $Li_4RuH_6$  and  $Ba_2RuH_6$ ,  $Ca_2RuH_6$ ,  $Na_4RuH_6$  and  $K_3RuH_7$  also have large enthalpy changes in hydrogen desorption, and only at high temperatures would they decompose to Ru and the corresponding A or AH (Table 1 and Table S1), which indicates that all studied Ru complex hydrides here have high thermal stabilities. Taking the facilely prepared  $Ca_2RuH_6$  as an example, the stability of the ternary Ru complex hydride under ammonia synthesis conditions was investigated in detail. The *in situ* SR-PXD characterization reveals that the ternary hydride remains the dominant phase until 923 K under  $N_2+3H_2$  of atmospheric pressure (Fig. 1a). The TPR-MS results show that  $Ca_2RuH_6$  is also resistant to diluted  $NH_3$  at temperatures below 570 K. After

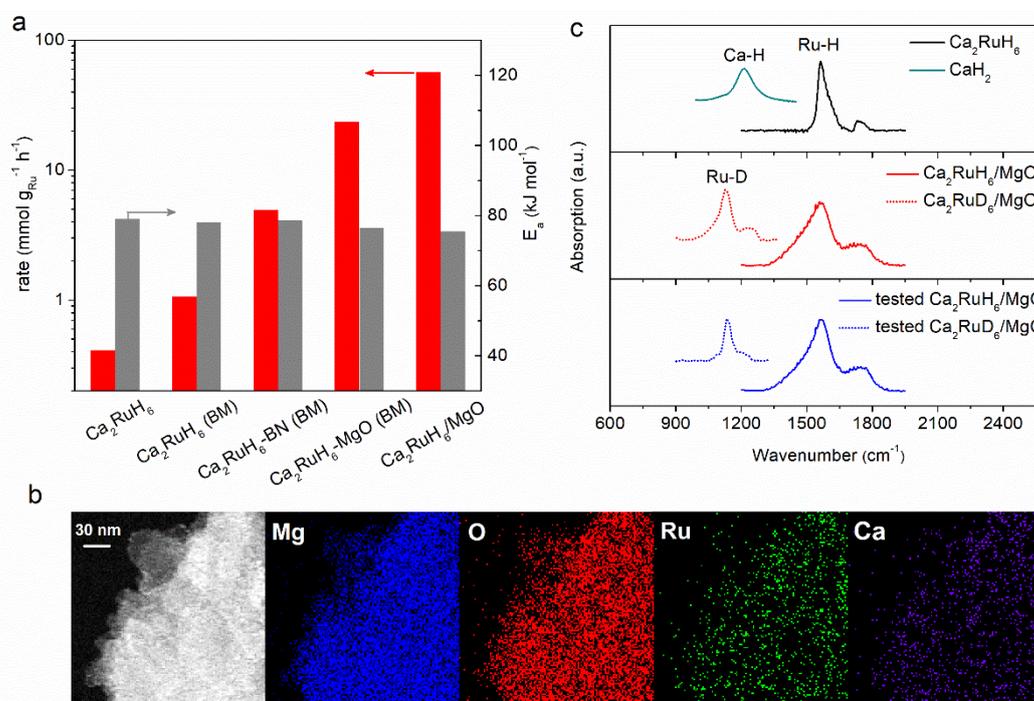
introducing H<sub>2</sub> into the diluted NH<sub>3</sub>, the Ca<sub>2</sub>RuH<sub>6</sub> phase remains stable up to 700 K (Fig. 1b). These experimental findings demonstrate that the bulk Ca<sub>2</sub>RuH<sub>6</sub> would stay stable under the ammonia synthesis conditions applied in this study (operation temperature from 473 K to 623 K, H<sub>2</sub> partial pressure from 0.4 to 7.5 bar).



**Fig. 1 a**, *In situ* SR-XRD characterization of Ca<sub>2</sub>RuH<sub>6</sub> sample under atmospheric N<sub>2</sub>-3H<sub>2</sub> and elevated temperatures (from 473 K to 923 K); **b**, TPR-MS profiles of Ca<sub>2</sub>RuH<sub>6</sub> in a diluted NH<sub>3</sub> gas (NH<sub>3</sub>:Ar=0.5:99.5) and a diluted NH<sub>3</sub>-H<sub>2</sub> mixture gas (NH<sub>3</sub>:H<sub>2</sub>:Ar=0.5:75:24.5).

We then performed activity test on the as-prepared bulk phase Ca<sub>2</sub>RuH<sub>6</sub> sample of an average crystalline size of ca. 60 nm. As shown in Fig. 2a, the Ca<sub>2</sub>RuH<sub>6</sub> sample exhibits an activity of ca. 0.4 mmol g<sub>Ru</sub><sup>-1</sup> h<sup>-1</sup> (or 0.22 mmol g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup>) at 1 bar and 573 K. Cracking the Ca<sub>2</sub>RuH<sub>6</sub> sample through ball-milling treatment can double its reaction rates. To further reduce its particle size as well as increase its surface area, we then ball-milled the Ca<sub>2</sub>RuH<sub>6</sub> sample with inert dispersers, such as BN and MgO. As shown in Fig. S1, ball milling the Ca<sub>2</sub>RuH<sub>6</sub> sample with BN and MgO can reduce the crystalline size of Ca<sub>2</sub>RuH<sub>6</sub> from ca. 60 nm to ca. 25 nm and 13 nm, respectively. As expected, the ammonia synthesis rates increase gradually with the decreasing crystalline size. The as-prepared Ca<sub>2</sub>RuH<sub>6</sub>-BN(BM) and Ca<sub>2</sub>RuH<sub>6</sub>-MgO(BM) samples outperform the bulk Ca<sub>2</sub>RuH<sub>6</sub> by 12 times and 57 times, respectively (Fig. 2a). We thus employed MgO as support and synthesized the supported Ca<sub>2</sub>RuH<sub>6</sub>/MgO catalyst. The as-prepared Ca<sub>2</sub>RuH<sub>6</sub>/MgO sample, with a Ru content of ca. 9.0 wt%, shows ca. 140-fold increase in activity from the bulk phase Ca<sub>2</sub>RuH<sub>6</sub>, but has a similar apparent activation energy of ca. 75 kJ mol<sup>-1</sup> as other Ca<sub>2</sub>RuH<sub>6</sub>-based catalysts (Fig. 2a and fig.

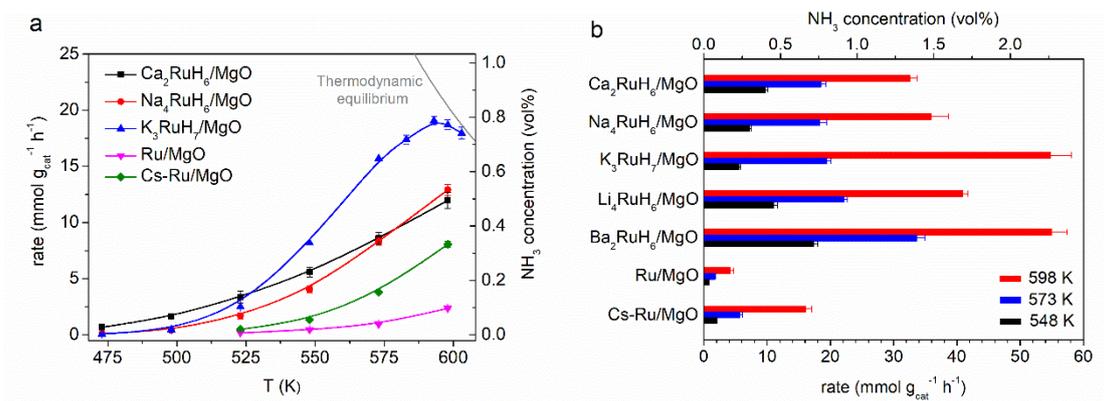
S2), showing the effective exposure of ternary hydride active sites in the supported catalyst. The STEM-EDS maps of the supported sample reveal that Ca and Ru are in proximity and dispersed evenly over the MgO support (Fig. 2b). Moreover, the  $\text{Ca}_2\text{RuH}_6/\text{MgO}$  sample has a similar Ru-H stretching band (peak frequency:  $1570\text{ cm}^{-1}$ ) as that of bulk  $\text{Ca}_2\text{RuH}_6$  sample, which is further confirmed by Ru-D stretching band (peak frequency:  $1120\text{ cm}^{-1}$ ) in the deuterated sample (Fig. 2c). The tested  $\text{Ca}_2\text{RuH}_6/\text{MgO}$  sample also exhibits similar Ru-H stretching vibration as that of bulk  $\text{Ca}_2\text{RuH}_6$  and that of fresh  $\text{Ca}_2\text{RuH}_6/\text{MgO}$  (Fig. 2c), which demonstrates that the ternary hydride active sites remain stable under the reaction conditions.



**Fig. 2.** **a**, Activities of  $\text{Ca}_2\text{RuH}_6$ -based catalysts at 573 K and the corresponding activation energies (Reaction conditions: catalyst loading 30 mg,  $\text{N}_2:\text{H}_2=1:3$ , flow rate  $30\text{ ml min}^{-1}$ , and 1 bar); **b**, STEM and elemental mapping images of  $\text{Ca}_2\text{RuH}_6/\text{MgO}$  sample; **c**, FT-IR spectra of  $\text{Ca}_2\text{RuH}_6$ ,  $\text{CaH}_2$ ,  $\text{Ca}_2\text{RuH(D)}_6/\text{MgO}$  and tested  $\text{Ca}_2\text{RuH(D)}_6/\text{MgO}$  (Test conditions:  $\text{N}_2:\text{H}_2(\text{D}_2)=1:3$ , 20 bar and 673 K).

Following a similar approach, other supported ternary complex hydride catalysts  $\text{Na}_4\text{RuH}_6/\text{MgO}$ ,  $\text{K}_3\text{RuH}_7/\text{MgO}$  were also synthesized, which possess the characteristic features of the corresponding bulk-phase ternary complex hydrides (Fig. S3). With an effective exposure of the ternary hydride active sites, these supported ternary hydride

catalysts show universal high activities, which outperform the Cs-promoted Ru catalyst (Cs-Ru/MgO), one of the most-active NH<sub>3</sub> synthesis catalysts, by 3-6 times at 573 K and 3-16 times at 523 K (Fig. S4). Increasing the N<sub>2</sub> partial pressure of the syngas can further enhance the performance of these ternary complex hydride catalysts. As shown in Fig. S5, the optimal molar ratio of N<sub>2</sub> and H<sub>2</sub> was found to be ca. 3:2. Under a N<sub>2</sub>:H<sub>2</sub> ratio of 3:2 and atmospheric pressure, the K<sub>3</sub>RuH<sub>7</sub>/MgO catalyst exhibits higher catalytic activity than Na<sub>4</sub>RuH<sub>6</sub>/MgO and Ca<sub>2</sub>RuH<sub>6</sub>/MgO catalysts at temperatures higher than 530 K, and the NH<sub>3</sub> concentration formed above 593 K can reach thermodynamic equilibrium even at a space velocity as high as 60000 ml g<sup>-1</sup> h<sup>-1</sup>; the Ca<sub>2</sub>RuH<sub>6</sub>/MgO catalyst functions well at lower temperatures, which outperforms the K<sub>3</sub>RuH<sub>7</sub>/MgO and Na<sub>4</sub>RuH<sub>6</sub>/MgO catalysts by nearly an order of magnitude at 473 K (Fig. 3a). The catalytic performances of these supported ternary complex hydride catalysts got further improved as the reaction pressure increased. Comparatively, under a total pressure of 10 bar and at temperatures above 573 K, the activities of these supported Ru complex hydride catalysts are ranked in the order of K<sub>3</sub>RuH<sub>7</sub>/MgO ≈ Ba<sub>2</sub>RuH<sub>6</sub>/MgO > Li<sub>4</sub>RuH<sub>6</sub>/MgO > Na<sub>4</sub>RuH<sub>6</sub>/MgO > Ca<sub>2</sub>RuH<sub>6</sub>/MgO; while at temperatures below 573 K, the activity order is Ba<sub>2</sub>RuH<sub>6</sub>/MgO > Li<sub>4</sub>RuH<sub>6</sub>/MgO > Ca<sub>2</sub>RuH<sub>6</sub>/MgO > Na<sub>4</sub>RuH<sub>6</sub>/MgO > K<sub>3</sub>RuH<sub>7</sub>/MgO (Fig. 3b). What' more, all ternary complex hydride catalysts investigated here considerably outperform most of recently reported Ru-based catalysts especially under mild reaction conditions (Table S2). It is worth noting that if these supported ternary complex hydride samples are oxidized and deactivated in air before reaction, their activities drop significantly to the level of Ru/MgO or Cs-Ru/MgO samples (Fig. S6), which demonstrates that the ternary hydride form is of critical importance for efficient catalysis.



**Fig. 3.** **a**, Temperature-dependent  $\text{NH}_3$  synthesis rates and corresponding effluent  $\text{NH}_3$  concentration of supported ternary Ru complex hydride catalysts ( $\text{Ca}_2\text{RuH}_6/\text{MgO}$ ,  $\text{Na}_4\text{RuH}_6/\text{MgO}$  and  $\text{K}_3\text{RuH}_7/\text{MgO}$ ) and Ru metal based catalysts ( $\text{Ru}/\text{MgO}$  and  $\text{Cs-Ru}/\text{MgO}$ ) at 1 bar (Reaction conditions: catalyst loading, 30 mg,  $\text{N}_2:\text{H}_2=3:2$ , flow rate  $30 \text{ ml min}^{-1}$ ); **b**,  $\text{NH}_3$  synthesis rates and corresponding effluent  $\text{NH}_3$  concentration of supported ternary Ru complex hydride catalysts ( $\text{Ca}_2\text{RuH}_6/\text{MgO}$ ,  $\text{Na}_4\text{RuH}_6/\text{MgO}$ ,  $\text{K}_3\text{RuH}_7/\text{MgO}$ ,  $\text{Li}_4\text{RuH}_6/\text{MgO}$  and  $\text{Ba}_2\text{RuH}_6/\text{MgO}$ ) and Ru metal based catalysts ( $\text{Ru}/\text{MgO}$  and  $\text{Cs-Ru}/\text{MgO}$ ) at 10 bar (The reaction conditions are the same as **a**).

The kinetic parameters of the supported ternary complex hydride catalysts and the reference Ru metal-based catalysts are summarized in Table 2 and Fig. S7. As we can see, the kinetic behaviors of these ternary complex hydride catalysts are closely correlated with the identity of alkali or alkaline earth cations. Generally, the  $\text{Ca}_2\text{RuH}_6/\text{MgO}$ ,  $\text{Li}_4\text{RuH}_6/\text{MgO}$  or  $\text{Ba}_2\text{RuH}_6/\text{MgO}$  catalysts exhibits smaller apparent activation energies ( $E_a$ ) than the Ru metal catalysts, thus enabling these ternary complex hydride catalysts particularly effective at relatively lower temperatures. While the apparent activation energies of  $\text{Na}_4\text{RuH}_6/\text{MgO}$  or  $\text{K}_3\text{RuH}_7/\text{MgO}$  catalysts are close to or even higher than that of the Ru metal catalysts, allowing them to achieve high activities at relatively higher temperatures. Moreover, the  $\text{N}_2$  orders for all ternary complex hydride catalysts are close to 1. The  $\text{Ca}_2\text{RuH}_6/\text{MgO}$ ,  $\text{Li}_4\text{RuH}_6/\text{MgO}$  or  $\text{Ba}_2\text{RuH}_6/\text{MgO}$  catalysts have positive reaction orders with respect to  $\text{H}_2$ , in clear contrast to the Ru metal based catalysts who have negative  $\text{H}_2$  reaction orders that are close to -1, suggesting that ammonia synthesis over these ternary complex hydrides is free from hydrogen poisoning. Although the  $\text{H}_2$  orders of  $\text{Na}_4\text{RuH}_6/\text{MgO}$  and  $\text{K}_3\text{RuH}_7/\text{MgO}$  catalysts are negative, they are still higher than that of the Ru metal based catalysts, showing a less inhibiting effect of adsorbed H on the surface of these ternary complex hydrides. The reaction orders of  $\text{NH}_3$  for all ternary

complex hydride catalysts are negative, indicating the inhibiting effect of NH<sub>3</sub>. Another prominent kinetic feature of this new class of ternary complex hydride catalysts is the balanced affinity towards H<sub>2</sub> and NH<sub>3</sub>, i.e. when the NH<sub>3</sub> inhibiting effect on the ternary hydride surface gets weakened, the H<sub>2</sub> inhibiting effect get strengthened. Such a characteristic strikes a balance between the rates of dissociative adsorption of H<sub>2</sub> and the rates of associative desorption of NH<sub>3</sub>, allowing all ternary complex hydride catalysts to exhibit superior mild-condition activities.

**Table 2.** Kinetic parameters of the supported ternary Ru complex hydride catalysts and reference Ru metal catalysts.

Catalyst	Reaction order <sup>a</sup>			E <sub>a</sub> (kJ mol <sup>-1</sup> )
	$\alpha(\text{NH}_3)$	$\beta(\text{N}_2)$	$\gamma(\text{H}_2)$	
Ca <sub>2</sub> RuH <sub>6</sub> /MgO	-0.57	0.94	0.26	75.4 (473-573 K)
Na <sub>4</sub> RuH <sub>6</sub> /MgO	-0.29	0.92	-0.32	115.4 (473-573 K)
K <sub>3</sub> RuH <sub>7</sub> /MgO	-0.36	1.17	-0.53	139.7 (473-573 K)
Li <sub>4</sub> RuH <sub>6</sub> /MgO	-0.59	0.91	0.30	71.2 (523-598 K)
Ba <sub>2</sub> RuH <sub>6</sub> /MgO	-0.63	0.92	1.00	63.9 (523-598 K)
Ru/MgO	-0.24	1.12	-0.86	94.8 (523-598 K)
Cs-Ru/MgO	-0.09	1.01	-0.82	112.4 (523-598 K)

<sup>a</sup>Reaction conditions: catalyst loading 30 mg, pressure 1 bar and temperature 573 K.

As reported by our previous studies <sup>22</sup>, a different reaction mechanism towards NH<sub>3</sub> formation over the lithium-ruthenium ternary hydride catalyst was demonstrated, in which N<sub>2</sub> undergoes non-dissociative hydrogenolysis over the electron-rich [RuH<sub>m</sub>] centers by the involvement of hydridic hydrogens in mediating electron and proton transfers and Li cations in co-stabilizing N<sub>x</sub>H<sub>y</sub> intermediate species. The unique configuration of the ternary complex hydride center allows all its components collaboratively involved in the catalysis, which creates an energetically more favorable pathway for N<sub>2</sub> activation and hydrogenation and thus endows superior

ammonia formation rates under mild conditions. Such a unique reaction mechanism might also hold true for barium/calcium/sodium/potassium-ruthenium hydride catalysts for the following reasons: 1) they share similar configurations with lithium-ruthenium hydride, where the H-rich  $[\text{RuH}_m]$  anions sit inside the framework of A cations with a Ru-Ru distance higher than 5 Å, favoring a cation-mediated non-dissociative reduction mechanism; 2) Ru in these ternary hydride compounds is in an ionic state and coordinated with multiple hydridic hydrogens, all creating an electron-rich environment for  $\text{N}_2$  reduction. Nonetheless, the change of alkali cation still has certain effect on the electronic and structural properties of ternary complex hydride surface, which further affects its affinity towards  $\text{N}_2$ ,  $\text{H}_2$ ,  $\text{NH}_3$  and some  $\text{N}_x\text{H}_y$  intermediates and hence causes changes in the macrokinetic behaviors mentioned above. We speculated that, on Li-Ru or Ca-Ru complex hydride surface, Li or Ca cations prefer to stabilizing  $\text{N}_2\text{H}_x$  ( $x=0, 1, 2, 3$ ) species on  $[\text{RuH}_m]$  center, thus reducing the barrier for  $\text{N}_2$  hydrogenation and facilitating  $\text{NH}_3$  formation at low temperatures; on K-Ru and Na-Ru complex hydride surface, K and Na cations have more benefits for destabilizing  $\text{NH}_x$  ( $x=1, 2, 3$ ) species on  $[\text{RuH}_m]$  center, thus promoting the desorption of  $\text{NH}_3$  product and increasing the reaction rates at high temperatures or high ammonia concentration; while on Ba-Ru complex hydride surface, Ba cations help to maintain a balance between  $\text{N}_2$  hydrogenation and  $\text{NH}_3$  desorption over  $[\text{RuH}_m]$  center, thus enabling better performance in the whole range of test temperature.

Hydrogenolysis of  $\text{N}_2$  to  $\text{NH}_3$  using  $\text{H}_2$  as the thermodynamically ideal reductant via concerted N-N weakening and N-H formation is an effective approach for mild-condition ammonia synthesis, as well as a scientific goal actively pursued in  $\text{N}_2$  fixation for more than half a century<sup>18</sup>. The non-dissociative  $\text{N}_2$  activation on a heterogeneous TM surface has been discussed before but was later found to be energetically unfavorable<sup>23-24</sup>. While for the well-defined TM hydride complex systems, until now only a few metallic polyhydride complexes have been reported to be capable of activating  $\text{N}_2$  and hydrogenating it to imido/amido units, but no

ammonia was formed<sup>25-28</sup>. The solid-state ternary ruthenium complex hydride series presented here may serve as the first complex compound catalysts that can achieve the non-dissociative hydrogenolysis of N<sub>2</sub> to NH<sub>3</sub>, which sets up a bridge linking research endeavor from heterogeneous and homogeneous nitrogen fixation. Based on the understanding of the synergized scenario over ternary complex hydride active center, we propose that, in the heterogeneous catalysis regime, creating a multi-component and electron-rich catalytic center might be more favorable for non-dissociative N<sub>2</sub> activation and hydrogenation under mild conditions, since the dynamic and synergistic engagement of all the components may contribute to manipulating the energetics of elementary steps with multi-degree of freedom, and thus allow a reaction pathway with suitable energetics for effective hydrogenolysis of N<sub>2</sub> to NH<sub>3</sub>.

### **Conclusion**

In summary, a series of ternary ruthenium complex hydride catalysts was demonstrated to function as efficient catalysts for mild-condition ammonia synthesis, where the ternary complex hydride itself forms a powerful active center and exerts a distinct pathway to facilitate the non-dissociative N<sub>2</sub> reduction to NH<sub>3</sub>. The present study not only makes a significant step towards the long-sought scientific goal, mild-condition catalytic ammonia synthesis, but also demonstrates the power of multi-component and electron-rich catalytic center to tackle the activation and conversion of inert molecules. What's more, it initiates complex hydrides as heterogeneous catalysts for the conversion of kinetically stable molecules, further unveiling the power of hydrides in catalysis.

## Experimental Details

### Materials and Catalyst Preparation.

**Preparation of bulk ternary ruthenium complex hydride samples.**  $\text{Li}_4\text{RuH}_6$ ,  $\text{Na}_4\text{RuH}_6$ ,  $\text{K}_3\text{RuH}_7$ ,  $\text{Ba}_2\text{RuH}_6$  and  $\text{Ca}_2\text{RuH}_6$  samples were synthesized by the calcination of ball-milled mixtures of Ru powder (Aladdin, 99.99% metals basis) with LiH (Alfa, 99.4%), NaH (Aladdin, 90%), KH (Aladdin, 30% dispersion in mineral oil),  $\text{BaH}_2$  and  $\text{CaH}_2$  (Alfa, 97%) at elevated temperatures and pressures, as has been described in earlier reports<sup>20, 29-31</sup>. The maximum reaction pressure and temperature of our in-house built autoclaves are 50 bar and 973 K. Under the limiting conditions of the autoclave, the  $\text{Na}_4\text{RuH}_6$  and  $\text{K}_3\text{RuH}_7$  can only be partially synthesized, which still have a certain amount of unreacted NaH/KH and Ru. Therefore, the as-prepared  $\text{Na}_4\text{RuH}_6$  and  $\text{K}_3\text{RuH}_7$  in this study were denoted as  $\text{Na}_4\text{RuH}_6^*$  and  $\text{K}_3\text{RuH}_7^*$ , respectively.  $\text{BaH}_2$  was obtained following the procedure described previously<sup>32</sup>.

**Preparation of ball milled  $\text{Ca}_2\text{RuH}_6$ -based samples.**  $\text{Ca}_2\text{RuH}_6$  (BM),  $\text{Ca}_2\text{RuH}_6$ -BN (BM) and  $\text{Ca}_2\text{RuH}_6$ -MgO (BM) samples were prepared via ball milling  $\text{Ca}_2\text{RuH}_6$  itself,  $\text{Ca}_2\text{RuH}_6$  and BN (Aladdin, 98.5%, 1  $\mu\text{m}$ ),  $\text{Ca}_2\text{RuH}_6$  and MgO in a  $\text{H}_2$ -filled vessel on a Retsch planetary ball mill (PM 400, Germany) at 150 r.p.m. for 3 h. The Ru content of  $\text{Ca}_2\text{RuH}_6$ -BN (BM) or  $\text{Ca}_2\text{RuH}_6$ -MgO (BM) sample is ca. 9.0 wt%. The MgO sample has a high specific surface area of ca. 534  $\text{m}^2 \text{g}^{-1}$ , which was synthesized according to the literature report<sup>33</sup>.

**Preparation of supported Ru metal based catalysts and supported ternary ruthenium complex hydride catalysts.** Two Ru/MgO catalysts with Ru contents of 8.7 wt% and 15 wt%, Cs-Ru/MgO catalyst with a Ru content of 7.3 wt%,  $\text{Li}_4\text{RuH}_6$ /MgO catalyst with a Ru content of 8.0 wt%, and  $\text{Ba}_2\text{RuH}_6$ /MgO catalyst with a Ru content of 5.0 wt% were prepared according to the procedure described in our previous report<sup>22</sup>.  $\text{Na}_4\text{RuH}_6$ /MgO,  $\text{K}_3\text{RuH}_7$ /MgO and  $\text{Ca}_2\text{RuH}_6$ /MgO catalysts were prepared in a similar way, except impregnating the Ru/MgO (8.7 wt% Ru/MgO for  $\text{Na}_4\text{RuH}_6$ /MgO and  $\text{K}_3\text{RuH}_7$ /MgO, 15 wt% Ru/MgO for  $\text{Ca}_2\text{RuH}_6$ /MgO) in the sodium-ammonia solution with a molar ratio of Na:Ru=4:1, potassium-ammonia

solution with a molar ratio of K:Ru=1:1, and calcium-ammonia solution with a molar ratio of Ca:Ru=6.5:1, respectively. The corresponding deuteride samples were obtained following the similar approach, except reduction in pure D<sub>2</sub> instead of H<sub>2</sub>.

**Characterization.** Fourier transform infrared (FT-IR) measurements were conducted on a Bruker Tensor II unit with a scan resolution of 4 cm<sup>-1</sup> and an accumulation of 32 scans each time. Powder X-ray diffraction (PXRD) patterns were recorded on a PANalytical X'pert diffractometer using a homemade cell covered with KAPTON film to avoid air and moisture contamination. *In situ* synchrotron radiation powder X-ray diffraction (SR-PXD) experiments were performed at the diffraction beamline P.02.1, DESY (Hamburg, Germany). The experimental procedure in detail was described in our previous study<sup>22</sup>. The Ca<sub>2</sub>RuH<sub>6</sub> sample was heated from 298 to 923 K with a ramping rate of 6 K min<sup>-1</sup> in a steam of flow gas (N<sub>2</sub>:H<sub>2</sub>=1:3, 5 ml min<sup>-1</sup>). The 2D images were then integrated using FIT2D software. Temperature-programmed reaction (TPR) measurements were conducted in a quartz-lined stainless steel reactor and the exhaust gases were monitored with an on-line mass spectroscopy (MS, Hiden HPR20). Samples (30 mg) were heated in a stream of specific gas (30 ml min<sup>-1</sup>) from room temperature to desired temperatures at a ramping rate of 5 K min<sup>-1</sup>. The morphology and composition of the catalyst were investigated using high angle annular dark field scanning transmission electron microscopy (HAADF-STEM, JEOL JEM-ARM200F) with an energy-dispersive X-ray spectrometer (EDX).

**Catalyst activity Test.** Ammonia synthesis was conducted in a stainless steel fixed-bed reaction with a quartz liner that operated with the supply of continuous-flow of extra pure N<sub>2</sub>-H<sub>2</sub> mixture gas (>99.9999%). Typically, 30 mg of catalyst was loaded in the liner tube on a bed of quartz wool and subsequently heated at a ramping rate of 5 K min<sup>-1</sup> under the given pressure and flow rate. The ammonia produced was trapped in a diluted sulfuric acid solution and the proton conductivity was recorded with time by a conductivity meter. The principle of the NH<sub>3</sub> quantification method has been described previously<sup>34</sup>. The activity data at each temperature was monitored when the catalytic performance reached a steady-state value. Blank test using the

same setup did not give any measurable activity at temperatures below 673 K and 10 bar.

**Kinetic studies.** The measurements of reaction order of N<sub>2</sub> or H<sub>2</sub> were carried out with a flow of mixed gas (N<sub>2</sub>, H<sub>2</sub> and Ar) under conditions (573 K, 1 bar, WHSV=60000 ml g<sup>-1</sup> h<sup>-1</sup>), where the effluent NH<sub>3</sub> concentration was kept constant. Our measurement conditions were far from equilibrium considering that the thermodynamic limit is ca. 2.1% under these conditions. The loading amount is 30 mg for Ca<sub>2</sub>RuH<sub>6</sub>/MgO, Na<sub>4</sub>RuH<sub>6</sub>/MgO and K<sub>3</sub>RuH<sub>7</sub>/MgO. The gas compositions of N<sub>2</sub>:H<sub>2</sub>:Ar were 5:50:45, 15:50:35, 25:50:25, 35:50:15, 45:50:5 for determining the N<sub>2</sub> order, and 20:40:40, 20:50:30, 20:60:20, 20:80 for determining the H<sub>2</sub> order, respectively. The NH<sub>3</sub> order was determined by changing the flow rate of syngas while keeping a constant N<sub>2</sub> to H<sub>2</sub> partial pressure. Apparent activation energies were measured under atmospheric syngas (H<sub>2</sub>:N<sub>2</sub>=3) with a flow rate of 30 ml min<sup>-1</sup>. The temperature range is 473-573 K for Ca<sub>2</sub>RuH<sub>6</sub>/MgO, Na<sub>4</sub>RuH<sub>6</sub>/MgO and K<sub>3</sub>RuH<sub>7</sub>/MgO.

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## Author contributions

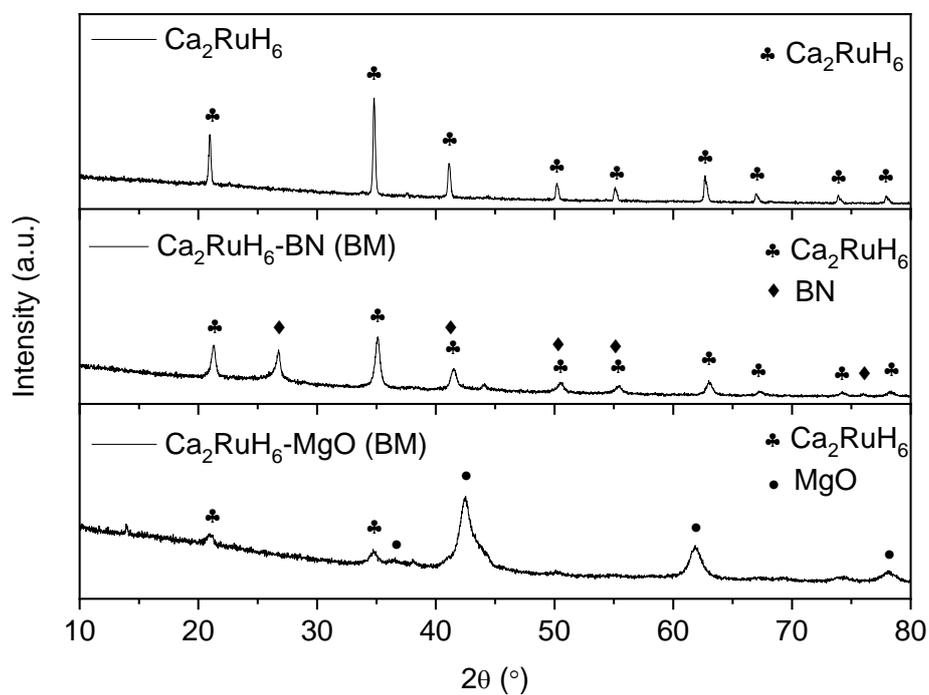
P. C. conceived the idea and supervised the research and wrote the paper. Q.W. conducted the experimental work. J.G. supervised the experimental work. All authors

participated the discussion and data analyses.

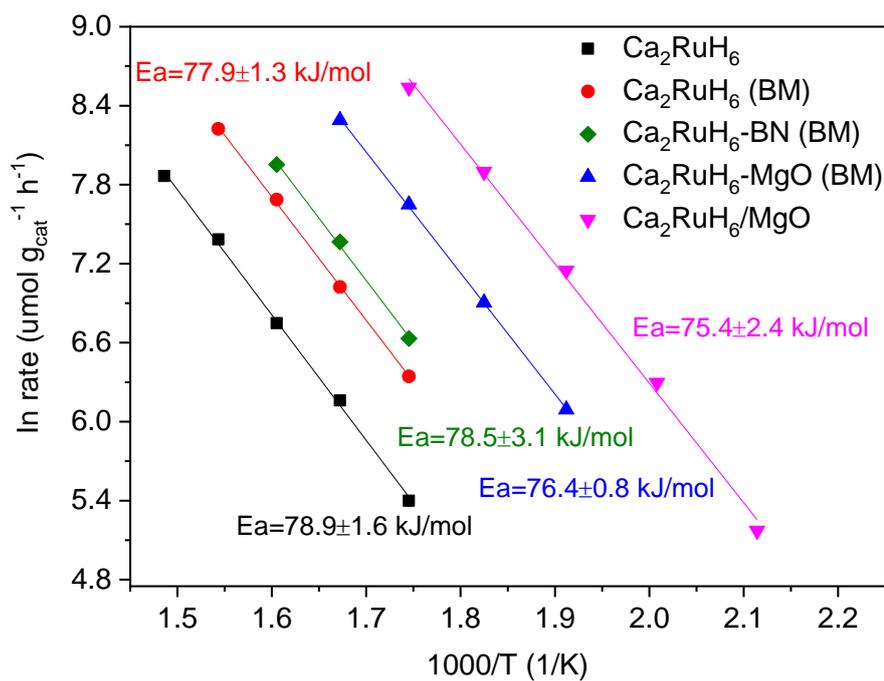
**Declaration of Interests**

Authors declare no competing interest.

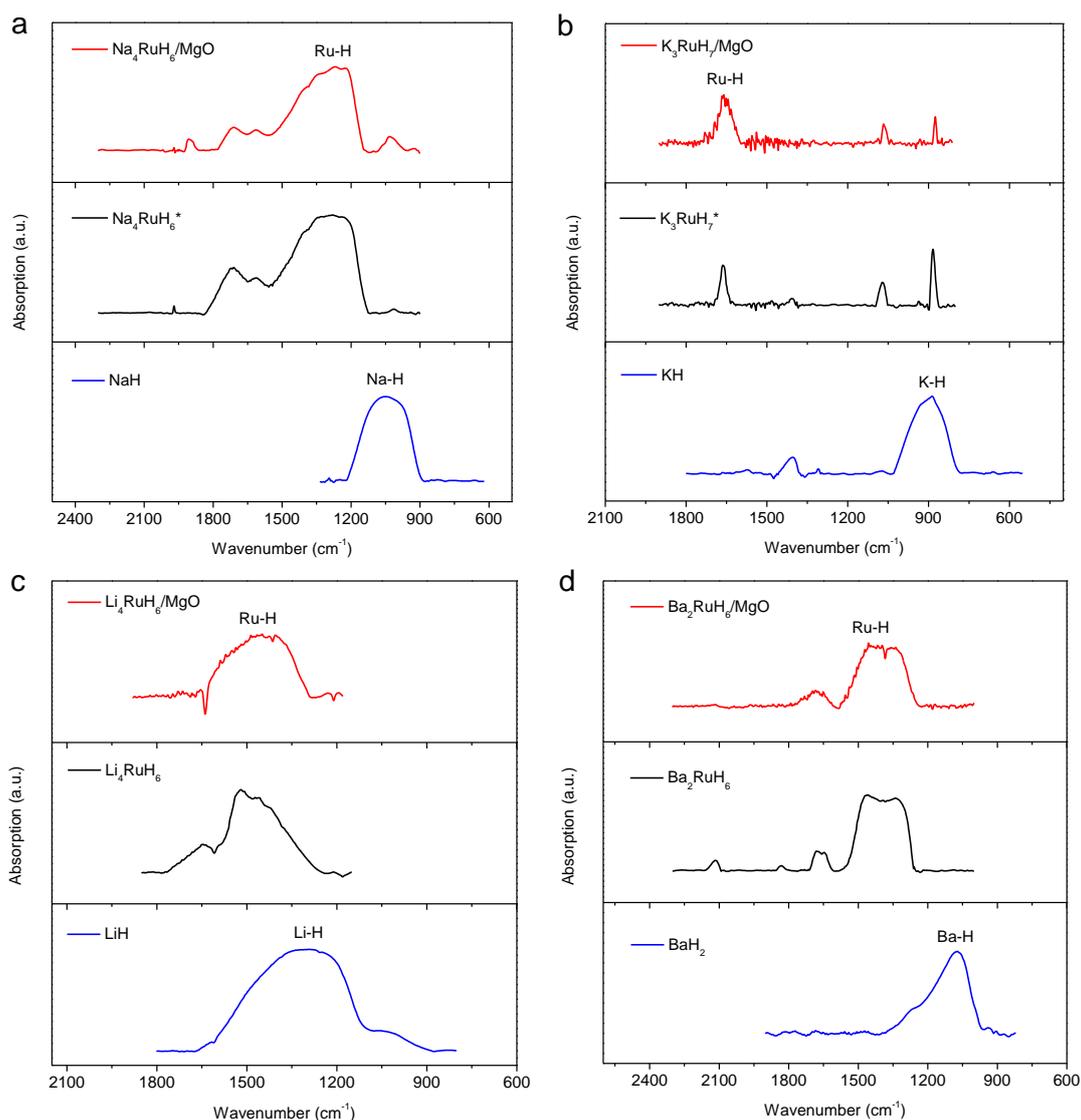
## Supplementary Information



**Fig. S1.** XRD patterns of  $\text{Ca}_2\text{RuH}_6$ , ball-milled  $\text{Ca}_2\text{RuH}_6$ -BN sample ( $\text{Ca}_2\text{RuH}_6$ -BN (BM)) and ball-milled  $\text{Ca}_2\text{RuH}_6$ -MgO sample ( $\text{Ca}_2\text{RuH}_6$ -MgO (BM)). The crystalline sizes of  $\text{Ca}_2\text{RuH}_6$ ,  $\text{Ca}_2\text{RuH}_6$ -BN (BM) and  $\text{Ca}_2\text{RuH}_6$ -MgO (BM) were estimated to be ca. 60, 25 and 13 nm, respectively, by using the Scherrer equation based on the collected XRD patterns.

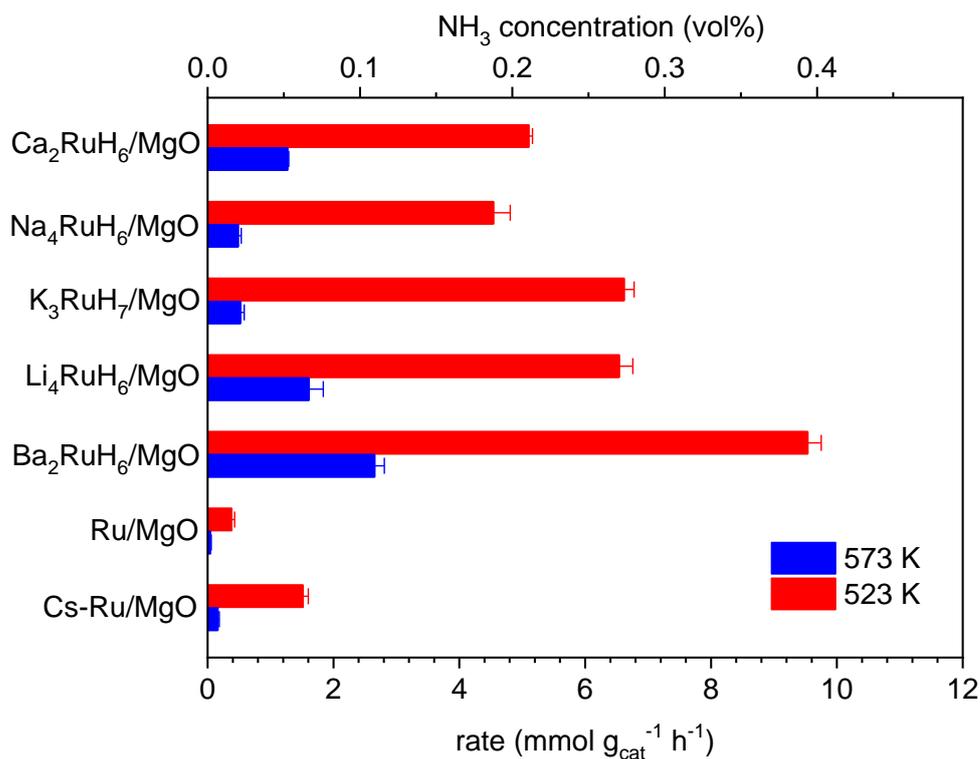


**Fig. S2.** Arrhenius plots of the  $\text{Ca}_2\text{RuH}_6$ , ball-milled  $\text{Ca}_2\text{RuH}_6$  ( $\text{Ca}_2\text{RuH}_6$  (BM)), ball-milled mixture of  $\text{Ca}_2\text{RuH}_6$  and BN ( $\text{Ca}_2\text{RuH}_6\text{-BN}$ -(BM)), ball-milled mixture of  $\text{Ca}_2\text{RuH}_6$  and MgO ( $\text{Ca}_2\text{RuH}_6\text{-MgO}$ -(BM)), and  $\text{Ca}_2\text{RuH}_6/\text{MgO}$  catalysts.

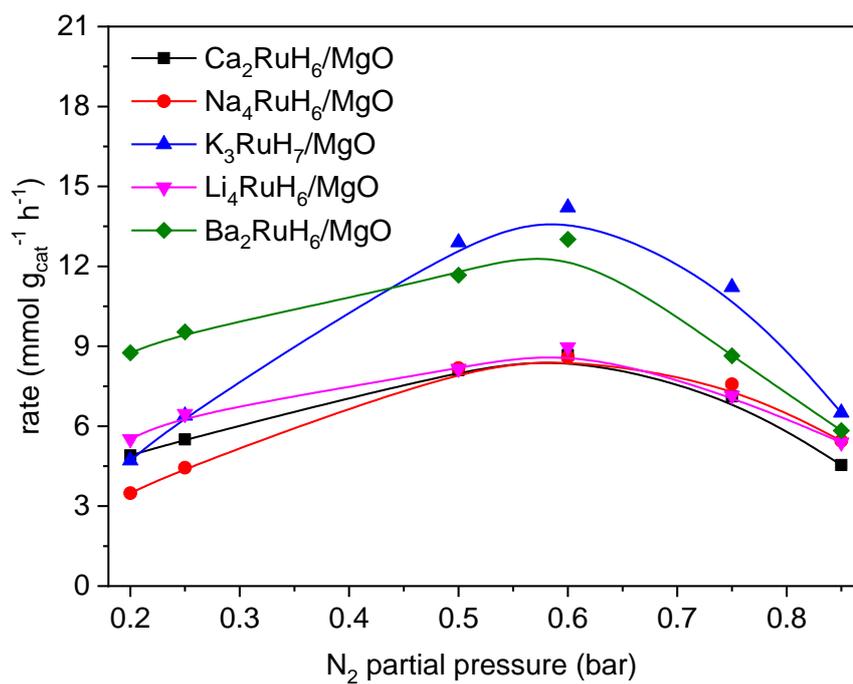


**Fig. S3.** **a**, FT-IR spectra of  $\text{Na}_4\text{RuH}_6/\text{MgO}$ ,  $^*\text{Na}_4\text{RuH}_6$  and  $\text{NaH}$ ; **b**, FT-IR spectra of  $\text{K}_3\text{RuH}_7/\text{MgO}$ ,  $^*\text{K}_3\text{RuH}_7$  and  $\text{KH}$ ; **c**, FT-IR spectra of  $\text{Li}_4\text{RuH}_6/\text{MgO}$ ,  $\text{Li}_4\text{RuH}_6$  and  $\text{LiH}$  and **d**, FT-IR spectra of  $\text{Ba}_2\text{RuH}_6/\text{MgO}$ ,  $\text{Ba}_2\text{RuH}_6$  and  $\text{BaH}_2$ . “\*” indicates that the as-prepared  $\text{Na}_4\text{RuH}_6$  and  $\text{K}_3\text{RuH}_7$  samples are in low purity, which still have a certain amount of unreacted  $\text{KH}/\text{NaH}$  and  $\text{Ru}$ .

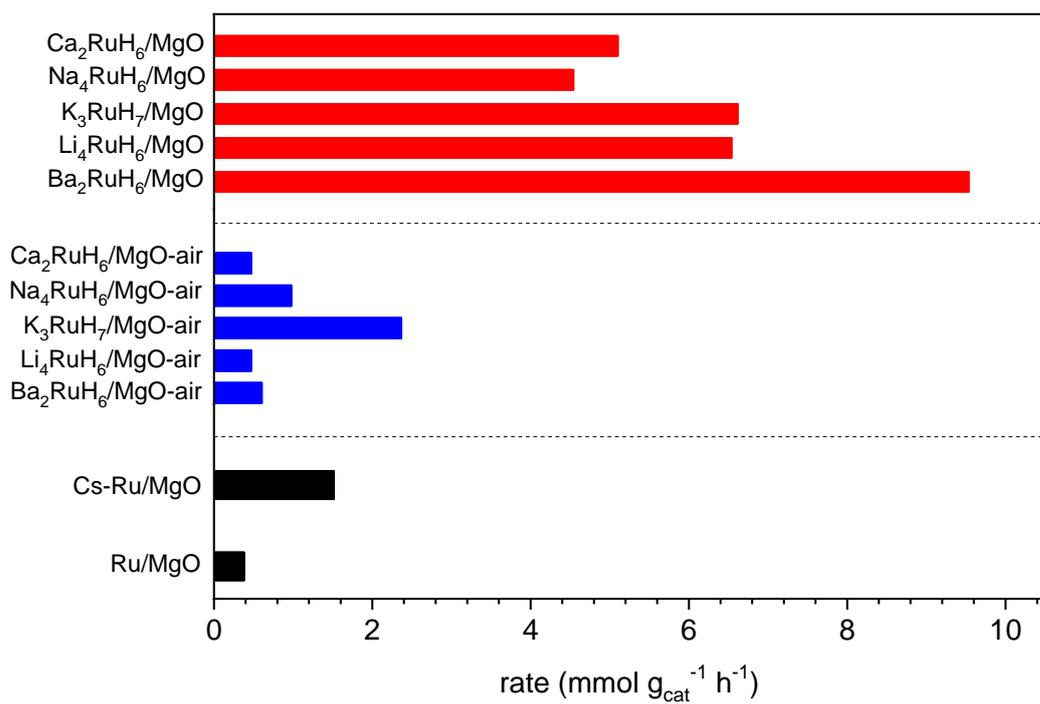
As shown, the Ru-H stretching bands of the as-prepared  $\text{Na}_4\text{RuH}_6$ ,  $\text{K}_3\text{RuH}_7$ ,  $\text{Li}_4\text{RuH}_6$  and  $\text{Ba}_2\text{RuH}_6$  are centered at 1280, 1660, 1500 and 1450  $\text{cm}^{-1}$ , respectively, which are obviously distinct from A-H vibrational modes of the corresponding  $\text{NaH}$ ,  $\text{KH}$ ,  $\text{LiH}$  and  $\text{BaH}_2$  reactants. The peak frequencies decrease with increasing Ru-H bond distances, which agree well with the theory-predicted results<sup>1-2</sup>. The IR spectra of the as-prepared supported ternary complex hydride samples show similar Ru-H stretching bands as the corresponding bulk ternary complex hydrides, indicating that the supported ternary complex hydrides have been successfully synthesized.



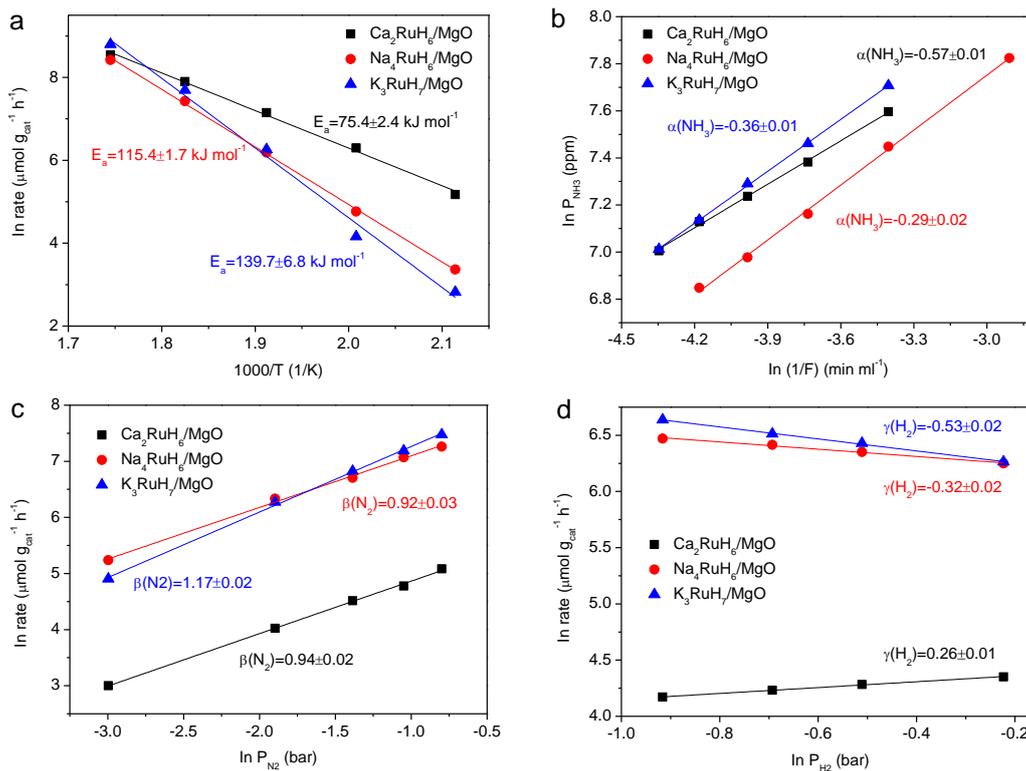
**Fig. S4.** NH<sub>3</sub> synthesis rates and corresponding effluent NH<sub>3</sub> concentration of supported ternary Ru complex hydride catalysts (Ca<sub>2</sub>RuH<sub>6</sub>/MgO, Na<sub>4</sub>RuH<sub>6</sub>/MgO, K<sub>3</sub>RuH<sub>7</sub>/MgO, Li<sub>4</sub>RuH<sub>6</sub>/MgO and Ba<sub>2</sub>RuH<sub>6</sub>/MgO) and Ru metal based catalysts (Ru/MgO and Cs-Ru/MgO) at 1 bar (Reaction conditions: catalyst loading 30 mg, N<sub>2</sub>:H<sub>2</sub>=1:3, flow rate 30 ml min<sup>-1</sup>).



**Fig. S5.** NH<sub>3</sub> synthesis rates of supported ternary Ru complex hydride catalysts as a function of N<sub>2</sub> partial pressure (Reaction conditions: catalyst loading 30 mg, flow rate 30 ml min<sup>-1</sup>, 573 K, and the total pressure of N<sub>2</sub>-H<sub>2</sub> mixture gas is 1 bar.)



**Fig. S6.** NH<sub>3</sub> synthesis rates of Ca<sub>2</sub>RuH<sub>6</sub>/MgO, Na<sub>4</sub>RuH<sub>6</sub>/MgO, K<sub>3</sub>RuH<sub>7</sub>/MgO, Li<sub>4</sub>RuH<sub>6</sub>/MgO, Ba<sub>2</sub>RuH<sub>6</sub>/MgO, Ca<sub>2</sub>RuH<sub>6</sub>/MgO-air, Na<sub>4</sub>RuH<sub>6</sub>/MgO-air, K<sub>3</sub>RuH<sub>7</sub>/MgO-air, Li<sub>4</sub>RuH<sub>6</sub>/MgO-air, Ba<sub>2</sub>RuH<sub>6</sub>/MgO-air, Cs-Ru/MgO and Ru/MgO catalysts at 573 K (Reaction conditions: catalyst loading 30 mg, flow rate 30 ml min<sup>-1</sup>, N<sub>2</sub>:H<sub>2</sub>=1:3, and 1 bar).



**Fig. S7.** **a**, Arrhenius plots of  $\text{Ca}_2\text{RuH}_6/\text{MgO}$ ,  $\text{Na}_4\text{RuH}_6/\text{MgO}$  and  $\text{K}_3\text{RuH}_7/\text{MgO}$  catalysts; **b** to **d** Dependence of ammonia synthesis rates on the partial pressures of  $\text{NH}_3$ ,  $\text{N}_2$  and  $\text{H}_2$ , respectively, under a total pressure of 1 bar at 573 K over  $\text{Ca}_2\text{RuH}_6/\text{MgO}$ ,  $\text{Na}_4\text{RuH}_6/\text{MgO}$  and  $\text{K}_3\text{RuH}_7/\text{MgO}$  catalysts.

**Table S1.** Thermodynamic calculations for the decomposition reactions of ternary ruthenium complex hydrides. The reaction enthalpy of  $\text{Li}_4\text{RuH}_6$  decomposition ( $\Delta_r H^0(\text{Li}_4\text{RuH}_6)$ ) was obtained following the pressure-composition-isotherm measurements described previously <sup>3</sup>. The reaction enthalpies of other ternary ruthenium complex hydrides decomposition are taken from Ref. <sup>4</sup> and Ref. <sup>5</sup>. The standard enthalpies of formation of other substances are taken from “NIST Standard Reference Number 69”. Therefore, the standard enthalpies of formation of ternary ruthenium complex hydrides can be evaluated by combining the  $\Delta_r H^0$  and  $\Delta_f H^0$  values.

Reaction	$\text{Li}_4\text{RuH}_6$	$\rightarrow$	$4\text{LiH}$	+	$\text{Ru}$	+	$\text{H}_2$	$\Delta_r H^0$ (kJ mol <sup>-1</sup> )
$\Delta_f H^0$ (kJ mol <sup>-1</sup> )	-455.1		-90.5		0		0	93.1
Reaction	$1/3\text{Na}_4\text{RuH}_6$	$\rightarrow$	$4/3\text{Na}$	+	$1/3\text{Ru}$	+	$\text{H}_2$	$\Delta_r H^0$ (kJ mol <sup>-1</sup> )
$\Delta_f H^0$ (kJ mol <sup>-1</sup> )	-305.7		0		0		0	101.9
Reaction	$1/3\text{Ba}_2\text{RuH}_6$	$\rightarrow$	$2/3\text{Ba}$	+	$1/3\text{Ru}$	+	$\text{H}_2$	$\Delta_r H^0$ (kJ mol <sup>-1</sup> )
$\Delta_f H^0$ (kJ mol <sup>-1</sup> )	-464.1		0		0		0	154.7
Reaction	$1/3\text{Ca}_2\text{RuH}_6$	$\rightarrow$	$2/3\text{Ca}$	+	$1/3\text{Ru}$	+	$\text{H}_2$	$\Delta_r H^0$ (kJ mol <sup>-1</sup> )
$\Delta_f H^0$ (kJ mol <sup>-1</sup> )	-525.0		0		0		0	175.0
Reaction	$2/7\text{K}_3\text{RuH}_7$	$\rightarrow$	$6/7\text{K}$	+	$2/7\text{Ru}$	+	$\text{H}_2$	$\Delta_r H^0$ (kJ mol <sup>-1</sup> )
$\Delta_f H^0$ (kJ mol <sup>-1</sup> )	-300.3		0		0		0	85.8

**Table S2.** Ammonia synthesis over recently developed Ru-based catalysts.

Catalysts	Metal content (wt %)	$r_{\text{NH}_3}^{\text{a}}$ (mmol g <sub>Ru</sub> <sup>-1</sup> h <sup>-1</sup> )		WHSV (ml g <sup>-1</sup> h <sup>-1</sup> )	Ref.
		573 K, 10 bar	573 K, 1 bar		
<b>Ca<sub>2</sub>RuH<sub>6</sub>/MgO</b>	<b>9.0</b>	<b>206</b>	<b>96</b>	<b>60000</b>	
<b>Na<sub>4</sub>RuH<sub>6</sub>/MgO</b>	<b>7.6</b>	<b>241</b>	<b>109</b>	<b>60000</b>	
<b>K<sub>3</sub>RuH<sub>7</sub>/MgO</b>	<b>8.2</b>	<b>237</b>	<b>191</b>	<b>60000</b>	<b>this work</b>
<b>Li<sub>4</sub>RuH<sub>6</sub>/MgO</b>	<b>8.0</b>	<b>275</b>	<b>114</b>	<b>60000</b>	
<b>Ba<sub>2</sub>RuH<sub>6</sub>/MgO</b>	<b>5.0</b>	<b>673</b>	<b>276</b>	<b>60000</b>	
Ru/C <sub>12</sub> A <sub>7</sub> :e <sup>-</sup>	1.8	94 (593 K)	41	36000	6
Ru/Ca <sub>2</sub> N:e <sup>-</sup>	1.8	228 (593 K)	93	36000	6
Ru/BaTiO <sub>2.5</sub> H <sub>0.5</sub>	2.5	---	19 (598 K)	66000	7
Ru/Ca(NH <sub>2</sub> ) <sub>2</sub>	10	158 (8 bar)	56	36000	8
Ru/Ba-Ca(NH <sub>2</sub> ) <sub>2</sub>	10	233 (9 bar)	90	36000	9
Ru/Pr <sub>2</sub> O <sub>3</sub>	5	18 (9 bar)	---	18000	10
Ru/La <sub>0.5</sub> Ce <sub>0.5</sub> O <sub>1.75</sub>	5	22	---	72000	11
Ru/BaO-CaH <sub>2</sub>	10	165 (9 bar)	69	36000	12
Ru/BaCeO <sub>3-x</sub> N <sub>y</sub> H <sub>z</sub>	4.5	111 (9 bar)	---	36000	13
Ba-Ru-Li/AC	4.8	---	1.5	62400	14
LaRuSi	37.7	---	4.7 (673 K)	36000	15

<sup>a</sup>Ammonia synthesis rates per gram of Ru under 573 K, 10 bar and 573 K, 1 bar (H<sub>2</sub>:N<sub>2</sub>=3 or 2/3), unless otherwise stated.

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