# Objects Interacting with Solidification Fronts: 1 Thermal and Solute Effects 2 Sidhanth Tyagi<sup>1,2</sup>, Hélène Huynh<sup>1</sup>, Cécile Monteux<sup>2,3</sup>, and Sylvain $Deville^{1,4,5}$ <sup>1</sup>LSFC, UMR 3080 CNRS/Saint-Gobain CREE, Saint-Gobain Research Provence, 84300 Cavaillon, France <sup>2</sup>Sciences et Ingénierie de la Matiére Molle, ESPCI Paris, PSL Research University, CNRS, Sorbonne Universités, UPMC Univ Paris 06, 75005 Paris, France. 8 <sup>3</sup>Global Station for Soft Matter, Global Institution for Collaborative Research and 9 Education, Hokkaido University, Sapporo, Japan. 10 <sup>4</sup>now with: Université de Lyon, Université Claude Bernard Lyon1, CNRS, Institut 11 Lumière Matière, 69622 Villeurbanne, France. 12 <sup>5</sup>Corresponding author. Email: sylvain.deville@univ-lyon1.fr. 13

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In many materials processing routes, objects such as bubbles or 15 particles interact with a moving solidification front. The output of 16 this confrontation, from instantaneous encapsulation to complete re-17 jection of objects, regulates the solidified microstructure and the spa-18 tial distribution of the objects, and thus the final properties of the 19 materials. Here we investigate by in situ cryo-confocal microscopy 20 how thermal conductivity and solute compete to control the interfa-21 cial curvature of the solidification front. We first validate the predic-22 tion of physical models in absence of solute, and then demonstrate 23 the dominating effect of solute. In the case of cellular front morphol-24

ogy, we show that thermal effects depending on the particle conductivity induce a distortion of ice crystals thereby modifying the final microstructure of the solid. Overall our results show that to successfully predict and control solidification microstructure in the presence of objects, physical models that take into account both thermal and long-range solute effects are now required.

Keywords: solidification, solutes, thermal conductivity, interfacial curva tures, microstructure

The interaction of solidification fronts with objects (droplets, bubbles, solid 33 particles or cells) is a common phenomenon encountered in a plethora of situa-34 tions, ranging from industrial to natural occurrences, such as the formation of 35 sea ice, growth of single crystals, metallurgy, cryobiology, or food science. The objects (soft or hard) exhibit different types of behavior while interacting with 37 a solidification front, from total rejection to complete or partial engulfment [2]. 38 The dynamics of this interaction influences the solidified microstructure and 39 the mechanical and functional properties of the materials. From homogeneous 40 particle distribution in particle-reinforced metal matrix composites to complete 41 rejection of inclusions or porosity management in castings and growth of single 42 crystals, distinct outcomes may be desired depending on the application. The 43 potential to actively govern the solidification microstructure is thus crucial. 44 The initial studies performed on encapsulation and/or rejection of particles by 45 a freezing front, moving at a velocity  $V_{sl}$ , considered either the interplay of van 46 der Waals and lubrication forces [5] or the change in chemical potential [25]. 47 Most of these physical models established a criterion of critical velocity  $(V_c)$ , 48 for a given size of an insoluble object or *vice-versa* (critical radius), to predict 49 whether the object will be encapsulated  $(V_{sl} > V_c)$  or rejected  $(V_{sl} < V_c)$  [2]. 50

Subsequently, the studies performed showed that the curvature of the solidification front plays a major role in solidification dynamics, as it influences the magnitude of both viscous and van der Waals forces in the gap between the particle and the front. Theoretically, the critical velocity reduces drastically for <sup>55</sup> concave interfaces as opposed to ideal planar interfaces [11].

The disjoining pressure, arising in the gap between the growing solid and the 56 particle, causes a deformation of the solidification front. However, it has been 57 predicted that the thermal conductivity deforms the front  $10^3$  times more than 58 the other parameters [18]. If a particle has a lower thermal conductivity than the 59 melt  $(k_p/k_m < 1)$ , the solidification front bulges towards the object and repels 60 it. In the opposite case  $(k_p/k_m > 1)$ , the solidification front bends away from 61 the particle and facilitates its encapsulation [27]. However, few experimental 62 observations exist to ratify these numerical simulations, owing to the associ-63 ated small time and space scales, as well as high temperatures of solidification, 64 especially for metals [17, 25]. 65

The thermal conductivity ratio criterion is not extensive and has been contrary in certain experimental predictions of repulsion and engulfment of foreign particles [23]. The presence of solute in the melt may also influence the interaction between a particle and a solidification front, as solutes are rejected by the solid and segregate at the solid-melt interface, leading to a colligative depression of the melting temperature.

Here, we demonstrate in a systematic manner the influence of thermal con-72 ductivity on the front curvature using in situ cryo-confocal microscopy. We de-73 pict that solute segregation at the front overrides thermal conductivity effects 74 and hence, not only controls the interfacial curvature but also the dynamics of 75 particle capture. Furthermore, in the case of cellular front morphology, insulat-76 ing particles, engulfed in the solid, induce a distortion of the surrounding ice 77 crystals due to persisting local temperature gradients, thereby modifying the 78 final microstructure of the solid. 79

### <sup>80</sup> Thermal conductivity controls the interfacial curvature

We perform solidification experiments with dilute aqueous dispersion of droplets, bubbles, and particles, of similar diameter  $\approx 50 \,\mu m$ , but varying thermal conductivity. We regulate the front velocity  $(V_{sl})$  by translating a Hele-Shaw cell,

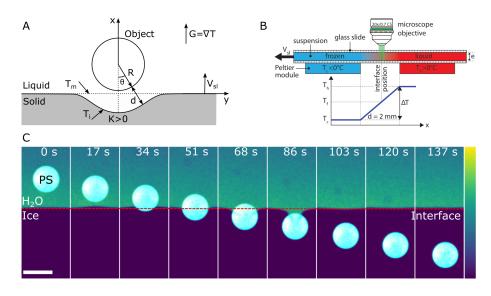


Figure 1: Objects interacting with a moving solidification font: principles and *in situ* confocal microscope imaging. (A) Model, sketch. (B) Experimental setup for *in situ* solidification experiments. A thin Hele-Shaw cell containing the suspension, emulsion or foam is pulled at a constant velocity  $(V_{sl})$ through a constant temperature gradient (G) established by Peltier elements. In steady state, the solidification front is thus at a constant position under the microscope objective. (C) Typical time lapse for a freezing particle-in-water suspension with a Polystyrene (PS) particle. The solidification front develops a bump ( $t \approx 17s$ ) in the vicinity of the low thermal conductivity solid ( $k_p/k_m < 1$ ). PS is in cyan, water in colormap viridis (fluorescence bar) while ice is in black. Scale bar =  $50 \,\mu m$ . <sup>©</sup> (2020) S. Tyagi *et al.* (10.6084/m9.figshare.12046560) CC BY 4.0 license https://creativecommons.org/licenses/by/4.0/.

- <sup>84</sup> under a confocal laser scanning microscope, along a temperature gradient (G) <sup>85</sup> imposed by two Peltier modules, as shown in Fig. 1. The independent selection <sup>86</sup> of the two parameters ( $V_{sl} \& G$ ) in our setup enables a uniform cooling rate <sup>87</sup> and an improved control over the front morphology.
- We observe a pronounced convex curvature (Fig. 2A) when the objects are thermally insulating compared to water  $(k_p/k_m < 1)$  and thus, the front tends to diverge towards them as they act as thermal shields causing the temperature in the gap behind them to be successively lowered. We used zirconia and stainless steel conducting particles and obtain a cusping of the front (Fig. 2A). The relatively higher thermal conductivity of the spheres  $(k_p/k_m > 1)$  enables a preferential heat flux from the melt to the front resulting in a concave depression.

Thus, the differing thermal conductivities result in a distortion of the isotherms away from the horizontal. The magnitude of the depression (convex or concave) depends on the thermal conductivity ratio of the particle to the melt  $(k_p/k_m)$ (Fig. 2B).

These observations are in agreement with the numerical model from Park 99 et al. [18]. This model is based on the computation of the particle velocity 100 when it is close to the front  $(d \ll R)$  and takes into account the balance of 101 hydrodynamic and intermolecular forces, solidification front surface energy, con-102 trast of the particle and melt thermal conductivities, and the flow caused by 103 the density change upon solidification. It encompasses an asymptotic analysis 104 in the lubrication approximation and theoretically predicts the curvature of the 105 front as a function of  $\gamma$  and  $(k_p/k_m)$ , shown in Fig. 2C, where  $\gamma$  is a dimen-106 sionless surface energy parameter,  $\gamma = (T_m \sigma_{sl})/(L_v G R^2)$ , where  $T_m$  is the bulk 107 melting temperature at constant pressure, G is the applied temperature gradi-108 ent,  $\sigma_{sl}$  is the interfacial tension between the solid and the melt, of the order 109  $3 \times 10^{-2} Nm^{-1}$ , and R is the radius of the spherical object. Our solidification 110 experiments correspond to  $\gamma \approx 3.5 \times 10^{-3}$  . We can see from Fig. 2C that when 111  $k_p/k_m > 1$ , the front is always concave and has a depression away from the 112 object. While for  $k_p/k_m < 1$ , three curvatures are feasible corresponding to 113 concave, concave-convex, and convex. The domain of concave-convex geometry 114 is limited to higher  $\gamma$  regions while it reduces to a confined zone when  $k_p/k_m$ 115 is close to 1 and  $\gamma < 10^{-1}$ . We could not investigate this region as it requires 116 either the use of minute objects  $(R < 5 \,\mu m)$  or the application of a small tem-117 perature gradient ( $G < 1 \times 10^2 Km^{-1}$ ), other parameters being constant for 118 the particle-in-water system. While using minute objects is inconceivable as 119 the interfacial curvature would be below the optical spatial resolution, using a 120 smaller temperature gradient would render a planar front thermodynamically 121 unstable owing to the supercooling [13]. 122

Interestingly, there seems to be no conspicuous digression in the dynamics of objects with  $k_p/k_m < 1$  or  $k_p/k_m > 1$ , which depict similar behaviour as can be seen in the time-lapse figure (Fig. 1C). We do not observe repulsion of neither the soft objects (oil droplet and air bubble) nor the insulating rigid particles in the system investigated, which rather tend to be encapsulated instantaneously. This trend is contrary to the previous studies [2], where a convex front tends to increase the critical engulfment velocity ( $V_c$ ) and facilitates repulsion of the object through a reduction of lubrication drag forces in the gap between the particle and the front [18].

All these predictions and results were obtained so far in pure systems. How-132 ever, almost all real melt systems consist of solutes in some form or the other, 133 be it desired (for imparting better mechanical and/or physical properties) or 134 undesired (such as impurities, inclusions etc...). It has been shown recently 135 that the dynamics of interaction of an object with a solidification front and the 136 critical role of solutes have been highly underestimated in the studies so far [7]. 137 We cannot use the existing models as they consider a dominant role of ther-138 momolecular forces, which are effective only at very short distances ( $\sim 10^{-10}$ 139 m) [2,18,21], while solute fields are long range (~  $10^{-4}$  m) [2,7]. We therefore 140 investigate how solute impacts the interfacial curvature. 141

## <sup>142</sup> Solute effects override thermal conductivity effects

We carried out freezing experiments with the same set of objects (oil droplets, 143 gas bubbles, and particles) in the presence of 1wt.% TWEEN80 (acting as a 144 model solute) aqueous phase. This surfactant, needed to stabilize the bubbles 145 and drops, is used here as a model solute that decreases colligatively the freezing 146 point in all systems. We assume the thermal conductivity ratio of the objects 147 to melt remains the same as shown in Fig. 2C. Thermal conductivity is a ma-148 terial property that depends primarily on temperature, and thus we expect no 149 significant changes to its value while adding small amounts of solute to water. 150 We observed only convex interfacial curvature in the absence of solute with 151  $k_p/k_m < 1$ , however, in the presence of solute, solely concave curvatures are 152 observed (Fig. 3A). In the presence of conducting objects with  $k_p/k_m > 1$ , the 153

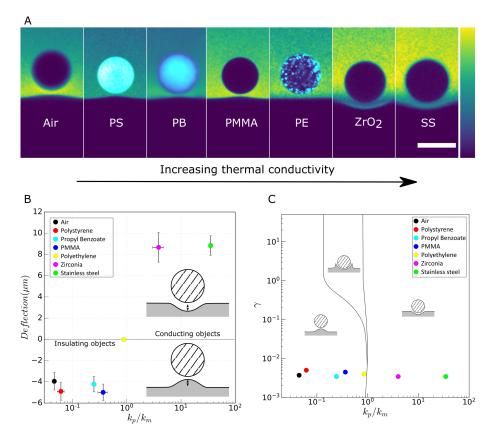


Figure 2: Thermal conductivity effects on interfacial curvature in absence of solute. (A) Insulating air-in-water bubble, polystyrene (PS) particle, propyl benzoate (PB) droplet, and Poly(methyl methacrylate) (PMMA) particle promote a convex curvature of the solidification front. Polyethylene (PE) particle does not affect the curvature. Conducting zirconia ( $ZrO_2$ ) and stainless steel (SS) particles result in a concave depression. We added a very small amount (0.01wt.%) of TWEEN80 to stabilise the foam and the emulsion, while no solute was present for the particle suspensions. PS, PB, and PE are in cyan, water in colormap viridis (fluorescence bar) while ice, air, PMMA, zirconia, and stainless steel are in black. Scale bar =  $50 \,\mu m$ . (B) Plot of front deflection versus ( $k_p/k_m$ ) for solidification of spherical objects in absence or at low concentration of solute. (C) Three distinct curvatures of the solidification front in the thermal conductivity ratio ( $k_p/k_m$ ) versus  $\gamma$  plane for a spherical particle, adapted from Park *et al.* [18]. <sup>©</sup> (2020) S. Tyagi *et al.* (10.6084/m9.figshare.12046560) CC BY 4.0 license https://creativecommons.org/licenses/by/4.0/.

front exhibits a much more pronounced concave depression as compared to the geometry observed in the absence of solutes (Fig. 4). Thus, the solute tends to play a dominant role and renders the solidification front concave regardless of the thermal conductivity ratio.

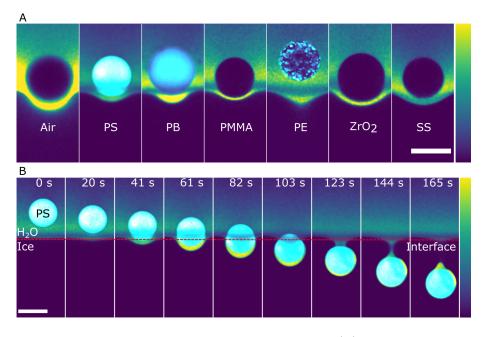


Figure 3: Impact of solute on the front curvature. (A) Concave depression of the solidification front with air bubble, polystyrene (PS), propyl benzoate (PB), poly(methyl methacrylate) (PMMA), polyethylene (PE), zirconia ( $ZrO_2$ ), and stainless steel (SS) particles. PS, PB, and PE are in cyan, water in colormap viridis (fluorescence bar) while ice, air, PMMA, zirconia, and stainless steel are in black. Scale bar =  $50 \,\mu m$ . (B) Typical time-lapse for a freezing particle-inwater suspension, with a PS particle, in the presence of solute: 1wt.% TWEEN 80. The solidification front bends away from the solid ( $t \approx 41s$ ) and eventually heals leaving a premelted film around the encapsulated particle. PS is in cyan, water in colormap viridis (fluorescence bar) while ice is in black. Scale bar =  $50 \,\mu m$ . (© (2020) S. Tyagi *et al.* (10.6084/m9.figshare.12046560) CC BY 4.0 license https://creativecommons.org/licenses/by/4.0/.

As an insoluble object approaches a solidification front, it obstructs the dif-158 fusion field, and leads to a build-up of solutes (rejected by ice) at the front. Since 159 growth from solutions depends on the concentration gradient of solutes at the 160 front, the liquidus temperature of the melt differs from the melting temperature 161 of the bulk composition. The change in liquid composition alters its transfor-162 mation temperature, referred to as constitutional supercooling [24]. Therefore, 163 the solute-rich region colligatively depresses the freezing point of the aqueous 164 phase. This distortion of the isotherm away from the horizontal manifests itself 165 as the concave depression of the solidification front. The resulting thin film, 166 visible in the high fluorescence crescent (Fig. 3) between the object and the 167

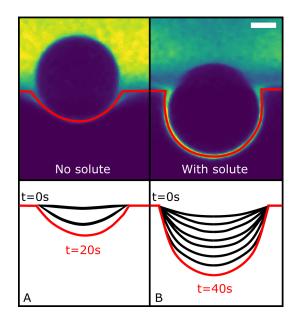


Figure 4: Maximum interfacial curvature depression with time observed before encapsulation, in absence (A) and presence (B) of solute; 1wt.% TWEEN80, for a conducting zirconia particle ( $k_p/k_m > 1$ ). Scale bar =  $20 \,\mu m^{\bigcirc}$  (2020) S. Tyagi *et al.* (10.6084/m9.figshare.12046560) CC BY 4.0 license https://creativecommons.org/licenses/by/4.0/.

growing ice, is driven by the tendency to reduce the interfacial free energy and 168 known as a premelted film [4, 20, 26]. The films are thermodynamically stable 169 below their bulk melting temperature and are extremely sensitive to the pres-170 ence of solutes (known as solute premelting). The solute premelted films are 171 quite evident in these experiments (Fig. 3B), however, we do not observe any 172 interfacial premelting in the absence or at low concentrations of solute (Fig. 1C). 173 The concave curvature of the front facilitates lateral solute diffusion causing the 174 front to accelerate, while engulfing the object with a solute-rich premelted film 175 around it. 176

These results depart from the behaviour predicted in most physical models, where thermal fields are expected to affect the curvature of the solidification front [2]. We believe the long-range solute field interactions (with a length scale of  $\sim D/V$ ) dominate over the short-range thermomolecular forces. This enforces the importance of purely diffusive (solute) effects during solidification as they

not only alter the interfacial curvature but also the nature and equilibrium 182 of forces on the particle. Solutes impact the premelted film thickness [26], 183 viscosity, undercooling [21], and can induce phoresis of suspended objects [1, 184 7] during freezing. Therefore, the prediction of the object behaviour when it 185 encounters a solidification front is not so trivial. We suggest that the criterion 186 of thermal conductivity ratio  $(k_p/k_m)$ , for concluding whether an object will 187 undergo engulfment or rejection, needs to be modified to account for long-range 188 solute field interactions. However, modelling of the solute effects is beyond the 189 scope of this study. 190

## <sup>191</sup> Solute and thermal conductivity effects in cellular growth

We have discussed so far the interfacial geometry for an ideal planar front mor-192 phology preceding particle encapsulation. We will now focus on the breakdown 193 of the planar front and the subsequent impact of thermal conductivity mismatch, 194 when a particle is engulfed. Most realistic systems present a scenario where a 195 planar shape is thermodynamically not stable. This can be attributed to a high 196 freezing velocity, constitutional supercooling, and the complete rejection of so-197 lutes from the solid phase, which produces a severe concentration gradient at 198 the front [16, 24]. The resulting perturbations destabilise a *steady-state* planar 199 front into regularly spaced cells through the propagation of Mullins-Sekerka in-200 stability [15]. Although these instabilities have been investigated for a long time, 201 we are not aware of any available quantitative models describing the capture of 202 isolated single particles by a non-planar (cellular or dendritic) front morphology. 203 At high solidification velocity  $(V_{sl} = 10 \times 10^{-6} m s^{-1})$  with 1wt.% TWEEN80 204 in the aqueous phase, we obtain a cellular front morphology with solute-rich 205 grain boundaries (Fig. 5). For bubbles (Fig. 5A), the front tends to be mod-206 erately convex  $(t \approx 3s)$  with a deflection away from the horizontal, owing to 207 the extremely low thermal conductivity of air, while it transforms into a con-208 cave depression in the proximity of the bubble (t > 3s). For the oil-in-water 209 emulsion (Fig. 5B), the solidification front stays at the same ordinate before the 210

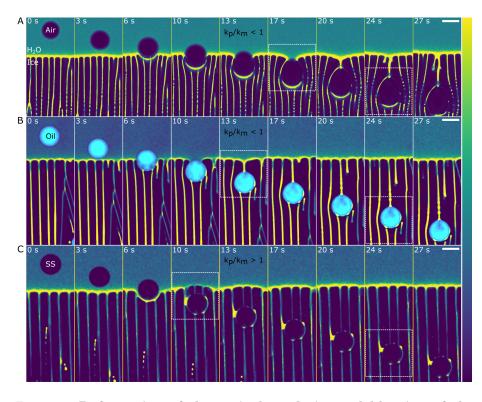


Figure 5: Deformation of the grain boundaries and blunting of the ice tip radius at the solidification front during encapsulation. (A, B, and C) Time-lapse of oil-in-water emulsion (A) with  $G = 10 \ Kmm^{-1}$ , air-in-water foam (B) with  $G = 15 \ Kmm^{-1}$ , and stainless steel sphere (SS) (C) with  $G = 10 \ Kmm^{-1}$ , at  $V_{sl} = 10 \times 10^{-6} \ ms^{-1}$ . Oil is in cyan, water in colormap viridis (fluorescence bar) and ice, air, and SS are in black. Scale bar =  $50 \ \mu m$ . © (2020) S. Tyagi *et al.* (10.6084/m9.figshare.12046560) CC BY 4.0 license https://creativecommons.org/licenses/by/4.0/.

droplet impingement (t < 3s), contrary to the depression in planar morphology (Fig. 3A). The stainless steel particles (Fig. 5C), being highly conductive, induce a concave cusping of the front  $(t \approx 3s)$ , which is further enhanced by the constitutional supercooling  $(t \approx 6s)$ .

The solutes are partially segregated into the grain boundaries and hence, the effective concentration gradient at the ice-water front is considerably reduced compared to the previous planar front situations. Cellular fronts redistributes the rejected solutes parallel to the temperature gradient. This diminishes the extent of constitutional supercooling, thereby averting an extensive cusping of the front and preventing a dominant role of solutes before encapsulation. Thus, the effective distance, between the object and the ice, at which solutes modify the interfacial geometry of a cellular front is considerably smaller.

After encapsulation, the insulating particles  $(k_p/k_m < 1)$  (Fig. 5A, 5B) de-223 form the grain boundaries in their vicinity (t > 10s) and alter the ice tip radius. 224 We believe the thinning of the grains around these particles is essentially related 225 to the local temperature gradients originating from the difference in thermal 226 conductivity ratio between the particle and the encircling crystal. The objects 227 remain at relatively higher temperatures for sufficient amount of time to mod-228 ify the solidified microstructure. Indeed, the grain boundaries do not undergo 229 geometrical modifications (Fig. 5C) with stainless steel sphere, as it is highly 230 conductive  $(k_p/k_m > 1)$ , and therefore, homogenises its temperature with the 231 surrounding ice instantaneously. 232

The rapid cryo-confocal microscopy enables us to follow in situ the evolution 233 of the microstructure. The front eventually heals and recovers its original cellu-234 lar spacing, which is a function of temperature gradient, solidification velocity, 235 and solute concentration gradient [15, 24]. The freezing of suspensions with 236 a cellular front is an attractive route for processing porous ceramics, metals, 237 and even composites [8]. An improved understanding of the critical parame-238 ters is thus desired to regulate the front morphology and the resulting material 239 properties [9]. The size and spacing of grains is an indispensable attribute 240 controlling the mechanical properties of a polycrystalline material (Hall-Petch 241 relationship) [12, 19]. Consequently, the heterogeneous microstructure can be 242 detrimental to an otherwise homogeneous finished product. Thus, solutes play 243 a key role in solidification and an in-depth understanding of their redistribution 244 mechanism is required. 245

### 246 Conclusions

<sup>247</sup> Cryo-confocal microscopy [7] exhibits great promise for the *in situ* analysis of <sup>248</sup> solidification mechanisms with foreign objects. We have demonstrated the role <sup>249</sup> of thermal conductivity mismatch on the distortion of solidification fronts in

the absence of solutes. Furthermore, our results show that both insulating and 250 conducting particles get engulfed by the front in contrast to previous theoretical 251 and numerical studies. In the presence of solute, the long-range solute field 252 interactions play a critical role on the front curvature and the evolution of the 253 solidification microstructure. With cellular front morphology, local temperature 254 gradients around the engulfed particles distort grain growth and further work 255 is required to correlate these observations to analogous real life systems. We 256 hope our extensive research with ceramics, metals, and polymers serves for the 257 formulation of a robust physical model with the incorporation of solute effects. 258

## <sup>259</sup> Experimental section

#### 260 Materials

- <sup>261</sup> Propyl Benzoate, TWEEN80, Difluoro2-[1-(3,5-dimethyl-2H-pyrrol-2-ylidene-N)ethyl]-
- <sup>262</sup> 3,5-dimethyl-1H-pyrrolato-Nboron (BODIPY), and Sulforhodamine B (SRhB)
- were obtained from Sigma-Aldrich. Zirconia  $(ZrO_2)$  spheres (Zirmil Y from
- Saint-Gobain ZirPro,  $50 63 \,\mu m$ ) were provided by Saint-Gobain Research Provence.
- We purchased fluorescent green Polyethylene  $(1 g \, cm^{-3}, 45 53 \, \mu m)$  and Stain-

less Steel  $(7 g cm^{-3}, 48 - 57 \mu m)$  microspheres from Cospheric LLC. We or-

dered monodisperse green-fluorescent Polystyrene (48.1  $\mu m$ ) and Poly(methyl methacrylate) (PMMA) (50.3  $\mu m$ ) from Micro Particles GmbH. Deionized water, filtered with 0.45  $\mu m$  Nylon membrane filters (VWR International), was used for the aqueous phase. The thermal and geometrical parameters which were important for our study are given in table 1 below. The material proper-

 $_{272}$  ties have values based on their typical conditions at 25°C and 1 atm.

### 273 Sample Preparation

The oil-in-water emulsions were prepared by using a microfluidic setup (microfluidic starter kit, Micronit Microfluidics, Netherlands) with pressure controlled flow pumps (Fluigent LineUP Flow EZ) and uncoated focused flow

Particle	R	$k_p$	$k_p/k_m$
	(m)	$(Wm^{-1}K^{-1})$	-
Air	$27 \times 10^{-6}$	0.026	0.046
Polystyrene (PS)	$24 \times 10^{-6}$	0.030 - 0.040	0.052 - 0.070
Propyl Benzoate (PB)	$28 \times 10^{-6}$	0.141	0.248
PMMA	$25 \times 10^{-6}$	0.167 - 0.250	0.293 - 0.439
Polyethylene (PE)	$26 \times 10^{-6}$	0.500	0.879
Zirconia $(ZrO_2)$	$28 \times 10^{-6}$	1.7 - 2.7	2.988 - 4.745
Stainless Steel (SS)	$28 \times 10^{-6}$	20.0	35.149

Table 1: Radius (R), thermal conductivity of the materials  $(k_p)$  and their ratio with the aqueous phase  $(k_p/k_m)$ , where  $k_m = 0.569 Wm^{-1}K^{-1}$ .

droplet generator chips (FF\_DROP), with a nozzle diameter of  $50 \,\mu m$ . The 277 flow rate of oil and aqueous phases were controlled using Fluigent Flow Unit 278 S  $(0 - 7 \mu L/min)$ . The oil phase consisted of propyl benzoate with  $10^{-4} M$ 279 BODIPY, and the aqueous phase was a  $10^{-5} M$  SRhB solution. The air-in-280 water foams were prepared by using the double syringe technique [10], with a 281 luer adapter as connective, and a liquid fraction of 50 %. For the foams, we 282 bubbled air through liquid perfluorohexane ( $C_6F_{14}$  98+%, Alfa Aesar) to ob-283 tain a gas composed of air and perfluorohexane vapour. Thus, we could delay 284 coarsening [3] and ensure the bubbles remained stable during the experimental 285 time-scales, typically varying from 4 to 6 hours at  $V_{sl} = 10^{-6} m s^{-1}$ . TWEEN80 286 was used as a non-ionic surfactant and solute to avoid long-range electrostatic 287 interactions. We used the same surfactant for stabilising both the oil-in-water 288 emulsions and the air-in-water foams. The particle suspensions were thoroughly 280 sonicated  $(30 - 40 \min)$  to ensure a homogeneous dispersion. The experiments 290 in the presence of solute were carried out by adding 1wt.% TWEEN80 to the 291 aqueous phase. We used the same solute and concentration for all systems to en-292 sure comparable results. The solutions were frozen in a rectangular Hele-Shaw 293 cell (h = 100  $\mu m$  and V = 100  $\mu l$ ), fabricated using two glass slides (Menzel, 294  $24 \times 60 \ mm$ , thickness  $0.13 - 0.16 \ mm$ ), and sealed with nail-polish at one end 295 to avoid evaporation. 296

#### <sup>297</sup> Freezing Stage

We performed directional freezing experiments, translating the sample along 298 a constant linear temperature gradient of  $10 \, Kmm^{-1}$ , using the cryo-confocal 299 stage described previously [6]. We carried out all the experiments at  $V_{sl}$  = 300  $10^{-6} ms^{-1}$ , unless stated otherwise. The solidification front tends to appear 301 immobile in the frame of observation, however, in the sample frame, it is the ice 302 solidifying (along  $\vec{x}$ ) at the velocity imposed by the pulling rate of the motor 303 (Micos Pollux Drive VT-80 translation stage PI, USA). We modified the stage by 304 substituting the aluminium plate with a copper serpentine sheet and discarding 305 the silicon carbide honeycomb interface. This led to an improved stability and 306 a more robust cooling setup. The temperature gradient was imposed with two 307 Peltier modules and controlled using TEC-1122 Dual Thermo Electric Cooling 308 Temperature Controller from Meerstetter Engineering, Switzerland. We can 309 thus decouple and control independently the solidification velocity  $(V_{sl})$  and 310 the temperature gradient (G). 311

#### 312 Imaging & Analysis

The images were acquired through a Leica TCS SP8 confocal laser scanning 313 microscope (Leica Microsystemes SAS, Germany), equipped with 488 nm (blue) 314 and 552 nm (green) lasers. We utilised the microscope at a scanning speed 315 of 600 Hertz, with  $1024 \times 1024$  pixels for imaging  $775 \times 775 \,\mu m$ , resulting in 316 1.7 seconds per frame. The high spatial resolution, coupled with rapid screening, 317 enabled us to observe the dynamics of objects interacting with solidification 318 fronts in situ. We used two photodetectors (PMT) to simultaneously image 319 three phases : 320

- 1. BODIPY ( $\lambda_{ex}$  493 nm ;  $\lambda_{em}$  504 nm), the dye incorporated into the oil droplets. The same emission spectrum was utilised to image the fluorescent colloids.
- 2. SRhB ( $\lambda_{ex}$  565 nm;  $\lambda_{em}$  586 nm), dissolved in water, to image the aqueous

<sup>325</sup> phase and the grain boundaries in ice.

32. Ice, does not fluoresce, as it has very low solubility for solutes [14] and
 hence, appears black.

The emission spectra of the excited fluorophores was captured using a nonimmersive objective (Leica HCX PL APO CS  $20\times$ ). The working distance of  $590 \,\mu m$  and an insulating foam cover facilitates the minimization of thermal perturbations on the freezing substrate. We used Fiji [22] and Python for image processing and data analysis.

### 333 Typical solidification parameters

Parameters	Particle in water
G $(Km^{-1})$	$1.0 \times 10^{4}$
$T_m(K)$	273.15
$L_v (Jm^{-3})$	$3.03 \times 10^8$
$\sigma_{sl} (Jm^{-2})$	$3.0 \times 10^{-2}$
$V_{sl} \ (ms^{-1})$	$1.0 \times 10^{-6}$
$\lambda$ $(m)$	$2.83\times10^{-10}$

Table 2: Typical solidification parameters for an object in front of an ice-water solidification front.  $L_v$ ,  $\sigma_{sl}$ , and  $\lambda$  adapted from Park *et al.* [18]

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# **Author contributions**

339 S.D. and C.M. designed and supervised the project, S.D, C.M. and S.T. designed

the experiments, S.T. and H.H. carried out the confocal microscopy, S.T. wrote

341 the code to analyze the data, S.T., C.M. and S.D. analyzed the data. All

<sup>342</sup> authors discussed the results and implications. S.T., C.M. and S.D. wrote the<sup>343</sup> manuscript.

# 344 Conflict of interest

<sup>345</sup> The authors declare no conflict of interest.

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