Progress Towards a Large-Scale Synthesis of Molnupiravir (MK-4482, EIDD-2801) from Cytidine

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Molnupiravir (MK-4482, EIDD-2801) is a promising orally bioavailable drug candidate for treatment of COVID-19. Herein we describe a supply-centered and chromatography-free synthesis of molnupiravir from cytidine, consisting of two steps: a selective enzymatic acylation followed by transamination to yield the final drug product. Both steps have been successfully performed on decagram scale: the first step at 200 g, and the second step at 80 g. Overall, molnupiravir has been obtained in a 41% overall isolated yield compared to a maximum 17% isolated yield in the patented route. This route provides many advantages to the initial route described in the patent literature

and would decrease the cost of this pharmaceutical should it prove safe and efficacious in ongoing clinical trials.

Introduction: Molnupiravir (MK-4482, EIDD-2801) is in development by Merck after licensing from Ridgeback Biopharmaceuticals as an orally dosed antiviral for the treatment of COVID-19.¹ Animal studies have shown successful inhibition of SARS-CoV-2² as well as prevention of viral transmission.³ If shown to be safe and effective in ongoing clinical trials, this compound would be an important tool in the toolbox of physicians working to counter the effects of the SARS-CoV-2 virus pandemic. Drug availability, however, depends on efficient and cost-effective synthesis of the drug molecule to ensure broad global access to this potentially valuable medication. The original synthetic route was disclosed by Emory University in 2019; this route made molnupiravir in 5 steps with uridine (1) as the starting material.⁴ Since the yield for the final two steps is not reported, this route has a 17% maximum overall yield (Scheme 1).



Scheme 1. Synthetic route of molnupiravir disclosed by Emory University in 2019.4

We previously demonstrated the potential of a two-step route from cytidine (8) to molnupiravir (7), which has many advantages over the previously patented route including cost and overall yield (Figure 1).⁵



Figure 1. This work (green) compared to previous work (blue).⁵

However, several challenges prevent the previously reported route from being implemented at manufacturing scale. Most notably, both the intermediate and the final API were purified by column chromatography, so we sought to develop alternate workup and crystallization procedures to provide pure material without chromatographic purification. Other opportunities for improvement included examining the surprisingly high cost of acetone oxime and refining process parameters such as reaction concentration, catalyst loading, and stoichiometry. Thus, we set out to re-examine this route to enable this process to be run at an increased scale.

Results and Discussion: The oxime ester acylating agent (9) proved uniquely suited to selective enzyme acylation (SI Section 2.1). Unfortunately, the acetone oxime used in the synthesis of the acylating agent (Scheme 2a) proved to be a major cost driver of our initial route investigation (SI Section 1).



Scheme 2. a) The synthesis of acylating agent 9 using acetone oxime (11) and isobutyryl chloride(12). b) Synthesis of acetone oxime (11).

Surprised by the high cost of such a simple material, we sought to determine the cost of synthesizing this material ourselves. Gratifyingly, we found that a reported procedure⁶ for acetone oxime synthesis provided 64% yield on our first attempt (Scheme 2b). Use of methyl *tert*-butyl ether (MTBE) to replace diethyl ether in the workup produced a yield of 71%. This method was repeated on 500 g scale with NaOH as base, and 73% yield was observed. We anticipate a significant reduction of the cost of acetone oxime prepared by this procedure compared to current commercial sources.

With a cheaper preparation of acetone oxime in hand, we also sought to improve the synthesis of oxime ester **9**. Our previous synthesis (Scheme 2a) used a slight excess of isobutyric acid chloride and triethylamine, and 50 volumes (V) of dichloromethane (DCM) as solvent. We found that we could increase the throughput of the reaction by decreasing the solvent to 30 V, as well as increasing triethylamine addition from 1.1 equivalents to 1.2 equivalents. These small changes afforded a 99% corrected yield on 35 g scale. This reaction was also scaled up significantly, to 200 g, with a 90% corrected yield. We hypothesize the slight drop in yield upon scale may be related to more facile exclusion of water at small scale. No purification was necessary as crude material was sufficient for use in the next step (*vide infra*).

Streamlined preparation of acylating agent **9** facilitated investigation of the enzymatic acylation of cytidine (Figure 1, Step 1). We first sought to investigate environmentally preferable solvents to substitute for 1,4-dioxane (dioxane).⁷ Unfortunately, extensive solvent screening (Figure 2, additional data in SI Section 2.2) did not reveal another solvent that worked as well as dioxane for the reaction.



Figure 2. Various solvents screened for the enzymatic acylation of cytidine (MeCN = acetonitrile, CPME = cyclopentyl methyl ether, 2-MeTHF = 2-methyl tetrahydrofuran).

Cyclopentanone appeared promising based on our initial screening, and its high boiling point (131 °C) opened the possibility for an increased reaction temperature that we hoped would accelerate conversion. Unfortunately, higher temperatures led to lower conversion (SI Section 2.3),

possibly due to release of the enzymes from the polymer beads⁸ or degradation of the product. The lower conversion with cyclopentanone led us to return to dioxane as the optimal solvent. Last, we did a cursory investigation to ascertain whether a lower temperature or concentration could benefit the reaction; we found that lowering the temperature to 40 °C lowered conversion (SI Section 2.4). We then screened other enzymes in dioxane and additional solvents, but the originally identified Novozym 435 (N435) was the most efficient and selective enzyme for the desired 5'-*O*-acylation (SI Section 2.5). It was determined that a lower the stoichiometry of acylating agent (4.0 equiv versus 5.0 equiv) could be used (SI Section 2.6); while the yield decreased slightly, we believe the savings in cost and purity offset the decrease in yield. Thus, 4.0 equivalents of oxime ester and 60 °C were selected as the optimal conditions.

Hoping to decrease further the amount of solvent needed for the reaction, a two-factor, four level full factorial screening of 20-100 solvent volumes and 50-400 weight percent enzyme loading were performed (Figure 3).



Normalize		rea Perce	nt of Des	irea Proa	uct 10	Normalize	Normalized LC Area Percent of Diacylated Product 14				
Enzyme Wt %								Enzyme	e Wt %		
		50	100	200	400			50	100	200	400
	20	40	38	52	71		20	12	10	11	15
Solvent	40	46	62	85	72	Solvent	40	10	10	11	7
Volumes	70	61	70	87	78	Volumes	70	9	9	10	6
	100	41	79	90	80		100	10	8	9	6

Figure 3. Assessment of solvent volume versus enzyme loading. See SI Section 2.7 for additional details.

We hoped that increased enzyme loading would allow us to decrease solvent usage, which would in turn improve the reaction throughput and process mass intensity (PMI). Unfortunately, our screening revealed that increasing concentration significantly hindered conversion; we hypothesize that this effect is due to the limited solubility of cytidine in dioxane. Ultimately, we chose conditions using 4.0 equivalents of oxime ester, 150 weight % N435, and 50 volumes of dioxane as solvent, due to the highest distribution of product **10** relative to remaining starting material **8** and diacylated product **14** (SI section 3.3).

Additionally, the breadth of data on regenerating and recycling N435, including repeated uses in organic solvents,^{8,9a-d} suggests that N435 could be recycled for this reaction as well. Reuse of the enzyme would further decrease the raw material costs associated with this route.

Upon scaling up the reaction, we noticed a slowed reaction rate, from 24 hours to completion at small scale to approximately 40 hours at 19 g scale (SI Section 2.8). We believe this change is related to differences in the stirring method used at different scales: we stirred using magnetic stir bars at 750 rpm for scales up to 1 g, while larger-scale reactions used an overhead stirrer set to 260 rpm. Using this same setup, the reaction was scaled ten-fold to 200 g with no change in performance.

Throughout the reaction optimization, the major impurity observed was diacylated product (14), the structure of which was confirmed as the N-acylated product via ¹⁵N-¹H 2-D NMR (SI Section 2.9). However, we also saw a consistent unknown impurity in the HPLC, constituting 5-10 LC area percent (SI Section 2.10). We noticed that this impurity increased in proportion with enzyme loading, leading us to believe that the impurity was leached from the enzyme beads by dioxane. Indeed, a control reaction confirmed that the impurity formed simply from stirring the enzyme beads in dioxane at 60 °C overnight and was not related to either the cytidine or the

acylating agent (SI Section 2.9). Isolation of this impurity yielded a yellow gel that did not ionize on LC-MS. We hypothesize that this material is a macromolecular compound leached from the Lewatit VP OC 1600 solid support; solubilization of the support in studies of N435 catalysis has been reported for some solvents.⁸ Fortunately, simply rinsing the enzymes with dioxane before use eliminated this impurity (SI Section 2.9). Thus, the main impurities remaining in the reaction were the diacylated product **14**, unreacted cytidine **8**, and excess acylating agent **9**. Allowing this reaction to cool to room temperature (20 °C) and then filtering enabled the removal of the enzyme beads as well as unreacted starting material (SI Section 3.2); this was due to cytidine's insolubility in room temperature dioxane.

The main challenge for purification was therefore removing excess acylating agent and diacylated product from the desired product **10**. Upon completion of the reaction, remaining cytidine starting material as well as the enzyme beads were filtered out and then dioxane was removed via rotary evaporation. We then determined three methods (A, B, and C) for the purification of **10** from compounds **14** and **9** (Table 1). Methods A and B were successful for the purification of desired product **3** up to purity of >99% on smaller scales (10–100 g), while purification C was successful on up to 200 g scale.

8 Scale (g)	Solvent vol.	enzyme wt.%	Oxime ester 9 equiv	Reaction Time (hours)	Product 10 IY	Purity ^a
20	40 V	150	4.0	38	60%	>99%
30	50 V	150	4.0	40	65%	>99%
100	52.5 V	150	3.2	43	68%	98%

100	60 V	150	3.2	43	70%	>99%°
19	50 V	150	4.0	42	66%	>99%
200	52.5 V	150	4.0	43	70%	96%

^aPurity determined by qNMR unless noted otherwise; ^bAdditional details for purification in experimental section; ^cPurity determined by HPLC (at 280 nm)

Workup A	Add acetone (10 V), reflux (30 min), cool then filter, rinse with MTBE (2V)
Workup B	Triturate with MTBE (10 V), add acetone (13 V), reflux, cool, then filter
Workup C	Add water (20 V): MTBE (20 V) to solid, extract MTBE layer with water (2 x), remove water from combined water extracts, add acetone (13 V), reflux, cool, then filter

The transamination reaction of intermediate (**10**) to MK-8842 (**7**) was previously reported in 96% yield with 94% purity via column chromatography.⁵ Previously, 70% aq. isopropanol was used as the solvent for this reaction; however, we chose to replace this with 70% aq. 1-butanol solution. We hypothesized that the decreased solubility of butanol in water (as compared to the solubility of isopropanol in water) would decrease the amount of hydroxylamine salts present in the organic layer post-reaction, thus leading to a more facile purification. The optimization of this transamination reaction began by using 4.5 equivalents of hydroxylamine sulfate relative to starting material **10**,⁵ which displayed good conversion of **10** to desired product **7** after 22 hours (SI Section 4.1). In addition to desired product formation, side product N-hydroxycytidine (NHC, **15**) was formed in this reaction in small quantities. It was determined that decreasing the stoichiometry of hydroxylamine sulfate from 4.5 equivalents to 2 or 3 equivalents led to very similar reaction conversion (Figure 4, SI Section 4.1) and increased the purity of the crude reaction mixture after workup, which simply involved separating the organic and aqueous layers and then removing the 1-butanol from the organic layer (crude purity, Table 2).

Table 2. Development of conditions for the transamination of compound 10 to molnupiravir (7).



Entry	Scale of 10	(NH ₂ OH) ₂ H ₂ SO ₄ equiv	Time (h)	7 crude purity ^a	7 LC area % ^b
1	1 g	4.5	22 h	73%	89%
2	1 g	3	22 h	85%	90%
3	1 g	2	22 h	84%	84%
4	5 g	3	22 h	97%	97%

^aPurity determined by qNMR; ^bDetermined by LCMS at 280 nm



Figure 4. The LC area percent of compounds 10, 7, and 15 in the crude reaction mixtures for entries 1-4 in Table 2.

After the development of successful small-scale conditions (5 g) the next goals were to scale up this reaction to 80 g and to develop recrystallization conditions for the crude reaction mixture. We found that increasing the scale from 5 to 10 to 20 g did not significantly affect the reaction time

(Table 3). However, increasing the scale to 80 g required an increased reaction time to 40 hours for similar conversion (Figure 5).

 Table 3. Scale up of the transamination of 10 to 7 as well as the isolated yields and purity of the isolated material.

Entry	Scale of 10	(NH ₂ OH) ₂ H ₂ SO ₄ equiv	Time (h)	7 crude purity ^a	7 LC area % ^a	7 isolated yield	Purity of isolated 7 ^b
1	10 g	3	24	92%	94%	48%	>99%
2	20 g	3	28	93%	96%	49%	>99%
3	80 g	3.2	40	80%	91%	58%	97%

^aBased on LCMS area percent at 280 nm; ^bPurity determined by qNMR





We found that the pre-crystallization purification of this reaction on 80 g scale worked the same as on a 1 g scale, by simply separating the aqueous and organic layers. In order to increase the purity of the final compound from 80-90% after this initial purification, recrystallization conditions were developed. Due the difference of solubility of compound **7** in cold versus hot water (Table 4), water was chosen as the recrystallization solvent. Thus, it was determined that after the solvent was removed from organic layer, **7** could be recrystallized in greater than 99% purity from heating to 65 °C and slowly cooling in water (2 V). After the initial recrystallization, the remainder of **7** remained in the aqueous filtrate. We anticipate that further recrystallizations of the filtrate would produce additional molnupiravir.

Table 4. Solubility of molnupiravir in water at various solvent volumes and temperatures.

	5 ℃	25 °C	40 °C	65 °C	80 °C	95 ℃
20						
15						
10						
5						
2						
1						
0.5						

Solution Temperature

Soluble
Partially soluble
Not soluble

Water Volume

Conclusion: In conclusion, we have developed an increased scale, chromatography-free, twostep route from cytidine to molnupiravir with an overall isolated yield of 41% and lower cost as compared to the originally patented route³ (SI Section 1), with further cost decreases possible if solvent and enzyme recycling are employed. We hope that further scale-up of this route will enable affordable, efficient preparation of this potentially crucial pharmaceutical for the global fight against COVID-19.

Methods:

General Procedures

For all compounds, ¹H and ¹³C NMR spectra were recorded on Bruker Avance III spectrometers (400, 500 or 600 MHz). Chemical shifts were measured relative to the residual solvent resonance for ¹H and ¹³C NMR (CDCl₃ = 7.26 ppm for ¹H and 77.2 ppm for ¹³C, DMSO-d₆ = 2.50 ppm for ¹H and 39.2 ppm for ¹³C). Coupling constants J are reported in hertz (Hz). The following abbreviations were used to designate signal multiplicity: s, singlet; d, doublet; t, triplet; hept, heptet; dd, doublet of doublet; m, multiplet. Reactions were monitored by HPLC (Agilent 1260 Infinity II LC) or LCMS (Agilent Technologies InfinityLab LC/MSD). Unless noted otherwise, reactions involving air-sensitive reagents and/or requiring anhydrous conditions were performed under a nitrogen or argon atmosphere with glassware oven-dried at 140 °C. Reactions requiring mechanical stirring were stirred using a Heidolph RZR 2020 overhead stirring apparatus. Purity was assessed by quantitative NMR (qNMR) with benzyl benzoate or dimethyl sulfone (Sigma-Aldrich TraceCERT grade) as reference standard. Reagents and solvents were purchased from Aldrich Chemical Company, Fisher Scientific, Alfa Aesar, Acros Organics, Oakwood, or TCI. Unless otherwise noted, solid reagents were used without further purification. Methylene chloride (DCM) and dioxane were taken from a solid-sorbant Solvent Dispensing System purchased from Pure Process Technologies. Other solvents were purchased in anhydrous grades and used as received.

Acetone oxime (11)

11 g Scale: To a solution of acetone (11.0 mL, 150 mmol, 1.0 equiv) and hydroxylamine hydrochloride (15.6 g, 225 mmol, 1.5 equiv) in HPLC-grade H₂O (300 mL) at RT was added Na₂CO₃ (28.6 g, 270 mmol, 1.8 equiv) in portions. The reaction mass was stirred for 19 hr at RT, after which it was extracted with Et₂O (5 x 80 mL). The combined organic extracts were washed with saturated brine (40 mL) and dried over MgSO₄. After filtration and solvent removal, the product was obtained as a white solid in 64% yield (7.051 g) and 98% purity (qNMR). ¹H NMR (400 MHz, CDCl₃) δ 8.33 (s, 1H), 1.90 (s, 3H), 1.89 (s, 3H). ¹H and ¹³C NMR matched reported literature values.⁶ Repetition of the reaction with MTBE instead of Et₂O in the workup improved the yield to 71% (7.735 g).

500 g Scale: To a solution of hydroxylamine hydrochloride (500 g, 7.20 mol, 1.1 equiv) in H₂O (670 mL) at 0-5 °C was added a solution of NaOH (270 g, 6.75 mol, 1 equiv) in H₂O (670 mL) dropwise. The reaction mass was stirred for 30 min at 0-5 °C and acetone (500 mL, 6.75 mol, 1 equiv) was added. The reaction mass was stirred for a further 2 hours at 0-5 °C, after which it was filtered and vacuum dried for 45 minutes yielding 450 g wet white solid. The solid was then dissolved in DCM (9.0 L, 20 V) and stirred for 15 min, after which the layers were separated. The DCM layer was dried with Na₂SO₄ and washed with DCM (2.25 L, 5 V), then dried, yielding a white solid in 73% yield (360 g). The material was carried forward without further purification.

Acetone oxime *O*-isobutyryl ester (9)

35 g Scale: Acetone oxime (35.0 g, 478.9 mmol, 1.0 equiv) was dissolved in dichloromethane (1050 mL, 30 V) under argon with mechanical stirring and cooled to 0 °C using an ice/water bath. Isobutyryl chloride (55.2 mL, 526.7 mmol, 1.1 equiv) was slowly added, maintaining the solution

temperature between 0-5 °C. Et₃N (31.46 mL, 574.7 mmol, 1.2 equiv) was added via syringe pump at a rate of 2 mL/min, again maintaining the solution temperature below 5 °C. Et₃N addition caused the evolution of vapor and the formation of solid precipitates. The reaction mass was stirred for 20 h and allowed to warm to room temperature. The reaction mass was then washed with H₂O (2 X 350 mL), 5% w/w solution of NaHCO₃ (2 X 250 mL), H₂O (1 X 350 mL), 1N aq. HCl (2 X 250 mL), H₂O (1 X 350 mL), and saturated brine solution (1 X 100 mL), followed by drying over MgSO₄. After filtration and solvent removal, the product was obtained as a pale yellow liquid in 68.81 g yield (99% corrected for purity) and 99% purity (qNMR, benzyl benzoate). The material was carried forward without purification. ¹H NMR (400 MHz, CDCl₃) δ 2.66 (hept, *J* = 7.0 Hz, 1H), 2.05 (s, 3H), 1.99 (s, 3H), 1.24 (d, *J* = 7.0 Hz, 6H). ¹H and ¹³C NMR matched previously reported values.⁵

200 g Scale: Acetone oxime (200 g, 2.74 mol, 1.0 equiv) was dissolved in DCM (6 L) and cooled to 0 °C using an ice/water bath. Isobutyryl chloride (325 mL, 3.01 mol, 1.1 equiv) and Et₃N (241 mL, 3.28 mol, 1.2 equiv) were slowly added, maintaining the solution temperature between 0-5 °C. The reaction mass was stirred for 20 h and allowed to warm to room temperature. The reaction mass was then washed with H₂O (2 X 2 L), 5% w/w solution of NaHCO₃ (2 X 1.4 L), H₂O (1 X 1.4 L), 1N aq. HCl (2 X 1.4 L), H₂O (1 X 2 L), and saturated brine solution (1 X 600 mL), followed by drying over Na₂SO₄. After filtration and solvent removal, the product was obtained as a pale yellow liquid in 385 g yield (90% corrected for purity) and 92% purity (qNMR). The material was carried forward without purification.

5'-O-isobutyryl cytidine (10)

30 g Scale: 45.0 g Novozym-435 was rinsed with 1,4-dioxane (2 x 100 mL) in a sintered glass funnel and dried under vacuum for 20 mins. To an oven-dried 3 L 3-neck RBF was added cytidine (30.0 g, 123.3 mmol), rinsed enzyme beads, 1,4-dioxane (1.5 L, 50 V), and crude acetone oxime *O*-isobutyryl ester (70.65 g, 493.4 mmol). The reaction mixture was heated to 64 °C using a heating mantle and stirred using a mechanical stirrer for 39 hours, monitoring by HPLC (see SI for HPLC traces). The reaction mixture was then cooled to room temperature and filtered and washed with dioxane (3 V). The solvent was removed by rotary evaporation, yielding the crude product as an off-white foam (the crude material for this reaction was then purified via purification method A, see SI Section 3.1 for other purification procedures).

Purification A: Acetone (300 mL, 10 V) was then added to solid then refluxed for 30 minutes. The suspension was allowed to cool to room temperature then cooled to 5 °C (12 hours). The white solid was then filtered and rinsed with MTBE (2 V) then allowed to dry at 40 °C (12 h) under vacuum to yield compound **10** (25.2 g, 65%, >99% purity by qNMR). ¹H NMR (500 MHz, DMSO) δ 7.58 (d, *J* = 7.4 Hz, 1H), 7.19 (d, *J* = 23.1 Hz, 2H), 5.76 (d, *J* = 3.7 Hz, 1H), 5.73 (d, *J* = 7.4 Hz, 1H), 5.40 (d, *J* = 5.2 Hz, 1H), 5.19 (d, *J* = 5.9 Hz, 1H), 4.28 (dd, *J* = 12.2, 3.2 Hz, 1H), 4.18 (dd, *J* = 12.1, 5.4 Hz, 1H), 3.99 – 3.94 (m, 2H), 3.93 – 3.87 (m, 1H), 2.58 (hept, *J* = 7.0 Hz, 1H), 1.11 (d, *J* = 7.0 Hz, 6H).¹H and ¹³C NMR matched previously reported values.⁵

200 g Scale: Novozym-435 (300 g, 150 wt %) was rinsed with 1,4-dioxane (4L) and dried under vacuum for 30 mins. Cytidine (200 g, 822 mmol, 1 equiv), rinsed enzyme beads, 1,4-dioxane (10.5 L, 52.5 V), and crude acetone oxime *O*-isobutyryl ester (471 g, 3.29 mol, 4 equiv). The reaction mixture was heated to 60 °C and stirred for 43 hours. The reaction mixture was then cooled to

room temperature and filtered and washed with dioxane (3 V). The solvent was removed by distillation.

<u>Purification C:</u> MTBE (20 V) and H₂O (20 V) were then added. The layers were separated and the organic layer was washed twice with H₂O. The combined aqueous layers were distilled to yield a white solid. Acetone (13 V) was added and the slurry was heated to 60 °C for 1 hour, cooled to room temperature, filtered, and dried, yielding 188 g (70% corrected) with a purity of 96.5% (qNMR).

Molnupiravir (7)

10 g Scale: 5'-*O*-isobutyryl cytidine (10.0 g, 32.0 mmol, 1.0 equiv) was dissolved in 70% aq. 1butanol (112 mL 1-butanol: 48 mL water) and then hydroxylamine sulfate (15.8 g, 96.0 mmol, 3.0 equiv) was added. The mixture was stirred vigorously and heated to 78 °C for 24 hours. The layers were then separated, and 1-butanol was removed from the organic layer via rotary evaporation to yield solid white, crude material (5.2 g, 92% purity via qNMR). This crude material was then dissolved in water (2 V) and heated to 65 °C for 30 minutes (60 minutes for 80 g scale). After completely dissolved, the mixture was allowed to cool to room temperature and then 5 °C without stirring. The solid was then filtered and washed with MTBE (2 V) to obtain molnupiravir (5.03 g, 48% yield, >99% purity by qNMR). 'H NMR (500 MHz, DMSO) δ 10.00 (s, 1H), 9.53 (s, 1H), 6.83 (d, *J* = 8.2 Hz, 1H), 5.72 (d, *J* = 5.5 Hz, 1H), 5.59 (dd, *J* = 8.2, 2.0 Hz, 1H), 5.36 (d, *J* = 5.6 Hz, 1H), 5.21 (s, 1H), 4.21 (dd, *J* = 12.0, 3.3 Hz, 1H), 4.14 (dd, *J* = 12.0, 5.1 Hz, 1H), 4.02 – 3.97 (m, 1H), 3.94 – 3.88 (m, 2H), 2.58 (hept, *J* = 7.0 Hz, 1H), 1.11 (dd, *J* = 7.0, 1.0 Hz, 6H). 'H and ¹³C NMR matched previously reported values.⁵ **80 g Scale:** 5'-*O*-isobutyryl cytidine (80 g, 255 mmol, 1.0 equiv) was dissolved in 70% aq. 1butanol (20 V) and then hydroxylamine sulfate (134 g, 817 mmol, 3.2 equiv) was added. The mixture was stirred vigorously and heated to 75-80 °C for 40 hours. The mixture was cooled to room temperature, the layers were then separated, and 1-butanol was distilled from the organic layer yielding solid white, crude material (85 g). This crude material was then dissolved in water (2 V) and heated to 60-65 °C for 60 minutes. After completely dissolved, the mixture was allowed to cool to room temperature and stirred for 1 hour, then cooled to 5-10 °C and stirred for 3 hours. The solid was then filtered and the wet washed with MTBE (3 V) to obtain 56.0 g molnupiravir. The purification was repeated again for a final yield of 50.0 g (58% corrected) with 97% purity (qNMR).

ASSOCIATED CONTENT

Supporting Information.

The following files are available free of charge. Additional experimental details and characterization, pdf

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