# Can the NIST adsorption database be used to highlight potential materials for gas separation?

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Scientific literature is replete with descriptions of novel adsorbent materials, making the selection of such adsorbents for gas storage and separation a trudging task, and often resulting in overlooked materials. Here, we use a high throughput methodology to process a dataset of 28 000 adsorption isotherms from the NIST adsorption database (ISODB) and generate key performance indicators applicable to ambient temperature binary separation on 1500 materials in the collection, with 30 adsorbed guests. The procedure is validated against high-quality laboratory isotherms to confirm the accuracy of the derived indicators. The results are then collated in a powerful online dashboard, which can be used to explore the binary correlations. Finally, we use this toolchain to scrutinize several challenging and industrially relevant case studies and highlight some materials which may be promising for further analysis.

 ${\bf Keywords:}\ {\rm gas}\ {\rm separation}\ ;\ {\rm high}\ {\rm throughput}\ {\rm processing}\ ;\ {\rm data}\ {\rm analysis}$ 

# 1. Introduction

A large proportion of the energy consumption of a raw ma-2 terials plant goes into separating various components of the 3 product stream. When the physical properties of the com-4 pounds to be separated are nearly identical, their concentration 5 is low, or when complex mixtures are present, traditional pro-6 cesses which rely on phase change, like distillation, may be 7 prohibitively expensive. Consequently, there are strong incen-8 tives to perfect and implement alternative separation avenues, q such as adsorption or membrane based processes<sup>1</sup>. 10

11 In the case of gas separation, the potential use of porous materials may bring many-fold improvements in efficiency and 12 selectivity. However, the selection process of a suitable material 13 for a desired application is limited by the large possibility space 14 of existing (or hypothetical) adsorbents. Zeolites, commonly 15 employed as adsorbents, come in many real<sup>2</sup> and possible<sup>3</sup> 16 structures. In the promising field of metal-organic frameworks 17 18 (MOFs), more than 80 000 structures have been experimentally identified in the Cambridge Structural Database (CSD)<sup>4,5</sup> and 19 many more predicted to exist  $^{6-8}$ . 20

One desirable approach which has recently garnered much 21 scientific interest is to predict well-performing materials 22 through the use of computation. Such *in-silico* high through-23 put approaches usually focus on a "bottom-up" approach: to 24 model or predict material properties and performance starting 25 from their chemical structure, or descriptors thereof. Us-26 ing such methods, possible materials have been identified for 27  $CO_2$  capture<sup>9–12</sup>, Xe-Kr separation <sup>13,14</sup> as well as storage of  $CH_4$ , <sup>5,15–17</sup>  $H_2$  <sup>18–20</sup>, and  $O_2$ <sup>21</sup>. 28 29

However, these methods cannot yet reliably generate predictions of synthesis pathways, thermal and chemical stability, or fully take into account structural features such as flexibility, defects, crystal size effects or interpenetration. While it may be only a matter of time until these challenges are surmounted (with promising advances being made<sup>22,23</sup>), there are likely many materials which already exist in the published literature but have not been considered for the specific function where they would excel. As a relevant example, a recent study has shown that one of the best currently performing thermoelectric materials could have been predicted 4 years before it was associated with this application<sup>24</sup>.

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This raises the question whether identifying materials for 42 a target separation could be feasible if it would be able to 43 scan all available literature. Associating materials with single 44 descriptive parameters, such as pore volume and surface area, 45 has already been attempted<sup>25</sup>. However, the task of convert-46 ing published adsorption data into a searchable database is 47 not trivial, as isotherms are usually given as graphical figures 48 rather than numerical data. Even if it would be possible to 49 infer plot values, the isotherms are reported in a plethora of 50 units, basis and formats. Excellent progress has been made 51 by NIST<sup>26</sup> to compile such a database. Currently the NIST 52 isotherm database (ISODB) comprises of more than 28000 53 isotherms recorded on over 4000 adsorbent materials, contain-54 ing mostly MOFs but also zeolites, silicas, and carbons. While 55 some of the datapoints are obtained from simulations, many 56 of the isotherms in the ISODB originate from experiments, 57 and are therefore a true indication of the performance of the 58 real material. 59

The potential of exploring such a comprehensive dataset is 60 clear. However, analysis should be performed carefully. Re-61 cently, Sholl and co-workers<sup>27</sup> have published a report putting 62 into question the reproducibility of isotherms, using CO<sub>2</sub> ad-63 sorption data from the same NIST database. Their findings 64 highlight a large variability inherent to measured isotherms, 65 as on average "one in five  $CO_2$  isotherms  $[\ldots]$  cannot be 66 used to provide information that is qualitatively reliable about 67 the properties of the material". A large contribution to this 68 divergence is likely accounted for by the variation introduced 69 through sample preparation and experimental methodology<sup>28</sup>. 70 However, it is often the case that the most important fac-71 tor in the repeatability of adsorption isotherms is not the 72 measurement procedure, but the material itself. 73

From a pragmatic, applications standpoint, one can ask 74

Electronic Supplementary Information (ESI) available: one PDF file with all referenced supporting information, and an animation of the online dashboard.

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whether it is possible to use the database to identify materials of interest for gas separation. In the following work, we attempt to further investigate the ISODB dataset using high-throughput processing to generate and compare simple, one-dimensional key performance indicators (KPI), such as initial Henry constant, uptake and working capacity. A powerful interactive dashboard is constructed to explore the data as a function of various adsorbates, pressures and materials. Several well-known materials are then highlighted and compared with controlled laboratory experiments to validate our approach. We then attempt to draw conclusions from the dataset with respect to various common separations and a pressure swing adsorption (PSA) setup in mind.

### 2. Materials and methods 88

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2.1. Isotherm selection and conversion. The entire dataset 89 in the NIST adsorption database was downloaded using the 90 publicly available API, which yielded  $\approx 28\,000$  single compo-91 nent isotherms. All further processing of the database was 92 performed using the pyGAPS software which was previously 93 developed by us<sup>29</sup>. Data in the ISODB comes from a variety 94 of published sources, including experimental and simulated 95 isotherms with a variety of adsorbates, temperatures and units. 96 In order to narrow down the dataset and ensure comparability 97 the following steps were taken. 98

- Only isotherms measured with 38 common adsorbates 99 were selected, such as simple probes, light hydrocarbons 100 and common vapours. 101
- Isotherms which could not be converted to  $mmol g^{-1}$ • 102 vs. bar were discarded. This includes data reported 103 on a volumetric material basis, simulation data which is 104 reported per unit cell, and fractional coverage isotherms. 105 All remaining isotherms were then converted. 106
- No isotherms with less than 6 measurement points were 107 selected, to ensure enough datapoints for latter processing. 108
- Possible outliers were removed by selecting isotherms 109 with pressure points under 100 bar, maximum loading un-110 der  $100 \text{ mmol g}^{-1}$  and an isotherm temperature of under 111 443 K. Any such isotherms are likely errors in the data 112 collection process and have little to no physical meaning. 113

The process of data collation reduced the number of 114 isotherms to  $\approx 15\,800$ . A distribution of the isotherms as 115 a function of adsorbate and temperature can be found in 116 Fig. 1. Isotherms were then selected in a  $(303 \pm 10)$  K temper-117 ature range. The resulting dataset contains 5800 isotherms 118 on 1503 materials with 30 adsorbates. It was assumed that 119 this range of temperature does not have a stark effect on 120 the amount adsorbed or other isotherm features. It should 121 be noted that certain temperature-critical effects, such as 122 structural transitions, may be sensitive to this approach. 123

**2.2. KPI selection.** Predicting the separation performance of 124 a material starting from pure component isotherms is not 125 trivial. Most attempts at creating an universal application 126 performance indicator (API) for a PSA separation rely on a 127 combination of scalar properties such as: total uptake, working 128 capacity, selectivity (approximated or predicted by methods 129 such as Ideal Adsorbed Solution Theory), enthalpy of adsorp-130 tion, surface area, etc. $^{30}$ . The performance indicator is often 131

further tuned with specific factors to account for the process in question, desired separation efficiency, regeneration cost and other constraints.

When working with a variable dataset, overprocessing of the data will propagate errors to an unmanageable degree. We therefore selected KPI which can be calculated directly from a pure component isotherm and are relatively robust. We 138 have chosen three such parameters: initial Henry's constant 139  $K_{H,i}$ , loading at a single pressure L(p), and working capacity 140 between two pressures  $WC(p_1, p_2)$ .

The initial Henry constant can serve as a useful metric to 142 evaluate the strength of the interaction between a probe and 143 the adsorption site. What is more, the ratio of two Henry con-144 stants can be a useful shorthand for estimating the selectivity 145 of a material  $^{31}$ . Two possible methods of obtaining the initial 146 Henry constant were considered: linear and virial model fitting. 147 The linear method fits a line to the initial part of the isotherm, 148 more sensitive to the quality of the low pressure data, but 149 applicable to all isotherm types and features, The virial model 150 attempts to fit the entire dataset with a virial isotherm  $^{32}$ , 151 then evaluates the resulting function at zero pressure. Full 152 details of the implementation of these methods are available 153 elsewhere<sup>29</sup>. It was found that both methods produce simi-154 lar results, as seen in Fig. S1. The slope method was finally 155 selected, as it is generally applicable. Uptake was calculated 156 by using a first order spline to interpolate between isotherm 157 points at various set pressures. No extrapolation above the 158 maximum recorded pressure point was performed. Working 159 capacity is calculated as the difference of two uptakes at differ-160 ent pressures. These latter KPI can be used as performance 161 metrics when considering the quantity of material required 162 for a separation. Furthermore, for a given pair of gases, the 163 ratio of uptakes can also be a means to highlight materials of 164 potential interest. Including the differential enthalpy of ad-165 sorption as a KPI, as proposed by Wiersum  $et \ al.^{30}$ , would be 166 desirable. However, the isotherms contained in the ISODB do 167 not contain direct enthalpy measurements, and the use of the 168 Clausius-Clapeyron method is susceptible to error. Therefore, 169 no inclusion of this metric was possible. 170

2.3. Data consolidation and outlier detection. The KPI from 171 the previous section were calculated for each isotherm selected. 172 Consolidating the data in order to obtain a single representa-173 tive point for each material was required. Therefore, for each 174 unique adsorbent the resulting KPI values were first passed 175 through gross outlier rejection, in order to remove any spurious 176 values resulting from non-physical isotherms. As such values 177 outside the  $1e \pm 8$  range were removed from further calcula-178 tions. For robust outlier detection, the interquartile range 179 (IQR) for distributions which had more than 4 datapoints was 180 first calculated. Points were considered outliers if they were 1.5 181 IQR below or above the lower or upper quartile, respectively. 182 For datasets with less than 4 values, no points were considered 183 as outliers. The median of the remaining points was taken 184 as the final KPI value. To give an indication of scale, the 185 standard deviation was used. In the case of materials with a 186 single isotherm, the values were calculated directly. 187

All the processing steps and resulting datasets are avail-188 able to download as Jupyter notebooks and JSON files on 189 the authors' GitHub page at https://github.com/pauliacomi/ 190 separation-explorer. 191



Fig. 1. A graphical description of the NIST ISODB dataset: the selected 15800 isotherms presented per adsorbate used and temperature at which the measurement took place. Colour represents number of isotherms on a log scale.

## 192 3. Results and discussion

3.1. Isotherm reliability. As it was clearly shown in the report 193 by Sholl and co-workers<sup>27</sup>, inherent variability exists in pub-194 lished adsorption data. This reproducibility issue can also be 195 seen in an analysis of specific surface area as calculated from 196 nitrogen physisorption at 77 K (available in the SI). There-197 fore, for the employed processing methods to be trusted, the 198 statistical approach detailed in the methods section should 199 first be validated. For this purpose, we have used an internal 200 isotherm database from the MADIREL lab, which contains 201 collated results from our previous work and can be considered 202 203 a high-quality reference. Most of these isotherms come from the work of Wiersum *et al.*<sup>30</sup>. Our database consists of  $\approx 450$ 204 isotherms measured on prototypical materials with various 205 simple probe gases and light hydrocarbons. 206

First, the databases were cross-referenced to find measurements with the same probes on materials present in both datasets. Then, the same KPI calculation methods and derivation of single-point values were applied to the MADIRELderived isotherms as to the NIST dataset. The common datapoints are displayed in Fig. 2.

It can be seen that the two KPI correspond surprisingly well. An obvious spurious point appears in butane adsorption on CuBTC, but otherwise a good correlation is seen between the two databases. While this validation does not test all materials, it gives a good indication that the statistical methods we have applied can be considered adequate for most cases.

3.2. Dashboard. Exploring such a large dataset is difficult with
conventional methods. We have therefore constructed an
interactive dashboard, which can be used to sift through the
resulting relationships. The dashboard is accessible online
at https://separation-explorer.herokuapp.com and can also be
downloaded and executed locally from the previous GitHub



Fig. 2. Comparison between KPI calculated on the basis of the internal MADIREL dataset and the materials from the NIST database. Colours denote gases, while marker shape denotes material. Error margins are not displayed.

link. To operate, the user selects two probes from the list of 225 available adsorbates. The dashboard then creates a table of 226 all corresponding materials, as well as graphs of the previously 227 discussed KPI. A snapshot of the  $CH_4$  and  $CO_2$  correlation 228 is presented in Fig. 3. Each point represents the median KPI 229 value for one material. Points only appear when both KPI 230 are available for each gas selected. The colour of the points is 231 used to indicate the number of datapoints it represents, with 232 grey points signifying values calculated from a single isotherm 233 on each material. 234

The dashboard allows for a high level of interactivity. Hovering over a point will display the material name, as well 236 as details about its dataset. One or multiple points can be 237



**Fig. 3.** Separation explorer dashboard overview of the CO<sub>2</sub>/CH<sub>4</sub> dataset. Top left: the table of all materials with at least one point on display, sorted by ratio of Henry constants. Top right: Henry constant correlation. Bottom left: uptake correlation at 10 bar pressure, value user-selectable in the slider beneath. Bottom right: working capacity in the 1 bar to 15 bar pressure range, similarly selectable. Colour of the points is representative of the number of isotherms available per material, with grey denoting only one datapoint for each gas. The NaN points are a result of no data being available for the material in the working pressure range.

selected directly from the table or the graphs in order to display the confidence range of the KPI as well as the material
name. The hovered or selected material is highlighted in all
relationships, to allow for an overview of its performance.

The pressure at which uptake is calculated, as well as the pressure range in which working capacity is determined is userselectable through the sliders under the respective graphs. The KPI at the selected pressure are displayed on-the-fly which allows to track their evolution at various increments. An example of such an animation can be seen in Supplementary Video 1.

If one material is selected, the isotherms which were used to calculate the respective KPI for each adsorbate are displayed below the dashboard, together with the median calculated uptake. The user can click on an isotherm to follow the link to the respective ISODB page of the publication.

Besides displaying the results in a graphical form, two per-254 formance indicators geared towards separation are calculated 255 for the selected gases and displayed in the table next to each 256 material. The simplest indicator is the ratio of the two Henry 257 constants, as an estimation for the selectivity of the material 258 towards the two gases as proposed by Knaebel<sup>31</sup>. A PSA selec-259 tion parameter is also calculated, similar to the one described 260 by Rege and Yang<sup>33</sup>, but using the Henry constant ratio in 261 place of the selectivity. 262

$$S_{PSA} = \frac{WC_1}{WC_2} \alpha_{12} \approx \frac{WC_1}{WC_2} \frac{K_{H,1}}{K_{H,2}}$$

263 The list can be sorted in order to highlight adsorbents which 264 may be well suited for a separation according to these indica-265 tors.

3.3. Case studies for varius separations. After validating the
processing methodology and developing a toolset to explore
the database from a binary separation perspective, we now
turn to several case studies to exemplify the insights that can
be extracted. We also attempt to highlight materials with
known separation performance, as well as some less explored
alternatives.

**3.3.1. CO<sub>2</sub>/CH<sub>4</sub>**. Observing the graphs displayed in Fig. 3, we can discern several self-evident trends. The adsorption of CO<sub>2</sub> clearly takes precedence over that of CH<sub>4</sub> in nearly all materials. This is to be expected, due to the quadrupole moment of former molecule and the relatively non-specific dispersion interactions of the latter.

279 The top 10 best performing materials as ranked by Henry constant ratio and the PSA selection parameter calculated 280 between 1 and 5 bar are displayed in Fig. 4. Unsurprisingly, 281 many zeolites, such as Zeolite LS-Ca-KFI or Zeolite NaX are 282 highlighted as top performers when considering the ratio of 283 Henry constants. It is well known that such materials are 284 promising for carbon capture from natural gas<sup>9</sup> due to their 285 strong interaction with  $CO_2$ . When considering the PSA selec-286 tion parameter, which also takes into account working capacity, 287 zeolites are less desirable due to the small uptake difference 288 between ambient pressure and higher pressures. Here, several 289 amine-functionalised mesoporous MCM-41 materials emerge 290 as possible candidates due to their high capacity for  $CO_2$ 291 adsorption compared to  $N_2$ . 292

In both graphs, the MIL-53 family of materials is seen to perform very well, which can be traced to to their flexible



Fig. 4. The top 10 materials for  $CO_2$ - $CH_4$  separations as ranked by the ratio of Henry constants (left) and the PSA selection parameter (right). Material labels are taken directly form the ISODB.

gate-opening behaviour. For example, in the iron variant MIL-53(Fe)<sup>34</sup>, the CO<sub>2</sub> opening step occurs at 5 bar while CH<sub>4</sub> does not re-open the structure at this pressure. It should be noted that the top performing material designated as "MIL-53" in Fig. 4 is actually the amino-terephtalic acid linker variant, or MIL-53 (Al)-NH<sub>3</sub><sup>35</sup>.

One further material which appears to show good performance according to both predictors is Sr-UPRM-5, a flexible titanium silicate templated either with tetrapropylammonium (TPA) or tetrabutylammonium (TBA), originally reported by Marcano-González *et al.*<sup>36</sup> and herein referred to as TPA-Activated or TBA-Activated, respectively.

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**3.3.2.**  $C_3H_6/C_3H_8$ . The difficulty of thermodynamic separation of a propane/propylene mixture can be discerned from the KPI correlation observed in Fig. 5. Both the Henry constant and the uptake at 0.5 bar are fairly closely matched.



**Fig. 5.** Correlation of Henry constant (left) and uptake at 0.5 bar (right) for propane and propylene, with several highlighted materials. Lines are guide for the eye at x = y.

Here, we can highlight three materials which are selective 311 towards propylene: CuBTC, TO-MOF and ZnBuPBDC. It 312 is well known that CuBTC preferentially adsorbs the unsatu-313 rated component due to the strong interaction of its copper 314 paddlewheel with the double bond  $^{37}$ . The second material is 315 part of an isostructural series of pillared MOFs tuned for ki-316 netic separations of propylene/propane mixtures<sup>38</sup>. However, 317 it is worth pointing out that, to our knowledge, no study of the 318 separation performance of ZnBuPBDC was ever performed<sup>39</sup>. 319

Another observation can be made by noting that an inverse 320 selectivity can be seen in ZIF-7, where propane is preferen-321 tially adsorbed over propylene<sup>40</sup>, predicted by its location in 322 the lower right quadrant of the Henry constant correlation. 323 324 It should also be specified that the calculated KPI take into 325 account only equilibrium isotherms. Therefore, any kinetic effects cannot be assessed, and are indeed more likely to lead 326 to well-performing materials. 327

3.3.3. Contaminants in post-combustion carbon capture. Traces of 328 water or sulphur and nitrogen oxides  $(SO_X/NO_X)$  in flue gas 329 have a profound impact on post-combustion carbon capture. 330 Due to strong interactions with the adsorbent material and 331 poor regenerability, such contaminants are detrimental to  $CO_2$ 332 adsorption performance. Indeed, this can be visualised by 333 334 comparing the KPI for the desired adsorbed component and 335 such contaminants. If selecting  $H_2O/CO_2$  we can observe that the initial Henry constant ratio is above unity for 80%336 of materials. This suggests a preference for water adsorption 337 over carbon dioxide. When the two components are  $SO_2/CO_2$ , 338 there are no ratios below 2. 339



Fig. 6. Correlation of Henry constant (left) and uptake at 1 bar (right) for H<sub>2</sub>O and CO<sub>2</sub>, with MIL-47(V) highlighted. Most materials are seen to have a preference for water

If considering materials which have a low selectivity for 340  $CO_2$ , it may be possible to identify adsorbents which could 341 be well suited for impurity-rich inlet streams. Here, we can 342 highlight MIL-47(V),  $^{41}$  as a MOF which appears to show a 343 weaker affinity towards water. It should be noted that the 344 only water isotherm available originates from a simulation 345  $study^{42}$ . 346

### 4. Conclusions 347

In this work we have shown that processing the NIST dataset 348 can allow for significant insight into the performance of pub-349 lished materials for specific separations. By comparing the 350 ISODB dataset against an internal high-quality standard, we 351 prove that the variability present in publication data does 352 not broadly affect the calculation of KPI such as Henry con-353 354 stant, uptake or working capacity. The obtained indicators were then incorporated in an online dashboard, which allowed 355 visual exploration of the material performance and trends of 356 various applications. 357

It should be noted that this study can only highlight a nar-358 row range of existing materials for cherry-picked applications, 359 with undoubtedly many more which may be of interest for 360 different topics. We encourage the reader to explore the online 36 dashboard at their own convenience. 362

As the methods of text scraping and digitisation improve, 363 the amount of experimentally-derived data available for further 364 processing will only increase. With a more powerful statistical 365 approach or a selected subset of isotherms like the internal 366 MADIREL database, more complex processing may be per-367 formed, such as prediction of binary separation selectivity 368 through Ideal Adsorbed Solution Theory. In the future, we 369 can also envisage a combined approach that would use such 370 real-world dataset processing to validate the *in-silico* high 371 throughput simulation methods currently employed. 372

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