

Identification of the mechanism of NO reduction with ammonia (SCR) on zeolite catalysts

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Short title: Clarification of the selective catalytic reduction mechanism

Abstract: Cu/Zeolites catalyze selective catalytic reduction of nitric oxide with ammonia. Although the progress has been made in understanding the rate-limiting step of reaction which is reoxidation of Cu(I)(NH₃)₂ with oxygen to restore the catalytically active Cu(II) site, the exact NO reduction chemistry remained unknown. Herein, we show that nitrosyl ions NO⁺ in the zeolitic micropores are the true active sites for NO reduction. They react with ammonia even at below/room temperature producing molecular nitrogen through the intermediacy of N₂H⁺ cation. Isotopic experiments confirm our findings. No copper is needed for this reaction to occur. However, when NO⁺ reacts, “freed up” Bronsted acid site gets occupied by NH₃ to form NH₄⁺ – and so the catalytic cycle stops because NO⁺ does not form on NH₄-Zeolites due to their acid sites being already occupied. Therefore, the role of Cu(II) in Cu/Zeolite catalysts is to produce NO⁺ by the reaction: Cu(II) + NO → Cu(I) + NO⁺ which we further confirm spectroscopically. The NO⁺ then reacts with ammonia to produce nitrogen and water. Furthermore, when Cu(I) gets re-oxidized the catalytic cycle then can continue. Thus, our findings are critical for understanding complete SCR mechanism.

One Sentence Summary: We clarify the long-standing unknown SCR mechanism.

Air pollution is one of the main health and environmental concerns in our (post)industrial society [1-3]. Worsening air quality is tied to toxic nitric oxide (NO) gas, the majority of which is emitted by vehicles exhaust. The ability of Cu/zeolites to scrub NO in the presence of ammonia was first discovered in Japan in the 1960s [4] for Cu/FAU zeolite. However, FAU framework is less stable

that the corresponding SSZ-13 and BEA zeolites [5]. Within the last decade, the ammonia selective catalytic reduction (SCR) technology was implemented on the large scale [5-19] for diesel engines on the basis of Cu(Fe) in BEA and SSZ-13 zeolites.

Remarkable advances have been achieved towards the goal of understanding the rate-limiting steps of the SCR mechanism [5-20]. Cu(II) ions are present in Cu/zeolite materials (they were shown to be more active and hydrothermally stable than Cu(II)-OH ions [5-20,25]. The rate-limiting step for low-temperature SCR was shown to be re-oxidation of reduced Cu(I)(NH₃)₂ complexes via the formation of transient (NH₃)₂Cu(II)-O₂-Cu(II)(NH₃)₂ dimers [17,18]. Despite that, the mechanism of the steps involving NO reduction with NH₃ remained largely unknown [5-20].

We selectively formed NO⁺ ion in H-BEA zeolite (typical helium ion images of H-BEA are shown in Fig. S6) by reaction of NO with sub-stoichiometric amounts of O₂ [21-23](Fig. 1A).

NO⁺ is formed through the following reaction (**Scheme 1** responsible for spectra in Fig 1A):



NO⁺ occupies two different cationic positions with the corresponding N-O stretching frequencies at ~2133 and ~2175 cm⁻¹. The same type of chemistry also occurs on H-SSZ-13 (Fig. S1). Please note that adsorption of NO₂ also produces NO⁺ but with stoichiometric NO₃⁻ amounts due to N₂O₄ disproportionation (Fig. S2). Pulling the high vacuum (~10⁻⁷ Torr) (with quick heating to 150 °C) allows to remove excessive NO and O₂, leaving zeolite with NO⁺ adsorbed in it (Fig. 1B).

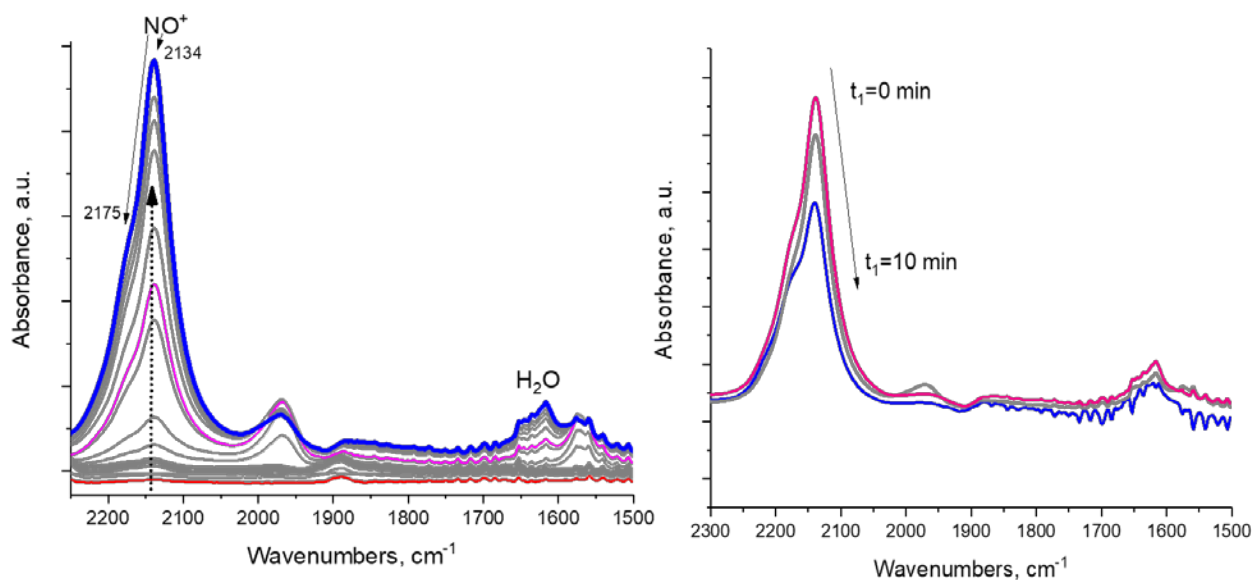
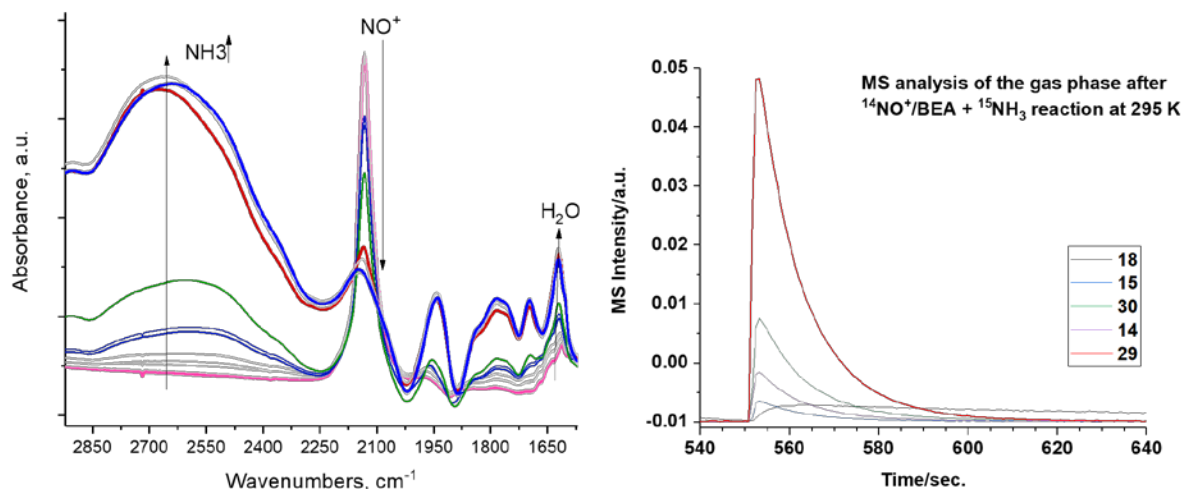


Fig.1 H-BEA Zeolite with Si/Al ~ 15. **A (left spectrum)**: *in-situ* FTIR during first sequential NO adsorption (0.1 Torr equilibrium pressure), followed by sequential O₂ addition (0.17 Torr total eq. pressure – when O₂ is added, NO⁺ begins to develop in significant amounts); **B (right spectrum)**: FTIR after pulling high vacuum 10⁻⁸ Torr from time=0 to time=10 minutes at 150 °C. Spectra were recorded after cooling back to 297 K.

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We exposed the NO⁺/Zeolite to ¹⁵N-labeled ammonia at room temperature 297 K (Fig. 2A). Ammonia first occupies Bronsted acid sites forming NH₄⁺ complexes (which interact with more NH₃ and the pores are filled with (NH₃)_x cluster networks interacting with NH₄⁺ ions [24,27]). During this, NO⁺ reacts with ammonia, leaving no new visible NO stretches (Fig. 2A).



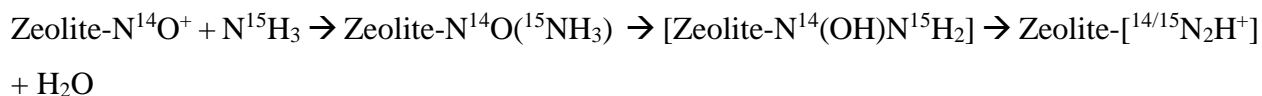
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Fig. 2. H-BEA zeolite with Si/Al~15. **A (left spectrum)**: *in-situ* sequential FTIR during ¹⁵NH₃ adsorption (total equilibrium pressure 0.020 Torr) on NO⁺/H-BEA sample at room temperature. Ammonia reacts with NO⁺. Gas phase from that reaction was analyzed with the mass spectrometer attached to the IR cell (Figure 2B shows formation of ¹⁴N¹⁵N dinitrogen with the characteristic 29 mass signal).

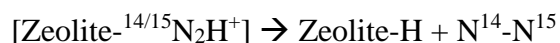
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The analysis of the gas-phase product with mass-spectrometry reveals a major peak at 29, corresponding to ¹⁴N-¹⁵N molecules (Fig. 2B). Thus, NO⁺ reacts with ammonia with the formation of molecular nitrogen already at room temperature. Only the following sequence can be envisioned (Schemes 2 and 3) (note that NO⁺ does not necessarily have to be bound to zeolite, it most likely is solvated by NH₃; the designation Zeolite-NO⁺ is just a representation of NO⁺/H-zeolite system in which NO⁺ may be solvated or semi-solvated by ammonia molecules):

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N_2H^+ (hydronium diazonium cation) is extremely unstable. Its immediate decomposition to N_2 and H-Zeolite is what drives this reaction. Despite that, we find that at sufficiently high molecular N_2 pressure in the cell (~ 15 Torr) we can observe the N-N stretch of $-\text{HN}_2^+$ complex at 2334 cm^{-1} even at room temperature (Fig 3A), which was previously shown to form only at low temperatures upon N_2 interaction with Bronsted acid sites (Fig. 3B) [26]. Thus, we can observe the intermediate of this reaction indirectly.

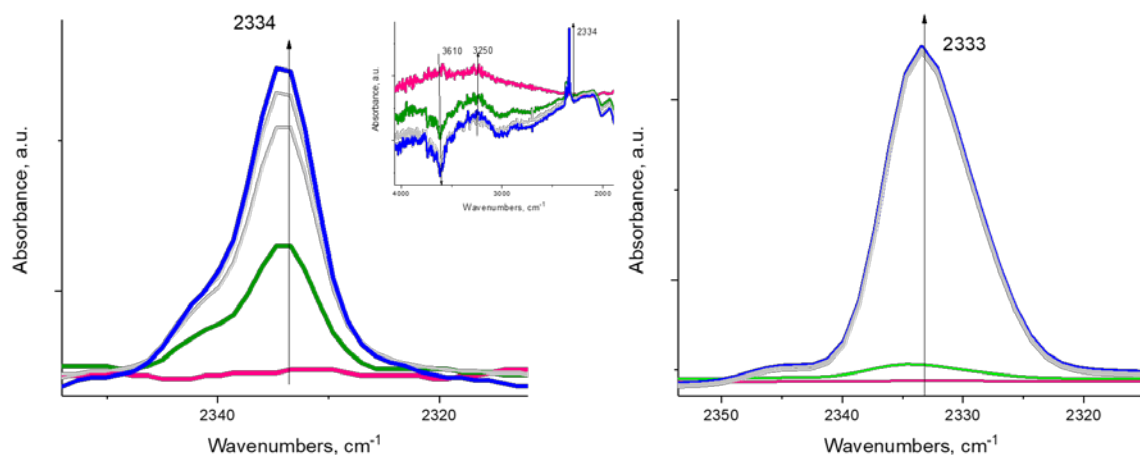


Fig. 3. **A (left spectrum):** *in-situ* FTIR during sequential dinitrogen N_2 adsorption (equilibrium pressure ~ 15 Torr) on H-BEA at 298 K. Zeolite- $[\text{HN}_2^+]$ complex can be observed even at room temperature. Inset shows that N_2 interacts with Bronsted acid sites of Si-OH-Al zeolite groups (OH stretch of such groups is located at $\sim 3610\text{ cm}^{-1}$). **B(right spectrum):** *in-situ* FTIR during Adsorption of only ~ 0.1 Torr N_2 on the same H-BEA tablet (equilibrium pressure is 0.001 Torr) at 77 K produces N-N stretches of N_2 adsorbed on Bronsted acid sites. Note that in this case even low equilibrium pressure of nitrogen produces intense N-N stretches.

To further prove the reaction proceeds through diazo compound, we chose aniline PhNH_2 (which is equivalent to ammonia molecule but with 1 hydrogen atom substituted by a phenyl group) and reacted it with NO^+ in BEA zeolite. Phenyl group stabilizes the formation of PhN_2^+ salts (phenyl diazonium salts) through the mesomeric effect, and thus, unlike alkyl diazonium salts, aryl diazonium compounds are stable and characterized by N-N stretches in $\sim 2,250\text{-}2,300\text{ cm}^{-1}$ region [28], more specifically $\sim 2,280\text{ cm}^{-1}$ for phenyl diazonium in solution [28]. Indeed, we monitored the reaction of NO^+ and PhNH_2 , spectroscopically: NO^+ band went down and a new N-N stretch appeared at $\sim 2270\text{ cm}^{-1}$, corresponding to the N-N vibration of Ph-N_2^+ fragment (Fig. 4).

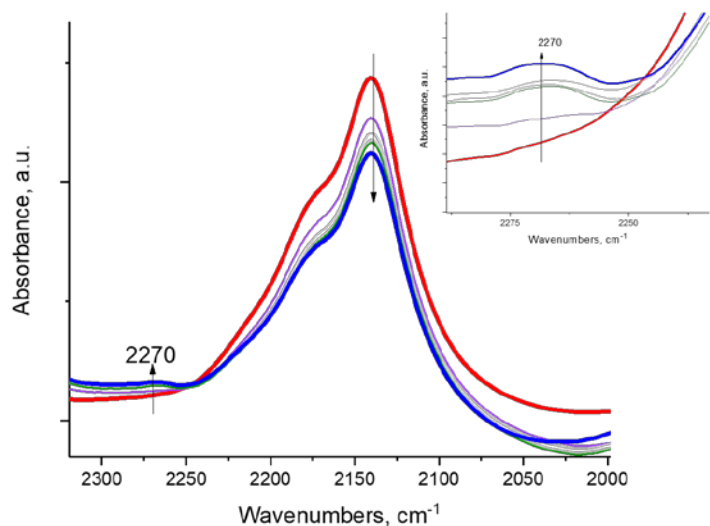


Fig. 4. *in-situ* FTIR during sequential ~ 0.3 Torr aniline PhNH_2 adsorption (equilibrium pressure ~ 0.03 Torr) $\text{NO}^+/\text{H-BEA}$.

- 5 NO^+ in H-SSZ-13 (with Si/Al ~ 12 ; typical HAADF-STEM images of this sample are shown in Fig. S7) similarly reacts to NH_3 (Fig. 5), with concomitant N_2 evolution (confirmed with mass-spectrometry):

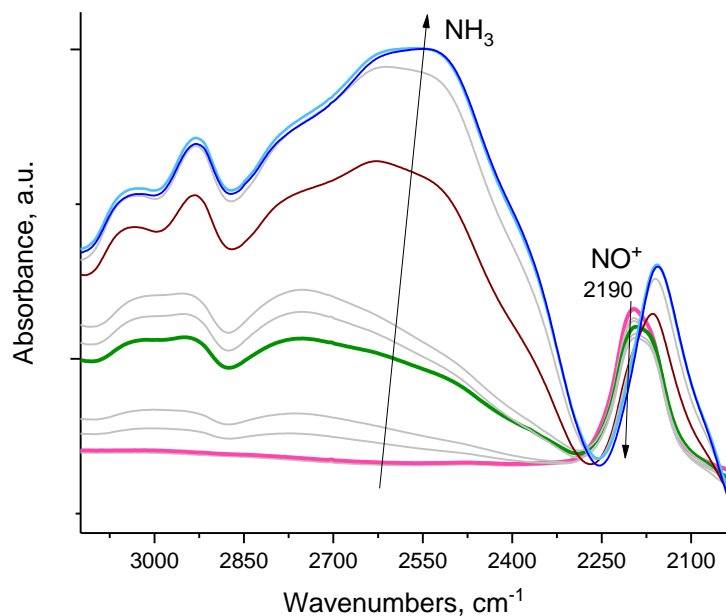
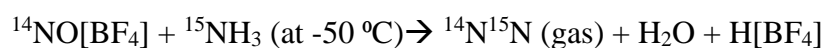


Fig. 5. H-SSZ-13 zeolite with Si/Al ~ 12 . In-situ sequential FTIR during $^{14}\text{NH}_3$ adsorption (total equilibrium pressure ~ 0.15 Torr) on $\text{NO}^+/\text{H-SSZ-13}$ sample at room temperature. Ammonia reacts with NO^+ as evidenced by the disappearance of NO^+ stretch. The intense band at ~ 2110 cm^{-1} is due to zeolite interactions with NH_3 . Pulling vacuum on the sample at 120 $^\circ\text{C}$ produces spectra showing no NO^+ stretches (Fig. S3), consistent with complete reaction of NO^+ .

Thus, NO⁺ (which is produced from NO+O₂ reaction/it can also form from N₂O₄ disproportionation on zeolites if sufficient NO₂ concentration is present [29]) is the critical intermediate in conversion of NO on zeolites. *Copper is not even required to observe the NO⁺ reduction by NH₃.*

Moreover, we reacted inorganic nitrosyl salt NO⁺ with ¹⁵NH₃ and observed ¹⁴N-¹⁵N in the gas-phase (consistent with our findings for NO⁺ in zeolites, *this reaction takes place vigorously even at temperatures as low -50 °C*) (**Scheme 4**):



This reaction (**scheme 4**) most likely proceeds through N₂H⁺ intermediate as well.

For NO⁺ in zeolite, once it reacts with NH₃ with the release of N₂, the Bronsted acid is freed up from NO⁺ and then immediately occupied by ammonia with the formation of NH₄⁺. This “kills” the reactivity as we cannot produce NO⁺ species anymore since their production requires Bronsted acid sites, as evidenced by FTIR (**Fig. S4**): indeed, no NO⁺ evolves in above-trace-amount upon NO+O₂ reaction on NH₄-zeolite (**Fig. S4**). Only at elevated temperature, when some NH₃ can desorb and free up a portion of Bronsted acid sites to re-form NO⁺, the reaction can proceed catalytically. Indeed, bare H-BEA zeolite is catalytically active for NO reduction with NH₃ in the dry streams (see **Fig. S5** for reactivity at 200 and 150 °C with time-on-stream) (measurable activity is observed).

NO⁺ are formed in zeolite through **Scheme 1** (see earlier discussion in the manuscript).

With these new data, we can finally explain the role of Cu in zeolites for SCR. As is well-established in the literature, Cu(II) ions are required for the active continuous catalytic reaction to proceed [5-20]. In the presence of NO, Cu(II) ions can produce NO⁺ via the formal 1-electron reduction of Cu(II) (analogous chemistry is observed, for example, for Pd(II) in zeolites [30] where Pd(II) was shown to be reduced to Pd(I) by NO pulse with concomitant formation of NO⁺) (**Scheme 5**):

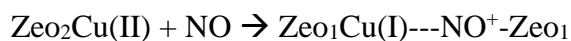


Fig. 6A shows spectroscopic evidence of Cu(II) reduction by NO (when Cu(II) is first reduced to Cu(I) before NO adsorption, basically very little NO^+ formation occurs because electron transfer does not take place as demonstrated in Fig 6B).

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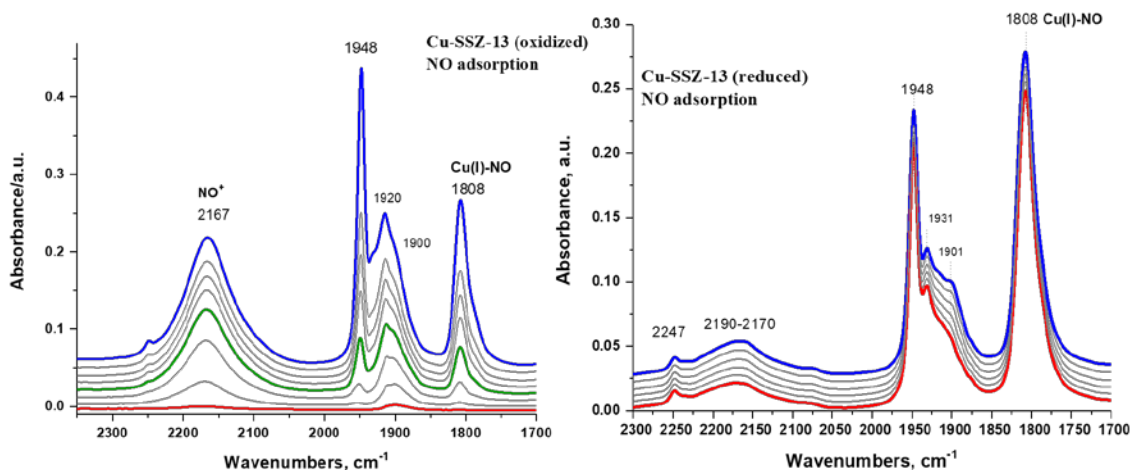


Fig. 5. 1 wt% Cu/H-SSZ-13 sample with Si/Al \sim 12. **A(left)**: in-situ FTIR during 1 Torr NO adsorption on oxidized sample. NO^+ and Cu(I)-NO evolve simultaneously from Cu(II) reduction by NO. **B(right)**: the same sample (tablet) was reduced in the IR cell: 1 Torr NO adsorption (same equilibrium pressure) after reduction.

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We have previously been able to refine with solid-state ^{15}N NMR studies that, indeed, NO is capable of reducing Cu(II) to Cu(I) in H-SSZ-13: the resulting complex had Cu(I) and NO^+ in proximity to each other, with NO^+ located side-on towards copper ion [20].

Therefore, now we conclude that the role of copper is to promote NO^+ formation (because Bronsted acid sites get occupied by NH_4^+ after NO^+ reaction with NH_3 on bare H-Zeolite, they cannot contribute to NO^+ formation as we showed earlier in the text). The resulting NO^+ reacts with ammonia to reform N_2 . The $\text{Cu(I)(NH}_3)_2$ complex, in turn, gets re-oxidized back to Cu(II) with oxygen as the rate-limiting step [17,18].

In summary, this study resolves the previously missing chemistry of the SCR reaction on zeolitic materials and explains the role of Cu for SCR. For the first time, NO^+ is shown to be the crucial reactive intermediate without which the reaction cannot proceed. The catalytic reaction is suggested to proceed through the formation of previously unrecognized diazo-complex N_2H^+ . The role of copper is to be a redox active center which facilitates the formation of NO^+ from NO while

simultaneously getting reduced to Cu(I). During the rate-limiting step, Cu(I) gets re-oxidized by O₂ to Cu(II), thus completing the catalytic cycle.

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Data and materials availability: All data is available in the main text or the supplementary
10 materials.

Supplementary Materials:

Materials and Methods

Supplementary text

Figures S1-S7

5 **Identification of the mechanism of NO reduction with ammonia (SCR) on zeolite catalysts**

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20 **Materials and methods**

BEA with Si/Al ratio ~ 15 was synthesized in the presence of fluoride anions according to a procedure developed by Cambor et al. [S1] The gel composition was as follows SiO₂: xAl₂O₃:(0.54 + 2x)TEAOH:(0.54 + 2x)HF:(7 + 2x)H₂O. The absence of alkali cations requires only a calcination step (550 °C in flowing air), decomposing the organic cation (TEA⁺) to convert it into Brønsted acidic H-Form.

30 Na/SSZ-13 zeolite with Si/Al 12 was hydrothermally synthesized using the following recipe: 0.8 g of NaOH (Sigma Aldrich, ≥ 99%) was dissolved in 50 ml of deionized water. 17 g of TMAda-OH (Sachem Inc., 25% N,N,N-trimethyl-1-adamantyl ammonium hydroxide) was added as structure directing agent. 0.75 g of Al(OH)₃ (Sigma Aldrich, ~54% Al₂O₃) was slowly added to the solution and stirred at 400 rpm until it was completely dissolved. 20.0 g of LUDOX HS-30 colloidal silica (Sigma Aldrich, 30 wt% suspension in H₂O) was added slowly to the solution until a uniform gel was formed. The obtained gel was sealed in a 125 mL Teflon-lined stainless steel autoclave with a magnetic stirring

bar. Hydrothermal synthesis was carried out at 160 °C under continuous stirring at 400 rpm for 4 days. After synthesis, the zeolite cake was separated from the suspension by centrifugation, and washed with deionized water. It was then dried at 80 °C under N₂ flow overnight, and calcined in air at 550 °C for 5 h in order to remove the SDA. NH₄/SSZ-13 was obtained by ion exchange of the as-prepared Na/SSZ-13 zeolite with 1 M NH₄NO₃ solution at 80 °C for 5 h. The process was repeated three times. H-form of zeolite was obtained by calcining in air at 550 °C for 5 hours. Ion-exchange with Cu(II) to produce Cu/SSZ-13 was performed in the presence of copper nitrate. The resulting sample was calcined at 550 °C in air.

NO[BF₄] nitrosyl tetrafluoroborate (99%) was purchased from Strem Chemicals and stored cold in the absence of moisture.

All the chemicals used were the highest-grade purity available.

HAADF-STEM analysis was performed with a FEI Titan 80–300 microscope operated at 300 kV. The instrument is equipped with a CEOS GmbH double-hexapole aberration corrector for the probe-forming lens, which allows for imaging with 0.1 nm resolution in scanning transmission electron microscopy mode (STEM). The images were acquired with a high angle annular dark field (HAADF) detector with inner collection angle set to 52 mrad.

Helium ion microscopy (HIM) images were obtained using 35 keV He ions with 0.1 pA beam current at normal incidence. Secondary electrons were detected using an Everhart–Thornley detector. For HIM imaging, a very thin layer of carbon (<1 nm) was coated using a carbon sputter deposition system as the samples were completely insulating. The instrument resolution was 0.35 nm.

The *in-situ* static transmission IR experiments were conducted in a home-built cell housed in the sample compartment of a Bruker Vertex 80 spectrometer, equipped with an MCT detector and operated at 4 cm⁻¹ resolution. Mass-spectrometer is attached to the cell to monitor different gaseous species present. The powder sample was pressed onto a tungsten mesh which, in turn, was mounted onto a copper heating assembly attached to a ceramic feedthrough. The sample could be resistively heated, and the sample temperature was monitored by a thermocouple spot welded onto the top center of the W grid. The cold finger on the glass bulb containing CO (99.995%) was cooled with liquid nitrogen to eliminate any contamination originating from metal carbonyls, while NO (99.95%) was cleaned with multiple freeze–pump–thaw cycles. ¹⁵NH₃ (15N, 98%) was purchased from Cambridge Isotopes. Special research-grade oxygen (purity 99.995%) was purchased from Oxarc.

The NO reduction by ammonia (in the presence of oxygen) was carried out in a typical quartz the plug-flow reactor. 120 mg of H-zeolites was used for reaction tests. The composition of the gas flowing through the catalyst was ~ 360 ppm NH₃, 360 ppm NO, ~12 % O₂ balanced with nitrogen. The total flow rate was ~ 300 sscm/min. Concentrations of reactants and products were measured by the MKS FTIR analyzer.

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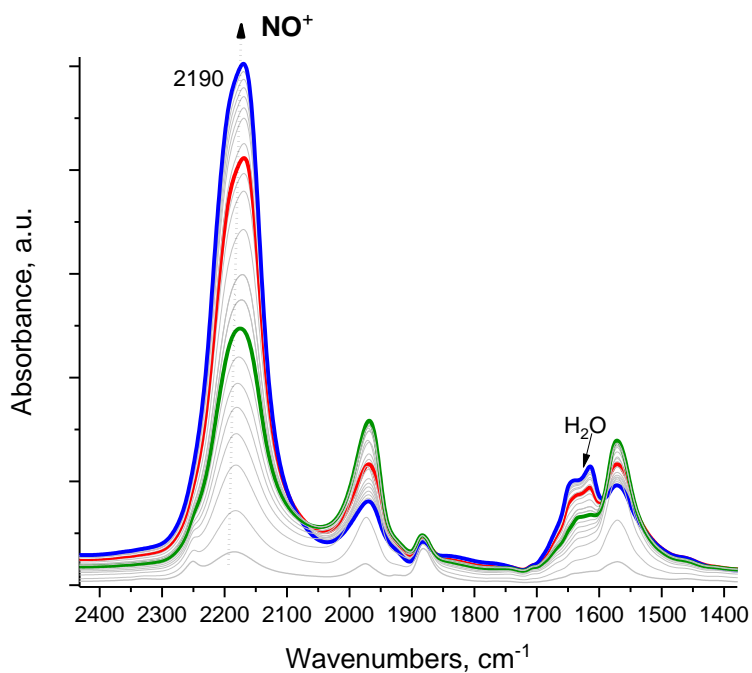


Fig. S1. *In-situ* FTIR during sequential NO (0.5 Torr) and O₂ (0.1 Torr) co-adsorption on H-SSZ-13 with Si/Al~12 at room temperature.

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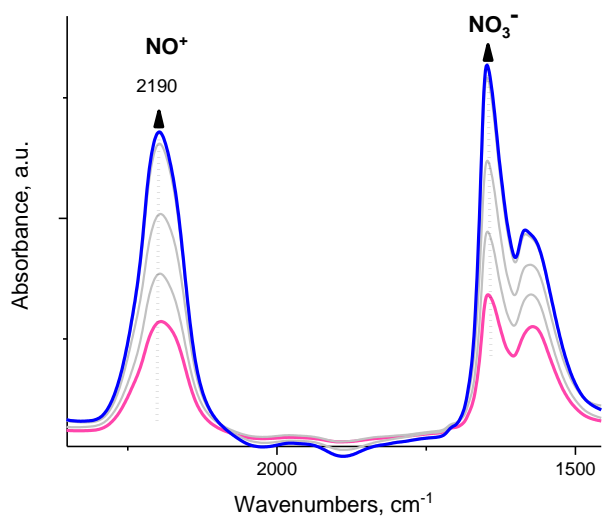


Fig. S2. *In-situ* FTIR during sequential NO₂ (0.5 Torr) on H-SSZ-13 with Si/Al~12 at room temperature. NO₂ forms N₂O₄ in the pores and immediately reacts with H-SSZ-13 to form NO⁺ and HNO₃.

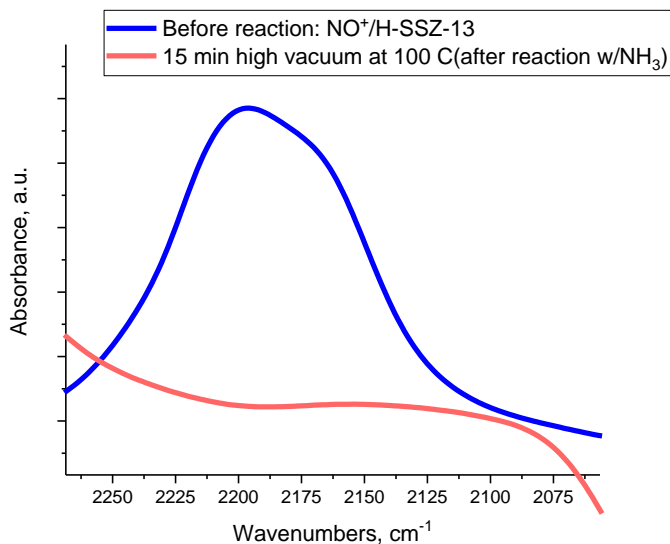
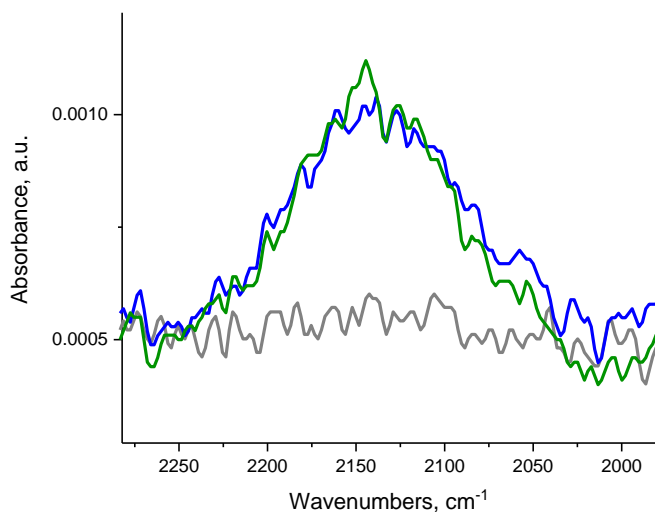
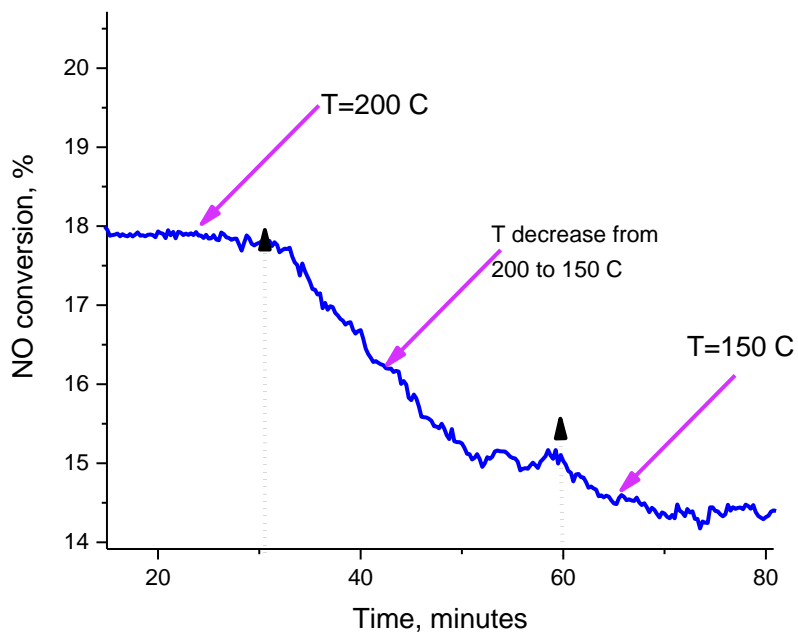


Fig. S3. Continuing from Fig 5 in the Main Text. FTIR of the N-O stretching region of NO⁺/H-SSZ-13 system before reaction with ammonia, and after reaction with ammonia (at room temperature), and after pulling high vacuum at 100 °C for 15 minutes.



Figs. S4. Continuing FTIR experiments after the ones performed in Fig 2A. After reaction between NO⁺/H-BEA with ¹⁵NH₃, the sample was vacuumed at room temperature and new baseline was collected (gray spectrum). 2 Torr NO + 0.7 Torr O₂ were then reacted with the sample: the resulting spectra (green and blue) show that because NH₃ occupied Bronsted acid sites of zeolite with the formation of NH₄-Zeolite (ammonia is strongly adsorbed and cannot be desorbed at room temperature even to a small extent), only extremely small amounts of NO⁺ can be formed (intensities barely above the noise level).



Figs. S5. NO conversion (%) vs time-on-stream for H-BEA Si/Al ~ 15 sample under dry conditions (conditions specified in experimental section).

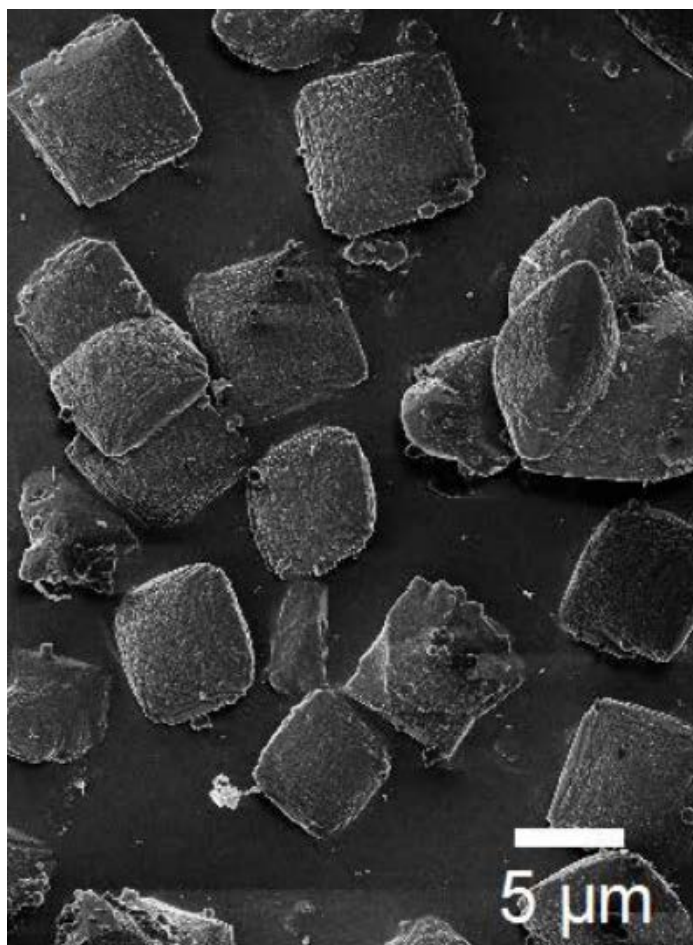


Fig. S6. Typical Helium Ion Microscopy (HIM) image of H-BEA crystals with Si/Al ~ 15.

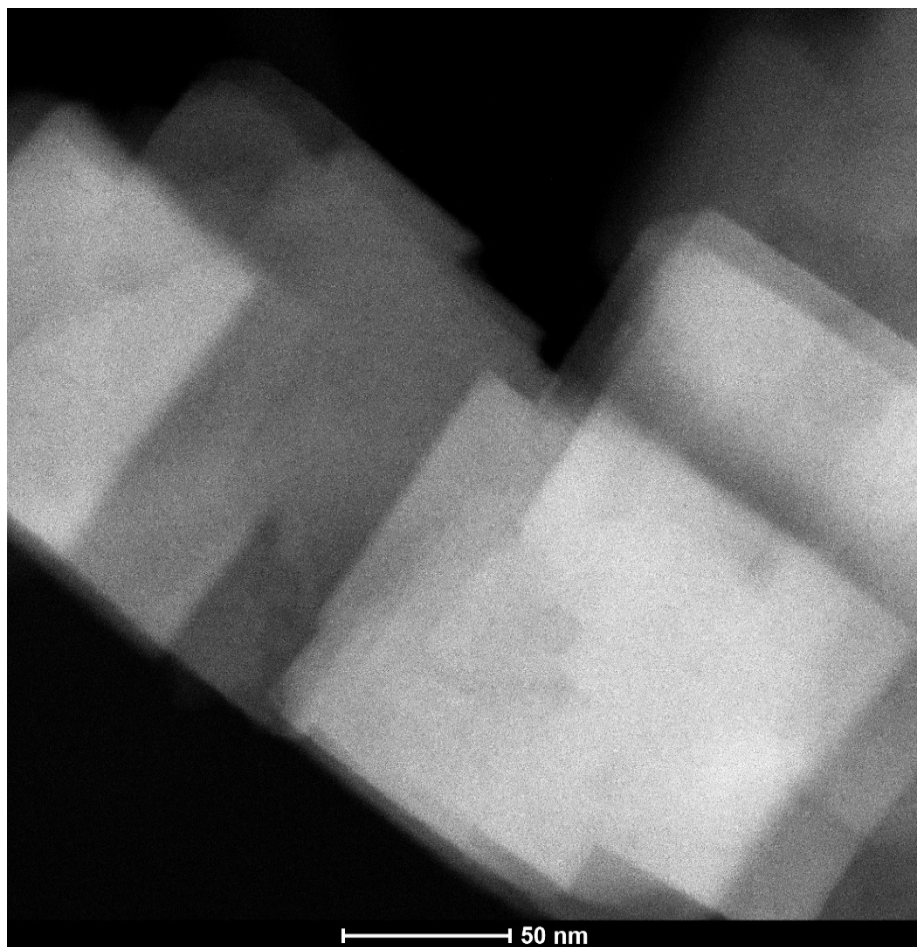


Fig. S7. Typical HAADF-STEM images of SSZ-13 crystals.